

# Additive Manufacturing of Soft Polysiloxane-based Bio-structures with Heterogeneous Properties

by

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### **Author's Declaration**

This thesis consists of materials all of which I authored or co-authored: See the Statement of Contributions included in the thesis. This is a true copy of the thesis, including any required final revisions, as accepted by the examiners.

I understand that my thesis may be made electronically available to the public.

## Statement of Contributions

I would like to acknowledge my co-authors who contributed to the research described in this thesis:

- Prof. Ehsan Toyserkani: Supervision of the research, providing the original idea for the current thesis, editing and reviewing papers, providing experimental facilities.
- Prof. Mihaela Vlasea: Guiding the research work in the area of powder bed binder jetting of silicone, brainstorming, providing experimental facilities.
- Prof. Leonardo Simon: Guiding the project of curing kinetics of silicone polymer, providing experimental facilities.
- Dr. Mehrnaz Salarian: Running the CT scanning experiments and analyzing the nano-CT data.
- Dr. Charles Dal Castel: Running the FTIR spectroscopy experiments and analyzing the results.
- Robin Darleux: Helping in running the experiments for material extrusion of silicone and finite element modeling of the extrusion process.

## Abstract

This thesis is concerned with the development of novel additive manufacturing (AM) systems and methodologies for high speed fabrication of complex material-graded silicone structures with controllable internal features consistently. To this end, two AM systems were developed, each pertaining to a specific phase of silicone rubber.

The first system integrates material extrusion and material jetting AM systems. This system is designed to process the paste-like silicone rubbers at high viscosity levels ( $> 400,000 \text{ mPa}\cdot\text{s}$  at  $10 \text{ s}^{-1}$ ). In this system, the outer frame of each layer is made by extruding a highly uniform silicone strand at  $5 \text{ mm/s}$  printhead velocity. Once the perimeter is laid down on the substrate or the previous layer, a piezoelectric-based printhead with a translational speed of over  $100 \text{ mm/s}$  covers the internal section of layer by depositing uniform droplets of silicone at predefined locations. The printing parameters for both extrusion and jetting techniques were tuned using statistical optimization tools in order to minimize the surface waviness of printed parts. The optimized surface waviness values obtained are  $8 \mu\text{m}$  and  $3 \mu\text{m}$  for jetting and extrusion, respectively. Moreover, parts with solid density of over 99% and mechanical performance similar to the bulk material were manufactured by tailoring the rheology of silicone ink.

A combination of powder-bed binder-jetting (PBBJ) system and micro-dispensing material extrusion form the second hybrid AM system. The three-dimensional (3D) shape forming of silicone powder is made possible for the first time using this system. The tomography results for the fabricated parts reveal a porous structure ( $\sim 8\%$  porosity). This AM process is introduced as a the proof-of-concept. The porosity of structures can be tuned by improving the silicone binder delivery method so that binder droplets with pico-liter volumes can be dispensed.

The characterization techniques used for materials and additively manufactured parts include confocal-laser profilometry for investigating the surface quality of printed parts, differential scanning calorimetry (DSC) for investigating the curing mechanism of heat-curable silicone inks, Fourier transform infrared (FTIR) spectroscopy for controlling the curing kinetics and surface cohesion of UV-curable silicones, dynamic mechanical analysis (DMA) tests for tuning the rheological properties of silicone inks under different shear stresses, rheometry for establishing the viscosity threshold for jetting of silicone inks at different temperatures, scanning electron microscopy (SEM), particle size analysis, and powder rheometry for establishing guidelines for the size, shape, cohesiveness, flow, and shear stress resistance of silicone powders, uniaxial tensile test, tearing test, and durometry for identifying the mechanical characteristics of 3D printed parts, and computed-tomography (CT) scanning for quantifying the porosity of parts.

The systems and fabrication methods introduced in this research, with high commercialization readiness levels, were concluded to have great impact on the manufacturing of functionally-graded complex bio-structures. This has been validated through high speed fabrication of multiple heterogeneous bio-structures. Moreover, the proposed techniques can be used for the fabrication of other silicone-based products.

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## **Dedication**

*To my family.*



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# List of Abbreviations

**2D** two-dimensional 36

**3D** three-dimensional 3

**adj MS** adjusted mean of squares 43

**ADSA-P** axisymmetric drop shape analysis profile 32

**ALE** arbitrary Lagrangian-Eulerian 40

**AM** additive manufacturing 1

**ANOVA** analysis of variance 43

**CAD** computer-aided design 8

**CB** carbon black 11

**CCD** central composite design 57

**CFD** computational fluid dynamics 40

**CNC** computer numerical control 8

**CT** computed tomography 8

**DEA** dielectric elastomer actuator 16

**DF** degree(s) of freedom 43

**DoE** design of experiments 29

**FDM** fused deposition modeling 8

**FEM** finite element modeling 28, 29

**FRE** freeform reversible embedding 10

**HTV** high temperature vulcanized 17

**LED** light-emitting diode 36

**LOPP** low one-photon polymerization 14

**MEMS** microelectromechanical systems 40

**NPP** normal probability plot xxv, 174

**PBBJ** powder-bed binder-jetting 3, 9, 24, 97

**PDMS** polydimethylsiloxane 12

**PI** photoinitiator 14

**PPJ** piezoelectric-pneumatic jetting 16, 58

**RSM** response surface methodology 43

**RTV** room temperature vulcanized 21

**SLA** stereolithography 8

**SLS** selective laser sintering 8

**SS** sum of squares 32

# List of Symbols

- $a$  characteristics of length 57
- $CT$  close time of nozzle 58, 64–67, 69, 78, 176–179, 182–184, 187
- $\theta_c$  contact angle 18, 32, 33, 166
- $CyT$  cycle time of nozzle xxi, 59, 64, 66, 78, 176–179
- $c$  capillary constant 32
- $DD$  diameter difference 104, 105, 115, 191, 193
- $\rho$  density 32, 40, 57, 164, 165
- $D$  diameter of the nozzle 58, 99, 101
- $\delta$  Dirac delta function 165
- $\epsilon_f$  elongation at break 19, 21, 91, 93, 96, 122, 195
- $\epsilon$  thickness of transition layer in level-set method 165
- $F_f$  friction between fluid and internal wall of nozzle 28, 166
- $Fr$  dispensing frequency 101, 104, 105, 115, 121, 191–193
- $\Gamma$  reinitialization factor in level-set method 165
- $g$  acceleration of gravity 32, 165
- $w$  half of the maximum width of the droplet 47, 49, 51, 54, 56
- $H$  height of printed pattern 28, 99, 101, 104, 105, 115

$h'$  the height of the droplet created on the substrate 47, 51, 54  
 $h_z$  length of the tapered zone of nozzle 28  
 $h$  the distance between the nozzle tip and the lowest point of the pendant droplet 47, 49, 51, 54, 56, 191, 193  
 $I$  identity matrix 165  
 $ID$  inner diameter 104, 105, 115, 191, 193  
 $K$  coefficient of power law 58  
 $L$  length of the nozzle 58  
 $G''$  loss modulus 18, 19, 22, 77, 84, 88, 96  
 $LT$  layer thickness 101, 104, 105, 115, 121, 191–193  
 $N$  normal to the interface 165  
 $OD$  outer diameter 104, 105  
 $Oh$  Ohnesorge number 57, 58  
 $OT$  open time of nozzle xxi, 59, 64, 66, 78, 176–179  
 $\phi$  level set-function 164  
 $P$  pressure 28, 32, 35, 37, 39, 40, 43, 46, 56, 58, 64, 66, 78, 106, 165, 169, 172, 173, 176–179  
 $PT$  pulse time of nozzle 58, 64–67, 69, 78, 176–179, 182–184, 187  
 $Q_{pne}$  jetting rate due to pneumatic force 58  
 $Q_{pzt}$  jetting rate due to the piezoelectric force 58  
 $R_1$  principal radius of curvature 32  
 $R_2$  principal radius of curvature 32  
 $\lambda$  relaxation factor in Carreau-Yasuda model 30, 31  
 $R_s$  internal radius of nozzle 28

$RW$  raster width 40, 46, 65, 70, 82, 172, 173, 188  
 $\beta$  slip length 166  
 $n$  slope of the power law region 30, 31, 58  
 $G'$  storage modulus 18, 19, 22, 77, 84, 88, 96  
 $Str\%$  stroke 58, 64–67, 78, 176–179, 182–184  
 $F_{st}$  surface tension force 165  
 $\gamma$  surface tension 18, 28, 32, 57, 165  
 $T_s$  tear strength 19, 21, 23, 91, 96, 122, 195  
 $T$  temperature 64, 66, 78, 176–179  
 $\sigma_f$  tensile strength 19, 21, 23, 91, 93, 96, 122, 195  
 $t$  time 33, 41  
 $a$  width of transition in Carreau-Yasuda model 30  
 $v$  velocity 28, 35, 37, 39, 40, 43, 56, 64–66, 70, 78, 169, 172, 173, 176–179, 188  
 $\nu_n$  normal component of velocity field 164  
 $\nu$  velocity field 164, 165  
 $\mu$  dynamic viscosity 28, 30, 40, 57, 164, 165  
 $V$  pulsed voltage 58, 64–67, 78, 176–179, 182–184  
 $W_q$  root mean square of surface waviness 36, 39, 40, 43–46, 56, 63–65, 70, 74, 168, 172, 188  
 $W_{avg}$  average value of width measured over a line xxii, 36, 39, 43–45, 63, 67, 68, 70, 168, 169, 176–178, 182  
 $W_d$  width of the deposited fluid 28  
 $WD$  working distance 35, 37, 39, 40, 43, 46, 56, 64, 66, 78, 82, 169, 172, 173, 176–179

$W_{s.d.}$  standard deviation of width measured over a line (uniformity) 36, 39, 43–45, 63, 168, 169, 176–178

$\sigma_y$  shear yield stress 84



# Chapter 1

## Introduction

### 1.1 Overview

Silicone is a biocompatible material with unique properties that make it suitable for fabrication of biomedical and medical devices. Silicones are inert polymers that are composed of the metalloid, silicon (Si), as well as other elements like carbon, hydrogen, oxygen etc. Walter Noll defines it as “an organosilicon polymer in which the silicon atoms are bound to each other through oxygen atoms, the silicon valences not taken up by oxygen being saturated by at least one organic group [1]”. Unique properties of silicone such as thermal stability, strength, flexibility, biocompatibility, and biodegradability can be traced back to this organic-inorganic molecular structure.

Silicone has been used for a variety of medical applications since its initial commercialization in 1946, mainly owing to its biocompatibility and thermal stability. Different forms of silicone have been used for the production of different classes of implants including orthopedic [2, 3], stomach [4], heart valve [5], cranio-maxillo-facial [6], and mammary [7]. Medical-grade silicones are also used in phantoms, pharmaceuticals, drug delivery devices, lubricating injection devices etc. To be considered medical-grade, a silicone is required to pass certain tests such as histopathology cultures and common biocompatibility tests before being used in contact with human tissue. Luria has reported different applications of this class of silicone in a comprehensive review [8].

The numerous biomedical applications of silicone highlight the importance of an efficient manufacturing method that enables fabricating multi-scale functionally-graded structures from this material. Recent research findings in the area of manufacturing of silicone products suggest that [additive manufacturing \(AM\)](#) can be used to achieve this goal. AM is a

general term used to describe a family of manufacturing technologies that fabricate a solid structure layer-by-layer through deposition, polymerization, melting, sintering, or binding of materials. By eliminating the expensive and time-consuming tooling step, removing any limits in the design of products, and enabling the control of the properties of every voxel of the structure, AM has provided the manufacturing industry with unprecedented flexibility. On the other hand, in the new trend of digitization of manufacturing, known as industry 4.0, AM is depicted as the main fabrication method for the end-user products. To realize the smart manufacturing fully, it is crucial to investigate the AM of novel functional materials. Silicone is one of these new materials.

## 1.2 Motivation

Conventional methods for the production of silicone structures (e.g. molding, soft lithography, and their derivatives. [9–15]) have a number of limitations and disadvantages such as their inability to fabricate highly complex and integrated structures. To better understand the limitations of conventional silicone manufacturing techniques and their consequences in biomedical area, the fabrication of silicone prostheses is considered in the following.

The loss of a body organ and its associated function can cause psychological disorders in patients, and can lead to their social isolation [16, 17]. Depending on the type and severity of the body function loss, approaches such as physiotherapy, corrective surgeries, and the use of prosthetics and/or orthotic devices may be adopted. In many cases, the use of a reversible prosthetic restoration is the preferred option. This highlights the importance of realistic-appearing prostheses, especially for those used to correct cranio-maxillo-facial trauma [18–20], in helping patients to move forward in their recovery process.

Conventional prostheses production methods are costly and time consuming, and the patients must be physically present for most of the design and manufacturing steps. The production process also requires high technical experience [21, 22]. In addition, the process of making an impression of the defect can cause patient discomfort. For example, for the production of a nasal prosthesis, the airway may need to be covered for a long period of time. Also, the impression materials, e.g., plaster, are heavy and may cause distortion to the underlying tissue, potentially resulting in a mismatch between the produced prosthesis and the morphology of the defect area [23]. In some patients with infectious disease, making an impression using direct contact techniques is impossible [24]. Moreover, the prostheses need to be replaced after some time (from a few months to a few years) due to the changes in their color and physical properties, requiring the patient to undergo

this tedious process multiple times. Despite all their shortcomings, these conventional techniques are still being practiced in most of the prosthetics centers [25].

To address these shortcomings, research on the direct AM of silicone as an alternative method with higher design flexibility has gained momentum from both academia and industry in the last few years. In case of the prosthesis production, silicone AM can increase the products accuracy, decrease the patients consultation time and discomfort during the impression-taking step of casting, and lower the dependency of final quality on the clinicians skills. More generally, AM of silicone can positively impact the medical/biomedical sector through:

- High speed production of functionally-graded silicone structures by varying the properties of every building unit.
- Converting the passive silicone objects to smart structures by embedding materials responsive to external signals.
- Fabricating micro-scale silicone patterns which cannot be achieved by conventional molding techniques.

Motivated by the research gap in this field, we have investigated the feasibility of AM of silicone in two different phases (high viscous fluid and powder). For viscous silicone paste (400,000  $mPa.s$  at  $10 s^{-1}$ ), we were able to jet uniform droplets of silicone at a high frequency due to the considerable shear energy produced by piezoelectric-actuated changes in the volume of the fluid reservoir at an unprecedented printing velocity of 100  $mm/s$  and printing resolution of 500 - 600  $\mu m$ . This method is the first reliable system for fast fabrication of viscous thermosets. In another method, the silicone powder scaffold is [three-dimensional \(3D\)](#) printed in a [powder-bed binder-jetting \(PBBJ\)](#) system followed by the dispensing of a liquid silicone binder to encapsulate the silicone particles and produce a soft elastomer object upon thermal curing. This method makes the fabrication of porous 3D structures made from silicone powder possible for the first time.

### 1.3 Thesis Objectives

The objective of this thesis is “developing high speed AM systems and methods for the fabrication of heterogeneous silicone structures”. The target speed is at least three times the translational speed of extrusion-based printheads ( $> 60 mm/s$ ). On the other hand, the

shape forming of structures where different sections are made of three different materials (at least one silicone polymer) as well as internally porous silicone parts are the heterogeneity levels pursued in this research. To this end, the following tasks were undertaken:

- Development of a hybrid multi-nozzle AM system composed of material extrusion and material jetting for processing highly viscous silicone pastes.
- Optimization of printing parameters for material extrusion and material jetting for highly viscous silicone pastes.
- Elimination of the quality flaws in material jetting system for highly viscous silicone pastes through developing a novel trajectory pattern.
- Optimizing the rheological properties of highly viscous silicone pastes for material jetting.
- Mechanical characterization of silicone parts fabricated via material jetting.
- Development of a hybrid AM system composed of material extrusion and powder-bed binder-jetting for processing of silicone powder.
- Characterization of internal features of parts fabricated via powder-bed binder-jetting.

## 1.4 Thesis Outline

This thesis includes 7 chapters. Chapter 1 outlines the problem definition, motivation, and objectives of the present research. The related literature on the state-of-the-art silicone AM systems and tailoring silicone properties for AM is reviewed in Chapter 2. The feasibility of AM of viscous silicone pastes is investigated in Chapter 3 using material extrusion technology, and in Chapter 4 using material jetting technology. The printing parameters are optimized for both systems using statistical analysis tools. The rheological properties of silicone are tuned in Chapter 5 in order to control the level of porosity within the structure, and in turn reduce the difference between mechanical properties of the AM-made parts and the bulk material. Chapter 6 introduces a novel method for fabrication of porous silicone structures from silicone powder. In Chapter 7, conclusions and future work are outlined. Chapters 2 – 6 are adapted from author’s published work or manuscripts submitted for publication as following:

Chapter 2:

- Liravi, F., & Toyserkani, E. (2018). Additive manufacturing of silicone structures: review and prospective. (under review – journal of Additive Manufacturing)

#### Chapter 3:

- Liravi, F., Darleux, R., & Toyserkani, E. (2015). Nozzle dispensing additive manufacturing of polysiloxane: dimensional control. International Journal of Rapid Manufacturing, 5(1), 20-43. [26]
- Liravi, F., Darleux, R., & Toyserkani, E. (2017). Additive manufacturing of 3D structures with non-Newtonian highly viscous fluids: Finite element modeling and experimental validation. Additive Manufacturing, 13, 113-123. [27]

#### Chapter 4:

- Liravi, F., & Toyserkani, E. (2018). A hybrid additive manufacturing method for the fabrication of silicone bio-structures: 3D printing optimization and surface characterization. Materials & Design, 138, 46-61. [28]

#### Chapter 5:

- Liravi, F., Salarian, M., Dal Castle, C., Simon, L., & Toyserkani, E. (2018). High speed additive manufacturing of heterogeneous silicone bio-structures: mechanical characterization and trajectory planning. (under review – journal of Materials & Design)

#### Chapter 6:

- Liravi, F., & Vlasea, M. (2018). Powder bed binder jetting additive manufacturing of silicone structures. Additive Manufacturing, 21, 112-124. [29]

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# Chapter 2

## Background and Literature Review

### 2.1 Silicone

Silicones are synthetic polymers consisting of an inorganic silicon-oxygen (Si – O) backbone and organic groups attached to silicon atoms. Hence they inherit the inertness of inorganic materials as well as the softness and other structural features of macromolecules [1, 30]. Stable Si – O – Si structures are the basis for the generation of silicones. The covalent Si – O bonds, however, are not completely single bonded. They demonstrate a partial double-bonded behavior. The Si atoms are saturated with at least one radical organic group such as methyl (– CH<sub>3</sub>), ethyl (– C<sub>2</sub>H<sub>5</sub>), and phenyl (– C<sub>6</sub>H<sub>5</sub>) and their remaining valences will be saturated with oxygen. The general formula of silicone is  $R_n\text{SiO}_{\frac{4-n}{2}}$ ,  $n = 1, 2, 3$ . Figure 2.1 shows possible silicone structural units.

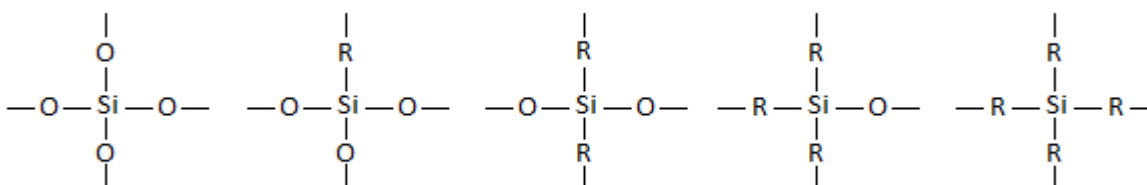


Figure 2.1: Silicone structural units. Adapted from [1]

The great chemical, physical, and surface properties of silicone can be justified through their chemical structure at molecular level including relatively long and flexible Si – O

and Si – C bonds, repetitive arrangement of silicon and oxygen atoms in the polymer chain, arrangement and type of the organic substituents, and the low intermolecular forces between organic groups. Longer backbone bonds and larger bond angles in addition to the alternation of Si – O – Si and O – Si – O bond angles along the silicone backbone result in more flexible structures. This highly flexible structure is the reason of silicones' low glass transition temperature, low melting point, and small viscosity-temperature slope. Long and flexible Si – O and Si – C bonds allow a freedom of rotation with an almost zero rotation energy compared to 14 *KJ/mol* rotation about C – C bonds [31]. Hence molecules can adopt the lowest energy configuration at interfaces resulting in the reduction of surface tension [32]. The explained chemical structure makes silicone retain their physical and chemical properties when exposed to elevated temperatures and also increases their oxidative resistance.

The Si – O is also a polar covalent bond with partially ionic properties. This property is a result of relatively large difference in electronegativity of silicon and oxygen atoms (1.8 and 3.5, respectively). The 1.7 difference in electronegativity causes a 37 to 51% ionic character for siloxane backbone [32]. This covalent bond is not a complete strong  $\sigma$  bond, but a combination of different linkages including  $\sigma$  and  $\pi$ . The partial ionic and partial double bond character of the siloxane are responsible for the strength of this polymer.

The organic groups in silicone have low intensity interactions with each other. These interactions between organic groups have a direct influence on surface properties of silicone. As a result, the type of organic group along with the flexibility of backbone chain can determine the surface tension, water repellency, wetting, and spreading properties of silicone [32, 33]. The combination of chemical inertness, thermal stability, hydrophobicity, and low surface activity of silicones make them a biocompatible polymer suited for biomedical applications [31, 34].

## 2.2 Manufacturing of Silicone Bio-structures

Eggbeer et al. (2012) have evaluated AM against conventional silicone production methods, and identified its superiority for prosthesis production in terms of the quality of final products [35]. They categorized silicone-based AM processes used to create maxillo-facial prosthetics as: (1) indirect AM of silicone; (2) direct AM of silicone. The same categorization is used throughout this thesis. In the indirect AM of prosthetics, casts are first 3D printed (mostly from thermoplastics) followed by the conventional casting of silicone bio-structure. Indirect approaches eliminate the need for the patient to be present during the manufacturing [12, 36]. The successful applications of indirect AM for the fabrication

of prosthetics used in maxillofacial surgeries have also been reported by several researchers [37–39]; however, the indirect use of AM does not have a significant effect on the total production time. Another disadvantage in manufacturing of shaped silicone parts using both conventional and indirect AM techniques is their inability in production of structures with variable property profiles such as a nasal prosthesis with different mechanical properties at its different sections [40]. Hence, researchers suggested the direct use of AM for the printing of elastomeric biomaterials [21, 35]. Although most of the recently introduced methods are not designed for the manufacturing of bio-structures, it is valuable to review them in order to identify the specifications of a viable AM process for medical-grade viscous silicones.

## 2.3 Indirect Additive Manufacturing of Silicone

One of the first attempts to eliminate the drawbacks associated with the conventional manufacturing of soft tissue prostheses involved the introduction of **computer-aided design (CAD)** packages, non-contact morphological measurement systems such as **computed tomography (CT)** scanning [41], and **computer numerical control (CNC)** systems. Chen et al. (1997) pointed out the distress induced by the conventional plaster-cast to the patient and proposed the production of a wax model based on the CT scan data using a CNC machine. Tsuiji et al. (2004) suggested the fabrication of facial prostheses by direct milling of the silicone rubber blocks [24].

In the early part of the millennium, researchers tried to incorporate AM techniques into prosthetic production methods. The indirect AM of silicone changes the fabrication of prostheses in the following manner: (1) Data acquisition of the target part can be achieved using CT scan, (2) the virtual reconstruction of the part and designing of the mold can be done using CAD systems, (3) and the mold can be fabricated using AM [42]. Different AM methods such as **stereolithography (SLA)** [43], **selective laser sintering (SLS)** [44], **fused deposition modeling (FDM)** [25], and material jetting [45, 46] have been employed by researchers for the production of both positive and negative molds for prosthetics. For instance, FDM-based 3D printers have been used to fabricate molds for a functional artificial heart [47] and a mitral valve [48]. In an alternative method, Palousek et al. (2014) proposed the fabrication of a prototype of the target part using AM and then using the prototype to produce the mold [36].

The indirect application of AM in the prostheses production has decreased the turn around time and cost of the process, provided a more flexible workflow, eliminated long patient consultations, and most importantly manufactured more realistic prostheses which can increase the patients satisfaction and speed up their rehabilitation. However, in these



processes, the extra steps of mold design and casting increases the production time. On the other hand, in a thorough review of AM-based prosthesis production techniques, Bibb et al. (2010) demonstrated that the conventional AM technologies, despite their potential effectiveness are not specifically designed to meet the needs of the prosthetics industry, and novel and/or modified AM technologies are needed to process biomaterials used in this field [49]. The application of AM in the prosthesis production can only be sufficient and worthy of clinical use only if the silicone is printed directly, and the prosthesis is produced without the use of a mold [41].

## 2.4 Direct Additive Manufacturing of Silicone

### 2.4.1 Adding Silicone in the Post-Processing Step

Eggbeer et al. (2012) proposed the first direct application of AM for the production of a nasal prosthesis using an acrylate-based material, TangoPlus (Stratasys, Minnesota, United States), in a commercial material jetting AM system (PolyJet). The fabricated body was wrapped over by a thin pliable silicone sheet [35]. Their experiment showed that the additively manufactured prosthesis has the same level of appearance quality as a similar nasal prosthesis made using the conventional molding technique. The direct AM method could improve the prostheses manufacturing process flow by potentially reducing the patients required consultation time. However, the mechanical properties of the substitute polymer were not similar to those of a medical-grade silicone. The poor mechanical properties of TangoPlus (tensile strength of  $\sim 1$  kN and tear strength of  $\sim 0.8$  N/mm) limit the application of this method in reality, as a prosthesis made using this material is susceptible to pre-mature tearing when used on a daily basis. The research did, however, point out the limitations of conventional AM methods for handling the viscous soft materials and showed the benefits of developing a manufacturing system for this class of materials.

The UK-based Company Fripp Design and Research and Zardawi et al. (2013) developed a different method for the direct fabrication of a prosthesis body from a material other than silicone. Their methodology was based on the PBBJ AM, in which the prosthesis is made from the starch powder and an aqueous binder, then the 3D printed part is infiltrated with the biocompatible silicone under different pressure conditions [50, 51]. Similar to the method presented by Eggbeer et al. [35], producing the prosthesis body from starch led to a decrease in the durability of prosthesis. These alternative materials are not as resistant to weathering conditions as silicones, resulting in the degradation of their mechanical properties and color fade over time. The advantage of the method introduced

by Zardawi et al. is an advanced color-match system and the jetting of colorful binders based on the patients skin tone resulting in the production of a fully-colored prosthesis body. Fig. 2.2(a) shows a nasal prosthesis made using this technique. The binding effect of silicone is demonstrated in Fig. 2.2(b-c).

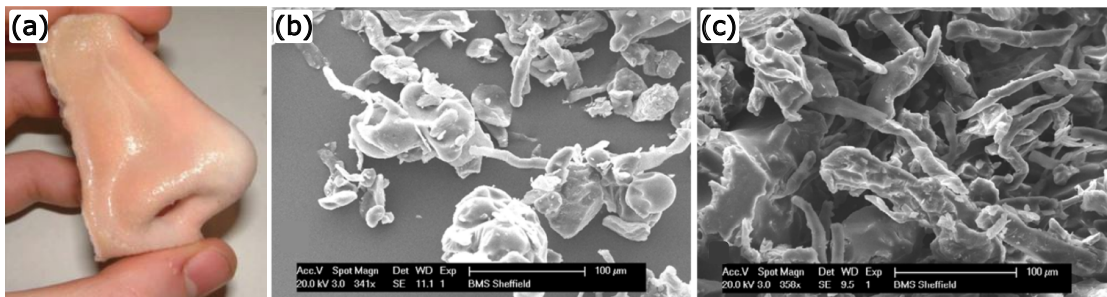


Figure 2.2: (a) Silicone-infiltrated structure made of starch powder using powder-bed binder-jetting technique; SEM of starch particles (b) before silicone infiltration and (c) after silicone infiltration. (b-c) (adapted from [52]).

### 2.4.2 Using Silicone as the Main Material

Since the early 2010s, researchers have been trying to directly print silicone using different AM methods such as SLA, material extrusion (e.g., nozzle dispensing and [freeform reversible embedding \(FRE\)](#)), and material jetting. A few companies have also started to modify these techniques in order to customize them for silicone indicating the existence of the market potential for 3D printed silicone parts.

#### Material Extrusion

Compared to other AM technologies, nozzle dispensing systems are well-suited for the deposition of a wide range of fluids, from low viscous liquids to thick pastes (up to  $6 \times 10^7$  mPa.s viscosity with a shear-thinning behavior) [53–55]. In comparison, the maximum material viscosities suggested for SLA and drop-on-demand inkjet printing processes are in the range of 300 - 5000 mPa.s [56, 57] and 10 - 100 mPa.s [53, 57, 58], respectively. This capability of material extrusion systems in deposition of viscous pastes is important due to: (1) the high shape-retention capability of viscous polymers, and (2) the high flexibility and resilience resulted from highly viscous silicones ( $> 10,000$  mPa.s) with longer polymer

chains [55]. Different dispensing mechanisms are being used to push fluids through a nozzle in material extrusion systems with pressure-actuated (pneumatic) and mechanical dispensing systems being the most popular [59]. The flow of material in these systems has been numerically modeled for the viscous moisture-curable silicone by Jin et al. (2015) [60].

Material extrusion AM was used by Mannoor et al. (2013) to print silicone, biological hydrogel, and conductive polymers to produce the scaffold of a bionic ear to be cultured *in vitro* in order to grow the cartilage tissue [61]. Their work was the first attempt to apply AM in the fabrication of functional prosthetics. The promising results of this research showed the vital role AM could play in the production of a new generation of prosthetics. The printed bionic ear is showed in Fig. 2.3(a-c). A micro-syringe dispensing technique used by Duoss et al. (2014) for the production of porous silicone structures with controllable mechanical properties was the first successful example of direct AM of silicone [62]. Moreover, they showed that this technique is able to dispense polymers with a viscosity as high as  $10^6$  *mPa.s* with reliable quality. Duoss et al. also showed that obtaining designed mechanical properties is possible with the extrusion-based AM of silicone as they were able to control the compression and shear strength of the printed structures by modifying their porosity and micro-structures [62]. This capability of extrusion AM can be used to produce smart prosthetics with heterogeneous and controllable properties compared to the passive structures produced via molding. Samples of vascular networks fabricated via material extrusion are shown in Fig. 2.3(d-f). Material extrusion technique has also been employed by other researchers to 3D print silicone-based structures for tissue engineering [63, 64], drug-delivery devices [65], stretchable electronics [66], sensing skin [67], actuators [68], foams [69], and membranes with designed properties [70–72].

In most of the abovementioned research, thermal-curable silicones were used as the raw material. Porter et al. (2017) investigated the feasibility of extruding UV-curable strands of low viscous silicone ( $7 \times 10^4$  *mPa.s* at  $10$   $s^{-1}$ ) followed by *in-situ* curing [73]. This method involves complications during the print such as nozzle clogging and deflection of silicone stream from the cured previous layers before reaching the substrate due to repulsive silicone surface charges. Porter et al. have suggested addition of 0.15 - 1 wt.% carbon black (CB) to the silicone which eliminates the electrostatic repulsion, and at the same time reduces the reflection of UV by previously laid silicone which is the main cause of nozzle clogging. In their research, the controlling factor in the amount of CB additive is its effect on the reduction of silicone UV curing depth.

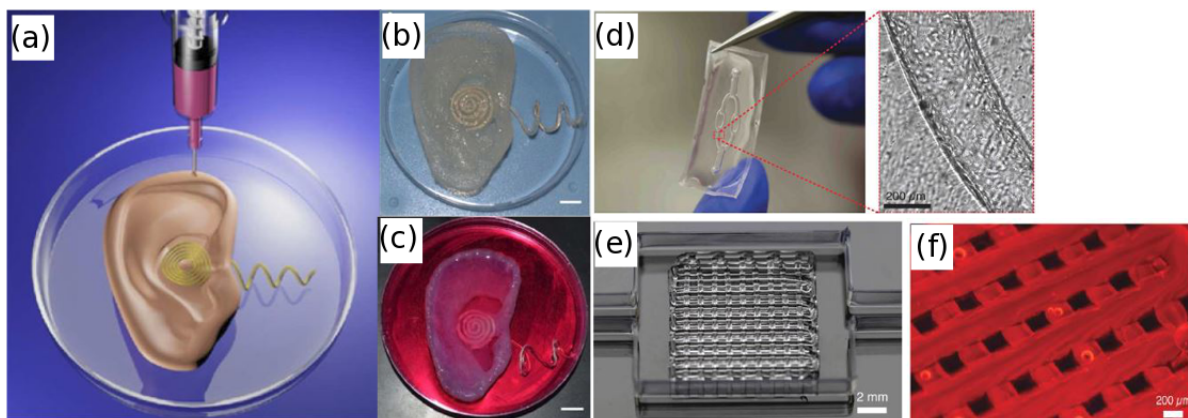


Figure 2.3: (a) Schematic view of the extrusion AM setup for printing of the bionic ear, (b) 3D printed ear, (c) in vitro culture of the 3D printed bionic ear for the cartilage tissue growth, (b-c) scale bars: 1 cm.(a-c) (adapted with permission from [61]. Copyright (2013) American Chemical Society); Images of (d) 2D and (e) 3D embedded silicone vascular networks fabricated by material extrusion AM, (f) Fluorescent image of the 3D vascular network after perfusion with a water soluble fluorescent dye demonstrates performance of the interconnected channels, (d-f) (adapted with permission from [63]. Copyright (2014) John Wiley and Sons).

### Freeform Reversible Embedding

FRE can be considered as a variety of material extrusion AM. Hinton et al. (2016) have developed a method based on FRE for AM of [polydimethylsiloxane \(PDMS\)](#) [74]. In this method, a vat of hydrophilic Bingham plastic acts as a support structure under low stress while the hydrophobic PDMS is extruded inside the vat. This technique, although only suitable for the extrusion of low viscous silicones (e.g. 3000 – 4000  $mPa.s$ ), is extremely useful for the fabrication of hollow structures and continuous freeforming. This method resolves the issue of maintaining the shape of printed structures during the long curing time required by heat- or moisture- curable silicones by providing a support structure which does not have an adverse effect on the surface of the features, and is easily removed using a chemo-mechanical process. Fig. 2.4(a-c) demonstrates the procedure of FRE AM of silicone and some of the printed parts. The width of the FRE printed PDMS linear features, height of the printed lines, and the printhead velocity were reported as 140  $\mu m$  – 400  $\mu m$  (depending on the nozzle size), 100  $\mu m$ , and 20  $mm/s$ , respectively. The main drawback of this method, as reported by the original authors, is the need for the pressure to be induced by the deposition of upper layers to make sure the layers completely adhere to

each other. The lack of such a pressure in the XY direction prevents the lateral adhesion.

O'Bryan et al. (2017) improved the quality and resolution of the silicone parts made using the FRE technique by replacing the aqueous supporting environment with an oil-based micro-organogel support material [75]. The similar oil-based nature of the silicone and the proposed micro-organogel facilitates the adhesion of printed silicone features both laterally and vertically. Moreover, it was found that increasing the viscosity of silicone resulted in the ability to print 30  $\mu\text{m}$  wide features. The reported surface roughness of 150  $\text{nm}$  demonstrates the ability of this 3D printing technique to fabricate the very smooth surfaces required for biomedical applications. Another advantage of this technique is its compatibility with UV-curable silicone, enabling the use of a material that will decrease the manufacturing time.

A slightly different FRE method was proposed by Fripp Design Ltd. for the AM of two part silicones [76]. In their commercial 3D printer, PICSIMA, the vat is filled with the base of a two-part silicone, and the curing agent is extruded through a nozzle inside the vat. Upon extrusion of the curing agent, the silicone solidifies and a 3D object is fabricated layer-by-layer. The major advantage of PICSIMA over other FRE-based techniques is the use of different commercially available silicones with a wide viscosity range as the raw materials that facilitates the fabrication of different bio-structures. Moreover, by controlling the concentration of curing agent or using multiple nozzles, this technique has the potential to fabricate functionally-graded structures with heterogeneous properties.

## Vat Photopolymerization

Femmer et al. (2014) introduced the first application of a vat photopolymerization system for 3D printing of functional microfluidic PDMS membranes [77]. They have used the commercial SLA system from EnvisionTEC (MI, USA) equipped with a digital micro-mirror device for this purpose.

As mentioned before, in vat photopolymerization machines, the viscosity of resin should be low enough to make sure a thin layer of fresh photopolymer with uniform surface is generated for printing of the next layer. To address this issue, Kim et al. (2016), modified SLA method for the fabrication of viscous soft materials [78, 79]. Although this technique is still in its initial phase, it could have a positive impact on the 3D printing of soft materials upon further improvements. Similar to regular SLA, the 3D structure is created by laser curing of the photopolymer inside the vat instead of its surface. In their proposed approach, there is no movement in the resin vat; this creates a hydrostatic environment which acts as a support structure. This support-free fabrication technique requires a sophisticated optics

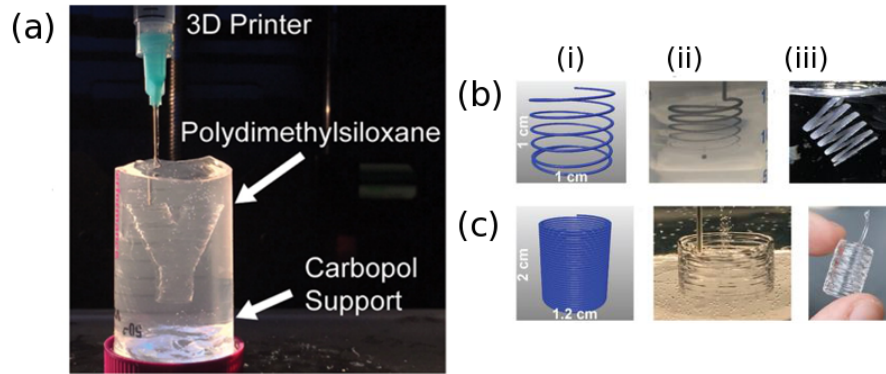


Figure 2.4: (a) The FRE setup for fabrication of silicone structures in Carbopol support vat. Samples of printed silicone structures with FRE system: (b) helix, (c) Cylindrical tube. (b-i) The toolpath for the helix, (b-ii) FRE printing of the helix structure, (b-iii) Helix after removal and cleaning, (c-i) The toolpath for the cylindrical tube, (c-ii) FRE printing of the cylindrical tube, (c-iii) The tube after removal and cleaning. (a-c) (adapted from [74]).

and low power UV curing system, known as [low one-photon polymerization \(LOPP\)](#), to control the light intensity. Also, the curing should only happen at the laser focal point. Hence, the properties of the [photoinitiator \(PI\)](#) used in the polymer should be evaluated to coordinate with the UV exposure set up. Although the reported resolution of this technique,  $1 - 2 \text{ mm}$ , is not comparable to other silicone 3D printing methods, it could be enhanced by improving the preliminary two-tier model developed for LOPP [80] as has been done for the other photopolymers used in the SLA process [81]. Details of this AM system are shown in Fig. 2.5(a-c). The image of the printed parts shows a high degree of discrepancy between the cylindrical CAD models and the printed pillars. The hydrostatic environment required for the 3D printing in this technique eliminates the problem of the flow of viscous materials during the print, however, the viscosity limit for the silicones compatible with this method is yet to be determined as highly viscous paste-like silicones cannot be easily poured into a resin vat. Moreover, degassing the silicone vat to produce a uniform media free of air-trapped areas would be challenging.

The Folchs research group at the University of Washington is also working on the fabrication of microfluidic devices for biotechnology applications by developing an SLA system customized for PDMS [82].

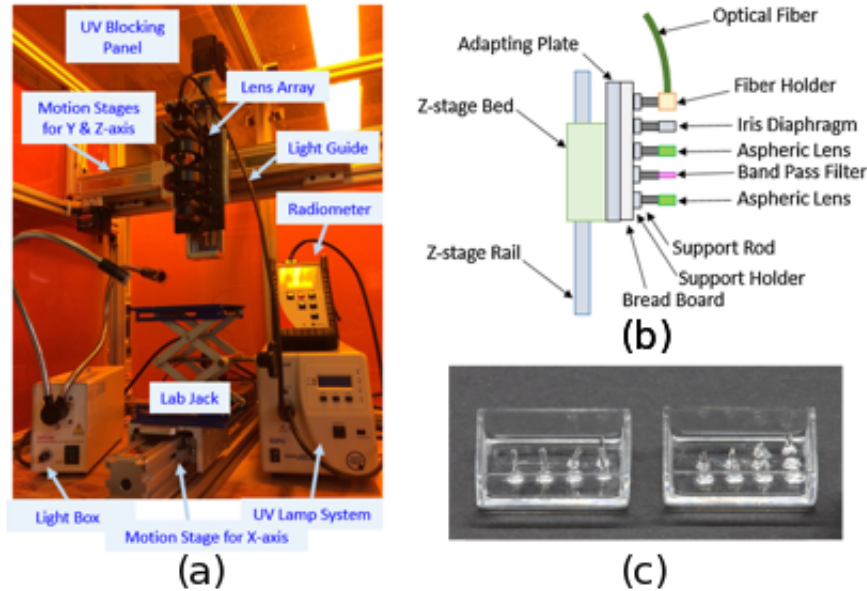


Figure 2.5: (a) The vat Photopolymerization setup for hydrostatic support-free AM of silicone structures, (b) The schematic view of the lens array used for the low one photon absorption polymerization, (c) The 3D printed silicone cylinders at multiple UV laser powers, (a-c) (adapted with permission from [78]. Copyright (2016) Elsevier).

## Material Jetting

The flexible UV-curable elastomers TangoPlus and TangoBlack were introduced by Stratasys to be used in their Connex 3D printer family, and later were used on J750 PolyJet 3D printers. These systems have been widely used by researchers to produce soft elastic objects. For example, inspired by the spider leg, Han et al. (2017) 3D printed a finger [83], and Mohammed et al. fabricated material-graded ear and nose prostheses, both from TangoPlus [84]. Even though, PolyJet with a vertical resolution of  $14 \mu\text{m}$  is capable of producing high quality digital colorful parts, it can only be used with the commercial materials that Stratasys provides. These materials lack the sufficient mechanical properties for special applications. Moreover, these commercial UV-curable elastomers are no replacement for silicone in terms of the biocompatibility and biodurability. However, this technique with an established multi-color printing technology already in place can provide a robust solution to the 3D printing of silicone, provided that the printheads are modified based on the rheological properties of the viscous elastomers, and the properties of raw materials used in the system are tunable [85].

Reitelshofer et al. (2016) proposed a multi-nozzle AM method for the production of stacked [dielectric elastomer actuator \(DEA\)](#) made of silicone and graphene using aerosol jetting [86]. Two aerosol streams containing two parts of a silicone were generated using a pneumatic atomizer. The two streams were combined in a chamber before being transferred to the nozzle and then printed on a substrate. This method can produce silicone layers with a thickness as low as  $10\ \mu\text{m}$ . However, in practice its application is limited by the maximum compatible viscosity ( $5\ \text{mPa}\cdot\text{s}$  for ultrasonic atomizer and  $1000\ \text{mPa}\cdot\text{s}$  for pneumatic atomizer) as well as the manufacturing speed ( $5 - 10\ \text{mm}/\text{s}$ ). The viscosity of the sample silicone used in their research is less than  $2000\ \text{mPa}\cdot\text{s}$ , and the ink was heated up to meet the viscosity requirement.

McCoul et al. (2017) demonstrated the possibility of fabrication of very fine silicone membranes ( $2 - 4\ \mu\text{m}$ ) with minimum surface waviness for multiple commercial silicones using piezoelectric drop-on-demand inkjet printing [87]. In these systems, applying a controllable square voltage signal flexes the piezoelectric ceramic behind the ink reservoir and in doing so jets a droplet of ink out of the nozzle. Fabrication of functional DEAs at a printhead speed of  $50\ \text{mm}/\text{s}$  has been showcased in this study; however, the inability of the proposed system in jetting of the electrodes as well as its incompatibility with intermediate to high viscous inks ( $> 40\ \text{mPa}\cdot\text{s}$ ) are limiting factors in rapid AM of complex 3D structures with tunable mechanical properties

Yang et al. (2013) have investigated the possibility of printing silicones with different viscosities using material jetting systems with dual [piezoelectric-pneumatic jetting \(PPJ\)](#) mechanism [88]. The results of their work show that material jetting methods are promising for printing of different Newtonian and non-Newtonian silicones with viscosities as high as  $100,000\ \text{mPa}\cdot\text{s}$ . However, droplet formation and jetting procedure in this method should be controlled and the printing quality should be optimized. Foerster et al. (2017) have also used this technique to fabricate porous silicone structures [89]. Similar PPJ system for jetting of viscous pastes at a velocity above  $100\ \text{mm}/\text{s}$  has been employed by Wacker Chemie for silicone AM [57]. Unlike regular inkjet printheads which can only handle fluids with a maximum viscosity of  $40\ \text{mPa}\cdot\text{s}$ , these piezoelectric/pneumatic systems can generate enough force to even jet pastes with  $1,000,000\ \text{mPa}\cdot\text{s}$  viscosity.

## 2.5 Silicone Development for Additive Manufacturing

The main challenge in the development of materials for biomedical applications is their chemical, structural and mechanical biocompatibility [90]. As mentioned in Section 2.1 The biocompatibility and biodurability of silicone can be justified through its chemical



structure at molecular level including the relatively long and flexible Si – O and Si – C bonds, the repetitive arrangement of silicon and oxygen atoms in the polymer chain, the arrangement and type of organic substituents, and the low intermolecular forces between the organic groups [31, 32]. However, the currently available silicones should be improved on three fronts for biomedical AM applications: (1) curing mechanism; (2) rheological properties and printability; (3) mechanical performance. Even though the development of silicone customized for AM is as important as the development of an AM system compatible for use with viscous non-Newtonian polymers, little research has been conducted in this area.

### 2.5.1 Curing System

The silicones reviewed in Section 2.4.2 were mostly two-part [high temperature vulcanized \(HTV\)](#) polymers. The HTV silicones need a few minutes to a few hours to at least be partially cured. This partial curing is necessary to allow the previously laid layers to tolerate the forces induced by the weight of upper printed layers. This slow polymerization rate increases the printing time required, if each silicone layer is to be cured after printing. Transferring the 3D printed structure to the oven after printing each layer also seems prohibitively cumbersome and reduces the printed part's accuracy. On the other hand, curing the silicone after printing multiple layers can result in losing the structural fidelity of the sample due to the weight of upper layers. Other difficulties associated with the heat-curable silicones such as the fast gelation time, short range of heat transfer when the heat beds are used, and potential for geometrical deformation have been pointed out in the study of Morrow et al. (2017) [91]. Therefore, the UV-curable silicones with the curing rate in the order of a few seconds can be a suitable replacement for both material extrusion and material jetting methods. Some silicone manufacturers such as Momentive, Novagard, Wacker, Elkem Silicones, and Shin-Etsu are already producing different types of UV-curable silicones. Some researchers have also started to develop their own UV-curable silicones or tune the commercially available ones for their AM systems.

Femmer et al. developed a UV curable silicone requiring 12 *s* irradiation at 440 *nm* UV for 100  $\mu\text{m}$  features to be cured for the production of separation barriers [77]. The controlling factor in their research is the gas permeability of the silicone. Their silicone was used in a vat photopolymerization system. A sample of the functional 3D printed membrane made from this silicone and its curing mechanism are shown in Fig. 2.6(a) and Fig. 2.6(b), respectively. Another UV-curable silicone targeted for vat photopolymerization processes was introduced by In et al. (2017) [92]. This silicone is a composition of commercially available UV curable silicone (Momentive), a silicone thinner (to adjust the viscosity of

the precursor), de-ionized water, and hydrophilic silicone. The results of their research showed that by adding water to the combination of UV-curable and hydrophilic silicone, the curing time could be decreased (Fig. 2.6(c)). The optimized curing time reached was approximately 20 s; however, this would need to be further reduced to be appropriate for 3D printing applications. The target of the research in [92] was manufacturing of solid phantoms for medical imaging.

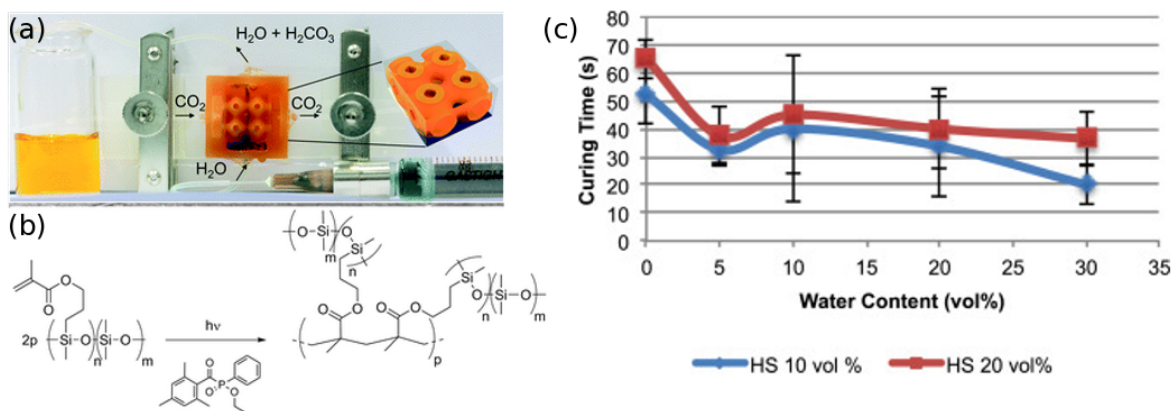


Figure 2.6: (a) Additively manufactured membrane made from the tuned UV-curable silicone. The change in the color of pH indicator from blue to yellow shows the permeability of CO<sub>2</sub> gas; (b) The photopolymerization process at molecular level in the developed silicone ink. (a-b) (adapted with permission from [77]. Copyright (2014) Royal Society of Chemistry). (c) Decrease in the curing time of UV-curable silicone by increasing the water content for inks with 10 vol.% and 20 vol.% hydrophilic silicone (HS). (adapted with permission from [92]. Copyright (2017) Elsevier).

## 2.5.2 Rheological Properties and Printability

The rheological properties of viscous silicones are important factors in the determination of their flow, droplet formation, and interaction with the surface. The effect of parameters such as viscosity, viscoelasticity, contact angle ( $\theta_c$ ), surface tension ( $\gamma$ ), interfacial energy, storage modulus ( $G'$ ), loss modulus ( $G''$ ), and capillary action, as well as the effect of fillers and additives on the extrusion, jetting, and flow of the viscous silicones should be comprehensively investigated.

Controlling the viscoelastic properties of silicone for material extrusion by optimizing the mixing ratio of low and high molecular weight silicones was used in the work of Robinson

et al. (2015) [67]. Based on their work, an ink containing 60 wt.% high molecular weight silicone and 40% low molecular weight silicone showed a solid-like response at low shear stress region to make sure it will not slump after extrusion and retain its geometrical fidelity. Similarly, the effect of silica fillers on the rheological properties of PDMS and its extrusion quality was studied by Lv et al. (2017) [93]. The results of their research show that adding a controlled amount of filler (15 – 20%) can create a solid-like paste with  $G'$  slightly above the  $G''$ , that is not so viscous that it cannot be extruded. Fig. 2.7(a-b) shows the changes in the viscosity and dynamic moduli by varying the weight percentage of filler. Similar shear-thinning behavior was reported by addition of 10 - 20 wt.% of treated silica to poly(diphenylsiloxane-dimethylsiloxane) copolymer (PDMS-co-PDPS) by Durban et al. (2017) [94]. The adoption of these approaches for developing customized silicone for AM assures the flow of silicone ink under the regular shearing at the nozzle while preventing the collapse of printed features.

Roh et al. (2017) developed a three-phase silicone ink customized for material extrusion [95]. Their developed ink consists of micro-particles of cured silicone, liquid silicone precursor, and water. In their technique, suspensions of cured silicone particles are covered with liquid silicone resulting in the formation of capillary bridges, which in turn produce a gel-like printable elastic ink. This procedure has been illustrated in Fig. 2.7(e). This porous silicone ink can be printed both in air or inside aqueous environment, meaning it can be used for *in vivo* 3D printing applications. The presence of cured silicone particles, however, may limit the resolution of the printed line features. Fig. 2.7(f) shows that adding a small amount of liquid silicone (2 vol.%) to create capillary bridges changes the viscoelastic properties of PDMS drastically. The cross-linked capillary suspension with  $G'$  higher than  $G''$  acts as an elastic paste. Thus, another mechanism for controlling the flowability and shape-retention of the silicone inks was introduced through this research.

### 2.5.3 Mechanical Performance

The mechanical characterization of elastomers including silicone has been extensively studied [96–102]. Silicones used in biomedical applications should generally demonstrate high tear strength ( $T_s$ ), tensile strength ( $\sigma_f$ ), and elongation at break ( $\epsilon_f$ ). Moreover, their hardness should be tuned for each application. For instance, in the case of the prosthetics, resilience, high elongation, and soft skin-like properties are necessary as they are usually removed for sleep and adhered to the skin when awake. This repetitive wearing/removing should be possible without the risk of damaging the prosthesis. Aziz et al. (2003) have investigated the mechanical properties of some commercial silicones used in prosthetics industry [103] (see Table 2.1), and pointed out the need for improvement in mechanical

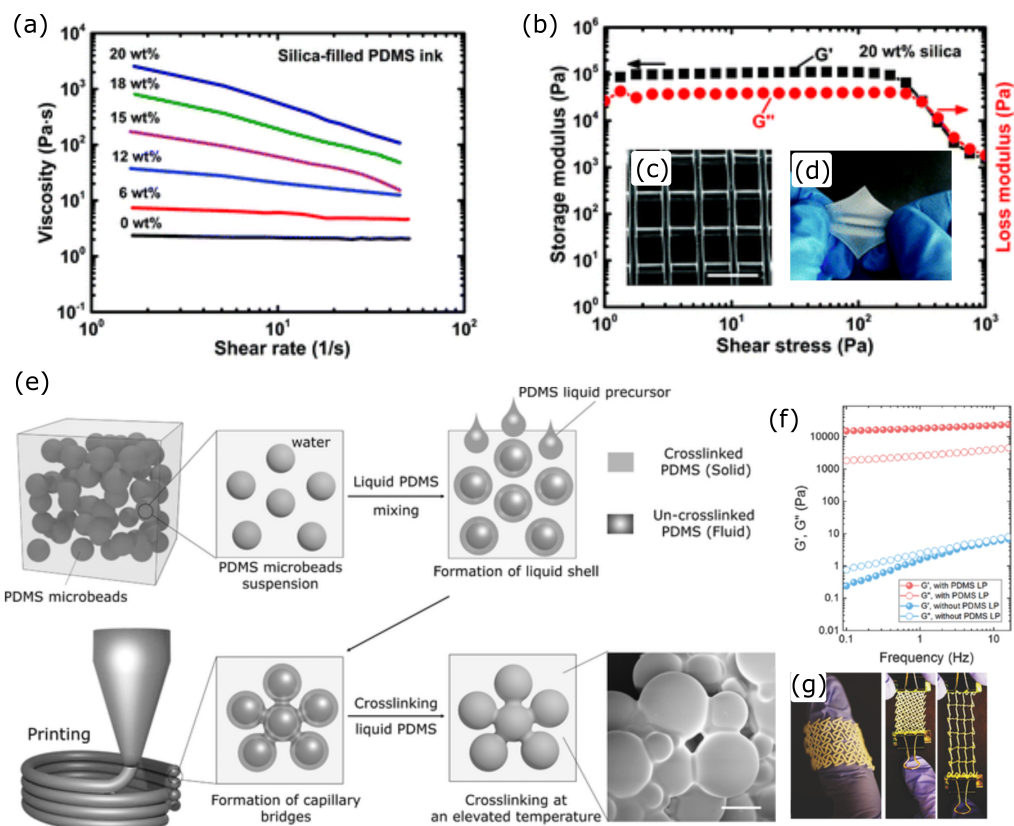


Figure 2.7: (a) The effect of silica on the viscosity of silicone; (b) 20% silica filler results in storage modulus greater than loss modulus for printing of porous parts with high shape retention; (c-d) sample of the 3D printed membrane; (c) The scale bar is 1 mm.(d) The 3D printed membrane under stretching. (a-d) (Adapted with permission from [95]. Copyright (2017) Royal Society of Chemistry). (e) The process of formation of capillary bridges; (f) The effect of capillary bridges on the storage and loss moduli of the PDMS; (g) A sample of flexible 3D printed structure from the capillary suspensions. (e-g) (Adapted with permission from [93]. Copyright (2017) Wiley and Sons).

and surface properties of currently available silicones. The shortcomings of current commercially available silicones and UV-curable elastomers in terms of their mechanical and

optical properties have also been well explained by Patel et al. (2017) [85].

Table 2.1: Mechanical properties of commercial silicones.

Property	Suggested Range
$\sigma_f$ [MPa]	5.5 – 8
$T_s$ [kN/m]	5 – 17
$\epsilon_f$ [%]	500 – 1200
Hardness [I.R.H.D.]	16 – 25

Ozbolat et al. (2017) have reported decreased level of air entrapment inside the silicone structures made using extrusion-based AM compared to molded structures resulting in the improvement of mechanical properties of AM-made silicone parts [104]. Based on their work, 1.5 - 4 % reduction in the porosity of silicone parts has showed an increase of up to 2-fold for  $\sigma_f$  and  $\epsilon_f$  for the parts with a printing path aligned with the uniaxial tensile test direction. Negligible difference in the stiffness of AM-made and bulk silicone has been reported in [73] as well.

Jindal et al. (2016 & 2017) proposed modifications to the PDMS structure to make it compatible with extrusion-based AM for maxillofacial prosthetics [105, 106]. They proposed an optimum combination of PDMS, catalyst, filler, and cross-linker to obtain the mechanical properties of commercial silicones typically used for the fabrications of facial prosthetics. The focus of their study was the development of a two-part **room temperature vulcanized (RTV)** silicone that undergoes a fast cure once extruded. In their study, Jindal et al. came to four conclusions about the effects of different components on silicone's mechanical properties. First, The combination of long (L) and short/medium (S/M) polymer chains (70% L – 30% S/M) improved mechanical properties. The short chains produced excessive local cross-links between the long chains resulting in higher tensile and tear strengths while the long chains maintained the elastomeric behavior of the substance. Second, increasing the amount of short/medium polymer chains (50% L - 50% S/M) resulted in a more brittle material, however, the hardness could be increased to up to 30 (Shore A). Third, increasing the amount of filler improved all mechanical properties, however, samples with more than 20 wt.% of filler were difficult to mix due to their high viscosity. 5 wt.% appeared to be the optimum amount of cross-linker. Fourth, higher concentrations of cross-linker increased the brittleness of the samples and reduced their flexibility [105]. The experimental results are summarized in Table 2.2. Once the optimum mechanical properties ( $3.5 \pm 0.6$  MPa for  $\sigma_f$ ,  $8.5 \pm 0.7$  kN/m for  $T_s$ , and  $24.3 \pm 0.5$  Shore A hardness) were achieved, they modified the curing system from an HTV to an RTV. The final silicone ink

could be cured in less than 1 minutes at room temperature after mixing the cross-linker and catalyst parts. In order to prevent slumping after extrusion, thixotropic agents were added to the silicone ink to increase its viscosity. This, however, resulted in a decrease in tear and tensile strength which was compensated for by addition of filler [106].

By taking advantage of the effect of crosslink density on the hardness and flexibility of polymers, Durban et al. developed silicones with a wide range of hardness from 10 to 70 (Shore A) tailored for material extrusion AM [94]. In their work, dihydrid chain extenders and short-chain vinyl-terminated PDMS have been used for decreasing and increasing of the crosslink density, respectively.

Foerster et al. demonstrated the effect of the cellular structures on the viscoelastic behavior of silicone parts fabricated via PPJ [89]. Based on their work, a higher level of porosity reduces both shear and loss moduli of the AM-made sample drastically, resulting in a less stiff structure; however, the highly porous structure showed a more thermally stable behavior for both  $G'$  and  $G''$  at 25 - 120 °C.

## 2.6 Discussion

The review of studies conducted on silicone AM showed that further work on development of AM systems and materials must be carried out. Table 2.3 summarizes 3D printing parameters such as lateral and vertical resolutions and printing speed, as well as the type of silicone used in the research work reported since 2013. Although not all parameters were reported in all papers, comparing the available results provides a clear understanding of the status of silicone AM research and highlights where there is room for improvement.

In material extrusion and FRE methods, the lateral resolution (i.e., the width of the printed linear features in XY plane) is adjusted by the amount of back pressure, nozzle velocity, inner diameter of the nozzle, and the stand-off distance between the nozzle tip and the substrate [104]. The latter is not applicable to the FRE where the period of elastic recovery and the interfacial interactions between the two phases affect the resolution [75]. Yuk et al. (2017) have extensively investigated the relationship between the nozzle velocity and stand-off distance to the pattern and dimensions of printed strands based on the viscoelastic properties of silicone [107]. The rheological properties of the silicone polymer also impact the lateral resolution of printed features if not cured *in-situ*. The silicone should be viscous enough so that it does not slump and is able to maintain its geometrical fidelity after being printed [105], and at the same time should demonstrate a shear-thinning behavior so that its viscosity is low enough for extrusion at the shear rate

Table 2.2: The mechanical properties of different combinations of PDMS chains with 5% cross-linker (adapted with permission from [105]. Copyright (2016) Elsevier).

	Long Chains (%)	Medium Chains (%)	Short Chains (%)	Avg. Mol. W. ( <i>kDa</i> )	Hardness (Shore A)	$\sigma_f$ (MPa)	$T_g$ (kN/m)
Composition A	70	20	10	29.4	24.3 ( $\pm 0.47$ )	3.52 ( $\pm 0.66$ )	8.48 ( $\pm 0.72$ )
Composition B	60	30	10	26.4	23.2 ( $\pm 0.37$ )	2.21 ( $\pm 0.54$ )	5.42 ( $\pm 1.61$ )
Composition C	60	20	20	25.7	24.7 ( $\pm 0.47$ )	2.79 ( $\pm 0.31$ )	5.87 ( $\pm 1.50$ )
Composition D	50	20	30	22	28.5 ( $\pm 0.76$ )	1.46 ( $\pm 0.29$ )	1.27 ( $\pm 0.36$ )

the ink experiences in the orifice. The minimum sufficient width reported so far is  $30\ \mu\text{m}$  by O'bryan et al. obtained by increasing the viscosity of the silicone ink and eliminating the interactions between the silicone surface and the support structure [75]. Femmer et al. reported printing  $100\ \mu\text{m}$  features, demonstrating the potential of vat photopolymerization techniques for the production of high resolution silicone parts [77]. This can be achieved by modeling the curing mechanism of the silicone while being exposed to UV light. The LOPP system introduced by Kim et al. has the maximum achieved raster width of  $1 - 2\ \text{mm}$  at the proof-of-concept stage.

Most researchers have not measured and reported the vertical resolution, and/or layer thickness, which controls the surface waviness and the general aesthetic aspects of the 3D printed objects. This property is controlled by the nozzle to the substrate off-set, the thickness of uncured layers of photopolymer, or the rheological properties of the ink for the extrusion, vat photopolymerization, and jetting systems, respectively. The minimum value reported for the vertical resolution is  $2\ \mu\text{m}$  (McCoul et al.) achieved by inkjet printing.

Generally, the speed of 3D printing is measured by the volume of material which is laid down, fused, or bound per unit of time. This important parameter has not been reported in most of the reviewed research work; however, the translational speed of printheads which has direct correlations with the 3D printing speed will be discussed in the following.

The nozzle speeds for material extrusion and FRE techniques are very similar. Depending on the pressure value, this speed in material extrusion can vary between  $1 - 20\ \text{mm}/\text{s}$ . The printhead speed for the aerosol jetting system reported by Reitelshofer et al. is  $5\ \text{mm}/\text{s}$  as well. The slow velocity of the mentioned methods can drastically reduce their adoption for clinical and industrial applications.

Up to now, drop-on-demand jetting systems has shown the highest velocity at around  $100\ \text{mm}/\text{s}$ . Unless systems capable of fabricating a 2D plane instantly, such as DMD-based SLA or [PBBJ](#), were employed for the production of silicone parts, jetting systems remain the fastest for the fabrication of highly viscous polymers such as silicone.

This review of sparse research in the area of silicone customization for AM shows the need for improvement in the polymerization mechanism of silicones, as well as their rheological and mechanical properties in parallel to the system development.

Considering long production time as the main hindrance to industrial adoption of AM in general, heat-curable silicones with the minimum gelation time of  $5\ \text{min}$  should be replaced with irradiation-curable systems in order to make silicone AM more attractive at a commercial level. Current trials investigating the development of UV-curable silicones have been limited to the vat photopolymerization techniques. In the future, UV-curable silicones should be developed for material extrusion and jetting systems as well. The



instantaneous curing, lack of surface tackiness after photopolymerization, long working hours under visible light, and biocompatibility will be key factors in development of such materials. A holistic study of the effects of silicone's rheological properties on its flow, extrusion, and jettability needs to be performed as well so that the behaviour of these non-Newtonian viscous fluids can be predicted and controlled. Tuning the mechanical properties of UV-curable silicone with optimized rheological properties is also necessary. Finally, the mechanical performance of the parts manufactured using any of the reviewed AM methods should be tested and compared to that of bulk materials.

## 2.7 Conclusion

The review showed that the feasibility of silicone AM in a PBBJ process has not been investigated before. Material extrusion and FRE methods can already shape form fully functional and complex structures, however, at a low speed. Among all, material jetting and DMD-based vat photopolymerization techniques seem to be able to provide solutions to the AM of silicone with a high throughput. For material jetting, improvements in three aspects of resolution, scalability, and multi-color printing are necessary. For the vat photopolymerization, the current challenge is design and development of affordable mask-projection laser-optical systems to build structures in the middle of polymer reservoir without crosslinking the voxels that are not going to be a part of the final shape. Complemented with customization of silicone properties for different AM processes, 3D printing might become the new standard approach for manufacturing of bio-structures.

Table 2.3: Comparison of the 3D printing features for the silicone AM techniques

AM Method	Authors / Company	Publication Year	Lateral Resolution ( $\mu\text{m}$ )	Vertical Resolution ( $\mu\text{m}$ )	Printing Speed ( $\text{mm}/\text{s}$ )	Curing System	Viscosity ( $\text{mPa}\cdot\text{s}$ )
Material Extrusion	Maunor et al.	2013	*	*	*	*	*
	Duoss et al.	2014	100-610	*	1-20	HTV	*
	Liravi et al.	2015	250-300	100	5-10	UV	40,000
	Schmalzer et al.	2016	*	*	*	HTV	*
Freeform Reversible Embedding	Hinton et al.	2016	140-400	100	20	HTV/Moisture	3,000-4,000
	O'bryan et al.	2017	30-700	*	2-10	UV	*
	Fripp Design Ltd.	2016	*	*	*	RTV	*
	Femmer et al.	2014	100-400	*	*	UV	*
Vat Photopolymerization	Kim et al.	2016	*	1000-2000	*	UV	*
	Reitelshofer et al.	2016	*	30	5	HTV	2,000
Material Jetting	Liravi et al.	2017	500-600	300	100	UV	40,000
	Wacker Chemie AG (ACEO)	2015	*	*	*	UV	*

\* Not reported

# Chapter 3

## Additive Manufacturing of Silicone via Material Extrusion

### 3.1 Introduction

Material extrusion is one of the seven classes of AM, based on the ASTM F 2792-12a standard [108]. Nozzle dispensing is one of the techniques used under this class of AM that has gained attention from academia and industry due to its emerging applications in different areas from electronics [109–111] and microsystems packaging [112] to tissue engineering [113, 114]. This technology has been reported to be the most widely used method in bio-manufacturing and life sciences [55, 115]. Material extrusion includes a wide range of different AM processes, and different definitions have been proposed for it. However, all of these definitions enumerate the following characteristics: (1) the ability to produce 3D objects; (2) the ability to manufacture on planar and non-planar surfaces; (3) the ability to process a wide range of materials including metals, polymers, ceramics, biomaterials etc.; and (4) the ability to fabricate structures at different dimensional scales from nano- to millimeter [112].

This flow-based manufacturing method produces 3D structures by depositing a continuous stream of the material onto a surface using a robotically controlled nozzle [59, 116]. The movement of nozzle in the z-direction and depositing a new layer of fluid on top of the previous layers and/or support structures makes the manufacturing of a 3D structure possible [53]. The deposited fluid turns into solid after dispensing by cooling, photo-curing, or solvent evaporation [59].

Different dispensing mechanisms are being used to push the fluids through a nozzle in a nozzle dispensing system with pressure-actuated (pneumatic) and mechanical dispensing systems being the most popular [59]. In pressure-actuated nozzles, a time-controlled compressed air is used to activate the deposition process. Simple mechanism of these nozzles along with their easy operation and maintenance are the reasons for their widespread adoption for in-house developed AM systems. Mechanical dispensing systems use either a screw-based or a positive-displacement mechanism which generate the required force for deposition by rotation of a stepper motor or linear displacement of a piston, respectively [55]. Although mechanical dispensing systems provide better control for low volume feed rates of fluids, they have a maximum force limit which will constrain their application in dispensing of highly viscous materials [53, 55]. As a result, among prevalent AM technologies, pressure-actuated nozzle dispensing system is more suited for the fabrication of 3D structures from viscous materials [54].

Vozzi et al. (2002) introduced the driving pressure produced by the compressed air ( $P$ ), polymer surface tension ( $\gamma$ ), and the friction between the fluid and the internal nozzle wall ( $F_f$ ) as the main forces that determine the flow of viscous materials in these systems [117]. In this dynamic fluid model, width of the deposited fluid ( $W_d$ ) can be calculated from the internal radius of the nozzle ( $R_s$ ), viscosity of fluid ( $\mu$ ), printing velocity ( $v$ ), height of the printed pattern ( $H$ ), length of the tapered zone of the nozzle ( $h_z$ ), and air pressure ( $P$ ) using Eq. 3.1. These significant forces are depicted in Fig. 3.1. Based on this work, an analytical model was developed to relate the injection process and dimensional parameters of the extrusion-based system [118]. In this two-tier model, first model estimates the flow of fluid through the nozzle and the second one predicts the dimensional parameters of the extruded fluid based on the results of first model. These models, however, assume that the material has a low viscosity, the fluid is Newtonian, and the flow is laminar throughout the dispensing system. These assumptions are not valid for injection of medical-grade silicones that are mostly non-Newtonian fluids with paste-like behavior. As a result, alternative methods such as statistical experimental design and [finite element modeling \(FEM\)](#) can be adopted to control the dimensional accuracy and surface quality of the deposition for different materials. Multiple research groups have used similar statistical analysis tools to improve the quality of their additively manufactured parts [119–121].

$$W_d = \frac{\pi R_s P}{8\mu V h h_z} \quad (3.1)$$

The feasibility of direct additive manufacturing of highly viscous silicone using material extrusion technique is evaluated in this chapter; moreover, the influence of process

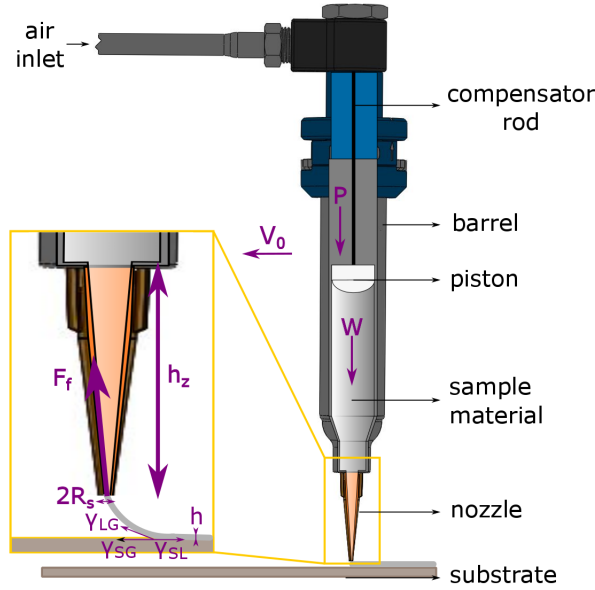


Figure 3.1: Influential forces in fluid dispensing: compressed air ( $P$ ), polymer surface tension ( $\gamma$ ), the friction between the fluid and the internal nozzle wall ( $F_f$ ), and the weight of fluid ( $W$ ). The width of the deposited fluid can be calculated from the internal radius of the nozzle ( $R_s$ ), viscosity of fluid ( $\mu$ ), printing velocity ( $V_0$ ), height of the printed pattern ( $h$ ), length of the tapered zone of the nozzle ( $h_z$ ).

parameters on the dimensional accuracy of printed silicone lines and the surface quality of printed silicone planes is investigated. To this end, different statistical techniques have been adopted. To conduct an initial investigation, [design of experiments \(DoE\)](#) has been used, followed by the response optimization to obtain the target dimensions using desirability function approach. In order to relate the significant parameters, an empirical mathematical model has been presented. The results of this study assure uniform and precise printing of highly viscous silicone which can be used as a basis for the fabrication of three-dimensional shapes using material extrusion technique. The surface properties of printed structures can also be controlled resulting in the fabrication of implants with desired surface texture that can eliminate the complications after the surgery. In other words, prosthetic implants with desired smoothness can be produced using this technique. The effects of surface properties of implants on their acceptance by body have been studied by different researchers [\[122, 123\]](#).

Finally, in order to predict the dimensions of extruded features, a [FEM](#) of the dispensing

of highly viscous silicone is presented. The modeling results are experimentally validated by comparing the simulated injection flow profile with that of the real process. The model is proved to be accurate in predication of the dispensing profile and the geometry of injected fluids.

## 3.2 Materials and Methods

### 3.2.1 Silicone

Commercial biocompatible silicone (RTV 800 – 400, Novagard Solutions, OH, USA) was used as-received for optimizing the extrusion process in this study. Similar silicone with lower viscosity (RTV 800 – 620, Novagard Solutions, OH, USA) was used to model the dispensing procedure. These two polymers are UV-curable, and contain the photoinitiator Irgacure TPO-L (BASF Corporation, MI, USA) which is sensitive to the long wavelength UV light (less than 500 *nm*).

#### Viscosity Measurement

The viscosity of RTV 800 – 620 was measured using a rotational viscometer (High Shear CAP-2000+, Brookfield, MA, USA). The experimental results (Fig. 3.2) demonstrate the shear thinning behavior of this polymer. Experimental results plotted in semi-logarithmic scale can be modeled using Carreau-Yasudas model (Eq. 3.2).

where  $\mu$  is the dynamic viscosity,  $\mu_0$  is the initial value of viscosity,  $\mu_\infty$  is the infinite value of viscosity (mostly zero),  $\lambda$  is the relaxation factor and represents the time after which the transition to non-Newtonian region happens,  $a$  is the width of transition (non-Newtonian) region, and  $n$  is the slope of the power-law region. Parameters  $\mu_0$  and  $\mu_\infty$  can be measured from the experimental data. Parameter  $a$  is considered to be 2. The values of  $\lambda$  and  $n$  are estimated by fitting a curve to the experimental data using the least square curve fit algorithm of MATLAB. The Carreau parameters are presented in Table 3.1.

$$\mu - \mu_\infty = (\mu_0 - \mu_\infty)(1 + (\lambda\dot{\gamma})^a)^{\frac{n-1}{a}} \quad (3.2)$$

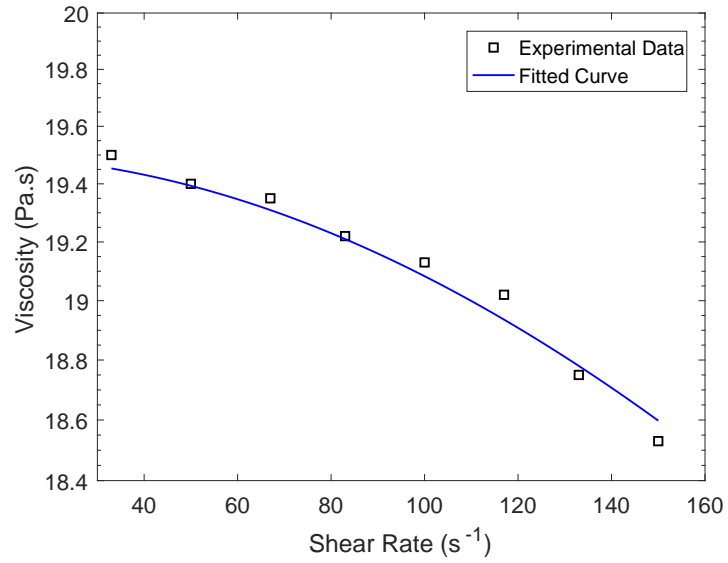


Figure 3.2: Viscosity vs. shear rate for silicone RTV 800 – 620.

Table 3.1: Rheological parameters of silicone RTV 800 – 620

$\mu_0$ (Pa.s)	$\mu_\infty$ (Pa.s)	$\lambda$ (s)	$n$
19.9	0	0.0016	0.79

## Surface tension measurement

Measurement of the surface tension of silicone (RTV 800 – 620) was carried out using an in-house developed instrument designed based on [axisymmetric drop shape analysis profile \(ADSA-P\)](#) technique. The details of development of this instrument can be found in [124]. The calculation of surface tension value is made by fitting the geometrical dimensions and profile of the pendant droplet to those obtained from Young-Laplace equation of capillary throughout the injection (Eq. 3.3):

$$\Delta P = \gamma \left( \frac{1}{R_1} + \frac{1}{R_2} \right) \quad (3.3)$$

where  $\Delta P$  denotes the pressure difference across the surface,  $\gamma$  denotes the surface tension,  $R_1$  and  $R_2$  are the principal radii of curvature. Images of the pendant droplet are captured during the injection and [sum of squares \(SS\)](#) of the normal distance between the experimental and theoretical points are minimized in [ADSA-P](#) method. After fitting the best curve to the profile of droplet, the software calculates volume, surface area, and surface tension of the droplet. This process is continued until a steady-state value for the surface tension is reached [125]. Fig. 3.3 shows the pendant silicone drop and the fitted Laplace curve. The density of silicone ( $0.87 \text{ g/cm}^3$  at  $18 \text{ }^\circ\text{C}$ ) is an input for calculating the surface tension which is plugged into the model by the following capillary constant:

$$c = \frac{\Delta \rho g}{\gamma} \quad (3.4)$$

where  $c$  is the capillary constant,  $\Delta \rho$  is the difference between the densities of silicone and air, and  $g$  is the acceleration of gravity [26]. The value of silicone/air surface tension measured with this technique is approximately  $18.9 \text{ mN/m}$ , which is very similar to the values reported in the literature for other silicone polymers [126, 127].

## Contact angle measurement

The measurement of contact angle ( $\theta_c$ ) between silicone (RTV 800 – 620) and glass slide and that of the silicone and plastic nozzle tip was carried out using the captured photos of the fluid (Fig. 3.4). The open source image processing software ImageJ was used for this purpose. As contact angle of silicone on the glass substrate varies with time, the value of contact angle was measured at  $1 \text{ s}$  time intervals and a regression model (Fig. 3.5) was fit to model its changes over time. Different values of  $\theta_c$  can be found in Table 3.2. Figure 3.5 shows samples of  $\theta_c$  measurement on different surfaces.



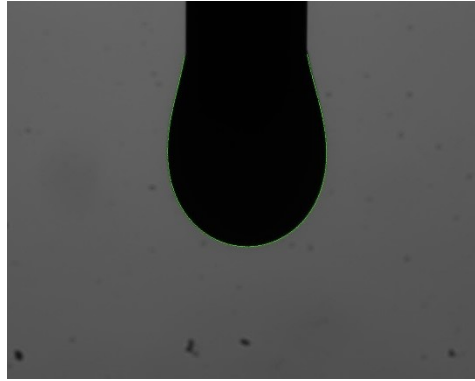


Figure 3.3: Silicone drop image captured using ADSA-P technique.

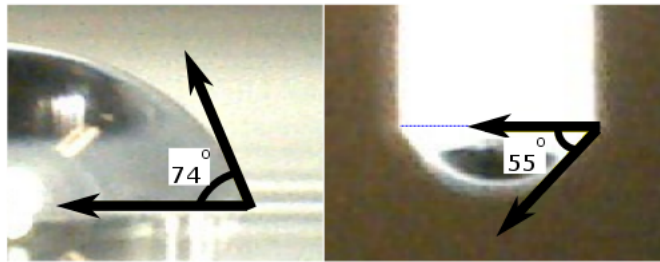


Figure 3.4: Contact angle between (a) silicone droplet and glass slide, (b) silicone and plastic nozzle tip.

Table 3.2: Contact angle between silicone and glass substrate vs. time.

$t$ (s)	4	5	6	7	8	9	10
$\theta_c$ (rad)	2.25	1.9	1.73	1.47	1.48	1.45	1.29

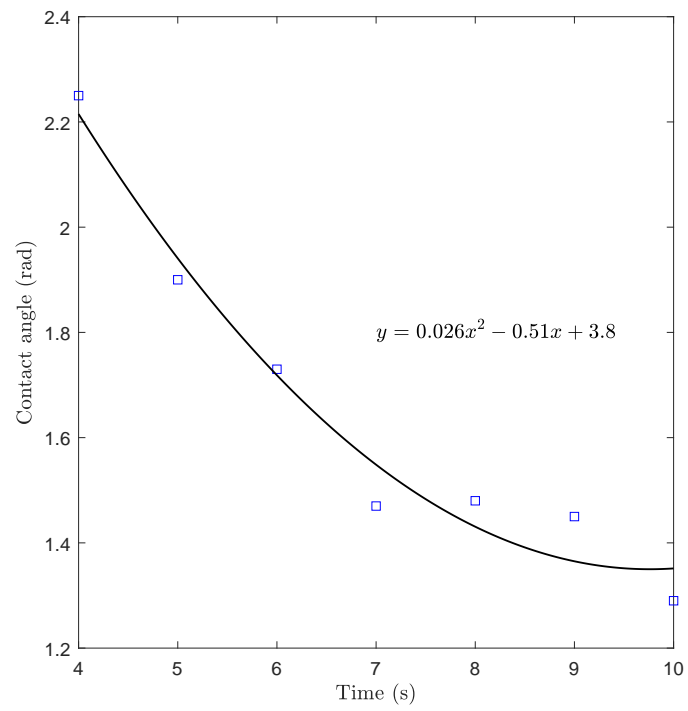


Figure 3.5: Fitted curve to the variations in the value of contact angle of silicone and glass substrate.

### 3.2.2 Experimental Setup

A pressure-actuated printhead has been used in our 3D printer. In this type of printhead, the time-controlled compressed air is used to activate the deposition process. The first step in AM of silicone products using material extrusion is developing a CAD model of the part. Then, the part will be fabricated layer-by-layer by direct deposition of silicone from a nozzle. The deposition process can be done using pneumatic or piezoelectric actuators. Another nozzle needs to be used to fabricate sacrificial support structures. For this study, an in-house-developed pneumatic micro-syringe deposition system that uses an air-powered dispenser (Ultimus<sup>TM</sup> V high precision dispenser, Nordson, OH, USA) is used and proved to be able to inject highly-viscous silicone consistently [128]. The additive manufacturing set up is shown in Fig. 3.6.

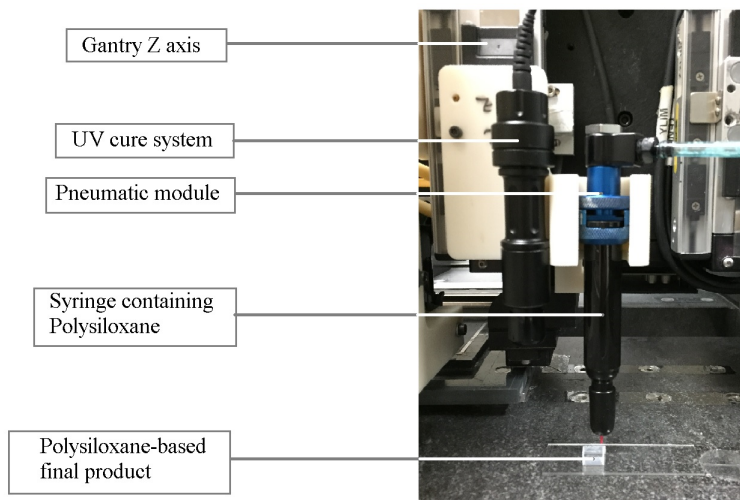


Figure 3.6: Components of the micro-syringe nozzle dispensing system.

### 3.2.3 Sample Preparation and Profilometry

The material extrusion technique was used to produce 1 *cm* straight silicone line features (RTV 800 – 400). Pressure ( $P$ ), printing velocity ( $v$ ), and working distance ( $WD$ ) (distance between the substrate and nozzle tip) were the process parameters that have been changed to print different samples. Before printing, the microscope slides used as substrate were washed with acetone and dried. Immediately after printing, silicone lines were cured with UV lamp for 10 *s* and left overnight to make sure that the full polymerization has happened.

Dimensional properties of lines: average width ( $W_{avg}$ ), uniformity ( $W_{s.d.}$ ), and surface waviness ( $W_{avg}$ ) were investigated using two-dimensional (2D) and 3D images produced by means of a 3D optical profilometer (UP series, Rtec Instruments, USA). The optical profilometer scans the printed silicone-based line patterns using a white light-emitting diode (LED) light source with a sub-micrometer vertical resolution. The scanning area has a dimension of  $1\text{ mm} \times 1\text{ mm}$ . High resolution 2D images were used to calculate width of samples at five different locations as shown in Fig. 3.7(a). A  $250\text{ }\mu\text{m}$  precision dispensing tip (Smoothflow tapered tip, Nordson Corporation, OH, USA) was used to print sample lines. The average of five values is considered as the average width of that sample and their standard deviation is considered as the measure of uniformity. In order to quantify the surface quality, the surface profile of sample at aforementioned five locations was obtained and, the difference between the highest peak and lowest dip for every plot was calculated and averaged out. The lower this value, the higher the surface quality will be. Figure 3.7(b) shows a sample of surface profile. Figures 3.8(a-d) shows the difference in the uniformity of width for some of the samples. Excessive pressure and low printing velocity create wide lines (Fig.3.8(a)). Figures 3.8(a-b) are products of suitable combination of process parameter values and have produced finer lines; however, the difference in their surface quality is obvious. Figure 3.8(d) shows failure in printing of a uniform line, mostly due to the large working distance or high printing velocity. Different level sets of process parameters result in different surface qualities. 3D images shown in Fig. 3.8(e-f) demonstrate this difference in the quality of surfaces. The printed line in Fig. 3.8(e) has a non-uniform surface with lots of fluctuations in one side. On the other hand, Fig. 3.8(f) shows a smooth surface with lower roughness.

In order to optimize the surface quality of the 3D plane features<sup>1</sup>, a layer of  $1\text{ cm} \times 1\text{ cm}$  silicone square was made on a silicon wafer. The 3D image of each sample was captured using an optical/laser profilometer (VK-X250, Keyence, Japan) at  $100\times$  magnification. The root mean square of surface waviness ( $W_q$ ) at the filter cut-off wavelength of  $0.08\text{ mm}$  was selected as a measure of the surface quality. Waviness is described as the uneven features that are repeated periodically on the surface at longer intervals compared to the roughness. The profile data was collected over 31 lines. The waviness was measured for each line, and their average was used as the final surface quality value. Figure 3.9 shows a sample of the waviness measurement and the surface profile.

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<sup>1</sup>The experimental results related to the surface quality of planes are adapted from author's published work [28].

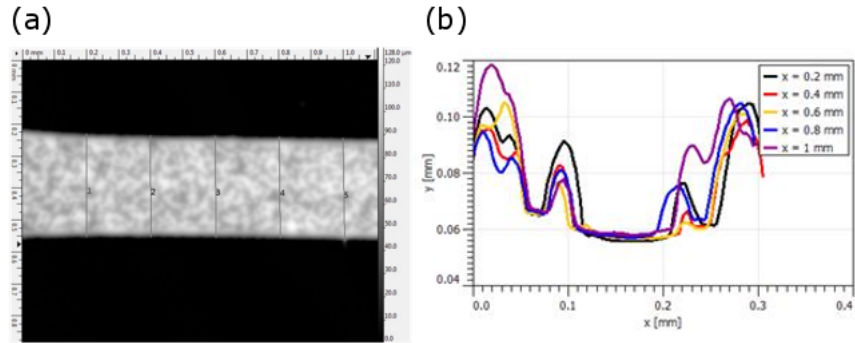


Figure 3.7: (a) Sample width five locations is measured. Average and standard deviation of five values are used as measures of sample width and uniformity, respectively; (b) Surface profile is used to calculate the difference between the highest peak and lowest dip as a measure of surface quality.

### 3.2.4 Time-lapse Imaging

A calibrated digital Microscope (Dino Lite, AnMo Electronics Corporation, Taiwan) was used to capture the geometry and location of the silicone (RTV 800 – 620) flow at predefined time intervals during the dispensing process. The microscope was fixed on its holder at the distance of 10 mm from the nozzle tip with a magnification of 42 $\times$ . Images of the dispensing process captured with digital microscope were used to validate the FEM results. The software DinoCapture was used to measure the geometrical and flow parameters.

### 3.2.5 Experimental Designs

An experimental procedure was designed to find the optimum treatment combination of the process parameters ( $P$ ,  $v$ , and  $WD$ ) to achieve the minimum line width without any significant reduction in the surface quality and uniformity. A review on the scientific background of DoE is provided in A.1. Two replicates of the experiment were conducted to capture the variance in the process with higher accuracy and two center points were chosen to study the curvature as well. The number of replicates was determined using power and sample size for 2-level factorial designs. As a result a 2-level full factorial experiment with 2 replicates and 2 center points was designed which resulted in 18 runs. It would have been possible to choose a resolution III design with 10 runs, but this design confounds main factors and second order interactions which will make it difficult to find

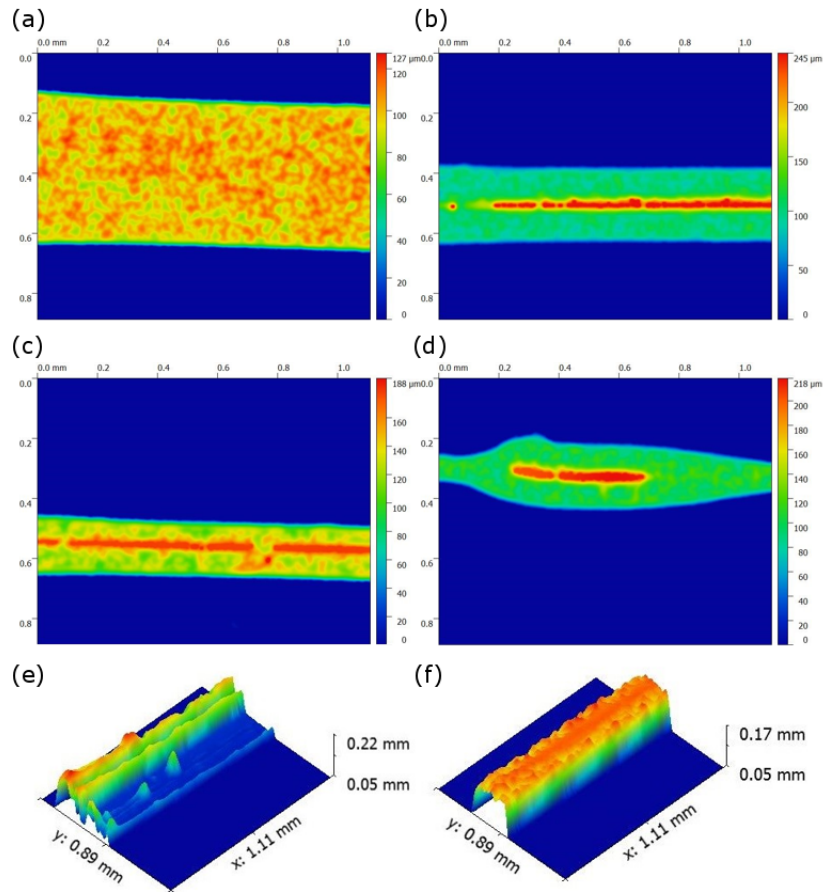


Figure 3.8: (a-d) 2D Profilometry results showing different width and uniformity variations of lines extruded using RTV 800 – 400 silicone based on changes in the process parameters, (a)  $P = 200 \text{ kPa}$ ,  $V = 5 \text{ mm/s}$ ,  $WD = 0.5 \text{ mm}$ , (b)  $P = 150 \text{ kPa}$ ,  $V = 7.5 \text{ mm/s}$ ,  $WD = 0.35 \text{ mm}$ , (c)  $P = 100 \text{ kPa}$ ,  $V = 5 \text{ mm/s}$ ,  $WD = 0.2 \text{ mm}$ , (d)  $P = 100 \text{ kPa}$ ,  $V = 5 \text{ mm/s}$ ,  $WD = 0.5 \text{ mm}$ ; (e-f) 3D Profilometry results showing different surface profiles based on changes in process parameters, (e)  $P = 200 \text{ kPa}$ ,  $V = 5 \text{ mm/s}$ ,  $WD = 0.5 \text{ mm}$ , (f)  $P = 150 \text{ kPa}$ ,  $V = 7.5 \text{ mm/s}$ ,  $WD = 0.35 \text{ mm}$ .

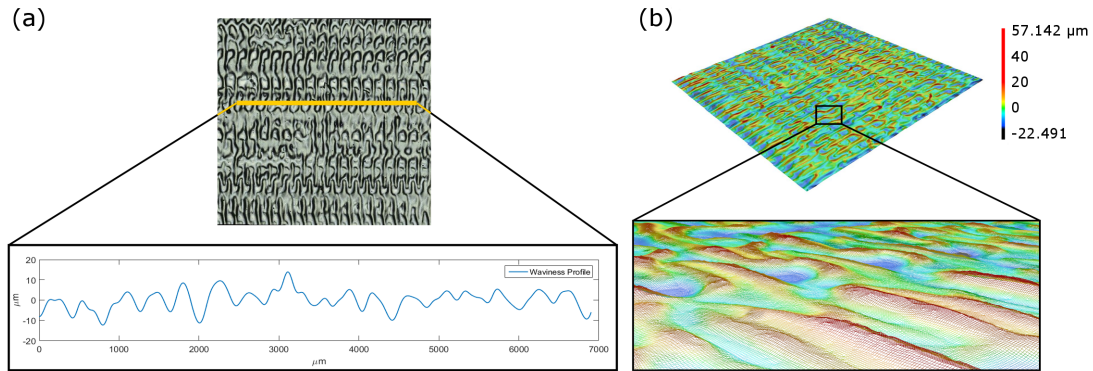


Figure 3.9: Sample of surface characterization for the RTV 800 – 400 silicone plane features: (a) the optical and laser image of the printed sample and the waviness profile obtained at the cut-off wavelength of  $0.08\text{ mm}$  over the scanning length, (b) 3D profile of the printed plane.

the significant factors. The experimental factors and levels for initial  $2^3$  factorial design are shown in Table 3.3.

At final stage, all responses were optimized simultaneously considering all the process parameters using the desirability function method. The details of this technique are provided in A.2. In the simultaneous optimization, the importance of  $W_{avg}$  and  $W_{s.d.}$  are considered three times and twice the  $W_q$ , respectively. The quality of the 3D printed products is highly dependent on the resolution of single lines that are the building units of every layer [129]. The less the width of the line features, the higher the quality of final structure. Consequently, the highest priority has been assigned to  $W_{avg}$  in the optimization process. On the other hand, the surface quality can be improved in the post-processing. Hence it gets lower weight in the optimization algorithm [130–132].  $W_{s.d.}$  is of a mid-level importance compared to the two other parameters.

Table 3.3: Levels of process parameters for optimization of line features in material extrusion technique for silicone RTV 800 – 400.

Experimental Factors	Low (-1)	Center (0)	High (+1)
$P$ (kPa)	100	150	200
$v$ (mm/s)	5	7.5	10
$WD$ (mm)	0.2	0.35	0.5

Similar experimental design was conducted to optimize the surface quality of the 3D layers (planes) printed via material extrusion. A  $2^4$  full factorial design with one center point was designed and replicated twice. The parameters under study are same as those investigated for the line features in addition to the  $RW$ . These four screening factors and their lower and higher levels are shown in Table 3.4. The resulting 34 treatment combinations were printed in a completely randomized order.  $W_q$  was measured for each sample as explained in Section 3.2.3.

Table 3.4: Six Influential factors and their treatment levels for the material extrusion of plane features.

Factors	Low Level (-1)	High Level (+1)
$RW$ (mm)	0.1	0.2
$v$ (mm/s)	10	20
$WD$ (mm)	0.1	0.15
$P$ (kPa)	150	200

### 3.2.6 Numerical Modeling

Different numerical methods have been proposed to simulate the motion of the interface of two immiscible fluids. These methods can be classified into three groups of Lagrangian, Eulerian, and arbitrary Lagrangian-Eulerian (ALE) methods [133]. In this chapter, Level-set method, an Eulerian method, is employed to simulate the dispensing of silicone using transient Navier-Stokes equations. The level-set method is explained in details in A.3. 2D and 3D finite element algorithms which are able to solve full non-linear Navier-Stokes equations for predicting the emerging and evolution of droplet of a Newtonian fluid have been developed by Wilkes et al. (1999) for the first time [134]. The equations governing the fluid flow in nozzle dispensing systems are provided in A.4.

A time-dependant two-phase laminar flow interface was chosen in COMSOL multi-physics 5.1. This interface is a part of both computational fluid dynamics (CFD) and microelectromechanical systems (MEMS) modules. The designed 2D axisymmetric geometry is presented in Fig. 3.10(a). Parts  $I$  and  $II$  represent the inner geometry of the tapered nozzle tip and air, respectively. The two fluids are distinguished by defining two different initial values for parts  $I$  and  $II$ . Air has been called from the COMSOL material library and silicone has been custom defined. The density of silicone ( $\rho$ ) was set as a constant value and its viscosity ( $\mu$ ) was defined using the Carreau model parameters, listed in Table 3.1.



The inner diameter of the nozzle and its distance from the substrate are shown in the Fig. 3.10(a) as well. The gap between the nozzle tip and air represents the plastic wall of the nozzle tip, and is modeled to prevent numerical errors at the initial phase of dispensing. Only the tapered part of the nozzle is modeled as the pressure gradient in the cylindrical upper part of nozzle and throughout the barrel is negligible [118].

The boundaries are marked in Fig. 3.10(a) with letters **a-g**. Boundary **a** is defined as pressure inlet. Pressure is applied to this boundary using the following equation:

$$P_{air}[step(t[\frac{1}{s}]) - step(t[\frac{1}{s}] - t)] \quad (3.5)$$

where  $P_{air}$  is the amount of pressure and  $t$  is the total time the pressure is activated. Function  $step$  is used to avoid inconsistent initial condition when pressure is applied and removed. This step function smooths the transition of the value of pressure from zero to  $P_{air}$  at time 0 and from  $P_{air}$  to 0 at time  $t$ . Boundary **b** is a no-slip wall and covers the wall of barrel. Boundary **c** models the microscope slide substrate as a wetted wall with contact angle presented in Fig. 3.4. The slip length is suggested to be equal to the average length of mesh. Boundary **d** represents the inlet of air with pressure zero. The initial interface of two fluids is defined in boundary **e**. Even at the highest vacuum pressure of the dispensing system (4.48  $kPa$ ), oozing of silicone creates a semi-spherical droplet before the printing, boundary **e** shows this aggregation of material at nozzle tip. Boundary **f** is a no-slip wall, and boundary **g** models the wetted wall with contact angle of  $55^\circ$ .

The effect of weight was considered by defining gravity for the entire geometry. In order to complete the design of FEM, the surface tension of silicone was introduced to the model as a user defined parameter. Considering the dependency of the quality of the results on the meshing, mesh independency analysis was done and a triangular mesh with 0.012  $mm$  and 0.084  $mm$  as the minimum and maximum element sizes, respectively, was selected. Fig. 3.10(b) demonstrates the mesh elements.

## 3.3 Results and Discussion

### 3.3.1 Optimizing the Extrusion of Line Features

#### Factor Screening

Dimensional accuracy and surface quality of the silicone lines manufactured with extrusion technology depend on many factors including the printing velocity, pressure, working dis-

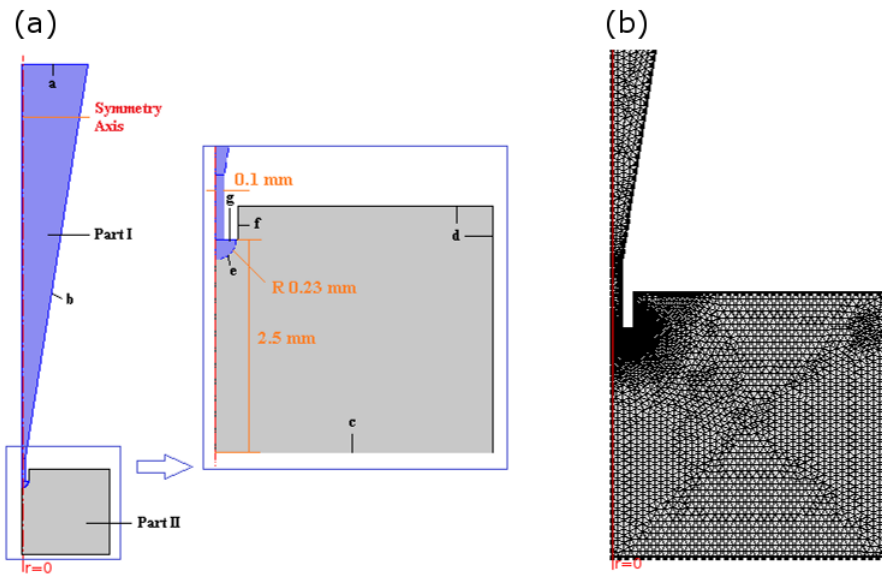


Figure 3.10: (a) Geometry and boundaries of the model: part *I* represents the silicone inside the nozzle tip, part *II* represents the air,  $r = 0$  is the symmetry axis, **a** is pressure inlet, **b** is no-slip wall, **c** is wetted wall, **d** is air inlet, **e** is initial interface of fluids, **f** is no-slip wall, **g** is wetted wall; (b) Meshing: triangular mesh was chosen for both domains, mesh independency analysis resulted in an optimized value of 10938 mesh elements with minimum and maximum sizes of 0.012 *mm* and 0.084 *mm*, respectively.

tance, substrate preparation, curing time, environmental conditions, etc. It is not feasible to study all these factors as it will be extensively time consuming. The most important process parameters ( $P$ ,  $WD$ , and  $v$ ) have been selected as controlling factors for the dimensional accuracy of printed parts. The factor screening design is shown in Table B.1. As explained in section 3.2.5 a total of 18 silicone lines based on different factor level combinations were printed and their width, uniformity, and surface waviness were investigated using a 3D optical profilometer.

Figure B.1(a-d) shows the significant process parameters for three different responses in a normal plot of standardized effects. Significant factors are highlighted in red in these plots and are far from the line indicating a lower P-value. In Pareto chart (Fig. B.1(d)), factors with a maximum value located left to the 2.262 line are insignificant. All three main process parameters and the interaction  $P \times v$  have a significant effect on  $W_{avg}$  at a 95% confidence level. For  $W_{s.d.}$ , only  $P$  and  $WD$  and their interaction are significant. None of the process parameters have a significant effect on  $W_q$ ; however, the Pareto chart for the surface quality shows that  $v$  and the interaction  $v \times WD$  have highest impacts on the final quality of the surface. After removing the insignificant process parameters and rerunning the model, process parameter coefficients in regression equation ( $\beta_i$ ) were calculated. The coefficient values are shown in Table B.2. Table B.3 also presents [analysis of variance \(ANOVA\)](#) and summary of average width and uniformity models after removing insignificant parameters.

As seen in Table B.3, all the parameters have a p-value of less than 0.05 meaning they are significant. Table B.3 also presents [degree\(s\) of freedom \(DF\)](#) and other parameters required for ANOVA for significant factors. The last two parameters both are the measures of variation of different terms of model with the only difference being consideration of DF for calculation of [adjusted mean of squares \(adj MS\)](#). R-squared and adjusted R-squared show how close the observations (measurements) are to the fitted regression line. The values of R-squared and adjusted R-squared for both models are above 90% showing a very good regression fit. The p-value of center points show that the curvature is not significant for both models. It means that the response value follows a pure decreasing or increasing path as we increase one parameter from low level to high level. In other words, the response value at the center is not higher or lower than that of the low and high levels. As a result, the regression model (Eq. 3.5) and its coefficients presented in B.2 are enough to relate the influential factors and responses, and there is no need to use [response surface methodology \(RSM\)](#). RSM is a method to explore the relationship between process parameters in the optimized area if the curvature is significant. This method is usually followed by factor screening and response optimization.

In order to make sure the models are valid, analysis of residual plots is required. Dif-

ferent residual plots are displayed in Fig. B.2 for average width. The residual plots show that the normality and independence assumptions are valid. The normal plot however shows two outliers at the beginning and end of the data series. More investigations showed that the outliers are associated with severely non-uniform prints. The purpose of the study is to prevent the generation of such non-uniform lines. It seems that there is not enough evidence indicating those outliers are caused due to any other reason such as a change in the experiment environment, operator, or measurement equipment. Hence, the analysis was continued without removing the outliers. Same analyses may be extended to uniformity and surface quality residual plots. There seems to be a slight lack of homogeneity of variance which may have arisen from the slight errors in calculation of width average in image processing software (operator error) or insufficient number of samples, but it is not significant enough to require corrective actions like logarithmic or square root transformations.

### Simultaneous Optimization of Responses

After screening the process parameters and calculating the regression coefficients, the response optimization was carried out in order to minimize the value of  $W_{avg}$ ,  $W_{s.d.}$  and  $W_q$ . The optimization was done simultaneously and the parameter levels are same as the levels presented in Table 3.7. Priority of the optimization was given to  $W_{avg}$  with an importance value of 3, followed by  $W_{s.d.}$  and  $W_q$  with importance values of 2 and 1, respectively. Table 3.5 presents the summary of response optimization. The target values and upper limits were calculated automatically based on the results of factor screening. Table 3.6 shows the optimized level set that minimizes the responses based on the importance levels provided in Table 3.5. It can be inferred that the low level ( $-1$ ) values for all three process parameters result in the narrowest silicone lines and best quality. The optimization result can be seen well in Fig. B.3. The level set combination  $-1, -1, -1$  result is predicted to give the average width of  $322.8 \mu m$ , standard deviation of  $3.8 \mu m$  for five measures of width (uniformity), and a maximum of  $43.5 \mu m$  difference in surface altitude over the measurement path (surface quality). Table 3.6 also presents 95% confidence and prediction intervals for every response. Mean of the population falls inside a 95% confidence interval. Also there is a 95% chance that the value of an observation falls within the range of a 95% prediction interval.

Table 3.5: Summary of response optimization.

Response	Goal	Target	Upper limit	Importance
$W_{avg}$ ( $\mu m$ )	Min	42.4	870.6	3
$W_{s.d.}$ ( $\mu m$ )	Min	0.5	32.75	2
$W_q$ ( $\mu m$ )	Min	8	290.3	1

Table 3.6: Response optimization predications.

Response	Fit	95% Confidence Interval	95% Prediction Interval
$W_{avg}$ ( $\mu m$ )	322.9	(240.5, 405.2)	(154.1, 491.6)
$W_{s.d.}$ ( $\mu m$ )	3.78	(0.32, 7.24)	(-3.96, 11.51)
$W_q$ ( $\mu m$ )	43.5	(-66.9, 154.0)	(-147.8, 234.9)

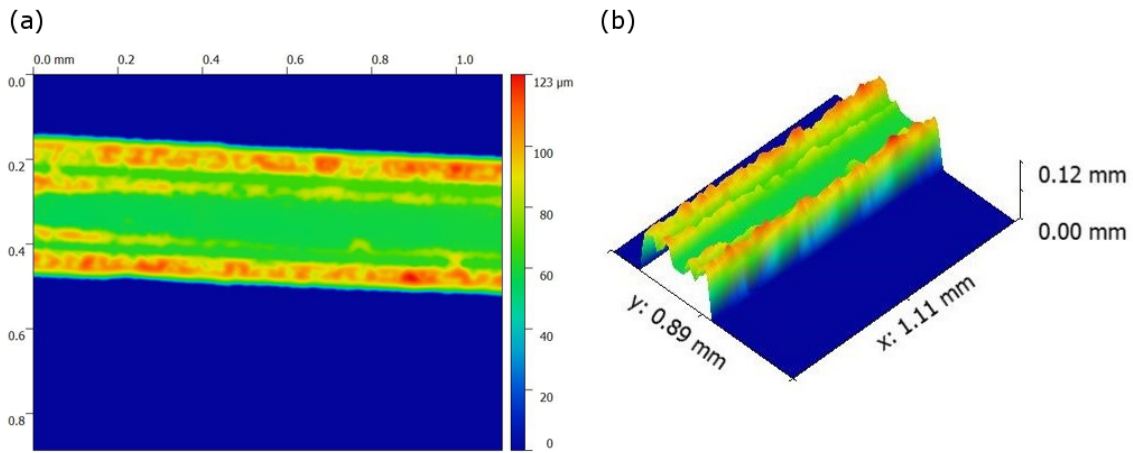


Figure 3.11: Profilometry results of the optimized line made from RTV 800 – 400 silicone at the 100  $kPa$  pressure, 5  $mm/s$  velocity, and 0.2  $mm$  working distance: (a) 2D top view, (b) 3D view.

### 3.3.2 Optimizing the Extrusion of Plane Features

Table B.4 contains the results of the full factorial model for the extrusion of plane features. The factors  $P$ ,  $RW$ , and  $WD$ , as well as the second order interactions of  $P \times WD$  and  $RW \times WD$  are determined to be significant in the initial ANOVA (Table B.5). After removing the insignificant factors, a reduced model with all significant factors was generated (Table B.6). Figures B.4, B.5, and B.6 do not show any deviations from the normal behavior for the residual plots which verifies the validity of underlying assumptions.

The plot of marginal means (Fig. 3.12) for both significant second order interactions  $P \times WD$  and  $RW \times WD$  reveal that at the low level of  $RW$  and high level of  $P$ , the amount of extruded silicone is large enough that the stand-off distance does not affect  $W_q$ . As a result, moving toward a very smooth surface in the optimization directions demonstrated in Fig. 3.13 can be achieved by increasing  $P$  and/or decreasing  $RW$ . The only constraint in this steepest descent method is jeopardizing the vertical resolution of the 3D printed parts by excessive increase in the pressure or designing a trajectory with very close printing roads. Thus, depending on the application and the internal structure of the target object, appropriate  $P$  and  $RW$  values can be selected based on the following regression model:

$$W_q = 5.685 - 1.914P + 2.21RW + 1.786D - 1.656PD + 1.459D \quad (3.6)$$

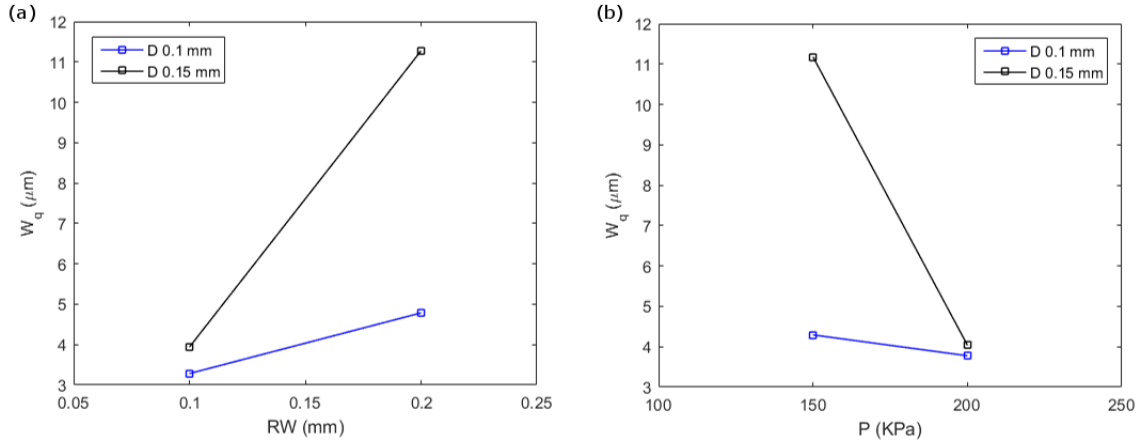


Figure 3.12: The plot of marginal means for the second order interactions (a)  $RW \times WD$ , (b)  $P \times WD$ .

Figure 3.14(a-c) shows the reduction in the  $W_q$  of the extruded plane features from  $22 \mu\text{m}$  to  $3 \mu\text{m}$  after conducting the DoE study.

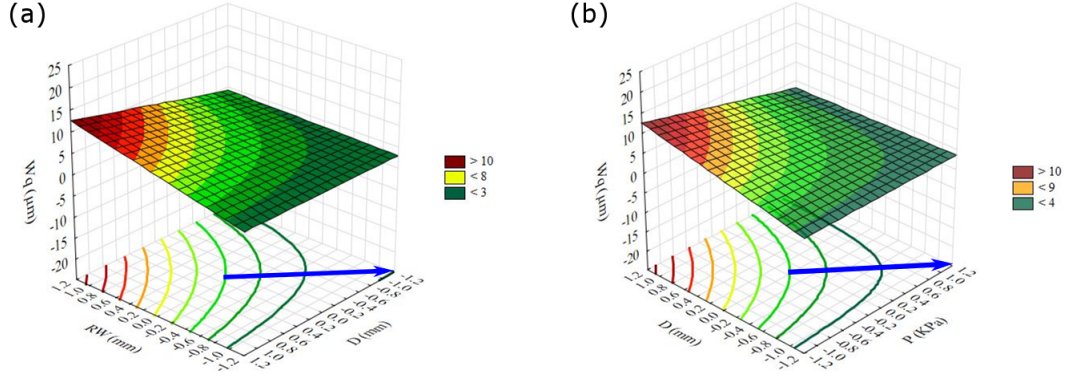


Figure 3.13: The contour plot and fitted response surface for (a)  $RW \times WD$  and (b)  $P \times WD$ . The blue arrows indicate the optimization path. The color-coded values of  $W_q$  are shown in the legends.

### 3.3.3 Finite Element Model of Silicone Dispensing

The experimental and simulation results of three different scenarios: (a)  $P_{air} = 100 \text{ kPa}$  for 3 s; (b)  $P_{air} = 100 \text{ kPa}$  for 5 s; (c)  $P_{air} = 150 \text{ kPa}$  for 3 s, were obtained. In order to investigate the validation of the finite element model, the following parameters were extracted from the model and measured experimentally at 1 – 10 s time period with one second intervals: (1) the distance between the nozzle tip and the lowest point of the pendant droplet ( $h$ ); (2) half of the maximum width of the droplet ( $w$ ); (3) the height of the droplet created on the substrate ( $h'$ ). Parameter 1 is to study the topology of the flow in terms of the relationship between time and location of the pendant drop. Parameters 2 and 3 represent the geometry of the droplet. These parameters are presented in Fig. 3.15. The measured parameters from the experiments and their corresponding model results are illustrated in Fig. 3.16(a-c), Fig. 3.17(a-c), and Fig. 3.18(a-b). The contour of the level-set model is considered as the geometrical boundary between the silicone flow and air.

#### Profile and Time of Flow

Figure 3.16(a-c) compares the distance of the lowest point of droplet to nozzle tip before the droplet is ruptured and separated from the nozzle for both the experimental trials and the finite element model. For three scenarios, the model and experimental values follow a similar increasing and decreasing trend. Moreover, the discrepancy between the

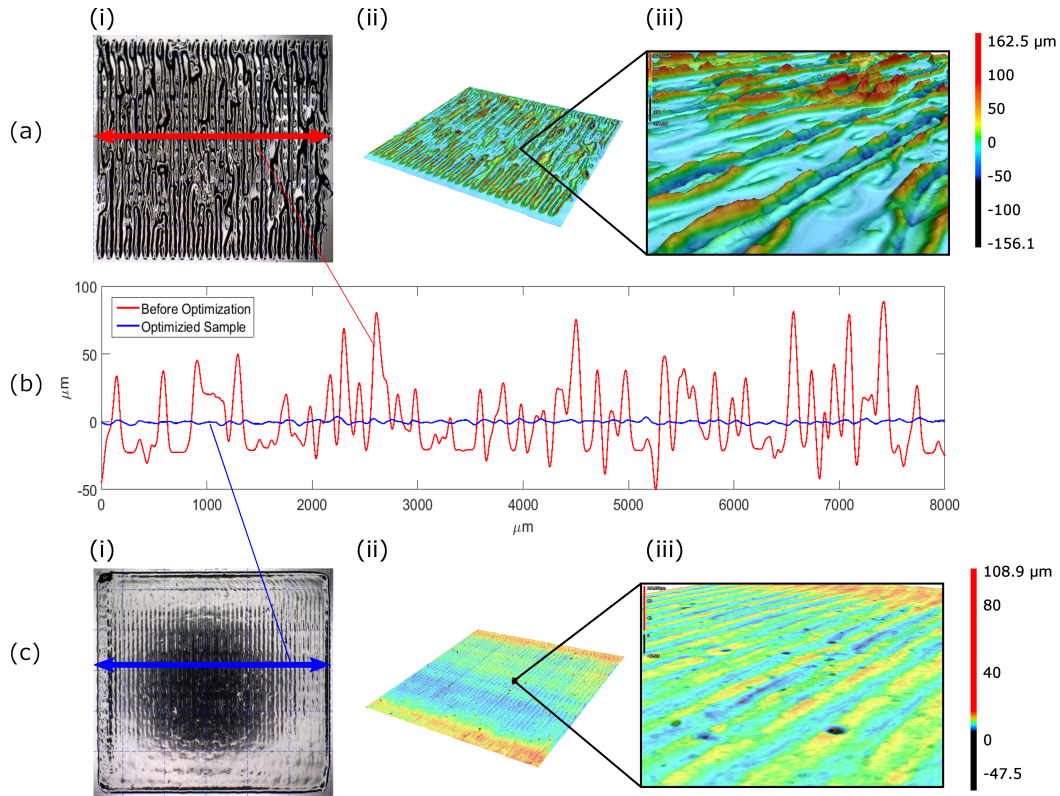


Figure 3.14: The optimization steps for extrusion of plane features: (a-i) a sample of the printed plane before the optimization showing periodic irregularities on the surface, (a-ii) the profilometry result for the plane before optimization with  $W_q$  of approximately  $22 \mu m$ , (a-iii) the magnified view of the surface structure before optimization; (b) A comparison between the waviness profile for the printed planes before and after optimization along the identified scanning lines: (c-i) a sample of the printed plane after the optimization showing a smooth surface, (c-ii) The profilometry result for the plane after optimization with a  $W_q$  of approximately  $3 \mu m$ , (c-iii) The magnified view of the surface structure after optimization.



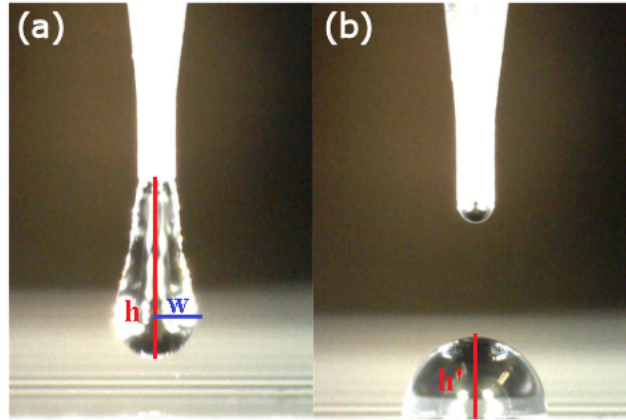


Figure 3.15: Selected parameters,  $h$  represents height of the pendant droplet,  $w$  represents maximum half width of both pendant droplet and droplet on substrate, and  $h'$  represents height of the droplet on substrate. Images of the flow were captured in pre-defined time intervals using a digital microscope.

experimental and simulation results is negligible. On average, there is a 3.8% difference between the predicted and experimental values for parameter  $h$ . Figure 3.19 compares the experimental and simulation results during the dispensing time for scenario b. By observing the results of Fig. 3.16(a), the importance of accuracy in the prediction of this parameter becomes clearer. This graph shows that applying 100  $kPa$  air pressure for 3  $s$  is not enough for the flow to reach the substrate. By changing the working distance of the nozzle, the suitable pressure can be selected that outputs the desired pattern width and prevents the creation of a dangling droplet. Fig. 3.16(b) and Fig. 3.16(c) show that the flow reaches the substrate at nearly the same time as in reality which verifies this claim. However, increasing the pressure increases the error between the experimental and model data. For example, in Fig. 3.16(c), the silicone flow under the air pressure of 150  $kPa$  reaches the substrate after 2  $s$ , however the simulation results show that there is an approximately 0.072  $mm$  distance between them at this time.

## Droplet Geometry

The main focus of this study was the prediction of the geometrical features of droplet ( $w$  and  $h$ ), which in turn provide the width and height of the line patterns that produce a 3D structure in nozzle dispensing systems. Fig. 3.17(a-c) illustrates the difference between the actual  $w$  and its corresponding simulation. On average, there is 4.5%, 6.2%, and

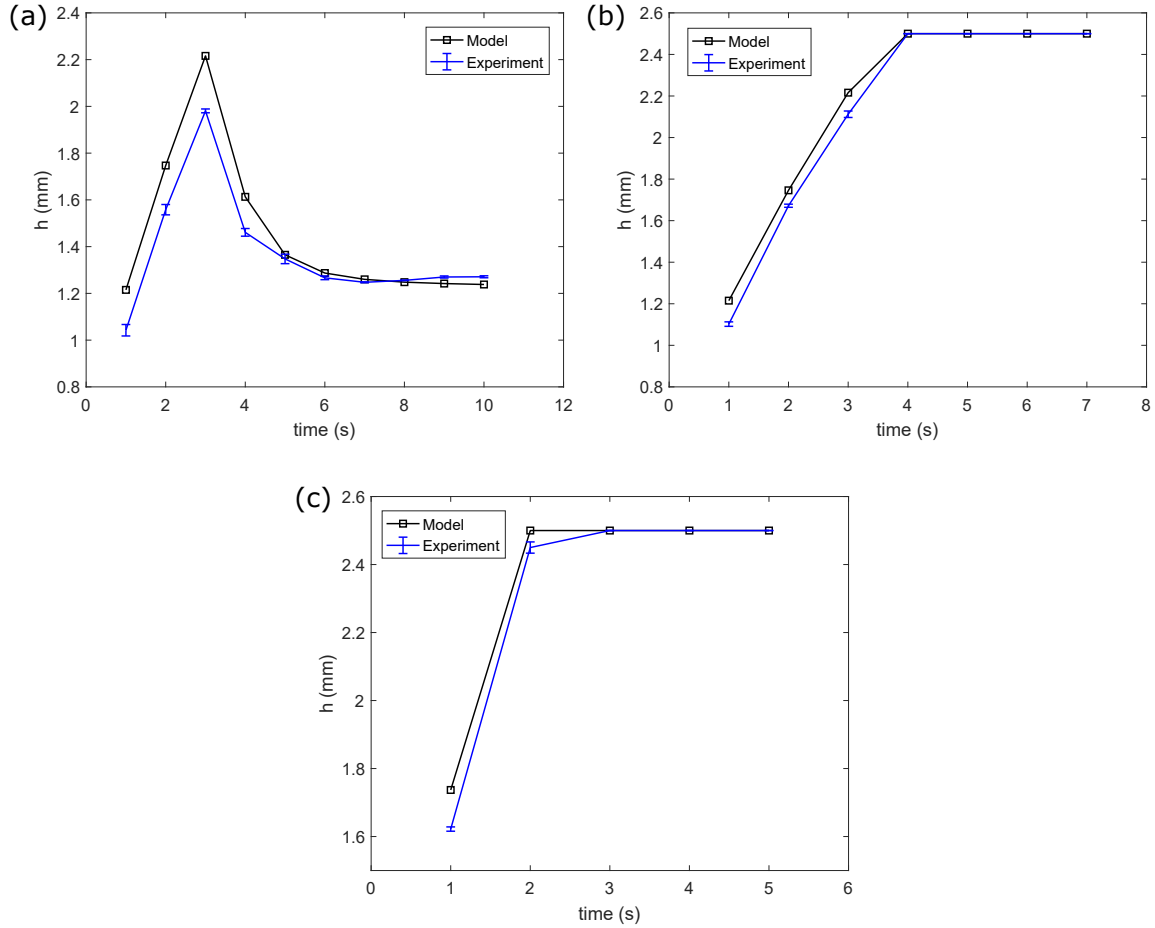


Figure 3.16: Distance between the nozzle tip and the lowest point of pendant droplet ( $h$ ) vs. time for (a)  $P_{air} = 100 \text{ kPa}$  for 3 seconds; (b)  $P_{air} = 100 \text{ kPa}$  for 5 s; and (c)  $P_{air} = 150 \text{ kPa}$  for 3 s. Experimental results are shown as error bars with average standard deviations of 0.04, 0.016, and 0.015 for scenarios a-c, respectively. All three graphs illustrate that the experimental and simulation data follow the same trend in terms of the topology of the flow. Also, the difference between the experimental and simulation data is more obvious as the air pressure increases. The difference between the experimental and simulation results is negligible (an average of 3.8%). In scenarios (b) and (c) the difference between the experimental and simulation results is zero after 4 and 3 s, respectively, which demonstrates the accuracy of the model in simulating the time at which the pendant droplet reaches the substrate.

12.9% difference between the simulated results and experimental values for scenarios a, b, and c, respectively. These relatively high difference values may arise from error in the measurement of experimental values and silicone parameters such as viscosity. Owing to the importance of the width of printed patterns, these percentage difference values should be considered as adjustment factors. As seen from the Fig. 3.16(b-c), the deviation between the models and experimental trials increases after the creation of the droplet ( $t > 4$  s), i.e., the model is more accurate in predicting the width of the pendant droplet. In Fig. 3.16(a), the droplet is not generated on the substrate due to insufficient time of activation of pressure. Hence, the pendant drop reaches to a stable point after 5 s without any significant changes in the width. Also the average deviation will increase as the pressure increases.

The graphs presented in Fig. 3.18(a-c) compare the height of the droplet on the surface ( $h'$ ) in the model and experiment. The results are plotted only for scenarios b and c, as no droplet is generated on the substrate in scenario a. Average percentage differences of 13.4% and 8.4% are measured for scenarios b and c, respectively. Although the difference values may seem considerable, the plots show that the difference between simulated and experimental values at the time when the droplet is separated from the nozzle tip (see Fig. 3.19 ( $t = 8$ s)) is the highest. By excluding the amount of difference at this point, the difference values are reduced to 7.5% and 5.6%, respectively.

### Sensitivity Analysis on Viscosity

The sensitivity of the finite element model was evaluated by varying the value of silicone viscosity. The viscosity value calculated in section 2.1 (19.9 Pa.s) was chosen as the standard value and the model was run at  $\pm 10\%$ ,  $\pm 20\%$ , and  $\pm 30\%$  deviations from this value. Table 3.7 shows the average deviations in the selected parameters after changing the value of viscosity. These changes for parameters  $h$  and  $w$  follow the same trend for all three scenarios. In other words, a 30% decline in the viscosity decreases the value of parameters the most; this change is reduced as the viscosity value gets closer to its standard value. Same analysis can be extended to the increase in viscosity. Parameter  $h'$  does not demonstrate an organized behavior. The main reason of the fluctuations in the average error for this parameter is the unpredictable and drastically different changes in the time and the location at which the droplet is ruptured and separated from the nozzle tip. Also, decreasing the value of viscosity usually has a higher effect on the parameters than increasing it. For example in scenario b, a 10% decline in viscosity yields a 5.9% reduction in the value of  $w$ , but the same amount of increase in viscosity only increases this parameter for 5%. It cannot be inferred that which parameter is more sensitive to the

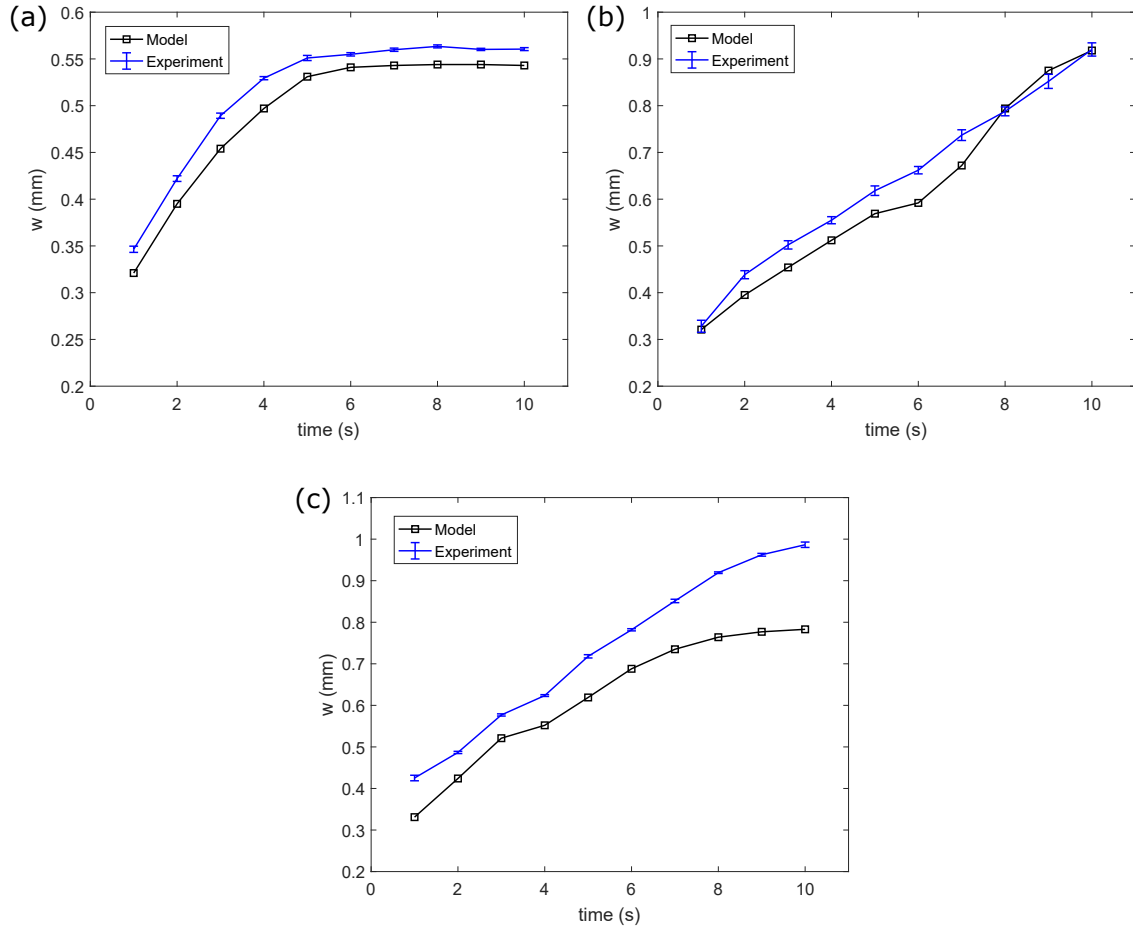


Figure 3.17: Half of the maximum width of droplet ( $w$ ) vs. time for (a)  $P_{air} = 100 \text{ kPa}$  for 3 s; (b)  $P_{air} = 100 \text{ kPa}$  for 5 s; and (c)  $P_{air} = 150 \text{ kPa}$  for 3 s. Experimental results are shown as error bars with average standard deviations of 0.007, 0.01, and 0.012 for scenarios a-c, respectively. All three graphs illustrate that the experimental and simulation results follow the same trend in terms of the topology of the flow; however, the difference between the results is considerable and the value of the difference needs to be taken into account in calculation of the width of the features.

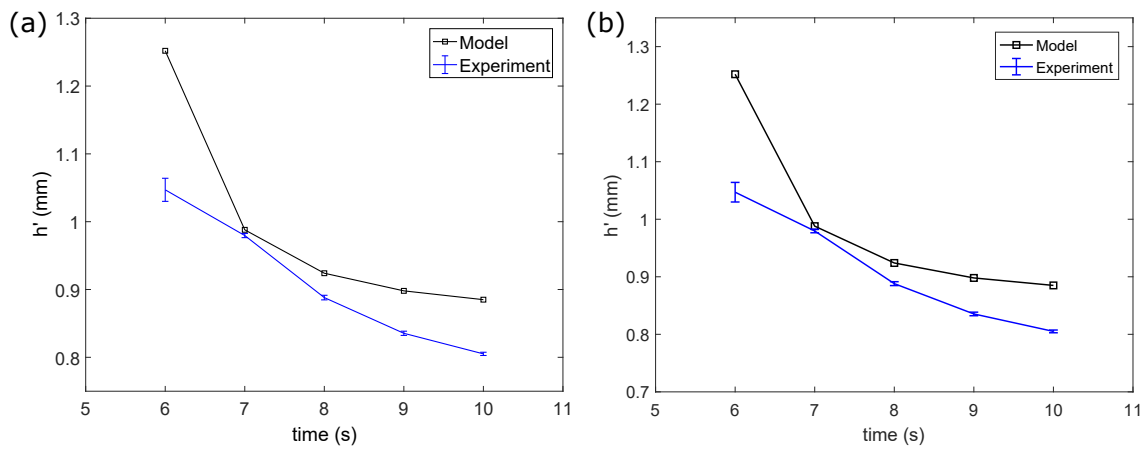


Figure 3.18: Height of droplet ( $h'$ ) vs. time for (a)  $P_{air} = 100 \text{ kPa}$  for 5 s; and (b)  $P_{air} = 150 \text{ kPa}$  for 3 s. Experimental results are shown as error bars with the average standard deviations of 0.016 and 0.02 for scenarios b-c, respectively. All two graphs illustrate that the experimental and simulation results follow the same trend in terms of the topology of the flow. The difference between experimental and simulation results at the time when the droplet is generated (separation of the droplet from the nozzle tip) for both cases is much higher than the rest of the dispensing process.

viscosity variations, however, it seems that the amount of time that a droplet is pendant from the nozzle may affect it. If we consider scenarios b and c as successful scenarios in which the droplet is formed on the substrate, then parameters  $w$  and  $h'$  are respectively the most sensitive and the least sensitive parameters to the changes of viscosity in these two scenarios.

Table 3.7: Effect of changes in viscosity on the location and the geometrical dimensions of silicone droplet dispensed through a nozzle with an inner diameter of  $100 \mu m$

Change in the value of viscosity		-30%	-20%	-10%	10%	20%	30%
		Average Error (mm)					
100 kPa - 3 s	$h$	-0.466 (-32.3%)	-0.394 (-27.3%)	-0.112 (-7.7%)	0.063 (+4.3%)	0.117 (+8.1%)	0.16 (+11.1%)
	$w$	-0.138 (-28%)	-0.098 (-20%)	-0.018 (-3.6%)	0.016 (+3.2%)	0.03 (+6%)	0.041 (+8.3%)
100 kPa - 5 s	$h$	-0.115 (-5.3%)	-0.115 (-5.3%)	-0.078 (-3.6%)	0.04 (+1.8%)	0.074 (+3.4%)	0.14 (+6.4%)
	$w$	-0.12 (-20.9%)	-0.073 (-12.7%)	-0.034 (-5.9%)	0.029 (+5%)	0.053 (+9.3%)	0.077 (+13.3%)
	$h'$	0.041 (+3.8%)	0.049 (+4.5%)	0.04 (+3.7%)	-0.094 (-8.7%)	-0.303 (-28.1%)	-0.374 (-34.6%)
150 kPa - 3 s	$h$	-0.118 (-5%)	-0.071 (-3%)	-0.025 (-1.1%)	0.02 (+0.9%)	0.069 (+2.9%)	0.107 (+4.6%)
	$w$	-0.123 (-19.8%)	-0.077 (-12.4%)	-0.034 (-5.5%)	0.031 (+5.1%)	0.06 (+9.7%)	0.086 (+13.9%)
	$h'$	-0.008 (-0.8%)	0.011 (+1.1%)	-0.003 (-0.3%)	-0.029 (-2.9%)	-0.18 (-18.2%)	-0.062 (-6.2%)

### 3.4 Summary

The optimization of line features study suggested that material extrusion technology is a promising method for additive manufacturing of highly viscous silicones. A  $2^3$  full factorial

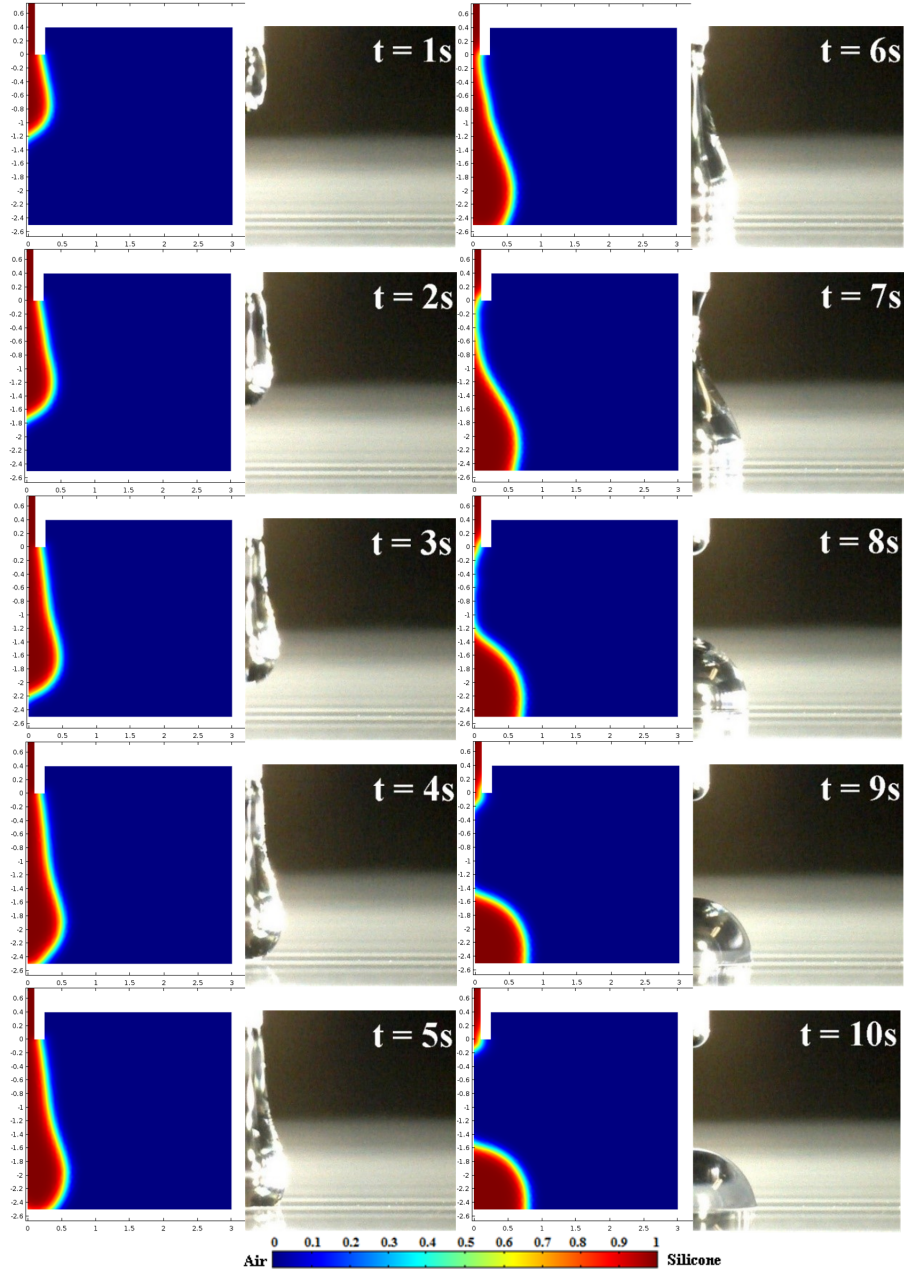


Figure 3.19: Comparison of the experimental trial and simulation for  $P_{air} = 100 \text{ kPa}$  for 10 s. The green band represents the boundary between silicone and air (contour 0.5).

design were employed to screen the effect of  $P$ ,  $v$ , and  $WD$  on the quality of the printed features. For the width of built samples, the effects of  $P$ ,  $v$ , and their interaction were the influencing factors.  $P$ ,  $WD$ , and their interaction also proved to affect uniformity of lines more than other factors. None of the factors were significant in the creation of rough surfaces at 95% level of confidence in the investigated parameter ranges. However,  $v$  and the interaction of  $v$  and  $WD$  show the highest effects on this response. Simultaneous response optimization was conducted to minimize all three responses. The level set treatment with  $P = 100 \text{ kPa}$ ,  $v = 5 \text{ mm/s}$ , and  $WD = 0.2 \text{ mm}$  is the optimum solution resulting in a highly uniform line with a width of  $322.8 \mu\text{m}$  and high surface quality. Comprehensive statistical analyses were also conducted to optimize the printing quality of material extrusion system when printing 3D plane features. The results showed that when working with optimum parameter values, the lateral resolution will be  $300 - 400 \mu\text{m}$  for the extrusion system. On the other hand,  $3 - 4 \mu\text{m}$  was obtained for  $W_q$  for the 3D printed planes while printhead was moving at  $5 \text{ mm/s}$  speed.

A finite element model was also developed to simulate the dispensing of silicone in material extrusion system. The effects of two process parameters, air pressure and time of its application, on the flow and geometrical properties of droplet were investigated by conducting the experimental trials. The results of the experiments were used to validate the model. The experimental results of  $w$  of the droplets are on average 4.5%, 6.2%, and 12.9% higher than the results of simulation for  $100 \text{ kPa} - 3 \text{ s}$ ,  $100 \text{ kPa} - 5 \text{ s}$ , and  $150 \text{ kPa} - 3 \text{ s}$  scenarios, respectively. These values can be employed as adjustment factors for the prediction of the geometry of droplet and consequently the width of printed hairpin lines. On the other hand, the model predicts the location of the pendant droplet and its height on the substrate with dependable average accuracy tolerances of 3.8% and 6.5%, respectively. Hence, the model can be used to determine the suitable combination of pressure value, pressure time, and working distance that guarantees the flow reaches the substrate and spreads on it while maintaining the uniformity of the printed feature. The sensitivity of different parameters to the changes in viscosity of silicone was evaluated showing that this material property affects the width of droplet the most and its height the least. The average changes of 11.1% and 3.6% were calculated from scenarios b and c for  $w$  and  $h$ , respectively. Overall, the developed model demonstrates the capability of yielding accurate and consistent results in terms of the location and geometry of the flow of highly viscous fluids.



# Chapter 4

## Additive Manufacturing of Silicone via Material Jetting

### 4.1 Introduction

Material jetting is another class of AM that has been adopted to 3D print the low viscous silicone polymer before [86] at a printing velocity similar to material extrusion ( $5\text{ mm/s}$ ). The review of previous research work reveals the lack of an AM system which is able to print high viscous silicones directly at a high throughput rate and with high quality. On the other hand, the shortcomings of conventional manufacturing methods (see Section 2.4) make the need for such a system clear. In this chapter, a material jetting technique that has been optimized using statistical tools to print uniform and smooth features from highly viscous silicone approximately 20 times faster than the current methods, is proposed. Statistical tools used in this work to optimize the printing quality (for line and plane features) include DoE, RSM, and [central composite design \(CCD\)](#).

The conventional material jetting system, formerly known as inkjet printing, is compatible with fluids having a maximum viscosity of  $40\text{ mPa}\cdot\text{s}$ . In these systems, fluids with a Ohnesorge number ( $Oh$ ) between 0.1 and 1 (or  $1 < Z < 10$  where  $Z = Oh^{-1}$ ) are considered jettable. Ohnesorge number is calculated according to Eq. 4.1:

$$Oh = \frac{\mu}{(\gamma\rho a)^{1/2}} \quad (4.1)$$

where  $\mu$  is the dynamic viscosity,  $\gamma$  is the surface tension of the fluid,  $\rho$  is the density, and  $a$  is a characteristics of the length. Medical-grade silicones with a minimum viscosity of

approximately 25,000  $mPa.s$  have an  $Oh$  value greater than 1. As a result, this class of polymers are not printable via conventional material jetting.

The new generation of jetting printheads, however, is theoretically able to jet the droplets of fluids with a viscosity of up to 1,000,000  $mPa.s$  at a high frequency in a repeatable and precise manner [135]. The dual PPJ mechanism in these printheads can provide enough force to eject a droplet of the viscous paste with a volume in the order of pico-litre. Figure 4.1 demonstrates the jetting mechanism in these systems. A sample of the pulsed voltage ( $V$ ) signal is shown in Fig. 4.1(a). In this printhead the valve is normally open, as a result, applying the actuation voltage (e.g. 95 V) moves the sealing ball downward and prevents the flow of fluid as it sits on the ceramic nozzle seat (Fig. 4.1(b).); The drop of voltage to a certain stroke percentage ( $Str\%$ ) results in the opening of the orifice, followed by filling of the orifice with the fluid due to the air back-pressure. The air pressure fills the orifice with the material (Fig. 4.1(c).); Fig. 4.1(d) corresponds to the grey region of the plot showing the closing ramp. In this step, the voltage signal rises up to the closing voltage resulting in the downward movement of the sealing ball and jetting of one droplet. The valve remains closed until the beginning of a new cycle.

In this mechanism, the volume of jetted droplet is a function of both the reversed piezoelectric and the pneumatic forces. The amount of material jetted due to the reversed piezoelectric force is controlled by the orifice close time ( $CT$ ), and that jetted due to the pneumatic force is controlled by the pulse time ( $PT$ ) according to Eq. 4.2 [88]. The experimental results presented in the following sections confirm the significant effect of  $PT$  and  $CT$  parameters on the quality of printed lines.

$$V = Q_{pzt} \times CT + Q_{pne} \times PT \quad (4.2)$$

where  $Q_{pzt}$  is the jetting rate due to the piezoelectric force, and  $Q_{pne}$  is the jetting rate due to pneumatic force. Eq. 4.3 is used to calculate  $Q_{pne}$ .

$$Q_{pne} = \left(\frac{\pi D^3}{32}\right) \left(\frac{4n}{3n+1}\right) \left(\frac{D\Delta P}{4LK}\right)^{\frac{1}{n}} \quad (4.3)$$

where  $n$  and  $K$  denote the power law constants of the fluid,  $D$  is the diameter of the orifice,  $L$  is the length of the nozzle, and  $\Delta P$  is the pressure difference.

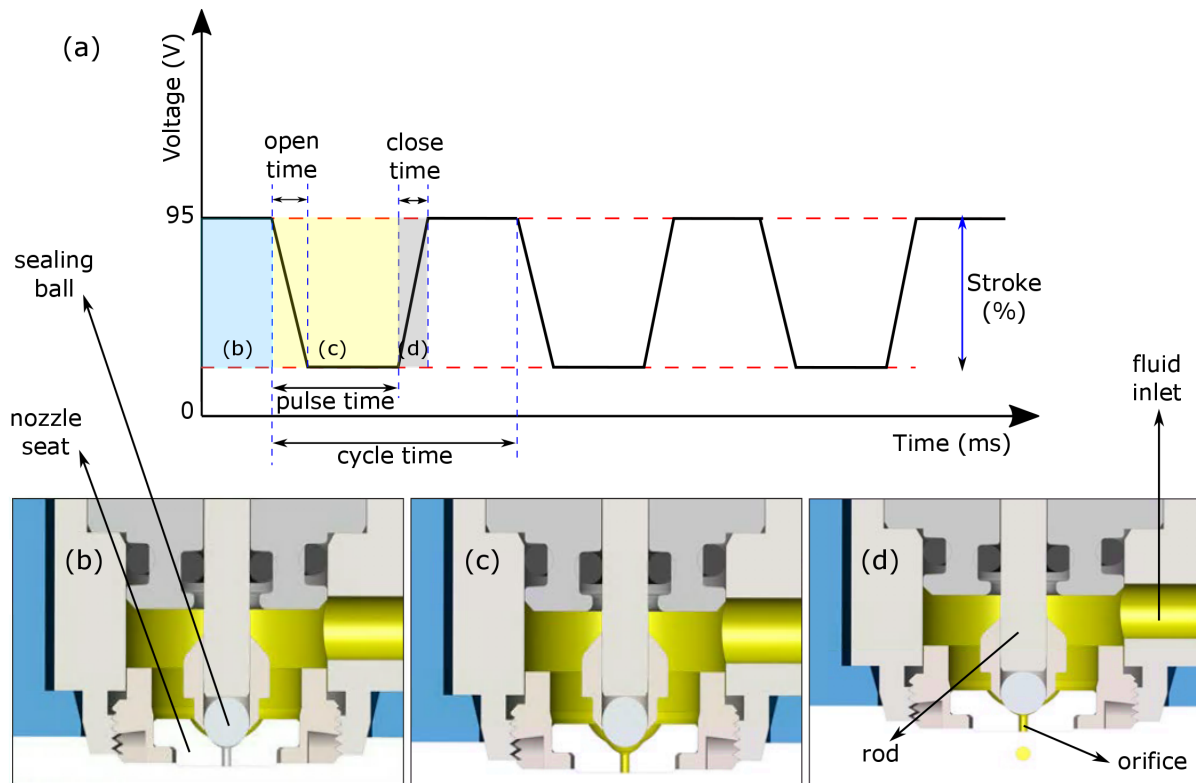


Figure 4.1: The working principle of the PPJ; (a) the plot shows the voltage signal sent to the piezoelectric stacks for three complete cycles,  $OT$  indicates how fast the valve is opened,  $CT$  indicates how fast the valve is closed,  $PT$  is the total time the valve is open, and the  $CyT$  is the total duration of one open/close cycle; (b) corresponds to the blue region of the plot showing the time duration that the valve is closed; (c) corresponds to the yellow region of the plot when the orifice is open and filled with the material; (d) corresponds to the grey region of the plot showing the closing ramp. ((b-d) adapted with permission from [www.nordsonfed.com](http://www.nordsonfed.com)).

## 4.2 Materials and Methods

### 4.2.1 Experimental Setup

Figure 4.2 shows the in-house-developed hybrid AM system and its components. This system consists of three PPJ printheads (Pico Pulse, Nordson EFD, RI, USA), one solenoid-actuated material extrusion printhead (xQR41 MicroDot™, Nordson EFD, RI, USA), one pneumatic material extrusion printhead (Optimeter™, Nordson EFD, RI, USA), and a UV lamp (365 nm, Edmund Optics, NJ, USA). Three controlling units (Pico® Touch, Nordson EFD, RI, USA) actuate the piezoelectric stacks by sending out the voltage signals, and one controller (ValveMate™ 9000, Nordson EFD, RI, USA) coordinates the air-pressure in the extrusion-based printheads. The 3-axis motion stage (E6V automated dispensing system, Nordson EFD, RI, USA) has been used to make the printing of 3D structures possible.

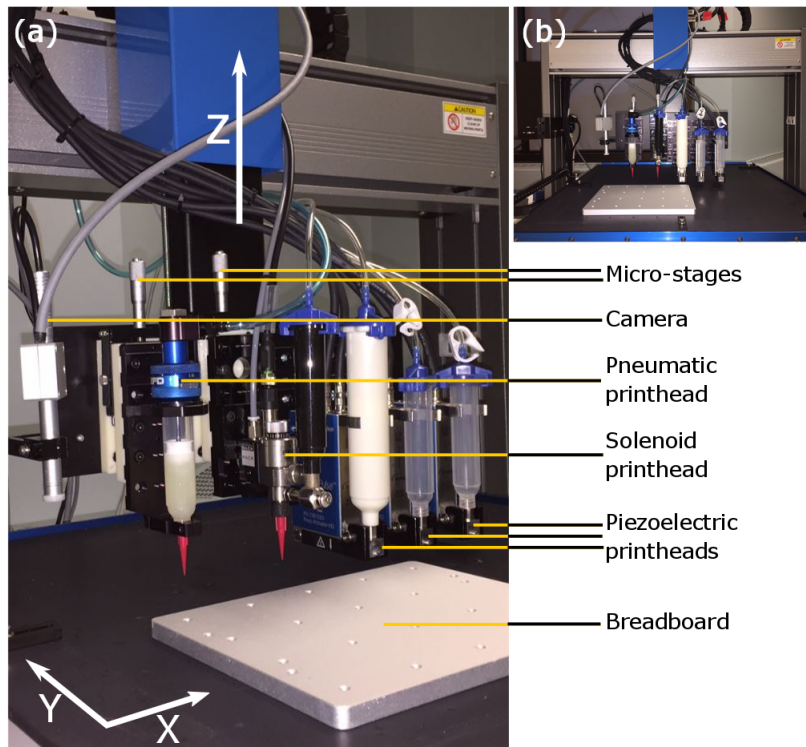


Figure 4.2: The overall view of the AM system: (a) main components; (b) front view.

## 4.2.2 Trajectory Design

Different area filling patterns have been used for the direct writing AM where rectilinear is the most prevalent. A common quality flaw in these techniques is the deposition of extra material where there is any change in the direction of movement as well as the start and stop points. The reason is the need for the reduction of printhead's speed to virtually zero when a point of direction change is approaching, followed by acceleration until the steady velocity is obtained [58]. If the deposition rate is not changed accordingly, more material will be dispensed at these points.

The PPJ method suffers from the overfilling phenomenon as well (Fig. 4.3(a-i)). To print lines with uniform width, the conventional rectilinear pattern was replaced by a custom pattern composed of separate parallel lines (Fig. 4.3(a-ii)). This led to eliminating the points of change in direction. Moreover, the delayed dispensing and early termination of dispensing [114] have been employed to reduce the effect of overfilling at the start and stop points of a line, respectively (Fig. 4.3(a-iii)). In other words, the printhead moves along the toolpath (which is a straight line) from the start point but the deposition is not started until it reaches a stable velocity (settling distance). Similarly, no deposition happens over a distance close to the end point where deceleration occurs (shutoff distance). To make sure the geometrical accuracy of the part is maintained, the trajectory lines are oversized to include the actual length of the line as well the settling and shutoff distances as shown in Fig. 4.3(b). The length of stabilization segments can be calculated based on the velocity and acceleration of gantry system.

To convert the digital 3D structures into the printing trajectory (G-code), the open source software Slic3r was used. The Slicer was modified slightly to include the custom pattern of parallel lines. The oversizing value is defined as a function of the width of perimeter lines through the pattern/perimeter overlap command of Slic3r. A text-processing python script was also developed that parses the G-code generated by Slic3r and translates it to the syntax compatible with our developed AM system. The lengths of settling and shutoff distance for each printhead are set in this script as well.

## 4.2.3 Silicone

The silicone described in Section 3.2.1 has been used in this research with a new PI, 2-Hydroxy-2-methyl propiophenone (3 wt.%).

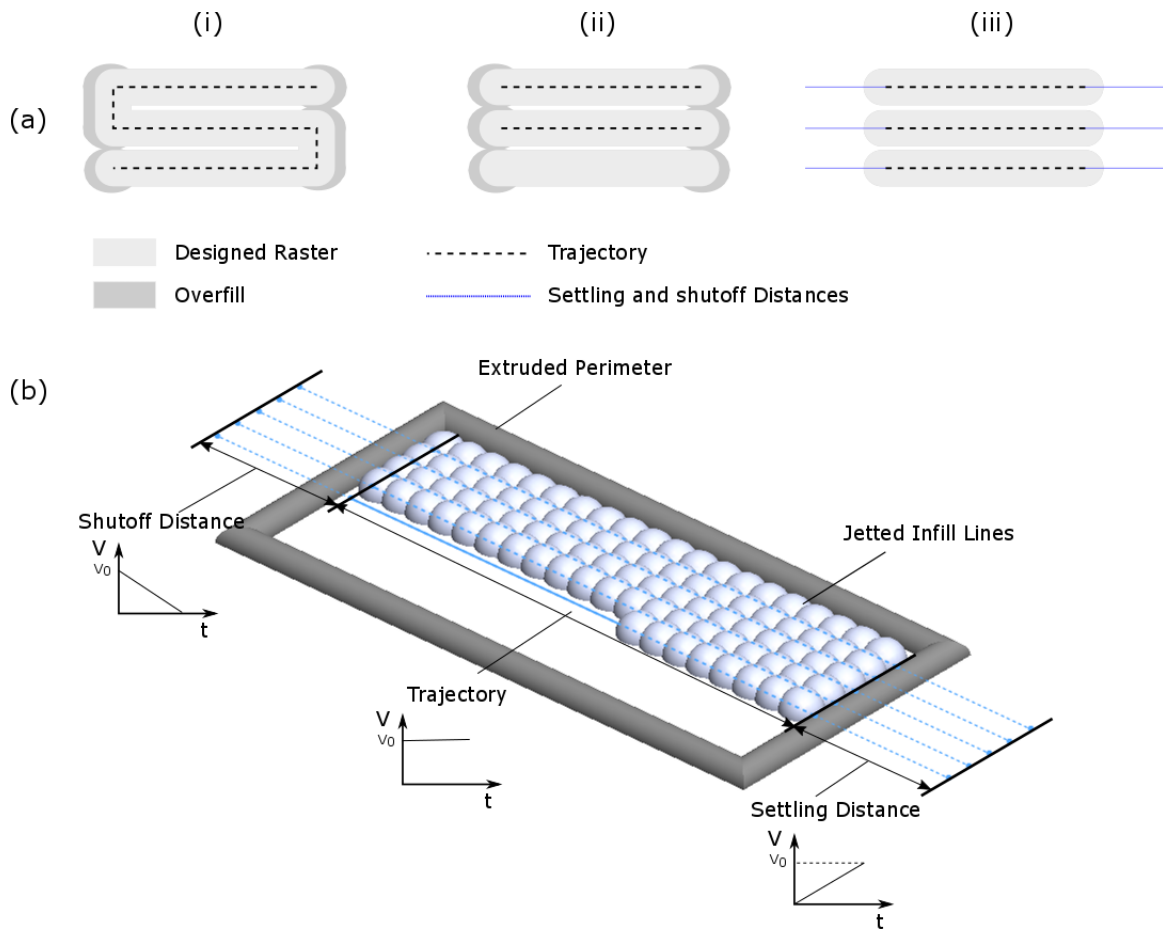


Figure 4.3: The effect of filling pattern on overfilling: (i) rectilinear, (ii) parallel lines, (iii) oversized parallel lines containing settling and shutoff distances. (b) The velocity plot for the printhead at different locations of trajectory.

#### 4.2.4 Sample Preparation and Profilometry

In order to optimize the line features printed via PPJ system, 5 *cm* lines were jetted for each treatment combination. The process parameter values for each treatment at different optimization stages can be found in Appendix C. Images of the printed features were taken using a digital microscope (AM7915MZT, Dino-Lite, Taiwan), followed by measuring the lines width at five equally distant locations as shown in Fig. 4.4. This procedure was replicated at three different sections of the line. The average of the values for each line was used as the average width of feature ( $W_{avg}$ ), and their standard deviation was used as a measure of the uniformity ( $W_{s.d.}$ ). Each of these two values were used as the response at different stages of the experiment. For example, the initial factor screening phase should lead to finding the treatment combination which yields a uniform continuous line, hence, the standard deviation of the width values was used as the response at this phase. On the other hand, in the optimization and surface response method steps, the resolution was maximized by selecting the average width as the response.

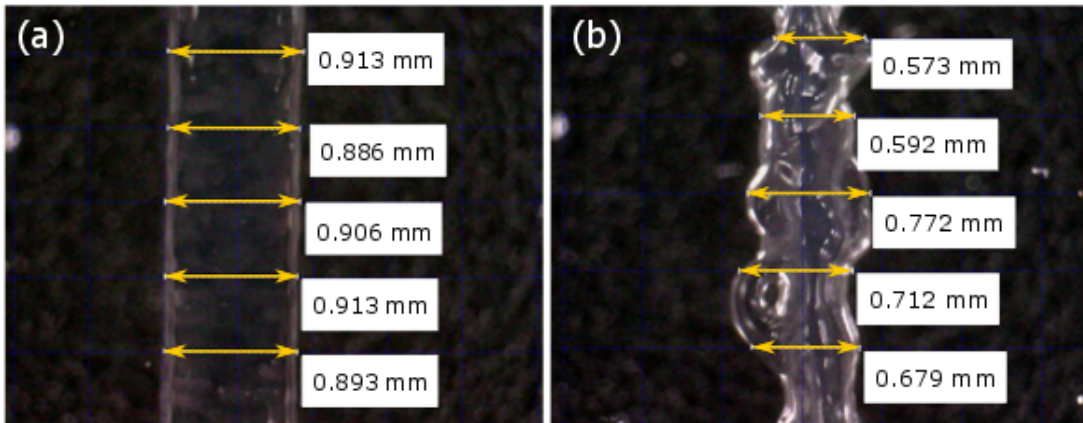


Figure 4.4: Samples of width measurement for the silicone line features; (a) uniform line with 0.012 *mm* standard deviation; (b) non-uniform line with 0.083 *mm* standard deviation.

In order to optimize the surface quality of the 3D plane features printed via material jetting technique, a layer of 1 *cm* × 1 *cm* silicone square was made on a silicon wafer according to each of the DoE treatments. The 3D image of each sample was captured using an optical/laser profilometer (VK-X250, Keyence, Japan) at 100× magnification. The root mean square of waviness ( $W_q$ ) at the filter cut-off wavelength of 0.08 *mm* was selected as a measure of the surface quality. Waviness is the uneven features that are repeated periodically on the surface at longer intervals compared to the roughness. The

profile data was collected over 31 lines.  $W_q$  was measured for each line and their average was used as the final surface quality value. Figure 3.9 shows a sample of the waviness measurement and the surface profile.

## 4.2.5 Experimental Designs

As explained in Section 3.1, the lack of analytical models explaining the flow of highly viscous non-Newtonian fluids justifies the need for the empirical models to relate the dimensional parameters of the printed building blocks (lines or beads) to the input parameters of the AM systems. Here, the statistical optimization tools (e.g., design of experiments) are used to create linear and quadratic empirical models to better understand these relationships.

Many factors control the quality and the printability in the PPJ mechanism. Ten influential factors were identified in the initial stage of working with the system. Table 4.1 shows these factors at their low and high levels. The significance of these working parameters was investigated using a  $2^{10-5}_{IV}$  fractional factorial screening design. The statistically significant factors were further studied in a  $3^{4-1}_{IV}$  fractional factorial design, and a linear regression model was fit to the collected data. RSM was adopted at the next step to move toward the optimized area [136]. Finally, a comprehensive non-linear regression model was formed based on the CCD. The experimental design has been carried out for a 100  $\mu m$  nozzle.

Table 4.1: Influential factors and their treatment levels for the material jetting of line features.

Factors	Low Level (-1)	High Level (+1)
$PT$ ( $ms$ )	0.37	0.43
$CyT$ ( $ms$ )	3.5	4
$T$ ( $^{\circ}C$ )	90	100
$V$ ( $V$ )	85	95
$Str\%$ (%)	80	90
$OT$ ( $ms$ )	0.15	0.2
$CT$ ( $ms$ )	0.15	0.2
$v$ ( $mm/s$ )	50	60
$WD$ ( $mm$ )	2	3
$P$ ( $kPa$ )	500	600



In the next step, using the optimized values of printing parameters for the line features, a new design was formed to optimize the surface quality of the 3D plane features printed via PPJ. The raster width ( $RW$ ) and printing velocity ( $v$ ) were selected as the input factors and the root mean square of waviness ( $W_q$ ) as the response. The high and low levels of the input factors are demonstrated in Table 4.2. Even though the optimized value of  $v$  is  $60\text{ mm/s}$  for printing a single line, this factor was included in this study to investigate the possibility of speeding up the 3D printing process without increasing the surface waviness. To this end, a  $2^2$  full factorial design with two center points and one replication was formed.

Table 4.2: Influential factors and their treatment levels for the material jetting of plane features.

Factors	Low Level (-1)	High Level (+1)
$RW$ (mm)	0.4	0.5
$v$ (mm/s)	60	100

## 4.3 Results and Discussion

### 4.3.1 Optimizing the Jetting of Line Features

The details of factor screening design and the values measured for the dependent variables can be found in Table C.1. The DOE analysis for the measured width averages (Table C.2) shows that only four factors ( $PT$ ,  $V$ ,  $Str\%$ , and  $CT$ ) are significant at 95% confidence level. The ANOVA results after removing insignificant factors are shown in Table C.3. All the remaining factors at the reduced model are significant; hence, they are accepted as the influential operating factors and will be investigated more in the future steps. Also, the residual plots (Figs. C.1, C.2, and C.3) show that the normality, independency, and variance consistency assumptions are valid.

After identifying the significant factors, a  $3^{4-1}_{IV}$  fractional factorial design was formed to minimize the width of the printed line features. The values of insignificant factors were selected based on the results of the factor screening experiment. The goal is decreasing the value of standard deviation, hence, factors with a positive effect value were fixed at their low levels and vice versa. Table 4.3 shows the fixed values of insignificant factors. Table 4.4 shows the selected three levels for the significant factors.

Table 4.3: The values of insignificant factors for jetting of line features.

Factor	Effect	Level	Value
$CyT$ (ms)	< 0	1	4
$T$ ( $^{\circ}C$ )	< 0	1	100
$OT$ (ms)	< 0	1	0.2
$v$ (mm/s)	< 0	1	60
$WD$ (mm)	> 0	-1	2
$P$ (kPa)	> 0	-1	500

Table 4.4: Three levels of significant factors for jetting of line features.

Factor	Low Level (-1)	Center (0)	High Level (+1)
$PT$ (ms)	0.35	0.37	0.39
$V$ (V)	93	95	97
$Str\%$ (%)	86	88	90
$CT$ (ms)	0.15	0.17	0.19

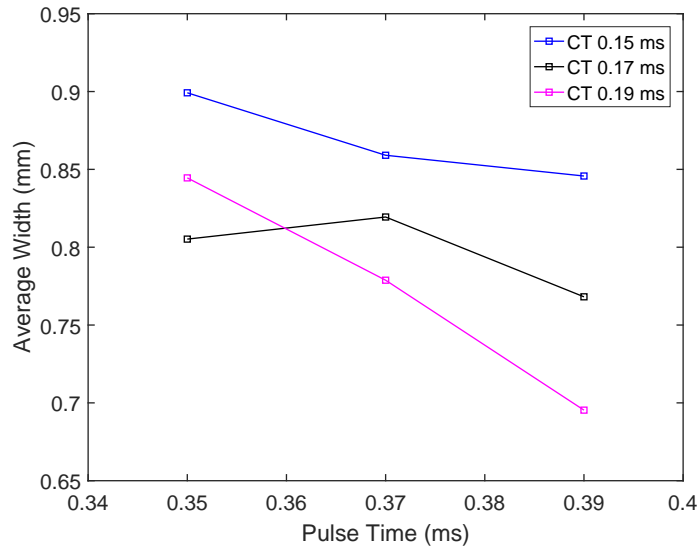


Figure 4.5: The plot of marginal means for the second order interaction  $PT \times CT$ . Setting both  $CT$  and  $PT$  factors at their higher levels results in the lowest average width for the jetted line features.

The details of  $3^{4-1}_{IV}$  fractional factorial design with one replication and two center points are demonstrated in Table C.4. The results of analysis of variance for this design (Table C.5) reveal that all four factors as well as the second order interaction of *PT* and *CT* are significant. Furthermore, none of the quadratic terms are significant in this experiment, i.e., there is no obvious curvature in the response surface at the investigating area. After reducing the model, no change was observed in the number of significant factors. The ANOVA results for the reduced model and the regression coefficients are presented in Tables C.6 and C.7, respectively.

The positive regression coefficients of the *V* and *Str%* indicate that the lower the values of these two parameters, the higher the printing resolution. Hence, it is recommended to set these two factors at their low levels. For the *PT* and *CT* parameters, their marginal mean plot will be investigated in order to decide on their optimized levels as their second order interaction (*PT* × *CT*) is significant. The marginal mean plot for the *PT* vs. *CT* is depicted in Fig. 4.5. This plot shows that there is not much difference in the  $W_{avg}$  when *CT* is equal to or less than 0.17 *ms*, regardless of the value of *PT*. On the other hand, when *CT* is set at its higher level (0.19 *ms*), the response value will be decreased by increasing the *PT*. Based on the marginal mean plot, fixing both *PT* and *CT* on their high level yields the best result, i.e., the highest printing resolution in terms of the line features width. In the next step, this initial estimate of the optimum operating conditions will be used to move toward the minimum width. The analysis of the residuals (Figures C.4, C.5, and C.6) does not raise any concerns in terms of the validity of the model as all the assumptions, i.e., normality, variance consistency, and independence have been met.

The method of steepest descent was employed to move toward the area containing the minimum value as fast as possible. Fig. 4.6 contains two contour plots and the steepest descent path. The vertical and horizontal axes show the coded values for *CT* and *PT*, respectively. The values of these two parameters can only be changed in 0.01 *ms* steps. The contour plots show that the coded value of 1.5 (uncoded: 0.2 *ms* for *CT* and 0.4 *ms* for *PT*) result in a maximum decrease of approximately 100  $\mu m$  in the average width of the features. As a result, this point (1.5 coded) was selected as the center of the CCD. Due to the limitations in the values that can be assigned to the *CT* and *PT*, only a CCD with face-centered axial point could be designed. The upper section of Fig. 4.6 shows the CCD as well as the fitted contour plot. It is observed from the plot that our first point has been accidentally located inside the optimum area resulting an average width of less than 600  $\mu m$ .

The degree of curvature seen in the contours reveals that the response surface is highly twisted and a second order regression equation is required to describe its behavior. The non-flat shape of the surface plot is illustrated in Fig. 4.7. The ANOVA results for the

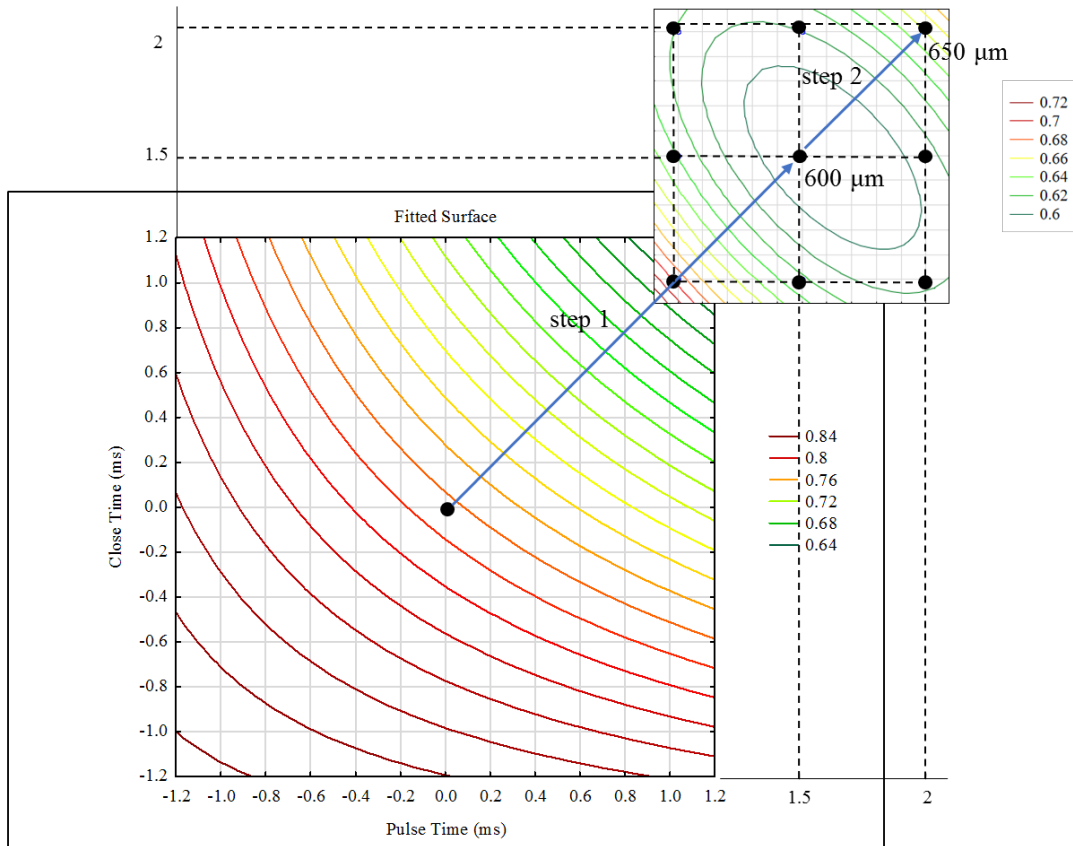


Figure 4.6: The fitted contour plots for the method of steepest descent. The first step corresponds to moving in the optimization direction (minimizing  $W_{avg}$ ) from the center of the first contour plot so that the movement path is perpendicular to the contour lines. The optimum region is found after two steps, and a new contour plot is formed around it using central-composite design. The color-coded legend shows the values of  $W_{avg}$

CCD are presented in Table C.8, which shows that only quadratic terms and second order interaction of the two factors are significant. However, due to the model hierarchy, the main effects cannot be eliminated. The regression coefficients are presented in Table C.9. The following quadratic model can be fit to the data at the optimum area:

$$W_{avg} = 0.593 - 0.012 \times PT + 0.025 \times PT^2 - 0.006 \times CT - 0.023 \times CT^2 + 0.027PT \times CT \quad (4.4)$$

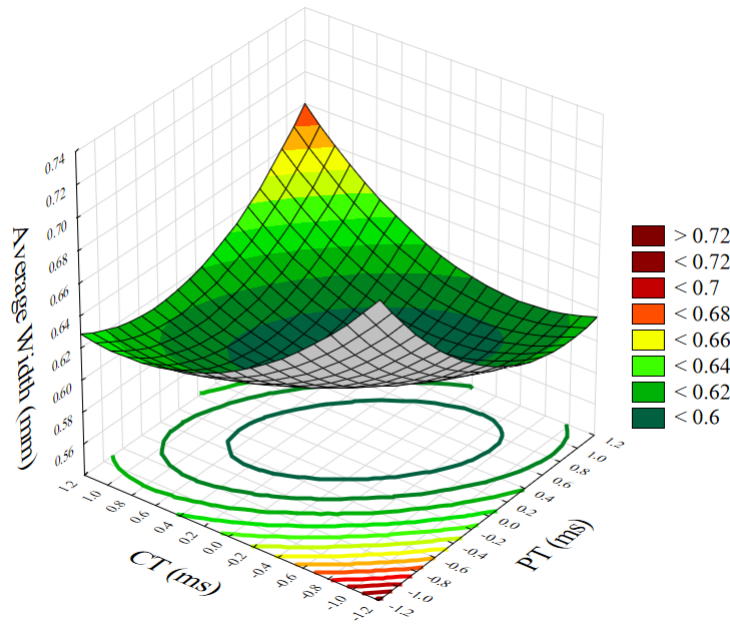


Figure 4.7: The fitted surface plot of the optimum zone. The convex shape of the surface plot assures the optimized point is not a local minimum at the selected parameter ranges.

The final results are compatible with the physical principles of PPJ systems. In these systems, the volume of jetted droplet is a function of both reversed piezoelectric and pneumatic forces. The amount of material jetted due to the reversed piezoelectric force is controlled by  $CT$ , and that jetted due to the pneumatic force is controlled by  $PT$  according to Eq. 4.1. The step-by-step improvement in the printing quality is illustrated in Fig. 4.8. A high degree of overspraying of satellite droplets with diameters as large as approximately  $250 \mu\text{m}$  was observed in the screening step (Fig. 4.8(a)). By reaching the optimized set of factor levels, uniform lines with no overspraying were jetted (Fig. 4.8(b)). At this step, the

average width of the lines was around  $800 \mu m$ , and uniform hemispherical cross-sections were achieved. Further optimization of the process parameters using the response surface analysis technique reduced the lines width to approximately  $580 \mu m$  with a high level of uniformity.

### 4.3.2 Optimization of Plane Features Jetting

The measured values can be found in Table C.10. Based on the residual plots (Figures C.7, C.8, and C.9), there is no concern in terms of the validity of analysis assumptions. The ANOVA results, shown in Table C.11, indicate that  $RW$  and  $v$ , as well as their second order interaction, are significant at 95% confidence level. However,  $v$  has a higher impact on  $W_q$  than the other two items. In order to find the path to optimized waviness value, the marginal means, contour, and surface plots were studied. All three plots indicate that increasing the velocity and decreasing the raster width will produce a lower surface waviness. Based on the regression coefficients presented in Table C.12, the following regression model can be fit to the experimental data:

$$W_q = 41.621 - 10.325V + 4.093RW + 4.301V \times RW \quad (4.5)$$

Setting the  $RW$  and  $v$  at their low and high levels, respectively, resulted in a smooth surface with approximately  $22 \mu m$  of  $W_q$ . The possibility of improving the surface quality using the method of steepest ascent was investigated. From the results shown in Fig. 4.10, it can be concluded that jetting the solid planes with speed of  $104 mm/s$  and raster width of  $0.39 mm$  (Coded values of  $+1.2$  for  $v$  and  $-1.2$  for  $RW$ ) yields the best surface quality with the average  $W_q$  of approximately  $8.1 \mu m$ . The step-by-step minimization of the waviness for the jetted plane structures is illustrated in Fig. 4.11. The optimization process has reduced  $W_q$  from  $40 \mu m$  (Fig. 4.11(a)) to  $8 \mu m$  (Fig. 4.11).

### 4.3.3 Printing Quality and Hybrid AM Method

Comparing the optimization results conducted for the silicone extrusion and silicone jetting in Chapters 3 and 4, respectively, demonstrates that material extrusion results in higher resolution and better surface quality.  $W_{avg}$  of a line printed via extrusion is approximately  $320 \mu m$ . The same parameter for a line printed based on the optimized jetting parameters is between  $500 \mu m$  and  $600 \mu m$ . These results are from a  $250 \mu m$  tapered needle for the extrusion and a  $100 \mu m$  nozzle for the jetting system. Printing lines with higher resolution

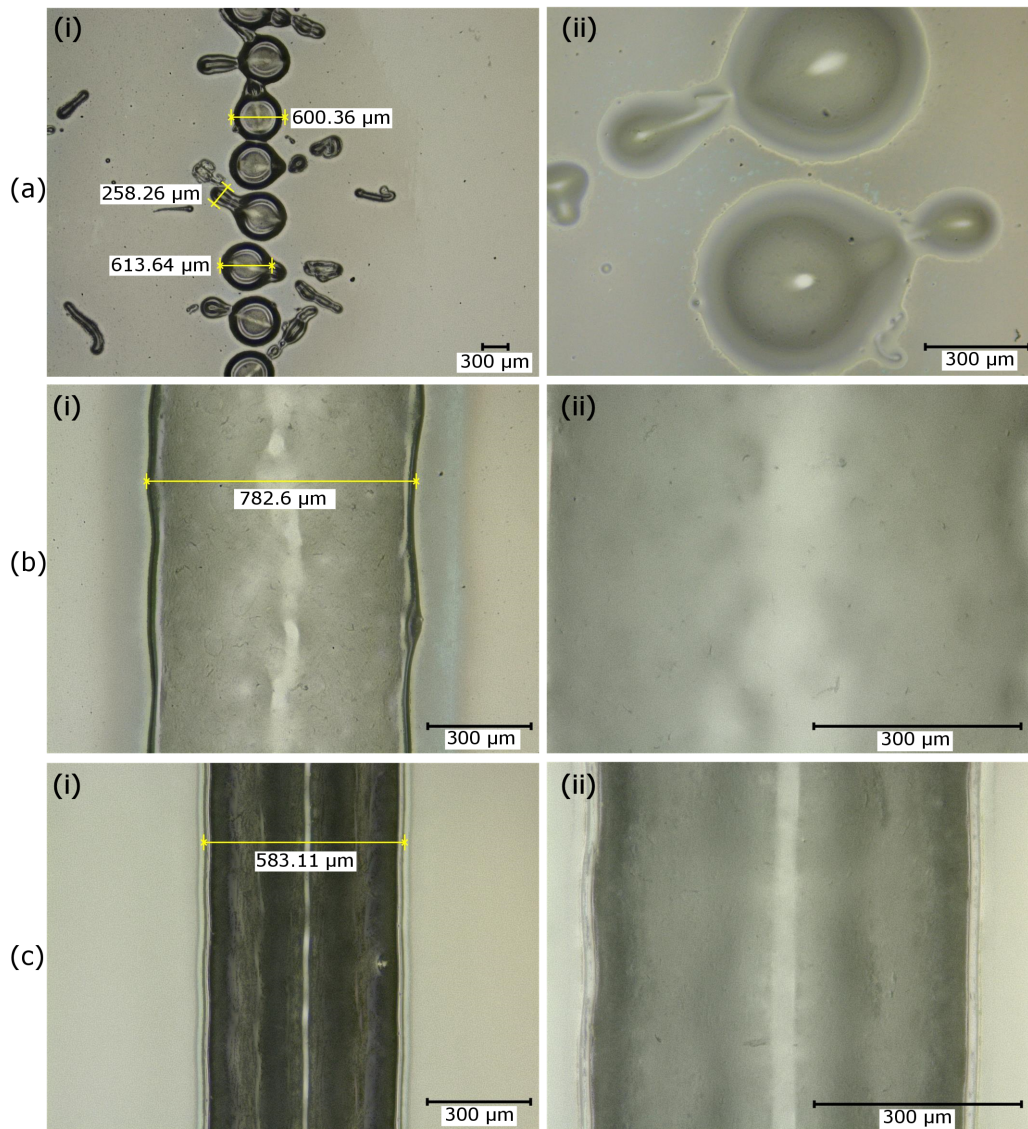


Figure 4.8: The optimization steps for jetting of line features; (a) Failed printed feature at factor screening steps, (a-i) 25 $\times$ , (a-ii) 100 $\times$ ; (b) Continuous line feature after the optimization step, (b-i) 100 $\times$ , (b-ii) 200 $\times$ ; (c) The line feature with improved resolution after response surface optimization, (c-i) 100 $\times$ , (c-ii) 200 $\times$ .

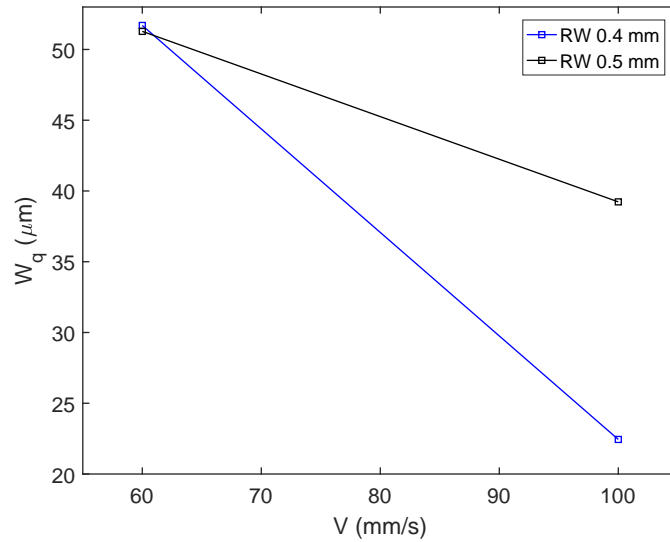


Figure 4.9: The plot of marginal means for the second order interactions  $V \times RW$ .

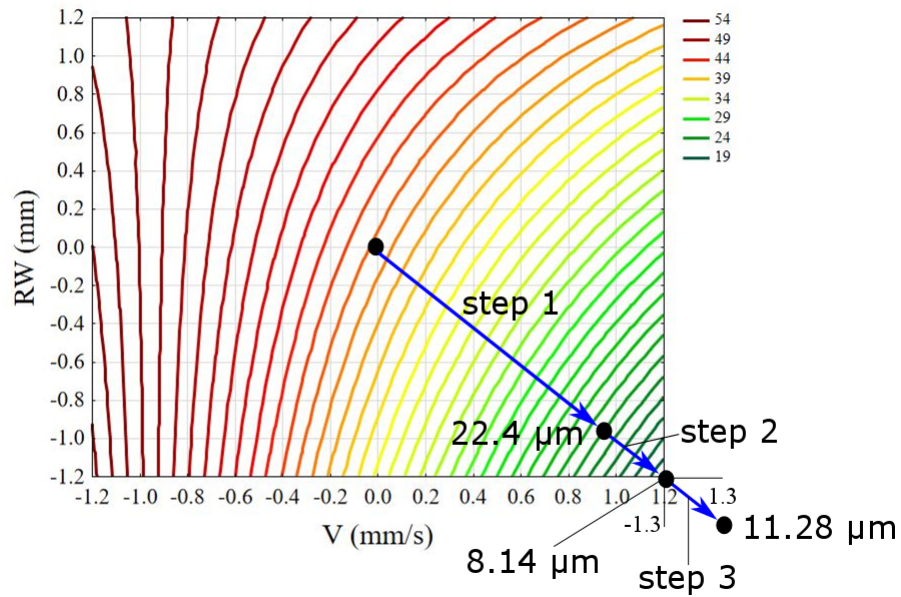


Figure 4.10: The fitted contour plot for the method of steepest descent. The first step corresponds to moving in the optimization direction (minimizing  $W_q$ ) from the center of the contour plot so that the movement path is perpendicular to the contour lines. The color-coded legend shows the values of  $W_q$



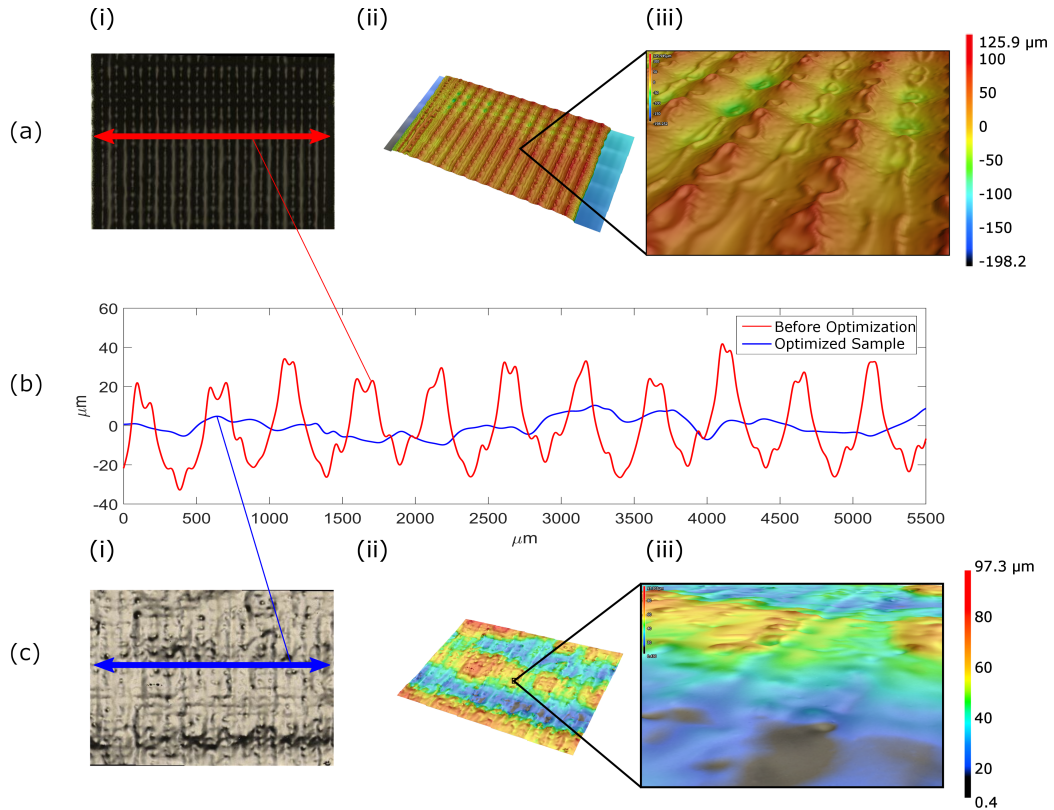


Figure 4.11: The optimization steps for jetting of plane features; (a-i) A sample of the printed plane before the optimization showing periodic irregularities on the surface;; (a-ii) The profilometry result ( $W_q$  of approximately  $40 \mu m$ ), (a-iii) The magnified view of the surface structure before optimization. (b) A comparison between the waviness profile for the printed planes before and after optimization along the identified scanning lines; (c-i) A sample of the printed plane after the optimization showing a smooth surface, (c-ii) The profilometry result ( $W_q$  of approximately  $8 \mu m$ ), (c-iii) The magnified view of the surface structure after optimization.

has been proven to be possible in the extrusion system with 100  $\mu m$  nozzles. However, using 50  $\mu m$  nozzle in the jetting system resulted in printing instability. In terms of the surface quality,  $W_q$  of the extruded plane features was measured to be 3 – 4  $\mu m$  after the optimization study. However, an optimized jetted surface had a  $W_q$  of 8 – 10  $\mu m$  with hollow spaces across its surface. The extruded lines were more uniform as well which makes the extrusion of pastes a better option for high quality 3D printed structures. However, the fact that the PPJ system can print a pattern at a velocity of 104  $mm/s$  compared to 5  $mm/s$  velocity of the extrusion system with only slightly inferior quality made us select it as the main printing method in our hybrid AM system.

In our proposed hybrid method, the outer frame (shell) of each layer is printed using the pneumatic material extrusion printhead. The PPJ printheads are used to print the infill patterns as well as the support structure at a fast rate. This new method takes advantages of both high velocity of the jetting system and the high quality of the extrusion system. This hybrid manufacturing model is illustrated in Fig. 4.12.

The optimization of the resolution and quality of the 3D printing building units at 1D and 2D levels results in the production of defect-free 3D structures. The proposed hybrid method is capable of printing structures 5 – 20 times faster than the material extrusion method; however, as the current printhead only jets the materials through one orifice, the high speed fabrication and characterization of 3D articles with considerable height to cross-section aspect ratio can be achieved through improving the process scalability by development of printheads that have hundreds of orifices and are capable of processing highly viscous polymers.

## 4.4 Summary

In this chapter, a novel hybrid AM method that combines material extrusion and material jetting techniques for the production of silicone-based bio-structures was introduced. This system takes advantage of the high printing quality of extrusion system as well as the high printing velocity of PJJ system. Comprehensive statistical analyses were conducted to (1) identify the working range of the input parameters for PJJ system; and (2) optimize the printing quality at 1D and 2D levels. The results showed that when working with optimum parameter values, the lateral resolution will be 500 – 600  $\mu m$ . On the other hand, 8 – 10  $\mu m$  was the optimized surface waviness value obtained for this process. These optimum values were reached when the jetting printhead was moving at 104  $mm/s$ . The efficient implementation of the proposed method for fabrication of large 3D parts is feasible through development of printheads containing arrays of multiple orifices in the future.

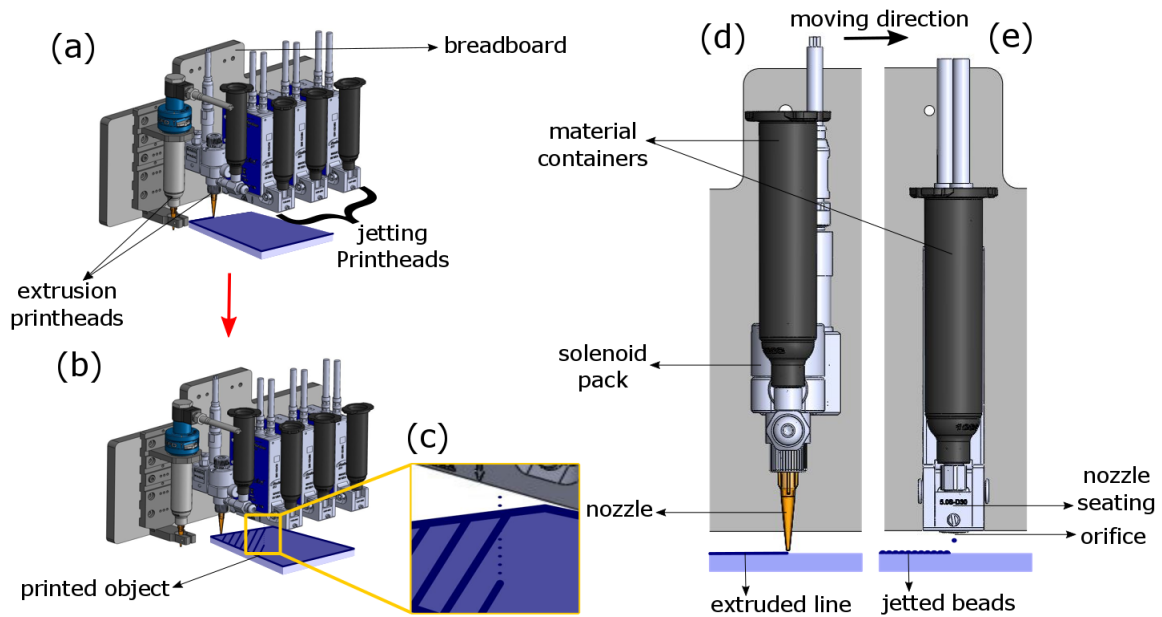


Figure 4.12: The working principle of the hybrid AM technique for printing of silicone; (a) The solenoid-controlled pneumatic printhead is forming the frame of a layer by extruding a continuous stream of silicone; (b) The PPJ printhead is filling the layer at a fast rate based on the program; (c) A magnified view of the PPJ of silicone showing the stream of droplets; (d) The front view of the material extrusion system; (e) The front view of the material jetting system demonstrating how the silicone beads form up a solid line.

# Chapter 5

## Mechanical Characteristics of Silicone Parts Made via Material Jetting

### 5.1 Introduction

To further optimize the PPJ technique for silicone AM, mechanical characteristics and internal structure of parts fabricated using this method should be investigated. Generally, most of the research in the area of mechanical characterization of AM-made silicone parts is related to material extrusion [94, 105, 106]. Regular thermal or piezoelectric inkjet printers are mostly used for the fabrication of films and patterns rather than a 3D structure. Consequently, the mechanical characterization for these drop-on-demand processes is mostly conducted at 2D level [137–139] including for silicone films [87]. Foerster et al. have investigated the effect of scaffolds porosity on the viscoelastic behavior of parts fabricated via PPJ [89]. Based on their work, lower solid density (more air voids) produces a less stiff structure by lowering the values of dynamic moduli. In this chapter, the effects of rheological properties of silicone ink on the internal porosity and tensile, tear resistance, and hardness of 3D parts made using PPJ is investigated for the first time. Decreasing the difference between mechanical characteristics of AM-made parts and the bulk silicone inks has been achieved by reducing the internal porosity of parts. Moreover, the crosslinking kinetics of inks has been studied to establish an in-situ curing policy for UV-curable silicone polymers.

## 5.2 Materials and methods

### 5.2.1 Ink Preparation

A viscous UV-curable silicone (800-400, Novagard, OH, USA), hereinafter known as silicone A, is diluted using a silicone with similar composition but lower viscosity (800-610, Novagard, OH, USA), hereinafter known as silicone B. To tailor the rheology of the 3D printing ink, silicone A and silicone B were blended at four different mixing ratios (A, 70A-30B, 50A-50B, 45A-55B by weight). The samples were mixed using a planetary centrifugal mixer (ARE 310, Thinky, Japan) at 2000 *rpm* for 30 *min* and defoamed at 2200 *rpm* for 15 *min*.

### Rheological Characterization

The shear dynamic moduli ( $G'$  and  $G''$ ) of silicone inks (A, 70A-30B, 50A-50B, 45A-55B) were measured in a stress sweep test using a rheometer (Bohlin CS) with a cone and plate (40 *mm*  $\setminus$ 4°) measuring system at room temperature. The stress sweep test was conducted in the shear stress range 1 - 500 *Pa* at a constant frequency of 1 *Hz*. The viscosity of A and 45A-55B inks was measured using a rheometer (RST-CPS-P, Brookfield Engineering, MA, USA). The tests were conducted for both inks at controlled temperatures  $25 \pm 0.01$  °C and  $100 \pm 0.01$  °C. The viscosity values were collected at 1 - 500  $s^{-1}$  shear rate range using 25 *mm*  $\setminus$ 1° and 50 *mm*  $\setminus$ 1° cone and plate geometries for inks A and 45A-55B, respectively.

### Fourier Transform Infrared Spectroscopy (FTIR)

The infrared spectra were recorded for silicones A and B with a microscope (Hyperion 1000, Bruker, MA, USA) equipped with a Mercury-Cadmium-Telluride (MCT) detector, attached to a FTIR spectrometer (Tensor 27, Bruker, MA, USA). The spectrometer is able to record up to 2 spectra per second at a resolution of 16  $cm^{-1}$ . The sample was placed between two Potassium Bromide (KBr) disks, and placed in the microscope stage operating in transmission mode. The thickness of the sample was adjusted ( $\sim 200$   $\mu m$ ) in order to result in a spectrum with appropriated intensity. UV radiation was performed with a UV light curing system (OmniCure S2000, Excelitas Technologies, ON, Canada) through a 5 *mm* diameter lightguide, and the iris was adjusted to be 20% open. The end of the fiber optic was placed at 5 *mm* from the KBr disk at an angle of 90°. The intensity of the incident UV light measured by a radiometer (OmniCure R2000, Excelitas Technologies, ON, Canada) was 3.54  $w/cm^2$  at 5 *mm* working distance.

## 5.2.2 Experimental Setup

The silicone parts were made using the hybrid extrusion-PPJ AM system, as presented in Chapter 4. In this Chapter, however, to study the mechanical characteristics and porosity of parts made via the PPJ technique, the fabrication of layers shell with extrusion was eliminated, and both the shell and core were jetted. The printing parameters for each ink are provided in Table 5.1. For all the parts manufactured for mechanical characterization and porosity analysis in this research, 2000% pattern/perimeter overlap and 10 *mm* settling and shutoff distances were selected. The alternating printing angles of 0° and 90° were selected for successive layers to achieve a weave pattern.

Table 5.1: PPJ printing parameters for different silicone inks.

Printing Parameters	A	70A-30B	50A-50B	45A-55B
<i>PT</i> ( <i>ms</i> )	0.4	0.4	0.4	0.4
<i>CyT</i> ( <i>ms</i> )	4	6	10	12
<i>T</i> ( <i>C</i> )	100	100	100	100
<i>V</i> ( <i>V</i> )	85	85	120	120
<i>Str%</i> (%)	80	80	75	75
<i>OT</i> ( <i>ms</i> )	0.2	0.2	0.2	0.2
<i>CT</i> ( <i>ms</i> )	0.2	0.2	0.2	0.2
<i>v</i> ( <i>mm/s</i> )	104	104	104	104
<i>WD</i> ( <i>mm</i> )	2	2	2	2
<i>P</i> ( <i>kPa</i> )	500	500	500	500

## 5.2.3 Mechanical Characterization

Tensile, tear resistance, and hardness tests were conducted in accordance with ASTM D412 (Die C), ASTM D624 (Die C), and ASTM D2240 guidelines, respectively. For preparing the cast specimens, plastic molds were 3D printed using a PolyJet system (J750, Stratasys, MN, USA). Silicones A and B have a dual irradiation-condensation curing mechanism. To make sure the full mechanical performance has been obtained, the samples were exposed to environment moisture for 7 days after UV curing. The tensile and tearing tests were conducted using a universal testing system (Tensometer 2000, Alpha Technologies, OH, USA) at velocity of 508 *mm/min* using a 1 *kN* load cell until failure was observed. The hardness of samples was measured based on their resistance to the indentation of a Shore 00 rigid ball using a handheld durometer (Shore S1, Shore Instruments-Instron, MA, USA).

## 5.2.4 Tomography and Porosity Analysis

To analyse the internal porosity of parts,  $0.5\text{ cm} \times 0.5\text{ cm} \times 0.5\text{ cm}$  cubic samples were manufactured using PPJ system for inks A and 45A-55B. The tomography data was captured for these samples using a nano-CT scanner (Xradia 520 Versa 3D X-ray microscope, Zeiss, Germany). Cone beam X-rays were transmitted through the silicone specimens. Optimized scintillators converted the X-rays to photons in the visible light spectrum. It is then magnified using a  $4\times$  objective lens, and lastly detected by a charge-coupled detector (CCD). To allow the 3D reconstruction, the specimen was turned around  $360^\circ$ , and a series of 2D images were captured. The X-ray CT scanning conditions are presented in Table 5.2.

Advanced image processing and porosity analysis were performed using a visualization and image processing package (Dragonfly Pro v3.0, Object Research Systems Inc., QC, Canada). The reconstructed dataset was segmented into the base silicone material and air voids (pores) by using routine image processing steps, including greyscale thresholding and morphological operations. Furthermore, the binarized images were obtained to be subsequently used for acquiring quantitative information such as total volume and size distribution of pores. 3D image analysis software ImageJ was employed to measure the relative density that represents the distribution of porosity throughout the part. To this end, 2D projections of the binarized porous dataset was divided by a binary mask in which each pore was filled using the ImageJ plug-in Fill Holes.

Table 5.2: Parameters of CT measurements.

Parameters	
Source-to-detector distance ( $mm$ )	21.11
Voxel size ( $\mu m$ )	4.0001
Voltage ( $kV$ )	40.18
Power ( $W$ )	3
Current ( $\mu A$ )	74.62
Source filter	Air
Exposure time ( $s$ )	2.5
Optical magnification	$4\times$
Camera binning	2
Number of projection	2001

### 5.2.5 Imaging

To visualize the slumping, droplets were jetted on a 5 *cm* linear pattern using inks A, 70A-30B, and 45A-55B based on the parameters of Table 5.1. The distance between the droplets was kept constant by jetting all the inks at similar frequency (83 *Hz*). For each ink, the printed lines were completely cured at 0, 10, 30, and 60 *s* after jetting. Images of the lines were captured after curing using a microscope (VK-X250, Keyence, Japan) at 50× magnification. The fractography study has been conducted by obtaining images of the tensile specimens at their failure surface using a scanning electron microscope (SEM) (Ultra Plus, Carl Zeiss AG, Germany).

### 5.2.6 Statistical Analysis

The differences between mechanical properties of AM-made and cast samples were evaluated using one-way ANOVA at 95% confidence level ( $p < 0.05$ ).

## 5.3 Results and Discussion

### 5.3.1 Curing Policy

Commercially available silicones are crosslinked using three main chemical reactions as shown in Fig. 5.1: (1) platinum-catalyzed hydrosilylation between vinyl groups and Si–H bond; (2) thiol-ene click chemistry between vinyl group and thiol group; (3) condensation reaction of alkoxy silane [140]. Hydrosilylation is the most common silicone curing method, however, it is a slow process that requires high temperatures. Thiol-ene reactions are photoinitiated and very fast, however, crosslinking will not happen in areas not irradiated. Condensation of alkoxy silanes can be performed at room temperature but it requires several hours to cure properly.

In order to overcome the limitations of thio-ene crosslinked silanes, the material used in this work uses a dual-cure mechanism that combines the fast, UV activated, thiol-ene click chemistry with alkoxy silane functionality so unexposed fractions of the material can also be crosslinked via condensation [141]. The material is formulated with two prepolymers as presented in Fig. 5.2. The prepolymer A is a thiol and alkoxy functional polysiloxane while prepolymer B contains vinyl and alkoxy functionality. It is worth mentioning that the viscosity of the material increases with the degree of polymerization,  $n$ , of the prepolymers.





The characteristic vibrations of the functional groups from both polysiloxanes before crosslinking is presented in Fig. 5.3(a). The peak assignments were performed according to Tingaut et al. [142]. It is important to notice that the silicon groups showed very strong peaks while the thiol and vinyl terminal groups are a lot less intense. This is an indication of a high degree of polymerization of the prepolymers before the crosslinking reaction.

The intensity of the peak at  $1673\text{ cm}^{-1}$ , corresponding to C=C stretching, was monitored as a function of the UV exposure time to study the development of the crosslinking reaction. As can be seen in Fig. 5.3(b-c), the intensity of the peak at  $1673\text{ cm}^{-1}$  is reduced when the sample is exposed to UV light reaching a minimum after around 20 s. The reduction of the intensity of this peak is expected as the crosslinking reaction advanced, as demonstrated in the mechanism shown in Fig. 5.1. At the same time, the peak at  $2500\text{ cm}^{-1}$ , corresponding to S-H stretching, was supposed to be reduced due to the reaction of S-H groups with C=C ones. However, due to the low intensity of the S-H peak, it was not possible to detect any significant change on this region.

Interestingly, the appearance of a peak at  $1712\text{ cm}^{-1}$  is related to the oxidation of the polysiloxanes by the UV light in the presence of air, leading to formation of C=O groups that are associated with this region of the IR spectrum.

From the spectra, we applied a method derived on Beers law that was based on the ratio of the characteristic to reference absorbance peak. Changes in the area under peak of the band at  $1673\text{ cm}^{-1}$  were calculated at different times to obtain the conversion and the results are shown in Fig. 5.4. The results showed that the viscosity of the sample has small effect on the polymerization reaction once both liquid and paste sample showed similar conversion plots, with complete conversion around 20 s. This makes designing a uniform curing policy for all inks (A, 70A-30B, 50A-50B, and 45A-55B) possible. An ideal curing mechanism for direct write AM will crosslink each layer after printing just enough to prevent the structural collapse or deformation due to the weight of upper layers while conserving the active surface to strengthen the cohesion of successive layers. Based on the conversion plots for silicones A and B (Fig. 5.4), the UV laser lightguide followed a trajectory pattern similar to that of the printhead with  $RW$  of 6 mm at  $WD$  of 5 mm so that each section of the printed layer with an approximate area of  $25\text{ mm}^2$  is exposed to UV light for 1 s. This corresponds to approximately 20% and 15% crosslinking for silicone A and silicone B, respectively. The curing was conducted after printing every two layer (longitudinal and transverse).

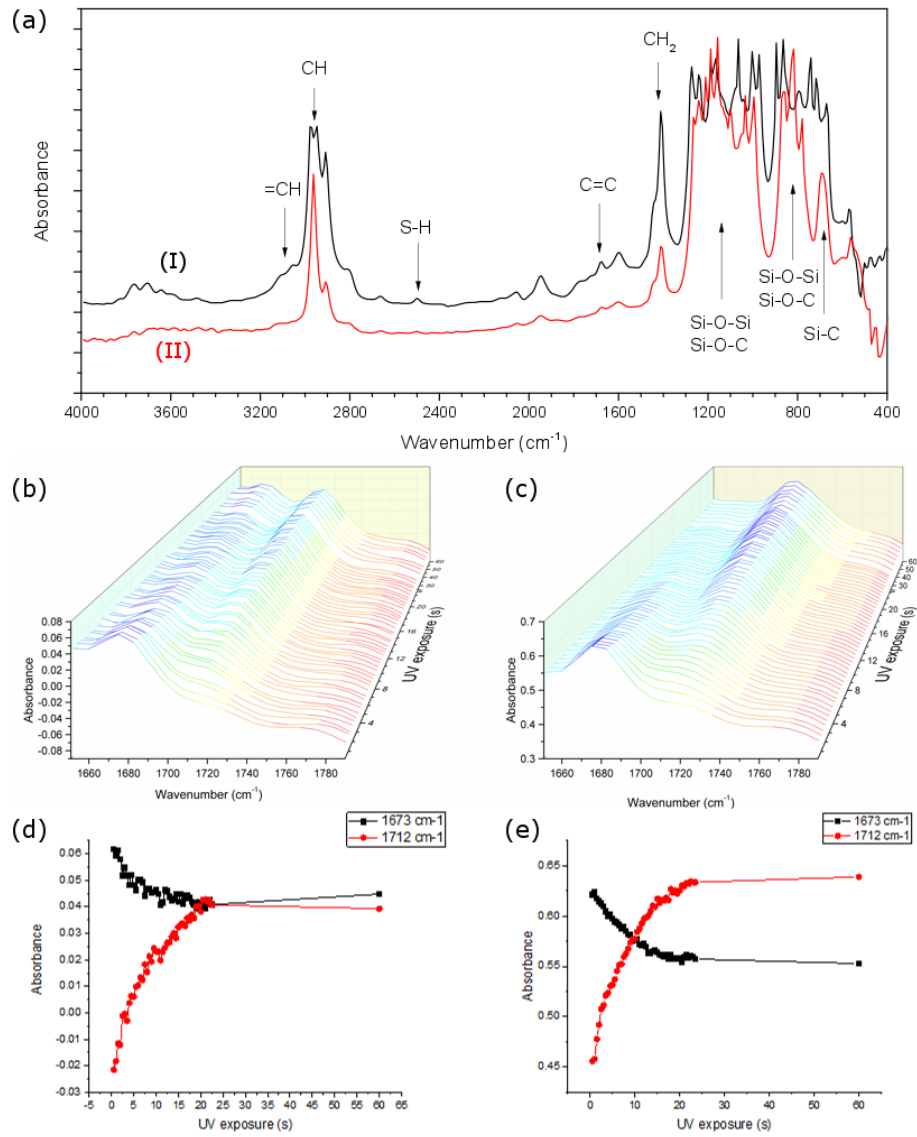


Figure 5.3: (a) FTIR absorbance spectra of (I) silicone A (II) silicone B; (b) FTIR spectra obtained at different UV exposure times for silicone A; (c) FTIR spectra obtained at different UV exposure times for silicone B; (d) Evolution of peaks at 1673 and 1712  $\text{cm}^{-1}$  for silicone A; (e) Evolution of peaks at 1673 and 1712  $\text{cm}^{-1}$  for silicone B.

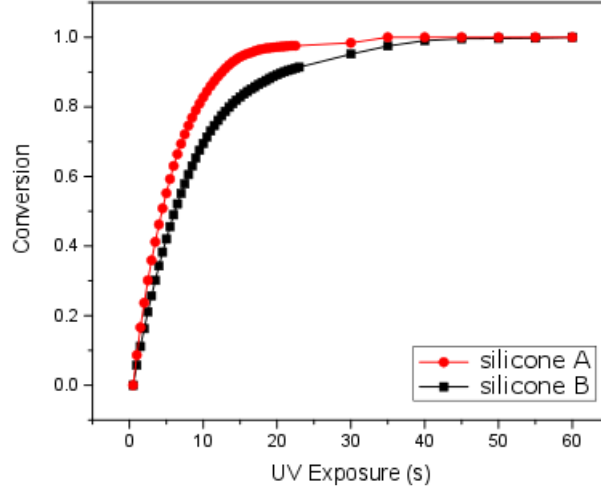


Figure 5.4: Conversion vs. time plots for silicones A and B.

### 5.3.2 Effects of Silicone Rheology on Internal Porosity of Parts

To investigate the shape retention properties of different blends of silicones A and B, the stress-sweep test was conducted (Fig. 5.5(a-d)). For pure silicone A,  $G'$  is more than  $G''$  with a high shear yield stress ( $\sigma_y$ ) of  $\sim 300 Pa$ , exhibiting a solid-like behavior (Fig. 5.5(a)). This difference between the dynamic moduli as well as the length of storage modulus plateau is decreased for 70A-30B ink (Fig. 5.5(b)). Similar trend is observed as the content of silicone B is increased (Fig. 5.5(c-d)). For 50A-50B ink, the value of  $G'$  is slightly higher than  $G''$  in low shear stress region with the yield stress of  $\sim 15 Pa$ . By increasing the weight percentage of silicone B to slightly more than 50%, ink 45A-55B with the dominant fluid-like behavior was obtained (Fig. 5.5(d)). The slumping on the glass substrate over time is compared for different inks in Fig. E.1. This test shows the initiation of droplets coalescence for ink 45A-55B almost after deposition. Creation of non-parallel contact lines for ink 45A-55B after the droplets are fully merged is acceptable in our proposed hybrid extrusion-jetting method as both the external and internal perimeters are extruded using ink A in this method.

The viscosity plots for inks with dominant solid-like behavior (A) and dominant fluid-like behavior (45A-55B) at two different temperatures of 25 °C (room temperature) and 100 °C (maximum working temperature of printhead) are compared in Fig. 5.5(e-f). The plots show a highly shear-thinning behavior for ink A with a viscosity of  $15 \times 10^5 mPa.s$

at shear rate of  $1 \text{ s}^{-1}$ . The high shear-thinning property causes a reduction in the viscosity to less than  $2 \times 10^5$  at shear rate of  $20 \text{ s}^{-1}$ . Increasing the temperature to  $100 \text{ }^\circ\text{C}$  results in a reduction in the viscosity of ink to  $6 \times 10^5 \text{ mPa}\cdot\text{s}$  at  $1 \text{ s}^{-1}$ . This lower viscosity makes the jetting of droplets easier, as a result,  $100 \text{ }^\circ\text{C}$  was selected as the printing temperature. Ink 45A-55B with the dominant amount of silicone B demonstrates similar shear-thinning behavior and lower viscosity. The value of viscosity for 45A-55B at  $1 \text{ s}^{-1}$  for this ink ( $3.7 \times 10^4 \text{ mPa}\cdot\text{s}$ ) is two orders of magnitude less than the viscosity of pure silicone. A. This value drops to  $10^4 \text{ mPa}\cdot\text{s}$  at shear rate of  $20 \text{ s}^{-1}$ . Similar to ink A, increasing the temperature results in the drastic reduction of viscosity ( $1.5 \times 10^4 \text{ mPa}\cdot\text{s}$  at shear rate of  $1 \text{ s}^{-1}$ ). Similar viscosity reduction ratio from  $25 \text{ }^\circ\text{C}$  to  $100 \text{ }^\circ\text{C}$  temperatures (0.4) is observed at low shear rate region for both inks.

X-ray CT scanning was used to observe and quantify the internal porosity of samples manufactured using PPJ technique for inks A and 45A-55B. To obtain the finest resolution for the parts, voxel edge lengths of  $4 \text{ }\mu\text{m}$  were used. Figure 5.6[(a-i)-(b-i)] represent the 3D visualization of voids internal to the part at scanning resolution of  $4 \text{ }\mu\text{m}/\text{pixel}$  in which pores are labelled by volume. Figure 5.6(a-i) shows that sample A consists of smaller number of pores while pores are dramatically larger compared to sample 45A-55B. This is also evident in the 2D slice rendering of pore distribution in XZ plane (Figure 5.6[(a-ii)-(b-ii)]).

These findings correlate well with the quantitative pore analysis from X-ray CT scans of the parts at  $4 \text{ }\mu\text{m}/\text{pixel}$ . As summarized in Table 5.3, the volume of the smallest detected pore is  $512.08 \text{ }\mu\text{m}^3$  for both samples, and any objects (pores) smaller than  $512.08 \text{ }\mu\text{m}^3$  were chosen to be noise, which corresponds to  $(2 \times \text{voxel size})^3$  for the noise filtration. The volume of the largest detected pore for sample A is  $2.34 \times 10^8 \text{ }\mu\text{m}^3$ . These large pores add up to the total pore volume of  $13.1 \times 10^8 \text{ }\mu\text{m}^3$  for sample A that is a considerable air void volume compared to  $0.7 \times 10^8 \text{ }\mu\text{m}^3$  for sample 45A-55B, and contributes to a much smaller relative density (89.17% for sample A vs. 99.65% for sample 45A-55B, respectively), while only 840 pores were detected for sample A vs. 3358 for sample 45A-55B.

Histogram of the pore volumes obtained at scanning resolution of  $4 \text{ }\mu\text{m}/\text{pixel}$  associated with samples A and 45A-55B are exhibited in Fig. 5.7(a-b). As seen, pore volume peak is in the range of  $10 \times 10^3 - 50 \times 10^3 \text{ }\mu\text{m}^3$  for sample 45A-55B, while pore volume peak is remarkably shifted to  $0.8 \times 10^6 - 10 \times 10^6 \text{ }\mu\text{m}^3$  range for sample A. Slice-wise relative density calculation of parts at  $4 \text{ }\mu\text{m}/\text{pixel}$  scan is shown in Fig. 5.7(c). Quantitative values for relative density are based on the analysis of each individual 2D cross section normal to the central axis. Therefore, the relative density of each tomography slice is calculated by the number of voxels that are identified as the solid phase compared to the total number of voxels identified as either solid or void within the boundary of the part. The lower average

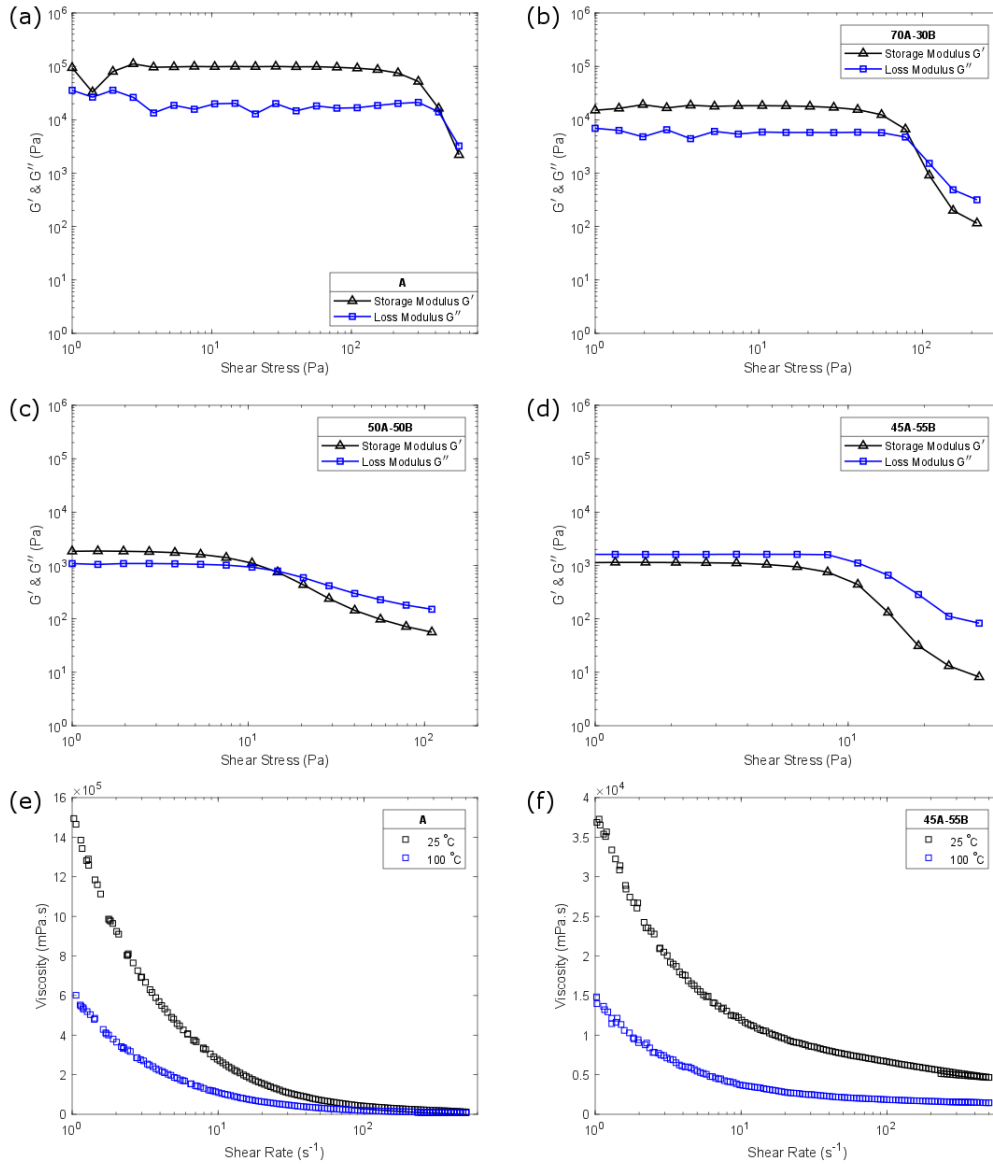


Figure 5.5: The stress-sweep results for (a) ink A, (b) ink 70A-30B, (c) ink 50A-50B, and (d) ink 45A-55B. The reduction in the solid-like behavior of inks is observed as the content of silicone B is increased. Shear-thinning Viscosity plots for (e) ink A and (f) ink 45A-55B at 25 °C and 100 °C. Elevated temperature reduces the viscosity value and facilitates the jetting process.

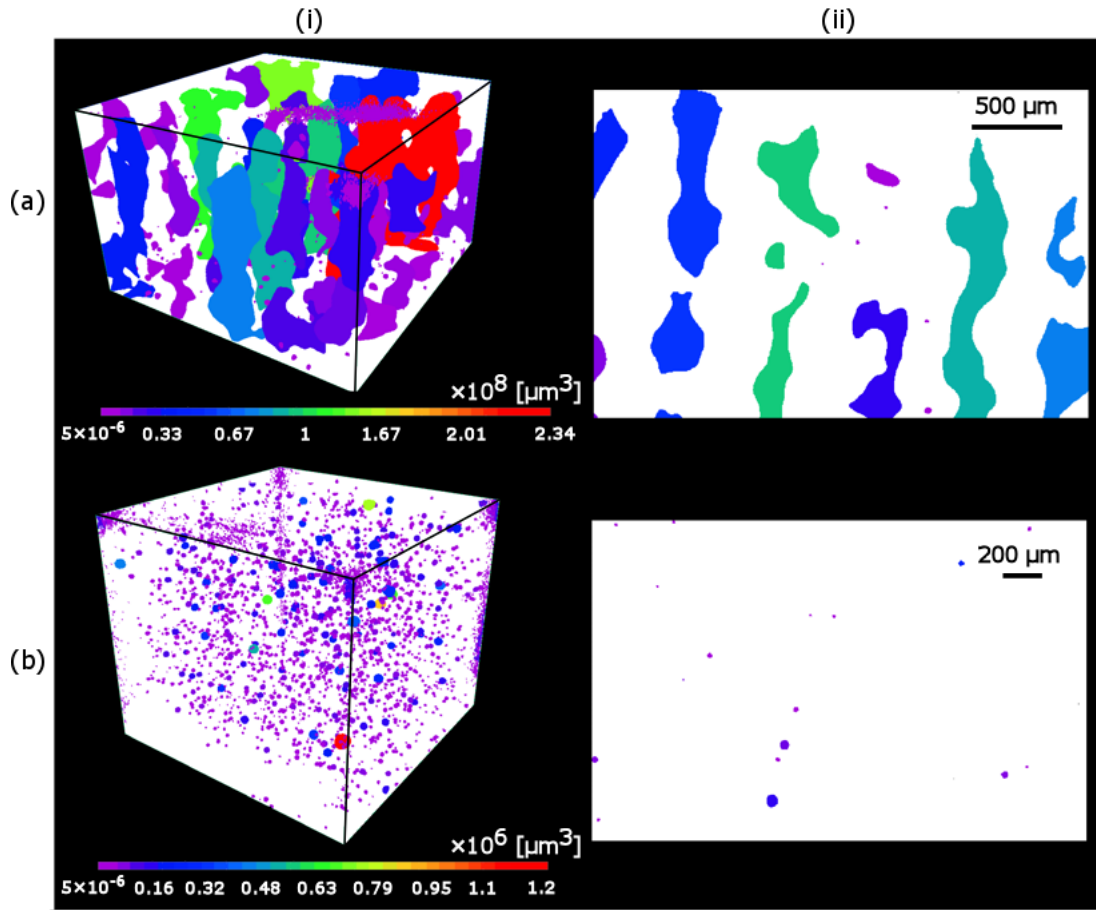


Figure 5.6: CT scan results for (a) sample A and (b) sample 45A-55B: (i) 3D rendering of porosities of parts at two scanning resolutions of  $4 \mu\text{m}/\text{pixel}$  showing the distribution of voids throughout the parts, (ii) 2D slice rendering of pore distribution in XZ plan.

Table 5.3: Summary of the tomography analysis results.

Parameter	A	45A-55B
Pore volume (voxels)	20541520	1104708
Pore volume ( $\mu\text{m}^3$ )	$13 \times 10^8$	$0.7 \times 10^8$
Number of detected pores	840	3358
Largest pore ( $\mu\text{m}^3$ )	$2.3 \times 10^8$	$18 \times 10^5$
Smallest detected pore ( $\mu\text{m}^3$ )	512.08	512.08
Relative density (%)	89.17	99.65

density for sample A (89.17%) is attributed to the existence of dominant large pores ( $0.8 \times 10^6 - 300 \times 10^6 \mu m^3$ ), which mainly do not exist in sample 45A-55B.

For material extrusion techniques, the shape retention capability of the ink after deposition determines its final resolution and printing quality. Tuning the rheological properties of silicone ink to obtain a shear-thinning viscous polymer with solid-like behavior ( $G' > G''$ ) that is extruded easily under the shear stress at the nozzle without slumping on the surface upon extrusion has been extensively investigated [67, 93–95, 104]. For successful AM of silicone using material jetting, however, a different rheological behavior is required, as in this technique, the building unit is a beaded line composed of adjacent droplets with a certain level of overlap as apposed to a uniform filament. In material extrusion or FDM techniques, air voids might be generated parallel to the printed filament. This difference is depicted in Fig. 5.8. This is the source of anisotropic mechanical properties and poor mechanical performance of extruded parts compared to the bulk material. Modifying the printing parameters such as raster width, back pressure and velocity can eliminate the percentage of air voids. In material jetting, if the deposited droplets do not merge, pores will also be generated along the printed lines resulting in even more inferior mechanical properties. On the other hand, if the ink is very low viscous, the printing resolution will be jeopardized. Even if the printing parameters are optimized to produce fully dense layers with high surface qualities (as was shown for ink A in Chapter 4), the gradual build up of viscous solid-like inks around the nozzle intensified by the deflection of silicone droplets from the previous silicone layers as a result of electrostatic repulsion described in [73] deteriorates the surface quality of higher layers by generating air voids. Reducing the air gap volume in a jetted structure can be achieved by: (1) increasing the jetting frequency; (2) curing the structure after the print instead of curing each layer; and (3) tuning the rheological behavior of ink. The first two methods might not be practical in all cases, as increasing the jetting frequency results in wider lines (lower resolution) and more overspraying, while not curing the printed layers will cause structural collapse and deviation from target height. As a result, the silicone ink should be tailored to be adequately flowable so that coalescence happens at the contact point of droplets to form a uniform filament without risking the well defined resolution of lines. The results of oscillatory shear stress tests (5.5) showed that this can be obtained using the ink 45A-55B. The slightly higher  $G''$  of this ink guarantees the slight slumping of ink under the effect of gravity upon exiting the nozzle, yet the ink does not slump too much so that the resolution of line is lost.

This conclusion is validated by studying the tomography results of parts fabricated using the viscous ink with solid-like behavior (A) and the ink with dominant liquid-like behavior (45A-55B). The CT scan results demonstrate a reduction in pore size and total pore volume for 2 orders of magnitude and 1 order of magnitude, respectively, by increasing



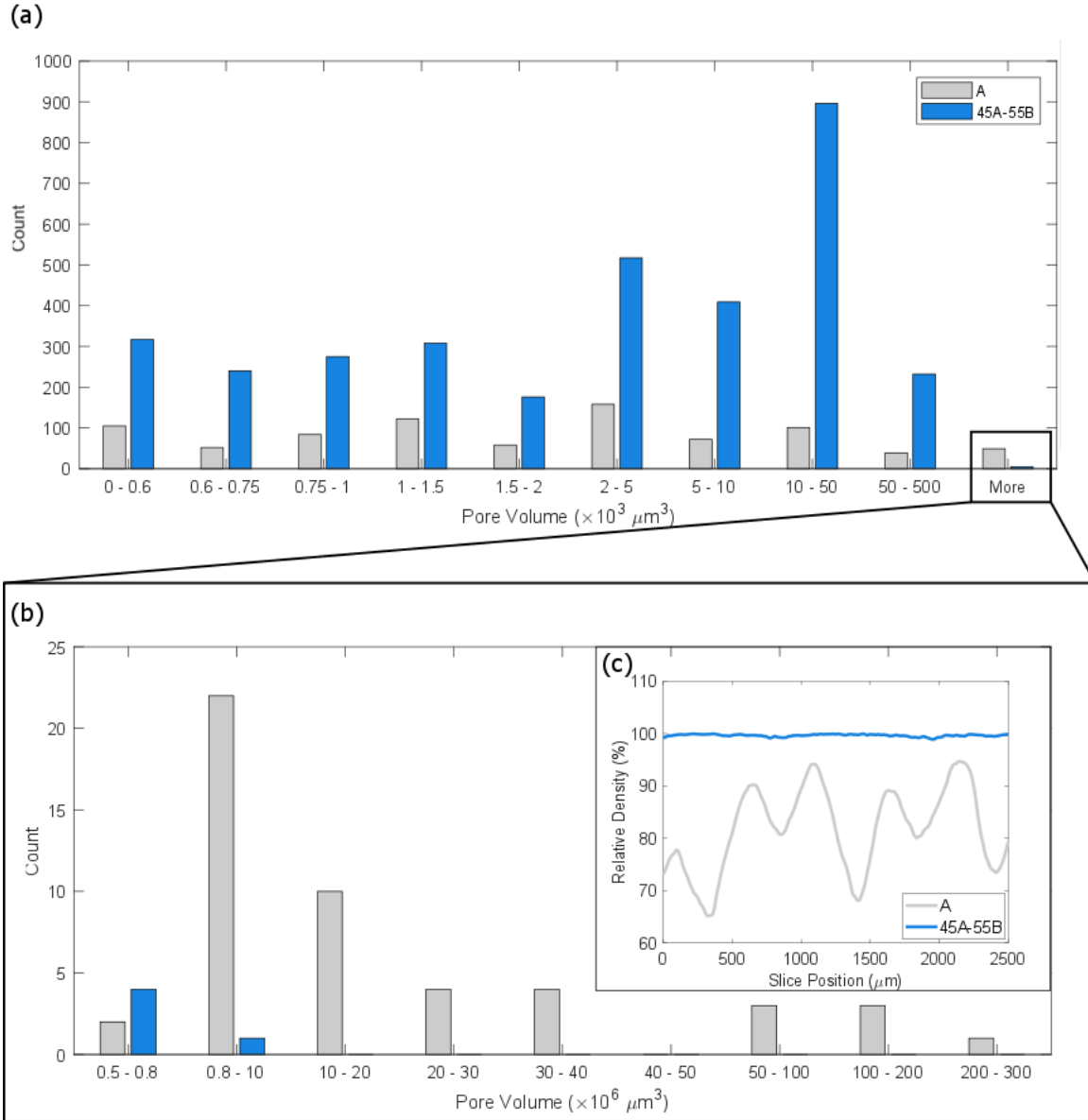


Figure 5.7: (a) Histogram of pore volumes obtained at  $4 \mu\text{m}/\text{pixel}$  for samples A and 45A-55B; (b) magnification of the histogram at higher volume size bins; (c) slice-wise relative density calculation at  $4 \mu\text{m}/\text{pixel}$  for samples A and 45A-55B.

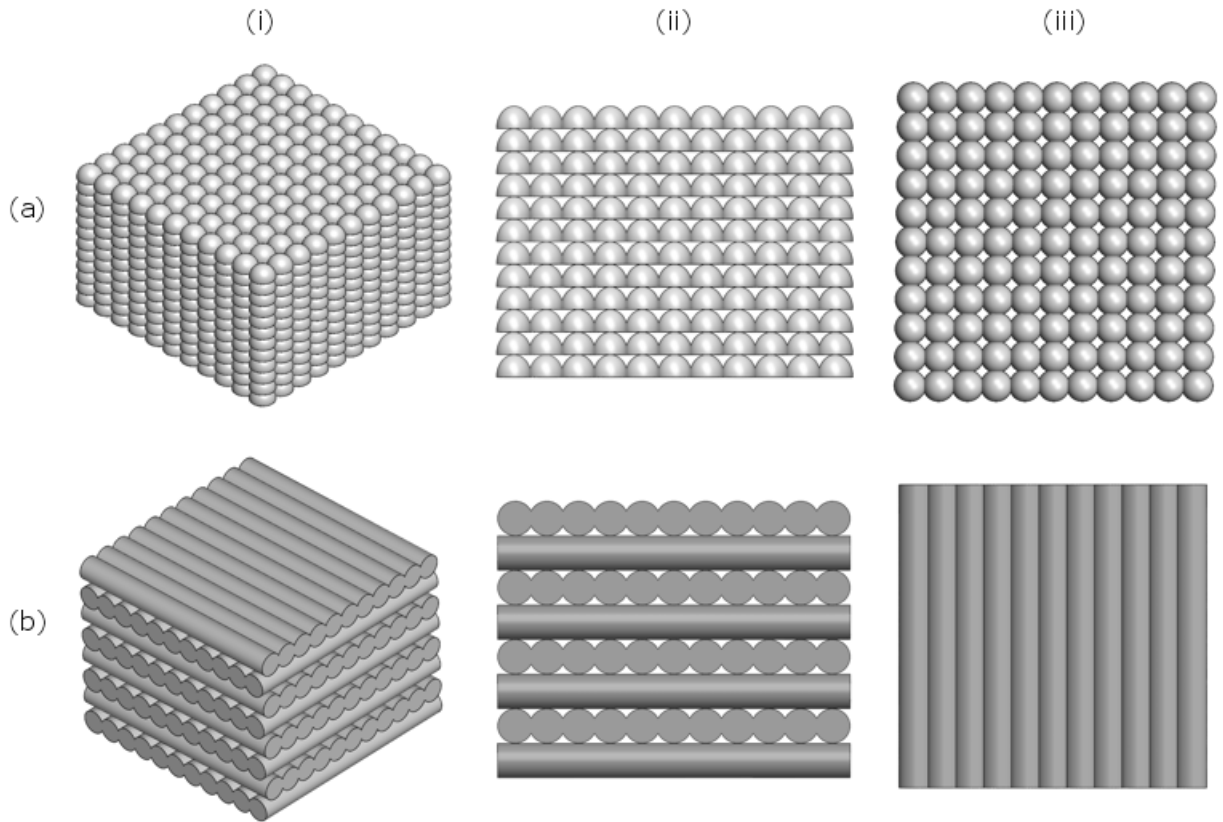


Figure 5.8: Schematic view of 3D structures made using (a) jetting and (b) extrusion. (a-i) 3D view; (a-ii) side view showing inter-layer pores; (a-iii) top view showing in-layer pores. (b-i) 3D view; (b-ii) side view showing inter-layer pores, (b-iii) no in-layer pore or air gap is visible if the strands overlap.

the amount of silicone B to 55 wt.%. However, this has increased the total number of pores by approximately 4 times, introducing many pores with sub-micron size diameter to the media. This has resulted in production of a structure with the least amount of pore volume ( $0.7 \times 10^8 \mu m^3$ ) and highest solid density (99.65%).

### 5.3.3 Effects of Porosity on Mechanical Performance of Parts

The uniaxial tensile test, tear resistance test, and durometry test have been carried out for inks A and 45A-55B (Fig. 5.9) for the parts made using PPJ (AM-made) as well as the molded bulk materials (cast).

Figure 5.9(a) shows 38.6% reduction in the average elongation at break ( $\epsilon_f$ ) for AM-made parts from ink A (381%) compared to its cast control sample (234%). For ink 45A-55B, the average  $\epsilon_f$  was reduced to 97.3% and 85.1% for AM-made and cast specimens, respectively. As a result, the difference percentage for this parameter has been reduced to 12.6% for ink 45A-55B. Similar behavior can be observed in Fig. 5.9(b) for the tensile strength ( $\sigma_f$ ). A significant 45.9% reduction in the value of  $\sigma_f$  from 1.35 MPa for cast to 0.73 MPa for AM-made specimens has been reduced to 2% difference between average  $\sigma_f$  of cast (0.49 MPa) and AM-made (0.5 MPa) samples.

The tearing resistance test results are demonstrated in Fig 5.9(c). For this property of the matter, the tear strength ( $T_s$ ) of cast and AM-made samples are not significantly different for inks A (0.66%) and 45A-55B (2.4%). For ink A, the average tear force is 10.85 kN/m for cast specimens and 10.77 kN/m for AM-made specimens. These values have been dropped to 1.003 kN/m and 1.027 kN/m for cast and AM-made specimens of ink 45A-55B, respectively. Similarly, the hardness values, shown in Fig. 5.9(d), are not significantly different for the two different fabrication methods for both inks. The average hardness value for cast samples of ink A is 73.2 (Shore 00) as opposed to 70.1 (Shore 00) for AM-made samples. The hardness of parts manufactured from ink 45A-55B is slightly less (66.5 and 64.5 (Shore 00) for cast and AM-made samples, respectively). The details of measurements and statistical comparison of mean values are provided in Table E.1. The corresponding stress-strain curves and tearing force plots are provided in Fig. E.2.

The adverse effect of pores on the mechanical performance as well as improving the strength of the parts by reducing the porosity level through modification of printing parameters has been extensively studied for extrusion-based systems [143–148]. Moreover, the quality of the inter-layer bonds can determine the strength of parts as well. The creation of strong cohesive bonds between successive layers was obtained through the *in-situ*

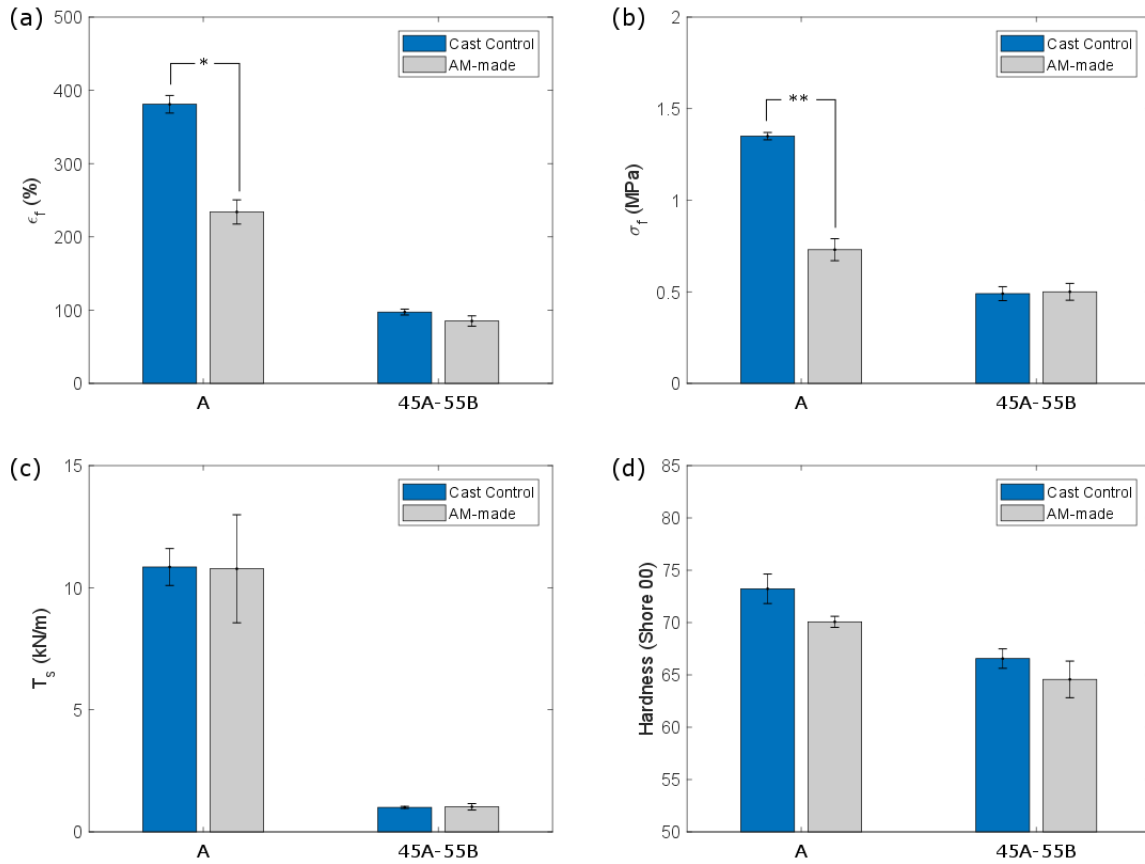


Figure 5.9: Comparing the mechanical characteristics of AM-made and cast samples made from inks A and 45A-55B ( $\alpha = 0.05$ ): (a) Elongation at break ( $\epsilon_f$ ), (b) tensile strength ( $\sigma_f$ ), (c) tear strength ( $T_s$ ), and (d) Shore 00 hardness. The p-value for significant difference between the average of parameters under study: \* 0.001, \*\* 0.00. (a-d)  $n = 3$ .

partial curing mechanism explained in Section 5.3.1. Thus, the significant difference between the cast and AM-made parts for both ultimate stress and strain ( $\sigma_f$  and  $\epsilon_f$ ) can be justified through the difference in their porosity. Sample A is  $\sim 19$  times more porous than sample 45A-55B. Small pores ( $< 0.5 \times 10^6 \mu m^3$ ) are visible in both samples with higher concentration in sample 45A-55B; however, sample A contains a significant number of large pores in the volume range  $0.8 \times 10^6 - 300 \times 10^6 \mu m^3$  (more than 50 pores in  $125 mm^3$ ). The tomography results (Fig. 5.6) shows that the small voids of sample 45A-55B are introduced to the structure during the jetting process and scattered throughout the structure with no special pattern which is similar to what might be seen during the casting; however, the large air voids of sample A seem to be made as a result of failed merging of adjacent beaded lines. The weak bond between lines in one layer as well as the stress concentration zones generated by the large pores throughout the testing section of tensile specimens leads to their pre-mature failure compared to cast samples. The insignificant difference for sample 45A-55B shows that the small spherical pores ( $< 0.5 \times 10^6 \mu m^3$ ) do not contribute much to lowering the tensile strength and elasticity of parts made via PPJ. The lower  $\sigma_f$  and  $\epsilon_f$  of ink 45A-55B is due to the use of silicone B with short-chain monomers. Similar reduction in resilience and strength has been reported for a silicone composed of short- and long-chain monomers at similar ratio by Jindal et al. [105].

The adverse effect of porosity on the tensile properties was corroborated by studying the fracture surface of tensile specimens A (Fig. 5.10(a)) and 45A-55B (Fig. 5.10(b)). Pores observed on the fracture surface of specimen A are marked in Fig. 5.10(a-i). In comparison, the fracture surface of specimen 45A-55B only contains one pore (Fig. 5.10(b-i)). The initiation of cracks from the edge of the pores and their propagation through the surface can be observed in Fig. 5.10(a-iii). On the other hand, the brittle nature of silicone B has resulted in a clean flat rupture through parallel vertical and horizontal cracks covering the entire surface from edge to edge which can be observed in Figs. 5.10[(b-ii)-(b-iii)].

The manufacturing method seems to have no influence on the tearing strength for both inks. This can be attributed to the fact that in type C specimen of ASTM D 624 standard, the initiation of tear happens at the right-angled stress concentration apex. The effect of this apex on the initiation of rupture surpasses the effects of stress concentration zones of small pores. Similarly, the effect of manufacturing method on the hardness is minimal. This effect on the hardness, however, is slightly larger compared to tear strength. Even for ink A, there is a statistically significant difference between the average hardness of cast and AM-made parts; however, because the p-value (0.041) is close to the significance level, the difference is considered to be experimentally insignificant. Moreover, hardness is the only parameter which is not sensitive to the change in the ink composition. Meanwhile, adding 55 wt.% silicone B to the composition of ink has reduced the tear strength by a

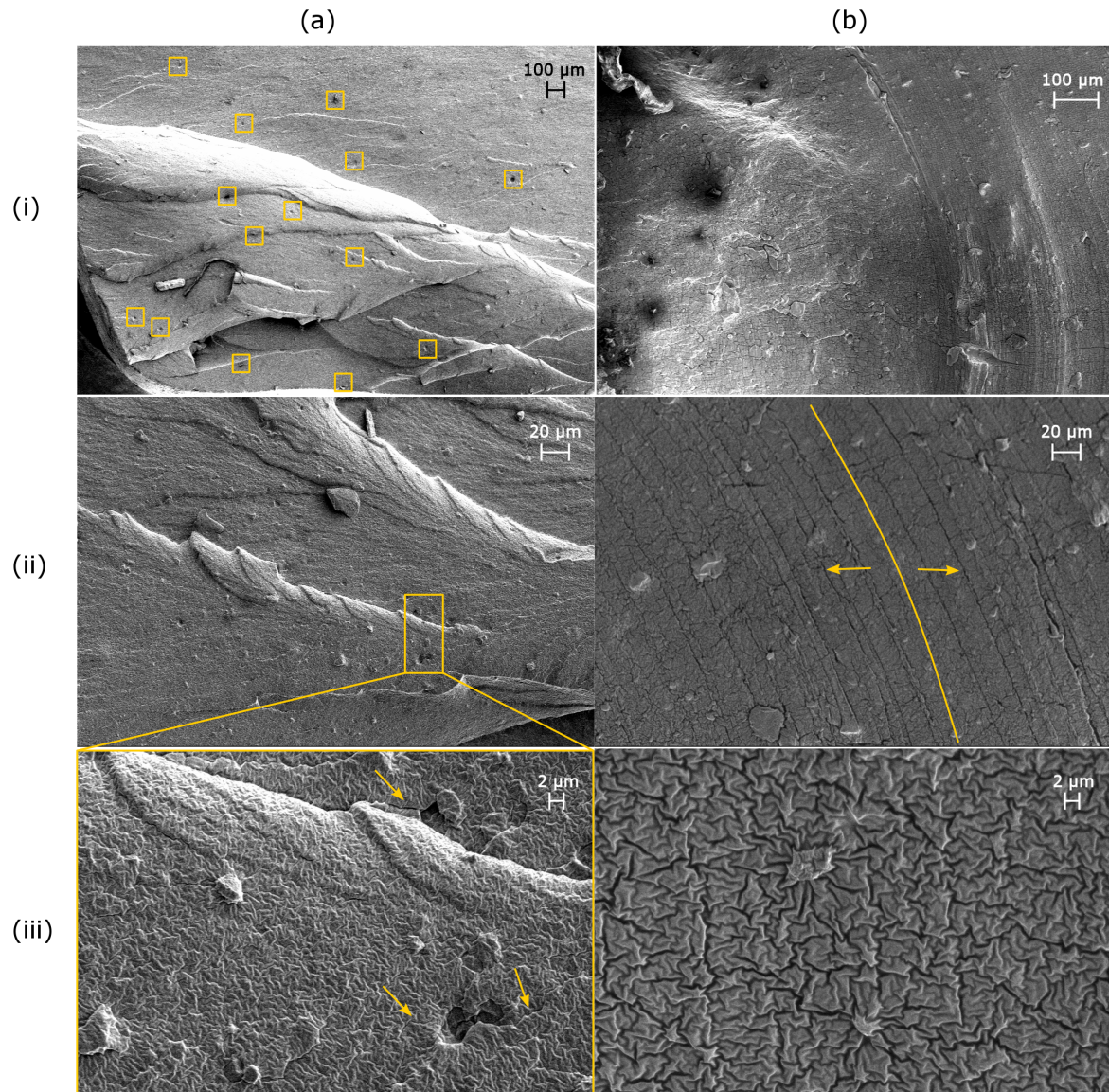


Figure 5.10: SEM of fracture surfaces of tensile specimens: (a) A, (b) 45A-55B. (a-i) Pores are visible on the fracture surface of the specimen A. The fracture surface is non-flat and irregular cracks are observed; (a-ii) and (a-iii) magnified view of fracture surface of specimen A. The failure cracks around pores are visible. (b-i) Non-porous flat fracture surface of specimen 45A-55B; (b-ii) The surface is covered with curved fracture lines parallel to the build direction. Shallower cracks are created perpendicular to the build direction. (b-iii) A magnified view of the fracture surface demonstrating the cracks propagation path.

factor of ten.

When considering the rheological properties of silicone ink for PPJ system, it is recommended that an ink with marginally higher loss modulus and low shear yield be used. This yields an almost fully dense structure with a mechanical performance similar to the bulk material.

## 5.4 Silicone-based Motion-Detector Sensor

The capability of the hybrid multi-nozzle AM method in fabrication of the heterogeneous bio-structures was investigated in the context of fabricating a wearable motion-detector sensor (Fig. 5.11). Motion-detector stretchable sensors can be attached to the skin or clothes in order to detect the motion (e.g. pulse). Thus, they can be used as health monitoring and rehabilitation assistance devices. The fabrication of stretchable sensors has been widely investigated using traditional methods such as casting which includes multiple time-consuming steps [149, 150]. Extrusion-based AM have been used to integrate dielectric and conductive inks into a 3D structure with a printing speed of 4 – 7.5  $mm/s$  as well [66, 67].

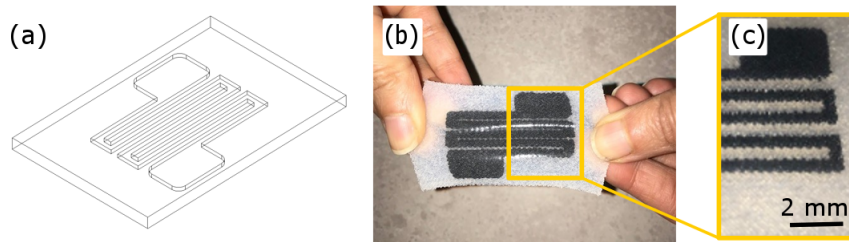


Figure 5.11: Flexible sensor printed using PPJ system: (a) CAD model of the sensor; (b) stretched sensor; (c) magnified view of the graphene-silicone pattern

We designed a sensor composed of a pattern of proprietary silicone-augmented graphene ink embedded within silicone. The CAD model of the sensor can be seen in Fig. 5.11(a). Silicone A has been used to improve the stretchability of graphene ink and 3D print the perimeter of each layer. The body of the silicone frame is made from the 45A-55B silicone ink with printing parameters introduced in Section 5.2.2. The printing parameters for the graphene-silicone ink are similar to those obtained in Section 4.3.2; however, the temperature of the ink was 25 °C. The stretchability and printing details are shown in

Fig. 5.11(b-c). The fabrication of this structure at 104  $mm/s$  from three different materials with various electrical and mechanical properties simultaneously at a high spatial resolution demonstrates the capability of the proposed hybrid AM method in production of heterogeneous structures at a higher efficiency compared to casting and with a higher speed compared to extrusion AM.

## 5.5 Summary

A comprehensive study of the effect of the rheology of different blends of short- and long-chain silicones on their porosity and mechanical performance was presented in this chapter. An ink with 45:55 wt.% of short-chain and long-chain silicone polymers showed a slightly higher  $G''$  than  $G'$  which resulted in the complete coalescence of jetted droplets without a significant loss of resolution. As a result, almost fully dense structures were produced. More importantly, it was established that the in-line porosity introduced to the part when using an ink with high yield stress leads to poor mechanical performance in terms of  $\epsilon_f$  and  $\sigma_f$  compared to the bulk material. The effect of AM on the mechanical performance of the part was improved by using the fluid-like ink. No significant difference in the average  $T_s$  and hardness of the parts based on the level of porosity was observed. The fabrication of a multi-material stretchable bio-sensor was showcased.



# Chapter 6

## Additive Manufacturing of Silicone via Powder-Bed Binder-Jetting Technique

### 6.1 Introduction

Research and commercial efforts in AM of silicone materials have focused on material extrusion, vat photopolymerization, and material jetting, with various degrees of success and technology-specific limitations. PBBJ, also known as 3D printing [151]; however, has not been used prior for the fabrication of silicone structures. This method relies on AM of parts by converting a CAD model into layer-by-layer images that are sequentially printed onto thin layers of powder. The printed liquid acts as a binder, consolidating the powder into a so-called green part once the binder is cured. The thin layers of powder are spread using a counter-rotating roller or a blade mechanism from a douser or a feed bed. The green part is porous and typically undergoes a series of post-processing protocols, which may involve de-powdering, thermal treatments, or matrix infiltration. The materials used for PBBJ AM are mainly ceramics, metals, or their composites [58]. In a recent review of AM materials, PBBJ methods had not been introduced as a manufacturing method for any kind of thermoset polymer including silicone [152].

The PBBJ AM technique has shown great compatibility with bio-materials for multiple applications [153–158]. There are three main advantages for PBBJ manufacturing approaches: (1) the ability to use a wide range of materials [58, 159–162]; (2) the degree of

freedom in manufacturing complex and scalable parts without the need for support structures [58, 163]; and (3) the high production speed with commercial systems performing often in the order of a few seconds per layer. In addition, PBBJ systems are capable of producing functionally graded structures [160, 164–167], with multi-material or multi-colour features [21, 51]. The versatility of this methodology is the driving factor in exploring PBBJ in manufacturing silicone structures. The most pressing drawbacks in manufacturing silicone parts via PBBJ is that the smallest feature size of conventional PBBJ equipment is limited by the size distribution of the powder [159, 162, 168, 169], the binder jetting resolution [159], and de-powdering constraints [159, 165, 169, 170]. For PBBJ, the minimum cavity feature size is typically considered at 500  $\mu m$  for de-powdering considerations, with a layer thickness in the order of 25 – 200  $\mu m$ . The powders used in PBBJ should comply with specific rheology and powder size distribution criteria to ensure uniform and defect-free layer properties in this layer thickness range. In addition, commercial PBBJ systems employ a single powder type during the build. The liquid binder is typically dispensed through a thermal or piezoelectric printhead, with a general limit in viscosity of less than 40 *mPa.s* to ensure proper material jetting, as well as fast infiltration through the powder substrate. The parts are typically exposed to a post-processing protocol for de-powdering, followed by heat-annealing, chemical setting, irradiation or infiltration, depending on the material system used. These post-processing steps typically result in part shrinkage or swelling and reduce the overall geometrical accuracy of the final product. The dimensional deviation can be considered in the CAD design stage by applying dimensional compensation factors.

To overcome some of the limitations in PBBJ, a new hybrid PBBJ and micro-deposition system was developed [118, 163] to target manufacturing of functionally-graded parts with multi-material and custom variable porous structures. This new system employs multiple powder feed mechanisms to dynamically select and deploy up to three different powder compositions to each layer, thermal and piezoelectric printhead delivery systems for jetting of various liquid binders, a variable counter-rotating roller mechanism to control powder compaction, a solid material dispenser for embedding discrete pore-generating sacrificial materials (porogens), and a micro-dispensing head for deposition of liquids throughout the porous matrix of the part at select locations.

In this chapter, the hybrid PBBJ AM system is used for the direct production of silicone structures. The system employs a material system composed of silicone powder as the base material in the substrate, a water-based liquid binder (Zb<sup>®</sup>60) that is jetted through a thermal printhead onto the powder substrate to develop the wetted layer outline of the parts, and a thermoset silicone liquid binder to impart the necessary structural integrity of each layer. The thermoset silicone binder is heat cured after printing a fixed number

of layers. Curing the thermoset silicone prevents any further permeation of subsequent silicone binder through previous layers, thus preserving the dimensions of the parts. The machine and material system is used to manufacture cylindrical shapes ( $5\text{ mm } D \times 3\text{ mm } H$ ) as part of a DoE.

## 6.2 Materials and Methods

### 6.2.1 Powder Silicone Materials

Two hybrid organopolysiloxane powders consisting of spherical silicone rubbers were used as received in this research. These powder samples offer all of the unique properties of a regular PDMS rubber including high thermal resistance, weatherability, and biocompatibility. The first powder (powder A) consists of silicone rubbers covered with a silicone resin (KMP-602, Shin-Etsu Chemical, Tokyo, Japan). The resin cover provides high resistance to impact by relaxing the stress, and improves the lubricity property. The rubber part is responsible for the resistance to extreme temperatures and abrasion. The second silicone powder (powder B) is made of pure spherical silicone rubbers without the resin coating (KMP-598, Shin-Etsu Chemical, Tokyo, Japan).

#### **Powder Size and Morphology Characterization**

The particle size distribution of the silicone powder samples and their sphericity and symmetry were verified using a dynamic image processing system (CamSizer XT, Retsch-Technology, Germany). The shadow of dispersed silicone particles illuminated by two LED sources were captured as they passed through a free-fall feed shaft in front of two cameras. The system measured parameters corresponding to the particle size distribution, sphericity, and symmetry in real time.

#### **Powder Dynamic Flowability, Shear Rate Sensitivity, and Bulk Properties Characterization**

A powder rheometer (FT4, Freeman Technology, UK) was used to determine the rheological properties of the silicone powders in response to multiple external conditions such as flow rate, aeration, and consolidation, its bulk properties such as compressibility and permeability, and its shear rate sensitivity. Before conducting each test, a uniform initial

state of stress was achieved at the conditioning stage by disturbing the particles gently through the helical movement of a blade.

### 6.2.2 Liquid Silicone Binder

The two-part thermal-curable liquid silicone rubber (JY-9010, Changzhou Juyou New Material Tech Co., China) was used with 100:1 main component to curing agent ratio. This silicone liquid is comprised of modified silica and Octamethylcyclotetrasiloxane which is a non-toxic organosilicon compound.

#### Viscosity Measurement

The viscosity of liquid silicone binder was measured at  $25 \pm 0.01$  °C using a digital cone and plate rheometer (RST-CPS-P, Brookfield Engineering, MA, USA) at  $200 - 2000$   $s^{-1}$  shear rate range by first increasing and then decreasing the shear rate value. The measurement data was collected at 15 points in 60 s for both ascendant and descendant curves.

#### Differential Scanning Calorimetry (DSC) Analysis

The analysis of the thermal behavior of liquid silicone binder was conducted using a DSC device (STA 449 F1, Netzsch, Germany) in the range of 25 - 160 °C with a heating rate of 5 °C/*min*. In order to measure the curing time, the isothermal test was carried out with a DSC device (MTDSC 2920, TA Instruments, DE, USA) at the equilibrium temperatures of 60 °C, 100 °C, and 110 °C. The curing behaviour was investigated in an inert atmosphere (Nitrogen), and each test was replicated three times.

### 6.2.3 Liquid Water-based Binder

An aqueous liquid binder (Zb<sup>®</sup>60, 3D systems, SC, USA) was inkjet printed onto the powder-bed to form the wetted precursor image of each layer. The Zb<sup>®</sup>60 includes 85 – 95% v/v of distilled water and 5 – 15% v/v of humectant and a proprietary polymer as a binding agent.

## 6.2.4 Experimental Setup

As the proof-of-concept, filled cylindrical structures ( $5\text{ mm } D \times 3\text{ mm } H$ ) were printed using the hybrid PBBJ AM system. The process of manufacturing the silicone structures starts with designing cylindrical CAD models and slicing the digital data into successive layers and execution steps for each layer. The hybrid PBBJ AM of a 3D object with both the structural powder material and the binder made from silicone has four stages as illustrated in Fig. 6.1 and described in detail as follows:

(1) A roller with a linear velocity of  $20\text{ mm/s}$  and rotational velocity of  $100\text{ rpm}$  spreads the silicone powder from a feeding bed (also called supply powder bed) to a build bed. This results in a flat layer of silicone powder with a fixed layer thickness ( $LT$ ) (Fig. 6.1(a)).

(2) The thermal inkjet printhead jets the water-based Zb<sup>®</sup>60 binder onto the powder surface based on the image corresponding to the layer being manufactured. The Zb<sup>®</sup>60 liquid binder acts as a glue spread onto the silicone powder substrate to generate the structure by binding the silicone particles according to the geometry of the slice and to wet the substrate in preparation for the liquid silicone binder. Steps (1) and (2) are repeated a fixed number of times called dispensing frequency ( $Fr$ ) before the deposition of liquid silicone is carried out (Fig. 6.1(b)) in step (3).

(3) The nozzle with inner diameter  $100\text{ }\mu\text{m}$  is located above the center of the structure with  $2\text{ mm}$  off-set. By applying  $100\text{ kPa}$  air pressure through a micro-syringe extrusion system (Optimeter, Nordson EFD, RI, USA), a droplet of silicone is dispensed to infiltrate the binder-wetted porous media substrate (Fig. 6.1(c)).

(4) The structure is then exposed to a temperature of  $100 - 120\text{ }^\circ\text{C}$  supplied via a thermal lamp for  $1\text{ min}$  to initiate and complete the polymerization of the two-part heat-curable silicone binder solution (Fig. 6.1(d)).

The four steps are repeated until the cylindrical structure is completed in a layer-by-layer fashion. The parts are left in the build bed for  $2 - 3$  hours. Finally, they are removed from the hybrid PBBJ system and air-heated at  $85\text{ }^\circ\text{C}$  to ensure the full curing.

## 6.2.5 Imaging

The liquid silicone binder droplet size at multiple pressure values were measured using a digital camera (AM7915MZT, Dino Lite, Taiwan) at  $21\times$  magnification. Images of the silicone binder droplets pendant from the needle tip were captured at  $1\text{ s}$  intervals between the moment the pressure was applied, up to the separation of the droplet. The

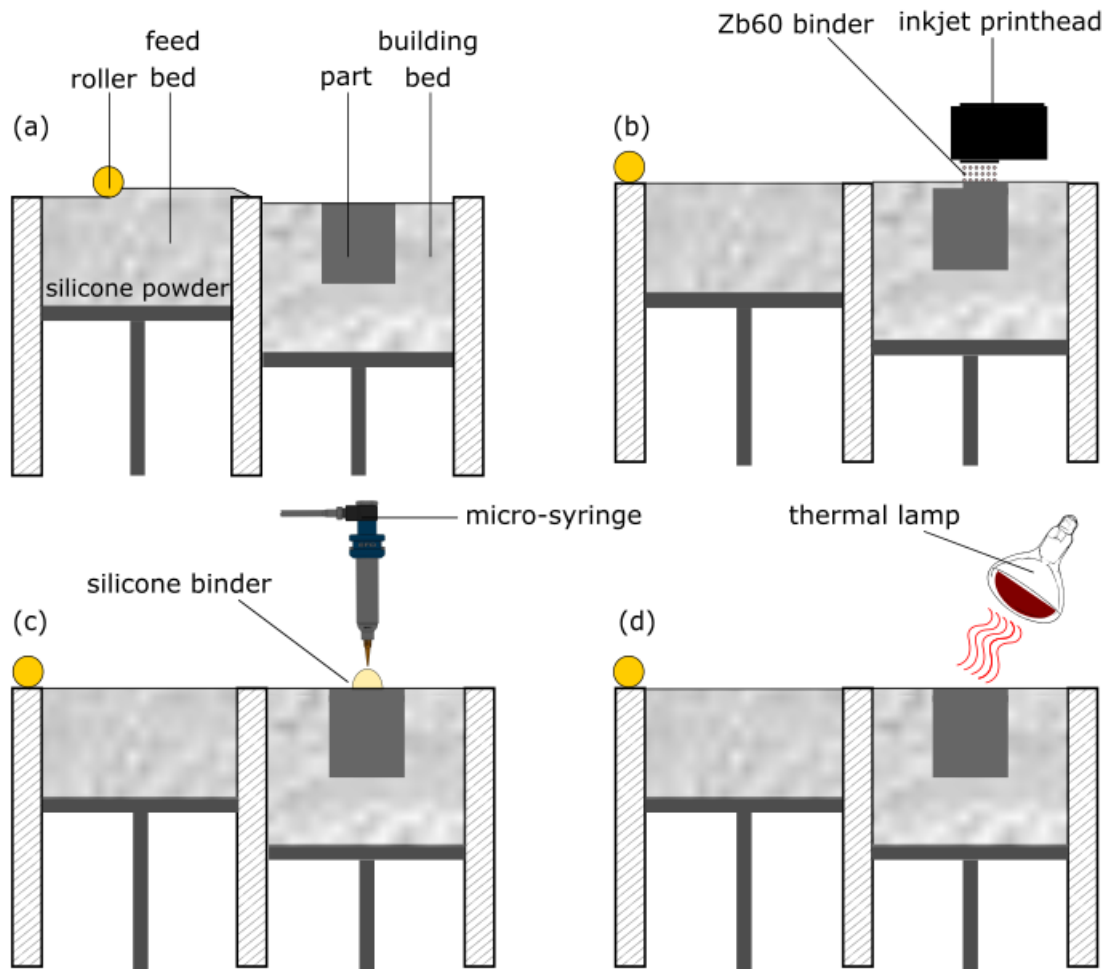


Figure 6.1: The schematic of hybrid PBBJ AM system. (a) spreading the silicone powder from feed bed onto the build bed; (b) wetting each layer by inkjet printing the water-based binder; (c) dispensing a droplet of silicone binder to fill up the silicone porous media using a pneumatic extrusion system; (d) partial curing of the silicone binder using a thermal lamp at 100 °C temperature.

maximum diameter of droplet before separation was measured using the image processing software DinoCapture (Dino Lite, Taiwan). The powder silicone particle morphology was investigated using SEM (Ultra Plus, Carl Zeiss AG, Germany) at accelerating voltages of 10 *kV* and 3 *kV* for powder A and powder B, respectively.

### 6.2.6 Part 3D Profilometry

Profiles of the additively manufactured samples were obtained using a laser confocal microscope (VK-X250, Keyence, Japan) at 100× magnification. The height and the diameter of the circles fitted to the cross-section of the cylindrical samples were measured using the software MultiFileAnalyzer (Keyence, Japan).

### 6.2.7 Part Computed Tomography (CT) Scan

The tomography of the entire printed structure was captured using a nano-CT scanner (Xradia 520 Versa, Carl Zeiss AG, Germany). The scanning parameters are provided in Table 6.1.

Table 6.1: CT scanning parameters

Parameters	Voxel size ( $\mu m$ )		
	4.05	1.4	0.727
Source Power ( <i>W</i> )	3	3	3
X-ray Energy ( <i>kV</i> )	40	40	40
Filter	LE2	LE1	LE1
X-ray Optic Lens	4×	20×	20×
Exposure Time ( <i>s</i> )	1	1	10
Number of Projections	801	801	1601
Binning Level	4	4	2

In order to calculate the solid phase density for 4.05  $\mu m$  resolution CT scan result, the original greyscale image was filtered with both a small kernel Gaussian filter, then with a larger kernel bilateral filter (2 voxel radius) which is an edge preserving Gaussian filter. A greyscale threshold was then determined manually to segment the dense particle phase

from the void and silicone binder phases. The exterior regions were masked from the part, to not be included in the porosity calculations. The masking was performed by eroding the surface down by a localized porosity threshold until the mask closely tracked the part surface. Then, each voxel within the masked region was given a distance value from the central axis, and another distance value from the base of the domain. These distance values were used to group voxels into radial and vertical position bins for the respective porosity distributions.

For separating three different phases of silicone powder, silicone binder, and air voids in the nano-scale CT scan results, the original greyscale image was first adjusted with a normalizing gradient to correct for artifacts associated with the sample exceeding the scanning field of view. A bilateral filter with a spatial radius of 2 voxel lengths was then applied to remove noise. Finally, the three phases were separated from each other in a combination of manual greyscale threshold selection and morphological image processing steps, including opening, closing, and three dimensional median filters. The image processing routine had to be carefully performed due to the large overlap in the histograms of the porous and polymer phases.

### 6.2.8 Hardness

A Shore 00 handheld durometer (Shore S1, Shore Instruments-Instron, MA, USA) was used to measure the hardness of 3D printed samples as well as samples of the silicone binder cured in a mold for comparison (cast control samples). The rigid ball was located on the center of the cylindrical samples, and the hardness value was captured after 1 s dwell time. Each reading was repeated three times for two replicates of samples manufactured under similar printing conditions.

### 6.2.9 Statistical Analysis

In order to optimize the 3D printing parameters, a multi-level experimental design was formed with  $LT$  and  $Fr$  as the control factors. Table 6.2 shows the levels of each factor. The height ( $H$ ), inner diameter ( $ID$ ), and the diameter difference ( $DD$ ) between the inner and outer circles fitted to the cross section of parts are the responses. The outer diameter ( $OD$ ) is the diameter of the largest circle fitted to the cross-section of the cylindrical parts so that it covers the entire cross-section including the irregular edges. The diameter of the circle that only covers the central parts of the cross-section and not the irregularity caused



by the lateral infiltration of silicone binder is  $ID$ . The difference between  $ID$  and  $OD$  is depicted in Fig. 6.2 and is the method used to calculate  $DD$ .

Table 6.2: Experimental design factor levels for PBBJ process.

Factor	Low Level (-1)	Center Level (0)	High Level (+1)
$LT$ ( $\mu m$ )	50	-	100
$Fr$	1 drop per 100 $\mu m$	1 drop per 200 $\mu m$	1 drop per 300 $\mu m$

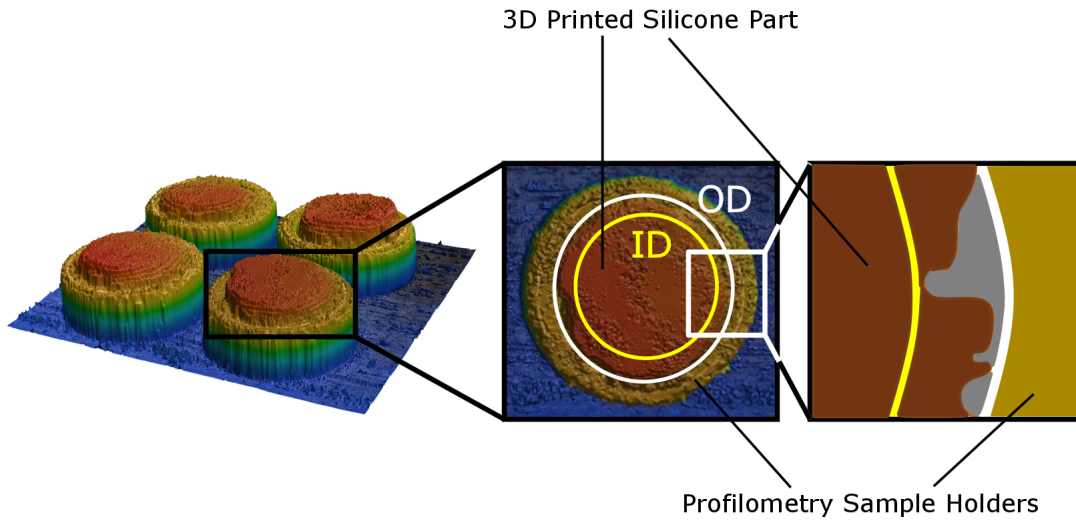


Figure 6.2: Sample of the 3D profile of the four replications of a part manufactured with similar printing parameters. The difference between the two circles fitted to the cross-section of each sample is shown in the magnified top view images.

The path to the optimized region for each parameter was found using RSM. Finally, all three responses were optimized simultaneously using desirability function technique (utility transfer function). The levels of significant factors were selected so that  $DD$  was minimized, and  $H$  and  $ID$  approached the target values of 3  $mm$  and 5  $mm$ , respectively.

A one-way Tukey ANOVA at 95% confidence level was employed to compare the hardness of parts manufactured under different 3D printing conditions.

## 6.3 Results and Discussion

### 6.3.1 Silicone Binder Viscosity and Droplet Size in Dispensing

Figure 6.3(a) shows the viscosity of silicone binder at the shear rate range of 200 - 2000  $s^{-1}$ . The viscosity vs. shear rate plot shows a Newtonian behavior with the constant viscosity of 78  $mPa.s$  at room temperature. The ascendant and descendant plots coincide as well showing the independency of the rheological behavior of the fluid on the shearing history. For a fluid with the shown viscous behavior, the syringe dispensing was tested under various pressures. It was found that varying the dispensing air back-pressure did not affect the volume of the dispensed droplet, however, it changed the separation time (see Table 6.3). With a pressure of approximately 100  $kPa$ , the droplet separated 8  $s$  after the pressure was applied providing enough time for the control of dispensing mechanism. Figure 6.3(b) shows the image of a silicone droplet captured before its separation from the needle tip with the inner diameter of 100  $\mu m$ . The diameter of the shown droplet is 1.54  $mm$ .

Table 6.3: Dispensing duration for one droplet at different air pressure values.

$P$ ( $kPa$ )	Dispensing Time ( $s$ )
30	15
50	10
100	8

The constant diameter of silicone binder droplet before separation from the needle tip under different pressure values allows the adjustment of the dispensing time by modifying the air pressure (Fig. 6.3a). The viscosity of silicone binder (78  $mPa.s$ ) is not very high so that it prevents the creation and separation of droplets, at the same time, it is not very low to cause fluid dripping (Fig. 6.3b). However, once dispensed on the dry powder bed, the infiltration process takes 10 - 20  $s$ . Moreover, this long infiltration causes the disturbance of silicone powder particle distribution in the layer. In order to minimize this issue, the powder surface was pre-wetted with the water-based binder. The utilization of water-based binder helps the proposed hybrid AM technique by: (1) binding the silicone particles temporarily together; (2) speeding up the process of silicone binder infiltration by enhancing the wetting properties of silicone particles. The aqueous binder is used to wet the powder substrate in order to accelerate the progression of the silicone liquid droplet from primary to secondary liquid spread [171]. Primary spread occurs when the sessile

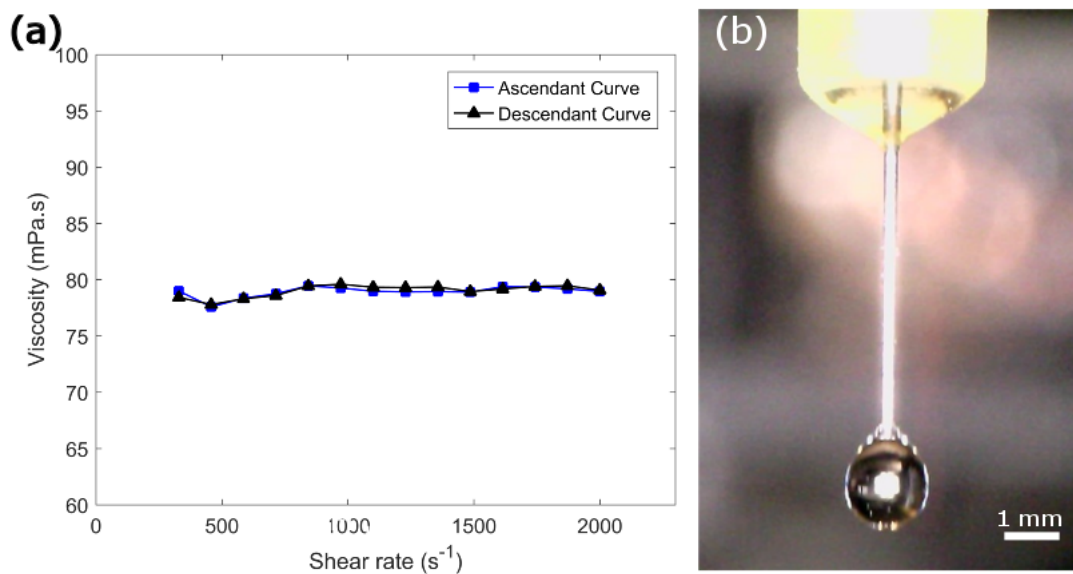


Figure 6.3: (a) The viscosity of silicone binder showing a Newtonian behavior at the shear rate range of 200 - 2000  $s^{-1}$ ; (b) The silicone binder droplet before separation from the needle with a maximum diameter of 1.54  $mm$ .

droplet volume (volume above the powder) is not zero, where the secondary spread occurs within the porous substrate only. In the absence of the aqueous binder, the primary spread could take more than 10  $s$ , while in the presence of the aqueous binder, the primary spread is reduced to approximately 1  $s$ . The infiltration process is schematically illustrated in Fig. 6.4.

### 6.3.2 Thermal Analysis of Silicone Binder

The exothermic silicone cross-linking process for the samples of silicone binder at various hold temperatures are depicted in Fig. 6.5(a). For all three replications of the experiment, the positive peak appears in the range of 75 - 90  $^{\circ}C$ . Thus, the maximum temperature of three tests (90  $^{\circ}C$ ) was selected for further investigation. The isothermal DSC results (Fig. 6.5(b)) at 90  $^{\circ}C$  show that the curing process is accelerated after 3 - 4  $min$  at equilibrium and takes approximately 2  $min$  to reach the maximum curing rate. Similar experiment conducted at 100  $^{\circ}C$  (Fig. 6.5(c)) shows that the curing happens right after the temperature equilibrium is reached. Increasing the temperature even further results in curing of the binder before reaching the target temperature (Fig. 6.5(d)).

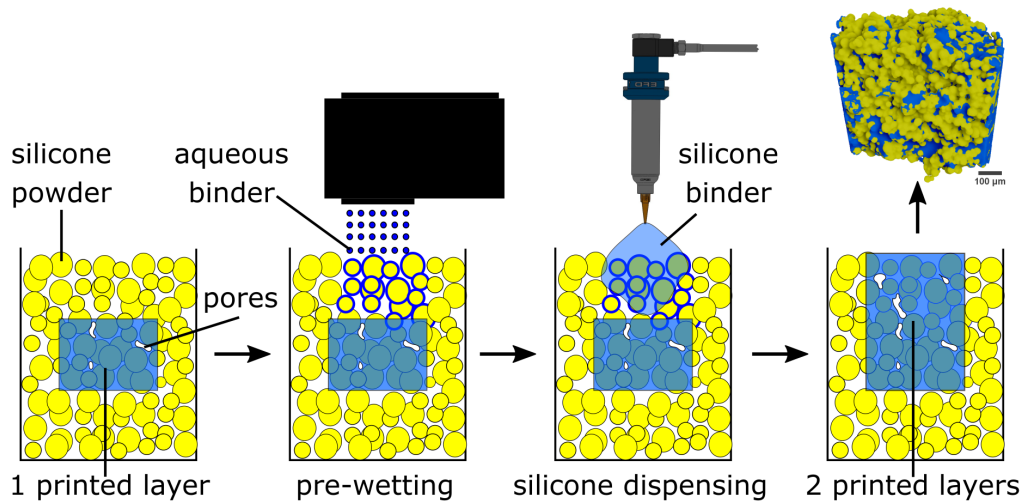


Figure 6.4: The infiltration of silicone binder in pre-wetted substrate.

Investigating the thermal behavior of the curing process of the liquid silicone binder is crucial in designing a curing mechanism that assures the geometrical accuracy of the parts is maintained by crosslinking the silicone binder after dispensing as fast as possible to prevent its penetration into the surrounding powder environment. The entire curing process for silicone binder at  $90\text{ }^{\circ}\text{C}$  takes approximately  $6\text{ min}$  which can prolong the manufacturing process. As a result, the silicone binder was exposed to a curing temperature between  $100 - 120\text{ }^{\circ}\text{C}$  for  $1\text{ min}$  using a thermal lamp. The changes in the powder surface temperature measured using a thermocouple (Fig. E.3) shows that the powder bed temperature reaches  $100\text{ }^{\circ}\text{C}$  after  $50\text{ s}$  and  $110\text{ }^{\circ}\text{C}$  after  $60\text{ s}$ . The isothermal plots at these two temperatures (Fig. 6.5(c-d)) demonstrate that curing happens immediately after reaching  $100\text{ }^{\circ}\text{C}$ , and a full cure takes less than  $1\text{ min}$ . As a result, the employed curing policy of  $1\text{ min}$  exposure to heat prevents both the unnecessary increase in the total manufacturing time and permeation of silicone binder outside the region of interest.

When considering the liquid silicone material and the rheological and thermal behavior during the curing, it is recommended that for manufacturing of such silicone structures, the following considerations should be met: (1) increasing the infiltration rate of liquid silicone binder by enhancing the wettability of particles through pre-wetting of the powder-bed; (2) preventing the permeation of silicone binder to the areas that are not supposed to be a part of final structure through instant curing; (3) tailoring the rheological properties of silicone binder (recommended viscosity range:  $70 - 90\text{ mPa}\cdot\text{s}$ ) so that it is not too viscous for common direct write AM techniques, yet viscous enough so that it does not permeate too

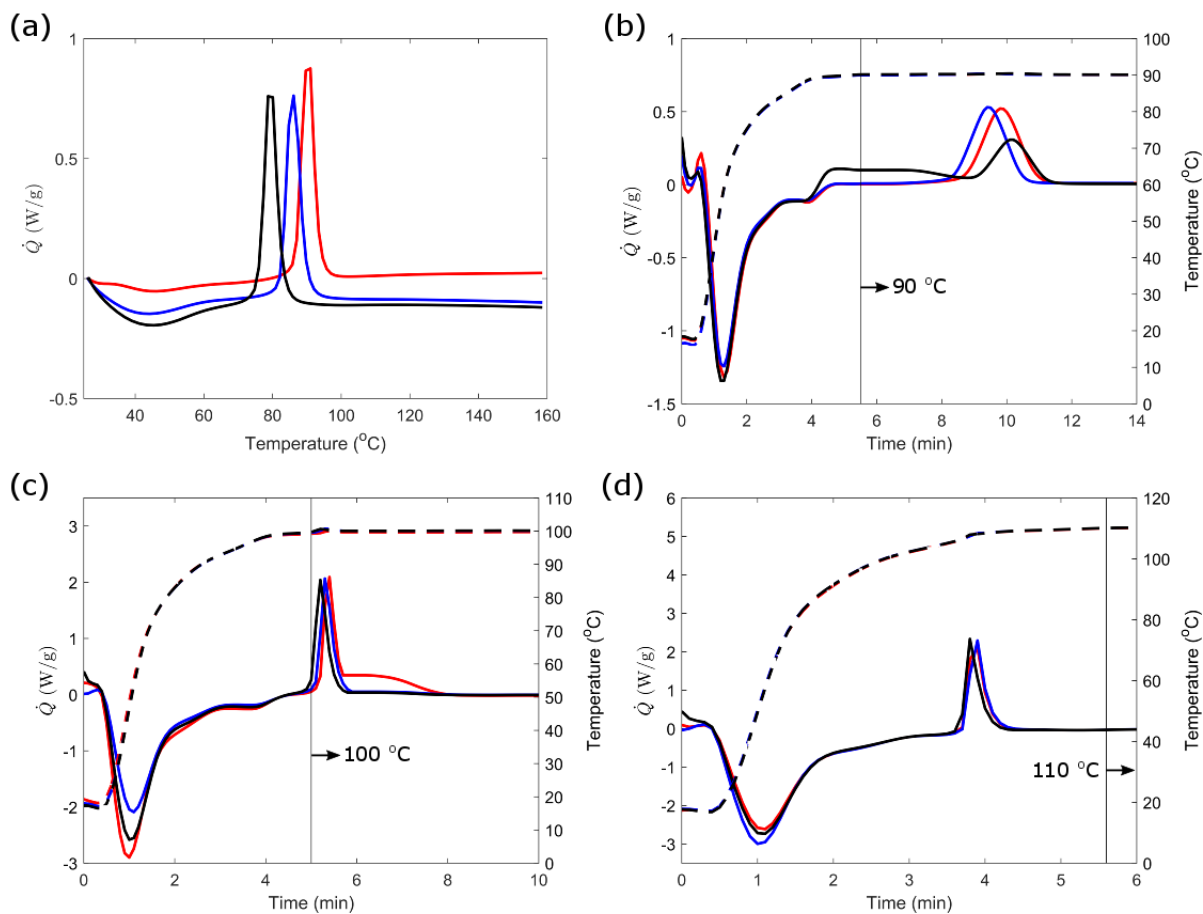


Figure 6.5: Thermal analysis results for silicone binder: (a) non-isothermal curves (heat flux vs. temperature); (b) isothermal curves at 90 °C; (c) isothermal curves at 100 °C; (d) isothermal curves at 110 °C; (a-d)  $n = 3$ , solid lines and dashed line corresponds to heat flux and temperature, respectively.

fast before crosslinking; and (4) increasing the resolution and accuracy of the technique by replacing the extrusion system with a DOD AM printhead in order to reduce the diameter of silicone binder droplets from 1.54  $mm$  to less than 300  $\mu m$

### 6.3.3 Silicone Powder Size, Morphology, and Rheology

The deep understanding of the powder rheology and properties is important in powder-bed AM processes in order to obtain a consistent and uniformly spread layer and minimize the printing variability. Thus, investigating the rheological properties of a silicone powder with successful flowability for AM would be beneficial for future development of silicone powder customized for powder-bed systems.

The SEM images of powder A (Fig. 6.6(a-c)) and powder B (Fig. 6.6(d-f)) show their effective spherical morphology. The particles of powder A appear segregated, while the particles of powder B have cohered together and produced large agglomeration of clusters surrounded by finer satellite particles. The powder particles in both powder A and B appear spherical in nature. Powder A had a fine coating in the as-purchased state, and this can be seen as surface flakes in Fig. 6.6(c). Powder B did not have any coating in the as-purchased state, and appears smooth in nature, as seen in Fig. 6.6(f).

The particle size distribution of powder A can be seen in Fig. 6.7 with an average particle size of 30  $\mu m$ . The shape analysis test for powder A showed a high level of sphericity (average value of 0.842 for four test replications where 1 represents the perfect circle). The symmetry index for the powder A was 0.963 as well (with 1 representing the full symmetry). Studying the particle size distribution and quantifying the sphericity of powder B was not possible due to its high degree of agglomeration and cohesiveness. However, the manufacturer reports particle size distribution of 2 - 30  $\mu m$  with an average particle size of 13  $\mu m$  for this powder.

The flow properties of silicone powders were measured based on their resistance to the movement of a blade which creates a flow pattern by its rotational and vertical movement. Guidelines provided in [172–174] have been used to interpret the powder rheology results. The energy required to establish this flow pattern for both powders is shown in Fig. 6.8(a). The first 8 repeated tests have been conducted at the same blade velocity, followed by the gradual decrease in the velocity in tests 9 - 12. At the fixed velocity region, the energy required for the flow is 15  $mJ$  higher for the powder B. The same pattern with lower difference in the value of energy can be observed for the lower velocities. The lower energy for the powder A shows that it is a non-cohesive powder with better flow properties. This

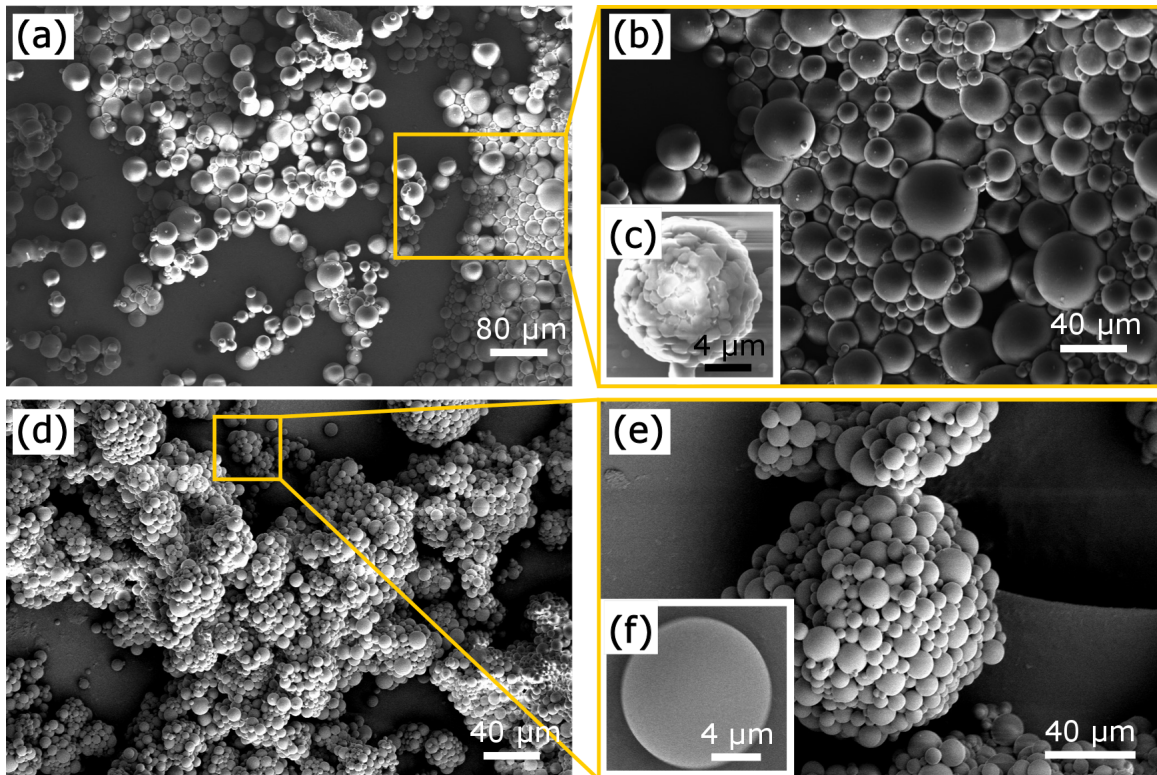


Figure 6.6: (a-c) SEM images for powder A shows spherical and symmetrical particles; (d-f) SEM images for powder B shows the creation of large clusters of particles due to cohesiveness of the powder.

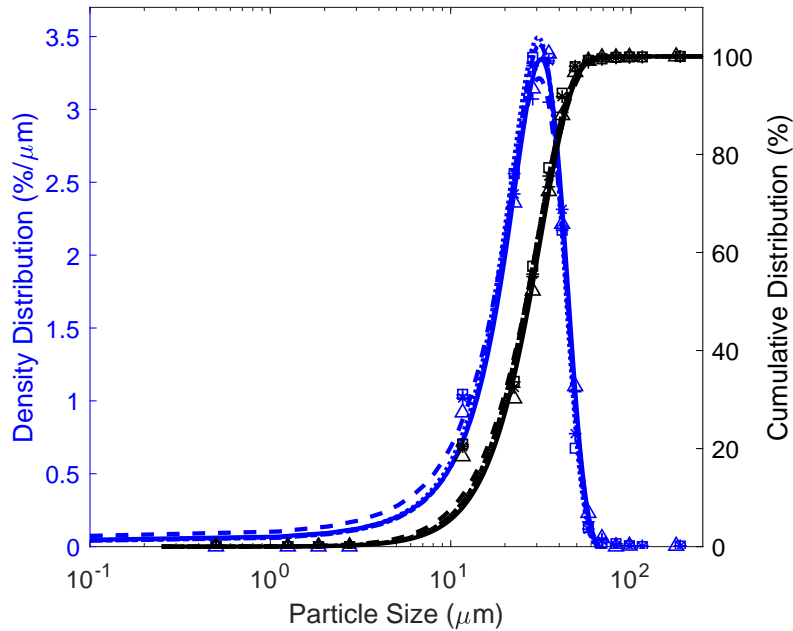


Figure 6.7: Particle size distribution for powder A ( $n = 3$ ).

conclusion will be reaffirmed through other permeation, aeration, compression, and shear tests.

A similar test was conducted for both powder types while they were conditioned with the air flow with varying velocities. The aeration test for powder A (Fig. 6.8(b)) and powder B (Fig. 6.8(c)) demonstrate drastically different behaviors. The energy required for the flow of blade has been reduced to almost zero for powder A even at a low air velocity of  $1 \text{ mm/s}$  and remained near zero for the higher velocities ( $2 - 5 \text{ mm/s}$ ) as well. As for the powder B, the zero plateau was never achieved even with an air velocity as high as  $150 \text{ mm/s}$ . The zero energy indicates a virtually fluidized powder bed that makes the rotation of the blade through the powder bulk easier. The sharp decrease in the amount of energy for the hybrid powder and reaching the fluidization state confirms the non-cohesive behavior of powder A.

The compressibility and permeability test results are shown in Fig. 6.8(d-e). In these two tests a sample of pre-conditioned powder is compressed under certain normal stress values. The compressibility test measures the change in the powder volume when exposed to normal stress, and the permeation quantifies the ability of the bulk powder in passing a fluid through its porous structure by measuring the air pressure needed in order to maintain



a constant air flow as the normal stress is increased. Figure 6.8(d) shows that powder B is 4 - 6 times more compressible than powder A at any given normal stress. Powders with lower compressibility have a more efficient packing of particles, and are less cohesive. On the other hand, the pressure drop for powder A is approximately 10 *mBar* more than that of the powder B which makes the hybrid powder A highly permeable to air.

The shear strength was measured at 7, 6, 5, 4, and 3 *kPa* normal stresses after pre-shearing the powder at 9 *kPa*. The higher value of shear stress at any given normal stress indicates a more difficult flow due to cohesiveness, irregular shape of particles, void-free structure etc. Powder A demonstrates lower shear yield loci for any normal stress compared to powder B making it less resistant to the flow during the recoating process.

Comparison of the shape and size of powders A and B (Fig. 6.6(a-f)) suggests that powder A could be a viable candidate for powder-bed AM. Powders A and B both have a narrow particle size distribution range and spherical shape which are both favorable powder characteristics for AM. However, the smaller particle size of powder B (almost half the size of powder A) increases the free surface area and consequently the friction and static forces between the powder particles. This will result in the inefficient packing properties and difficulty in powder spreading and layer recoating process [175]. The lower flowability under static and aerated conditions, lower permeability, and higher compressibility of powder B confirm the conclusions inferred from particle shape and size analyses. A high degree of agglomeration was observed in the SEM image of powder B (Fig. 6.6(d)). The reason behind the low flowability and permeability of silicone B could be the formation of tightly packed structures as finer separated silicone particles interlock through static friction to form powder agglomerations. The high compressibility is an indicator of the cohesiveness of powder B which justifies the agglomeration. An important characteristic of the powder feedstock used in AM is their shear stress as the particles slide relative to each other when transferred from the feeding compartment to the building compartment by the roller, and the initiation of the flow is dependent on overcoming the resistance to the flow. The lower shear stress for the powder A shows its better flow properties and less cohesive behavior. The lubricating effect derived from the resin coated hybrid powder A also contributes to its overcoming of the inter-particle shear forces.

When considering the powder silicone material and the rheological and morphology of the powders, it is recommended that for manufacturing of such silicone structures, the following considerations should be met: (1) spherical and symmetric powder particles; (2) average particle size between 30 - 40  $\mu m$  with a reasonably wide distribution range ( $\sim \pm 30 \mu m$ ) to provide an efficient particle packing in the powder-bed; (3) non-cohesive powder demonstrating limited compressibility (10 - 20 %) and high permeability to air; (4) powder with low shear yield (less than 2.5 *kPa* for normal pressure between 1 - 7 *kPa*) to decrease

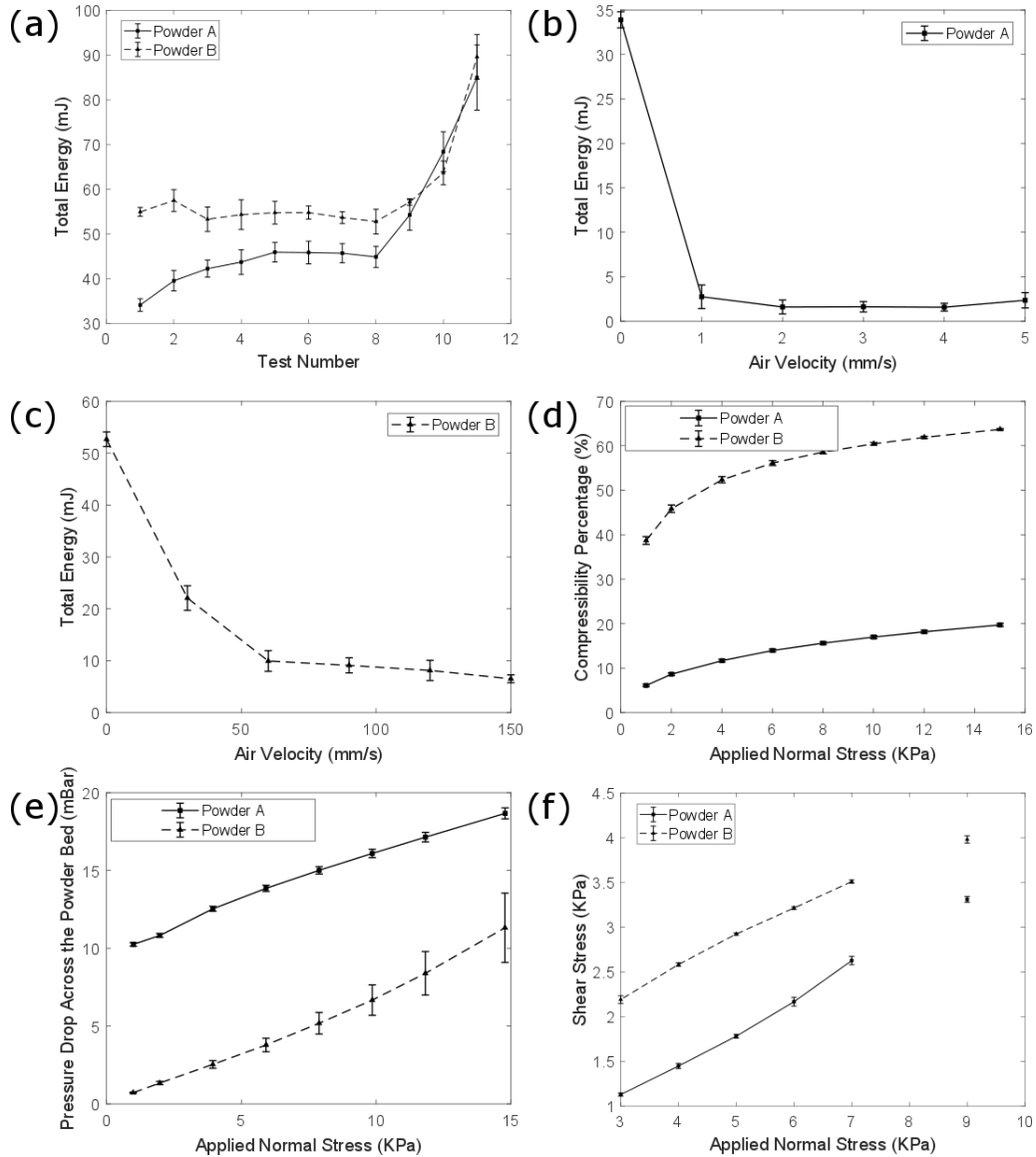


Figure 6.8: Silicone powder characterization results; (a) flow test for powders A and B; (b) aeration test for powder A; (c) aeration test for powder B; (d) compressibility results for powders A and B; (e) permeation results for powders A and B; (f) shearing test for powders A and B; (a-f)  $n = 3$ .

the resistance to flow during the recoating.

### 6.3.4 Part Shape Fidelity Characterization

The significance of  $LT$  and  $Fr$  on the dimensional accuracy of the 3D printed parts was evaluated using a multi-level experimental design. The details of design and the measured values for height and width can be found in Table D.1. The samples were manufactured in a completely randomized order according to the designed experiment. The responses were assumed to be independent.

The ANOVA results are shown in Tables D.2, D.3, and D.4 for  $H$ ,  $ID$ , and  $DD$ , respectively. The results show that for  $H$  and  $ID$ ,  $Fr$  has a significant effect at 95% confidence level. However, none of the parameters are significant at 95% confidence level for the  $DD$ . The response surface plots (Fig. 6.9([a-i]-[c-i])) demonstrate the path to the optimization for each of the responses. Marginal mean plots (Fig. 6.9([a-ii]-[c-ii])) confirm the ANOVA conclusions. The marginal mean plots for  $H$  and  $ID$  both show that the higher limit of  $LT$  ( $100\ \mu m$ ) yields dimensional values closer to the target. However,  $Fr$  of 1 drop per  $200\ \mu m$  and 1 drop per  $300\ \mu m$  produce the best results for  $H$  and  $ID$ , respectively. Thus, the desirability function technique was adopted to optimize the input parameters simultaneously (Table D.5). The simultaneous optimization of three responses showed that by setting  $LT$  and  $Fr$  both at their high level ( $100\ \mu m$  and 1 drop per  $300\ \mu m$ , respectively), the optimum results will be achieved. At this condition, the average values of  $ID$ ,  $H$ , and  $DD$  will be  $5.45\ mm$ ,  $3.77\ mm$ , and  $1.6\ mm$ , respectively.

The investigation of part shape fidelity through the experimental design showed that at the optimum condition,  $H$  and  $ID$  of the sample parts are  $0.45\ mm$  and  $0.75\ mm$  larger than their target values, respectively. Moreover, the optimized  $DD$  value of  $1.7\ mm$  will reduce the geometrical accuracy of the shape. The results show that further work in this area must be done in order to obtain higher geometrical accuracy. To this end, the effect of surfactants on the surface properties and the size of silicone binder droplet and the effect of additives to the powder system for controlling its fluid permeability properties will be investigated in the future work.

### 6.3.5 Part Internal Features

The CT scanning results at  $4.05\ \mu m$  voxel resolution for the entire AM-made silicone structure manufactured using  $100\ \mu m$   $LT$  and 1 droplet per 3 layers  $Fr$ . is shown in Fig. 6.10(a). A higher concentration of silicone powder is visible in the center of the

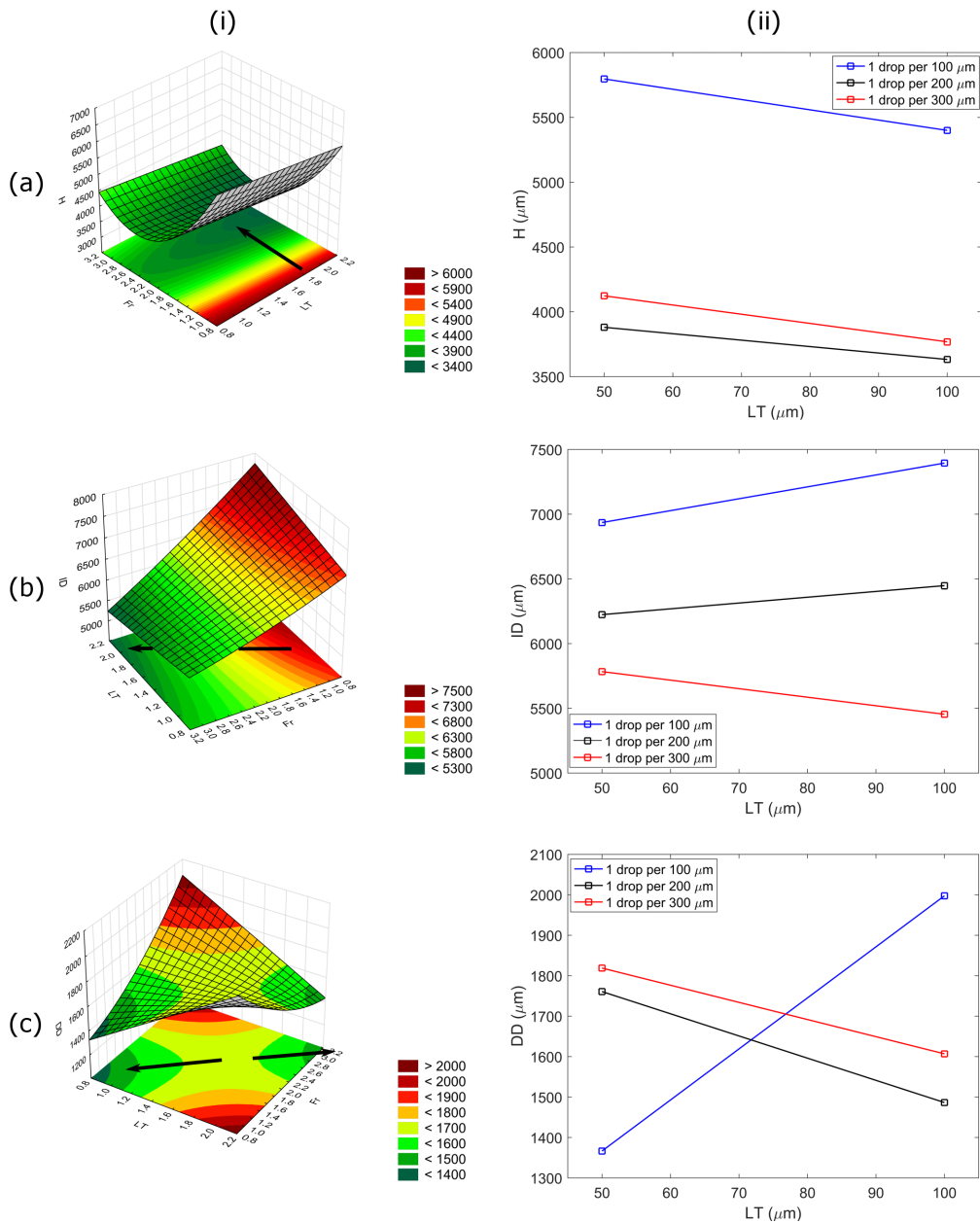


Figure 6.9: The optimization results for separate analysis of responses; (a-i) the contour plot and optimization path for  $H$ ; (a-ii) the plot of marginal means for  $H$ ; (b-i) the contour plot and optimization path for  $ID$ ; (a-ii) the plot of marginal means for  $ID$ ; (c-i) the contour plot and optimization path for  $DD$ ; (c-ii) the plot of marginal means for  $DD$ . The arrows show the path to the optimized regions

structure as opposed to its shell. The quantified vertical and radial particle phase fraction for each slice are plotted in Fig. 6.11(a) and Fig. 6.11(b), respectively, demonstrate that the particle phase fraction is dropped from 75% at core to 55% at the edge. This change in the density of powder however is less variant along the height of the sample (55% – 65%). A magnified view of two regions of interest inside the structure at higher resolution helps in distinguishing between the particle and cured binder phases. Figure 6.10(b) shows a zone inside the structure with visibly higher concentration of silicone powder particles. Comparing these images with the CT scan results of a central section of the structure (Fig. 6.10(c)) reveals that the difference in concentration of particles is much higher in radial direction. The overall solid particle phase density for this cylindrical structure is 59.8%. The remaining 40.2% of the entire volume is comprised of silicone binder and pores.

In order to separate the silicone binder and air pores, image processing was conducted on the CT scanning data obtained for a small section of the AM-made part at nano-resolution (727 nm voxel resolution). Figure 6.12(a) shows the overall view of the scanned samples. Silicone binder and pores are isolated in Fig. 6.12(b) and Fig. 6.12(c), respectively. Based on the quantification results of image processing, the sample is made of 70.5% silicone powder, 21.3% silicone binder, and 8.2% pore. Five of the largest pores are shown in different colors in Fig. 6.12(d).

Based on the CT scan data, the silicone part fabricated at optimum printing condition using the hybrid method consists of approximately 8.2% air voids (Fig. 6.12) which are distributed unevenly throughout the structure (Fig. 6.11). Moreover, despite the presence of regional pore interconnectivity at multiple locations in the AM-made sample, the pores of larger volume are actually isolated and trapped inside the part (Fig. 6.12(d)). As a result, a new dispensing method using piezo-dispensing should be investigated to determine the feasibility of dispensing smaller liquid silicone droplet volumes throughout the layer of interest to increase shape fidelity and control over the internal porosity. Printing droplets with volumes in the order of pico- or micro-liter provides higher control and flexibility over the total silicone binder volume infiltrated in each layer, and makes it possible to fill a certain percentage of the air voids. In such drop-on-demand systems, adjusting the actuation parameters in combination with translational velocity of the printhead can change the volume of droplets as well as the deposition frequency. Thus, multiple patterns from continuous lines to separate droplets can be laid down on the powder substrate which in turn make controlling the overall density of the structure possible. This provides an apparatus for fabrication of silicone structures with variable density profile from fully dense to highly porous with interconnected channels.

The CT analysis results illustrated in Fig. 6.11 showed a variability in silicone powder volume fraction radially, with more particles clustering in the center compared to the pe-

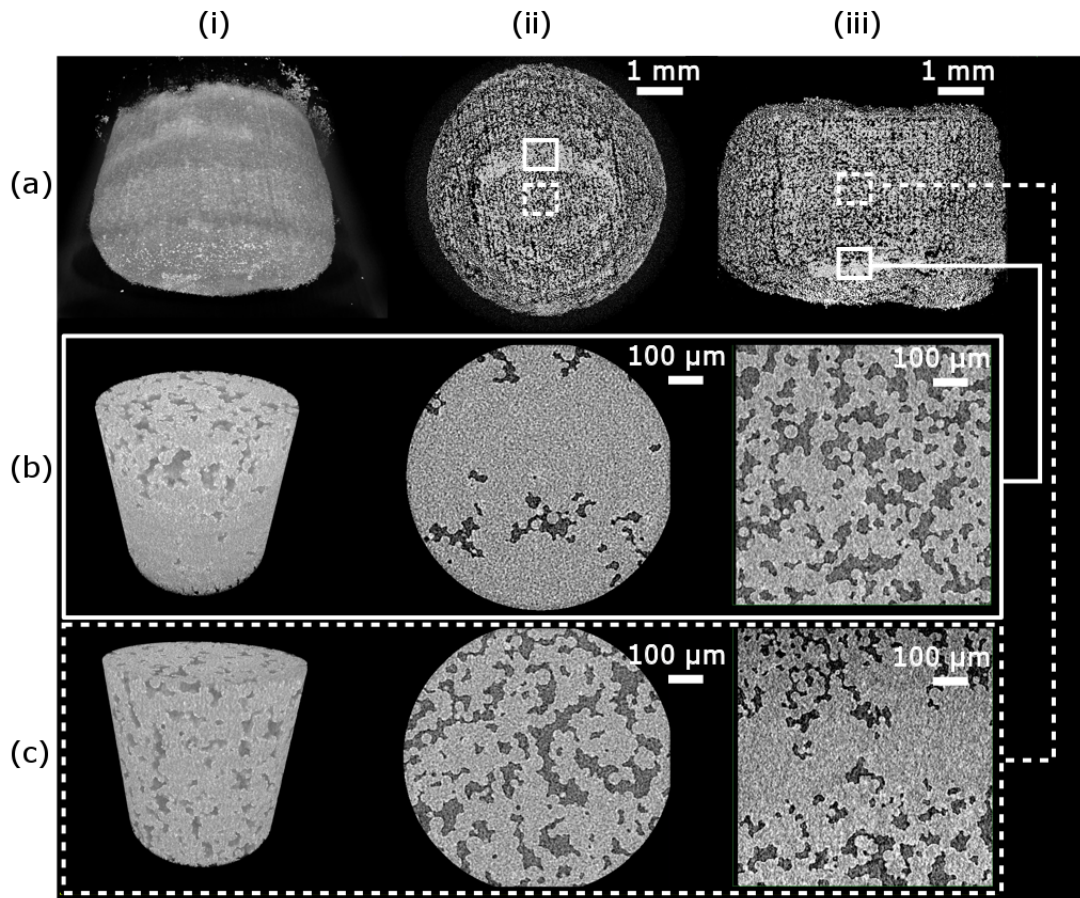


Figure 6.10: CT scan results for the silicone part made via hybrid PBBJ-extrusion system; (a) overall structure, (b) defect region with high particle density; (c) central region with regular particle density; (a-c) (i) 3D view, (ii) top view, (iii) front view; (a) CT scanning resolution:  $4.05 \mu m$ ; (b-c) CT scanning resolution:  $1.4 \mu m$ .

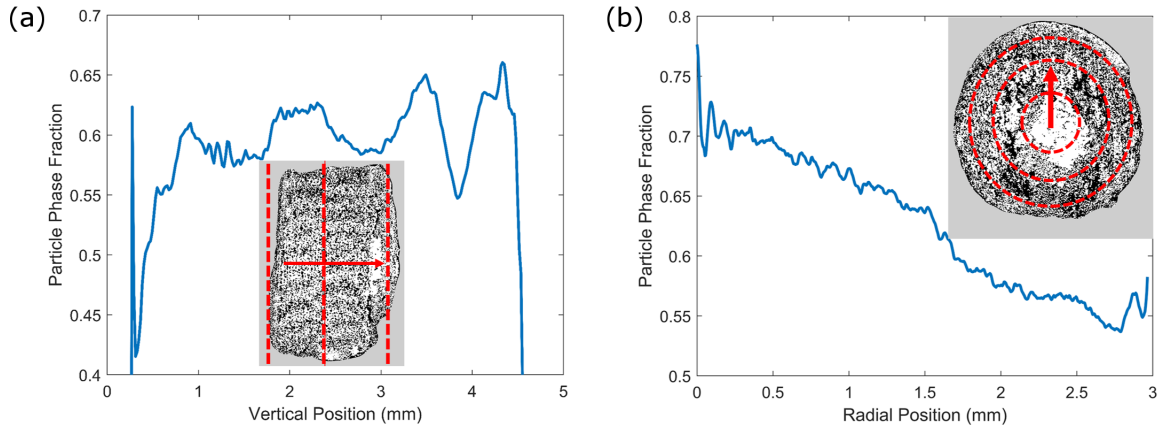


Figure 6.11: Silicone particle phase fraction vs. (a) vertical position and (b) radial position.

riphery of the parts. This is an artefact of the droplet deposition process. When infiltrating polymer solution droplets onto a porous substrate [176], the liquid permeation through the porous powder media is dependent on the droplet kinetics, porosity of the substrate, as well as the wetting angle of the powder material. Considering that the size of the liquid silicone droplet ( $\sim 1.54 \text{ mm}$ ) is significantly larger than the average powder particle size used in this study (powder Type A,  $30 \mu\text{m}$ ), the dynamic impact kinetics of the traveling droplet and liquid spreading mechanisms of the sessile droplet through the porous media can play a significant role in disturbing the powder [171]. The impact kinetics of the falling droplet can explain the regions of higher powder particle concentration at the bottom of the parts, as particles are displaced vertically [176]. The difference in powder fraction radially, from 75% volume fraction of particles in the centre of the part to 55% at the periphery, can be explained by the theory of droplet primary and secondary liquid spread [171]. In the primary spread, the liquid droplet meets the substrate and starts to imbibe the powder. During this phase, there is an instantaneous flow rate initiated at the liquid-powder interface. This generates a net force acting at the inlet powder boundary, thus particles can be dislodged and can travel within the sessile droplet radially, which may explain the different concentration of particles in the centre of the parts. Overall, the theory seems to suggest that smaller liquid silicone droplets would reduce the powder displacement and likely result in a more uniform component, furthering the need for a better liquid silicone delivery method.

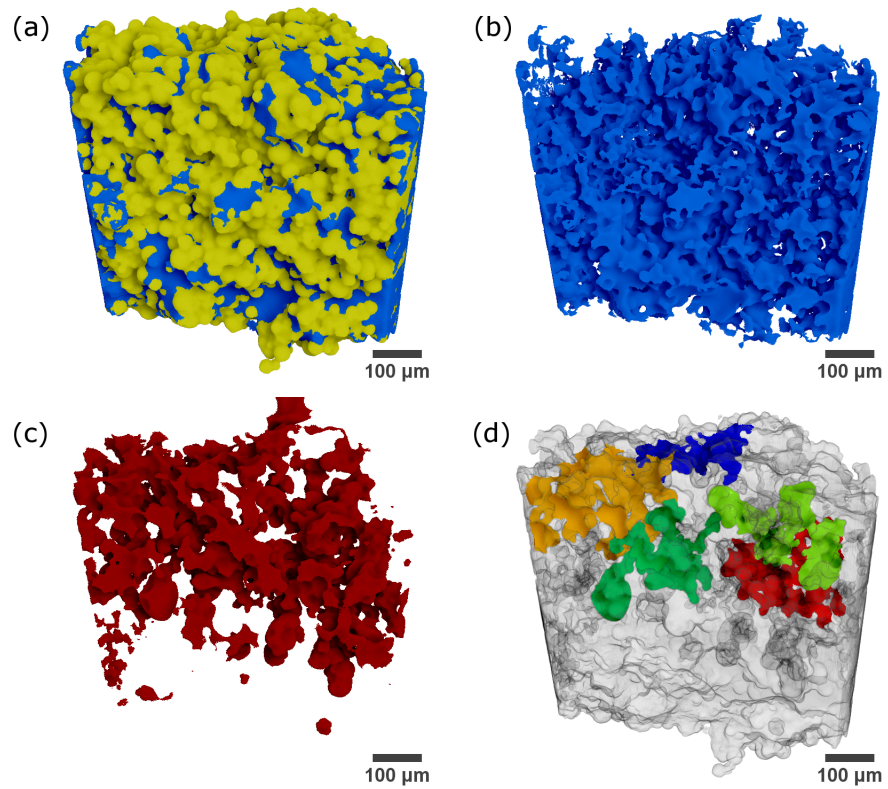


Figure 6.12: Separation of different phases of AM-made structure; (a) yellow: silicone powder, blue: cross-linked silicone binder; (b) isolated cross-linked silicone binder; (c) isolated pores; (d) largest air gaps in the pore network separated with different colors; (a-d) CT scanning resolution:  $727 \text{ nm}$ .



### 6.3.6 Part Durometry

Two sets of parts were 3D printed at optimized printing conditions ( $LT$  of 100  $\mu m$  and  $Fr$  1 drop per 300  $\mu m$ ). Three cylindrical parts from each batch were selected for the hardness test. The tests were replicated three times for each part. Similar testing approach was employed for the cured silicone binder molded based on ASTM D2240. The hardness test results are summarized in Table 6.4. The ANOVA study was used to compare the average hardness of AM-made cylinders, the results of which (Table 6.5) failed to show a significant difference between the hardness of the parts.

Table 6.4: The durometry results for the 3D printed cylinders and molded silicone binder ( $n = 3$ ).

Sample	Hardness (Shore 00)			
	test 1	test 2	test 3	Average
Cylinder 1 (batch 1)	80.5	85.6	80.9	82.3
Cylinder 2 (batch 1)	87.3	85.2	82.8	85.1
Cylinder 3 (batch 1)	80.7	80.1	81.5	80.8
Cylinder 1 (batch 2)	81.5	85.3	86	84.3
Cylinder 2 (batch 2)	85.3	84.3	85.2	84.9
Cylinder 3 (batch 2)	80.9	87.8	84.7	84.5
Total average for cylindrical samples				<b>83.6</b>
Molded silicone binder 1	81.5	80.1	75.4	79
Molded silicone binder 2	81.2	81.2	79.6	80.7
Total average for molded silicone binder				<b>79.8</b>

Table 6.5: ANOVA results for the hardness test.

Source	DF	Adj SS	Adj MS	F-Value	P-Value
Measurements	5	55.49	11.098	2.54	0.086
Error	12	52.47	4.373		
Total	17	107.96			

Similarly, the comparison of average hardness values for the AM-made cylinders and the pure silicone binder using a t-test does not show a statistically significant difference at 95% confidence level (Table 6.6). The average hardness is approximately 83.6 (Shore A) for

the 3D printed parts and 79.8 (Shore A) for the crosslinked silicone binder. The hardness of powder A, reported in the materials certificate, is 70 (Shore A).

Table 6.6: Comparing the hardness of 3D printed structures and molded silicone binder using t-test method.

	N	Mean	Std Dev	SE Mean
3D printed structures	6	83.64	1.72	0.7
Molded silicone binder	2	79.84	1.18	0.83

The durometry results for the AM-made samples show that different replicates of the same manufacturing process produce similar durometry results which indicate the reproducibility of the hybrid PBBJ-extrusion process. A full mechanical characterization will be carried out on the products of this AM method in the future. Specifically, the effect of the printing parameters on  $\sigma_f$ ,  $T_s$ , and  $\epsilon_f$  [103] should be investigated in order to make any required changes to the system of materials for each particular biomedical application.

## 6.4 Summary

In this chapter, a novel hybrid method combining PBBJ and deposition techniques for fabrication of 3D structures entirely made from silicone was introduced. Cylindrical samples optimized in terms of geometrical accuracy were showcased. The permeation of silicone binder in the powder bed was sped up by pre-wetting the surface with an aqueous binder. The rapid curing mechanism of the parts was designed based on the thermal analysis of the binder. Guidelines for efficient flowability of silicone powder were provided based on its rheological properties and shear sensitivity. The experimental results indicated that PBBJ technique is capable of processing thermoset powders. The main challenge remaining is integration of a multi-nozzle inkjet printhead compatible with medium to high viscous silicone binders to the system. Such a binder deposition system will increase the AM speed, improves the geometrical accuracy of the final products, and provides higher control over the properties of parts. Upon further improvement in the deposition of silicone binder, this hybrid method could be used for production of structures with the capability of controlled release of fluids for drug-delivery applications.

# Chapter 7

## Conclusions and Future Work

Development and characterization of additive manufacturing (AM) systems and the associated methodologies for fabrication of silicone structures has been pursued throughout this thesis. To this end, a custom multi-nozzle hybrid three-dimensional (3D) printer based on piezoelectric-pneumatic jetting (PPJ) was designed and developed that can deposit highly viscous silicone inks in a drop-on-demand fashion at high throughput rate, while the well-defined boundary of each layer is laid using a pneumatic micro-dispensing system. Moreover, a manufacturing methodology integrating direct write technologies with powder-bed binder-jetting (PBBJ) was introduced to shape form the silicone powder into a 3D structure for the first time. The effects of process parameters on the mechanical, surface, and internal properties of additively manufactured structures were investigated as well.

In PPJ, the entire structure is deposited in a drop-on-demand fashion. On the other hand, only a portion of structures volume is inkjet printed in PBBJ. Under normal conditions, the jetting of partial volume of the part and support-free fabrication technique should make PBBJ a faster method. However, we only obtained the objective of high speed silicone AM using PPJ method. In PBBJ, the time-consuming silicone binder deposition step using micro-dispensing slows down the process as the high speed of PBBJ process is mostly due to the use of inkjet printheads that have hundreds of orifices which can deposit a considerable volume of fluid as they pass over a large area. In thermal printheads, the evaporation of ink inside the reservoir is the source of energy for jetting. It is obvious that silicone with a high thermal stability (up to 300 °C) is not a good candidate for use in thermal inkjet printheads. Moreover, both piezoelectric and thermal inkjet printheads are limited by the viscosity of inks that can be printed. Silicone inks can be diluted using solvents such as toluene for use in piezoelectric printheads but other complications such as

shrinkage might happen after solvent evaporation. The current PPJ printheads have only one orifice too and their high throughput is mainly because of their high translation speed. As a result, the printing speed of the PBBJ technique can be improved by multi-orifice inkjet printheads for materials that experience a viscosity larger than  $40 \text{ mPa}\cdot\text{s}$  at the nozzle. Similar technology can further improve the throughput of PPJ as well.

In terms of the capability of producing heterogeneous structures, the PPJ system is currently able to print up to three materials at a high spatial precision. The number of materials can be increased by addition of printheads. The production of truly material-graded parts with various property profiles; however, is only possible by employment of the multi-orifice systems. In general, material jetting performs better than regular PBBJ systems for production of material-graded structures as it is prohibitive to incorporate hundreds of powder feed chambers into the system but PBBJ excels in rapid fabrication of porous structures.

This thesis contributed to the field of advanced manufacturing by addressing some of the current limitations in 3D printing of soft elastomeric structures through introduction of two systems that can be used to control the internal features of products and fabricate material-graded structures. Moreover, the shortcomings of the proposed systems were pointed out and suggestions for improvement of their speed and flexibility were made.

A summary of the technical conclusions and some of the future work proposed as a continuation to this thesis are provided in this chapter.

## 7.1 Thesis Conclusions

The following conclusions can be drawn from this thesis:

1. The hybrid extrusion-PPJ system was used successfully to fabricate complex 3D structures composed of multiple materials with various properties. Both extrusion and PPJ systems were capable of depositing a silicone paste with a viscosity of approximately  $1.6 \times 10^6 \text{ mPa}\cdot\text{s}$  (shear rate of  $1 \text{ s}^{-1}$ ) at  $25 \text{ }^\circ\text{C}$ .
2. Irradiance-curable silicones perform better in the context of AM due to their faster crosslinking rate (in the order of a few seconds) compared to heat- or moisture-curable silicones. The light irradiation systems can also be easily integrated into the AM system. Moreover, the ink containers and printheads can be protected from the light irradiation much easier than the heat leading to a lower chance of nozzle clogging.

3. According to the statistical optimization conducted, a combination of 100 *kPa* pressure, 5 *mm/s* printhead velocity, and 0.2 *mm* nozzle working distance for a 250  $\mu\text{m}$  nozzle results in dispensing of line features with an average width of 322.8  $\mu\text{m}$ . At 2D level, pressure, working distance, their interaction, and raster width control the surface quality. A combination of higher pressure and lower raster width yields in a lower surface waviness, however, at a risk of increasing the layer thickness through overprinting. 0.1 *mm* raster width, 200 *kPa* pressure, and 2 *mm* working distance generate a surface with a waviness of 3  $\mu\text{m}$ .
4. Among all the process parameters of PPJ system, pulse time, velocity, stroke, and close time have the highest effect on the quality of printed strands of silicone at the investigated region in Chapter 4. According to the statistical optimization conducted, pulse time of 0.4 *ms*, close time of 0.2 *ms*, stroke of 86%, and velocity of 97 *mm/s* result in a uniform line with an average width of 580  $\mu\text{m}$ . Increasing the velocity to 104 *mm/s* with a raster width of 0.39 *mm* yields a minimum surface waviness of 8  $\mu\text{m}$ .
5. Due to the lower surface waviness and higher width uniformity of extruded filaments compared to the jetted lines, the perimeter of each layer was printed using the pneumatic extrusion system so that the highest surface quality is obtained.
6. When printing a 3D silicone structure, even with the optimized process parameters, the quality of printed layers might differ as the height increases. This happens mainly due to the build up of the viscous material around the orifice after a certain time. This increases the level of porosity in the parts which leads to their deteriorated mechanical properties. This issue was resolved by tailoring the viscosity and rheology of ink.
7. Control over the internal porosity of parts was achieved by varying the rheology of silicone ink. The ink with a low shear yield stress obtained by mixing polysiloxanes with short- and long-chain monomers at 45:55 wt.% ratio. This ink flew under the effect of gravity just enough to merge the separated droplets into a uniform line, and resulted in a structure with a relative solid density of 99.65%. This eliminated the porosity introduced to the system as a result of material build up at orifice, deflection of droplets caused by the repulse of like electric charges on the surface of droplets and previously laid layer, and unsuccessful coalesce of viscous droplets.
8. For a silicone ink with dominant solid-like behavior and relatively large shear yield stress, the high level of porosity results in 45.9% and 38.6% decrease in the tensile

strength and elongation at break of the parts made via PPJ, respectively, compared to those of the bulk material. This difference was drastically reduced to 2% for tensile strength and 12.6% for elongation at break by lowering the porosity level through increasing the flowability of ink. Other characteristics such as tear resistance and hardness were not sensitive to the porosity level of the manufactured parts.

9. The hybrid PBBJ-extrusion printing methodology was used successfully to fabricate 3D structures based on silicone powder for the first time. The products are made fully from two different phases of silicone (i.e., powder and crosslinked rubber) as well as a water-based binder which leaves a biocompatible residue after evaporation. Thus, the products of this system can be directly applied to different biomedical applications.
10. The use of a silicone binder with low viscosity ( $< 100 \text{ mPa}\cdot\text{s}$ ) leads to faster percolation of binder in the powder-bed, and consequently higher manufacturing speed in hybrid PBBJ-extrusion method. Moreover, the pre-wetting of powders with water-based binder helps to speed up this infiltration process even more.
11. The shape and size of silicone particles affects the flow of powder and consequently, the quality of final parts. The use of spherical powder with an average particle size of  $30 - 40 \mu\text{m}$  and standard deviation of approximately  $30 \mu\text{m}$  is expected to show low shear yield and high flowability.
12. It was established that the parts fabricated via the PBBJ-extrusion system contain 8.2 vol.% air void which are locally interconnected and distributed unevenly throughout the structure. Generally, the structure is more dense at regions of the sample closer to the dispensing point. It can be concluded that the adoption of a method with higher control over the delivery of silicone binder could lead to control of the porosity of products. As a result, the fabrication of parts with variable density profiles from highly porous to fully dense will be possible.

The backbone of both AM methods introduced in this thesis is jetting. There are advantages and disadvantages to both methods; however, the challenges faced by both of them can be resolved through development of a multi-orifice material jetting printhead which can process fluids with various rheological properties from water to paste-like silicone, and mix different materials to adjust the properties of the prepolymer(s) during the print.

## 7.2 Recommendations and Future Work

The research work described in this thesis was intended to study the feasibility of rapid manufacturing of soft heterogeneous parts made from different phases of silicone which have not been investigated before, namely high viscous paste and powder, through additive methods. To this end, two systems and methods were introduced and characterized. To achieve our intended vision of developing commercially ready systems for additive manufacturing of silicone bio-structures, further research on software, hardware, material systems, and applications should be conducted.

### 7.2.1 AM of Silicone Based on the PPJ System

1. The use of experimentally-obtained regression models for the prediction of the effect of process parameters on printing quality for every new material and ink seems prohibitive. Even though, the established models in Chapters 3 and 4 can be used for inks with similar behavior to our sample silicone with slight modifications, developing analytical models for prediction of the geometry of viscous non-Newtonian droplets in PPJ techniques is recommended.
2. The developed PPJ system prints silicone structures 10 – 20 times faster than regular extrusion systems. However, in terms of the speed, it still falls behind the Poly-Jet systems with multi-orifice printheads. As a result, improving the scalability of this system by redesigning the piezoelectric-pneumatic printheads to include an array of orifices instead of one single orifice increases the chance of industrial adoption of this technique. Furthermore, such a technology can make the fabrication of fully colored bio-structures possible.
3. Tailoring the mechanical properties of silicone for different bio-medical applications based on the rheological guidelines provided in Chapter 5 should be pursued. Moreover, given the fact that irradiance-curable silicones are highly compatible with additive manufacturing systems such as jetting, extrusion, and stereolithography, commercial biocompatible photoinitiators need to be developed.

### 7.2.2 AM of Silicone Based on the PBBJ System

1. The parts fabricated via the PBBJ-extrusion system, demonstrated overprinting even at optimized process parameters of 100  $\mu m$  layer thickness, 1 silicone droplet per 300

$\mu m$  of powder, 20  $mm/s$  linear roller velocity, and 100  $rpm$  rotational roller velocity. In order to improve the geometrical accuracy of parts made via this system the following changes are recommended:

- (a) Replacing the extrusion-based system with a piezoelectric drop-on-demand system for delivering the silicone binder. This facilitates the jetting of droplets at pico-liter order. Coupled with a fast *in-situ* curing system, the overprinting issue as a result of lateral permeation will be resolved. It will also increase the manufacturing speed drastically.
  - (b) Mixing the silicone powder with solid additives such as polyvinyl alcohol (PVA) could restrain the overflow of silicone binder.
2. The investigation of the effect of process parameters on the mechanical characteristics and internal porosity of parts is recommended.



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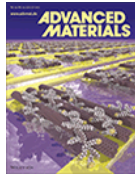
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### 3D Printing PDMS Elastomer in a Hydrophilic Support Bath via Freeform Reversible Embedding

Thomas J. Hinton<sup>†</sup>, Andrew Hudson<sup>†</sup>, Kira Pusch<sup>‡</sup>, Andrew Lee<sup>†</sup>, and Adam W. Feinberg<sup>\*††</sup>  
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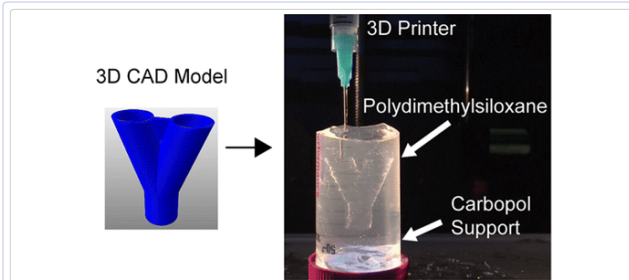
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Abstract



Polydimethylsiloxane (PDMS) elastomer is used in a wide range of biomaterial applications including microfluidics, cell culture substrates, flexible electronics, and medical devices. However, it has proved challenging to 3D print PDMS in complex structures due to its low elastic modulus and need for support during the printing process. Here we demonstrate the 3D printing of hydrophobic PDMS prepolymer resins within a hydrophilic Carbopol gel support via freeform reversible embedding (FRE). In the FRE printing process, the Carbopol support acts as a Bingham plastic that yields and fluidizes when the syringe tip of the 3D printer moves through it, but acts as a solid for the PDMS extruded within it. This, in combination with the immiscibility of hydrophobic PDMS in the hydrophilic Carbopol, confines the PDMS prepolymer within the support for curing times up to 72 h while maintaining dimensional stability. After printing and curing, the Carbopol support gel releases the embedded PDMS prints by using phosphate buffered saline solution to reduce the Carbopol yield stress. As proof-of-concept, we used Sylgard 184 PDMS to 3D print linear and helical filaments via continuous extrusion and cylindrical and helical tubes via layer-by-layer fabrication. Importantly, we show that the 3D printed tubes were manifold and perfusable. The results demonstrate that hydrophobic polymers with low viscosity and long cure times can be 3D printed using a hydrophilic support, expanding the range of biomaterials that can

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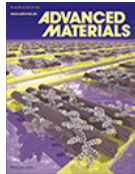
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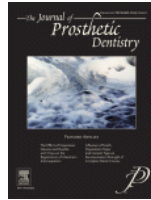
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# Appendices



# Appendix A

## Scientific Background

### A.1 Design of Experiments (DoE)

A systematic way to find the optimum combination of factors is to study the effect of each factor and interaction of different factors on the response. Design of experiments has been adopted by many research groups to investigate and optimize the quality of additive manufacturing processes [119, 129, 177, 178]. The screening experiment was performed to find out which factors have significant effects on width of the printed lines. As only three factors needed to be studied, a full factorial experiment was chosen. Factorial designs make it possible to simultaneously study the effects of different parameters and their interaction on response(s). It is also possible to find out how the effect of one factor changes when other factors are not constant. This simultaneous study of factor effects in DOE is done using analysis of variance (ANOVA) and hypothesis testing. Equations underlying the ANOVA procedure are from Montgomery (1984) and Mason (2003) books. Suppose a general experiment with three factors A, B, and C needs to be screened to find significant factors. Factor A has  $i$  levels ( $i = 1, 2, \dots, a$ ), factor B has  $j$  levels ( $j = 1, 2, \dots, b$ ), factor C has  $k$  levels ( $k = 1, 2, \dots, c$ ) and  $l$  represents the number of experiment replicates ( $l = 1, 2, \dots, n$ ). A total of  $abcn$  observations will be measured in a full factorial design. In order to conduct ANOVA, every observation will be decomposed into different components. The decomposed observations can be written as [179, 180]:

$$\mu_{ijkl} = \mu + \tau_i + \beta_j + \gamma_k + (\tau\beta)_{ij} + (\tau\gamma)_{ik} + (\beta\gamma)_{jk} + (\tau\beta\gamma)_{ijk} + \epsilon_{ijkl} \quad (\text{A.1})$$

where  $\mu$  is the overall main effect,  $\tau_i$  is the effect of  $i^{\text{th}}$  level of factor A,  $\beta_j$  is the effect of  $j^{\text{th}}$  level of factor B,  $\gamma_k$  is the  $k^{\text{th}}$  level effect of factor C,  $(\tau\beta)_{ij}$  is the effect of the

interaction between  $\tau$  and  $\beta$ ,  $(\tau\gamma)_{ik}$  is the effect of the interaction between  $\tau$  and  $\gamma$ ,  $(\beta\gamma)_{jk}$  is the effect of the interaction between  $\beta$  and  $\gamma$ ,  $(\tau\beta\gamma)_{ijk}$  is the effect of the interaction between  $\tau$ ,  $\beta$  and  $\gamma$ ,  $\epsilon_{ijkl}$  is the experimental error. The purpose of factorial design is to see if any of main effects, their second order combinations, and their third order combinations are significant. For doing so, following null hypotheses should be defined:

$$\begin{cases} H_0 : \tau_i = 0 \text{ for all } i; H_0 : \beta_j = 0 \text{ for all } j; H_0 : \gamma_k = 0 \text{ for all } k \\ H_0 : (\tau\beta)_{ij} = 0 \text{ for all } i, j; H_0 : (\tau\gamma)_{ik} = 0 \text{ for all } i, k; H_0 : (\beta\gamma)_{jk} = 0 \text{ for all } j, k \\ H_0 : (\tau\beta\gamma)_{ijk} = 0 \text{ for all } i, j, k \end{cases} \quad (\text{A.2})$$

The alternative hypotheses for all of the terms in Eq. A.2 would be at least one effect, e.g. , is not equal to zero (Montgomery et al., 1984). Let  $y_{\dots}$  be the total of all observations,  $y_{i\dots}$  be the total of all observations under the  $i^{th}$  level etc.,  $y_{ij\dots}$  be the total of all observations under the  $ij^{th}$  level etc., and  $y_{ijk\dots}$  be the total of all observations under the  $ijk^{th}$  level. The average of these values will be calculated by dividing them by their number and will be shown as  $(\bar{y}_{\dots})$  etc. Their total corrected sum of squares can be written as:

$$SS_T = \sum_{i=1}^a \sum_{j=1}^b \sum_{k=1}^c \sum_{l=1}^n (y_{ijkl} - \bar{y}_{\dots})^2 \quad (\text{A.3})$$

where  $SS_T$  is the total corrected sum of squares. Solving for Eq. A.3 and simplifying results we get:

$$SS_T = SS_A + SS_B + SS_C + SS_{AB} + SS_{AC} + SS_{BC} + SS_{ABC} + SS_E \quad (\text{A.4})$$

The means squares  $SS_i$ s is calculated by dividing them by their degrees of freedom ( $DF$ ) as follows:

$$MS_i = \frac{SS_i}{DF_i} \quad (\text{A.5})$$

Division of mean squares of factors and their combinations over the mean square of error will be distributed as F probability distribution. As a result, if this F-value is smaller than the critical F, the hypothesis will be rejected i.e. that factor is significant. Equation A.6 shows how F-value is calculated:

$$F_i = \frac{MS_i}{MS_E} \quad (\text{A.6})$$

Design of experiments fits a regression model to the three factors and their interactions that can be written as:

$$y = \beta_0 + \beta_1x_1 + \beta_2x_2 + \beta_3x_3 + \beta_{12}x_{12} + \beta_{13}x_{13} + \beta_{23}x_{23} + \beta_{123}x_{123} \quad (\text{A.7})$$

where  $Y$  is the response, the  $\beta_i$ 's are process parameter coefficients, and  $x_i$ 's are the process parameter values.

## A.2 Desirability Function Method

Where there is a need for optimization of more than one response, the desirability function method (also known as utility transfer function) is widely used. To this end, the value of every response will be converted to a number between zero and one which is called desirability. Desirability values closer to one demonstrate better results. The optimization algorithm chooses factor levels that maximize the overall desirability value [181, 182]. In this study, the minimization function will be used to calculate the individual desirabilities first. Considering  $d(y_i)$  ( $i=1, 2, \text{ and } 3$ ) as the desirability of response  $y_i$ , the minimization function will be:

$$d(y_i) = \begin{cases} 1 & \text{for } y_i < t_i \\ \left(\frac{u_i - y_i}{u_i - t_i}\right)^r & \text{for } t_i \leq y_i \leq u_i \\ 0 & \text{for } y_i \geq u_i \end{cases} \quad (\text{A.8})$$

where  $r$  determines the shape of the function; linear, convex, and concave for  $r = 1$ ,  $r < 1$ , and  $r > 1$ , respectively.  $u_i$  is the upper limit of the response  $y_i$ , and  $t_i$  is the target value of response  $y_i$ , i.e. the maximum value it can accept in this case. Then, the overall desirability function can be calculated as follows:

$$d_{total} = (d(y_1)d(y_2)...d(y_i))^{\frac{1}{i}} \quad (\text{A.9})$$

### A.3 Level-set Model

Level-set method was introduced by Osher and Sethian [183] in 80s to capture the interface of two fluids and the changes that interface goes through due to motion. This Eulerian method is applicable to analysis of the motion of interfaces e.g., the merging of two droplets in two or three dimensions.

In this method the curve is defined by a level-set equation  $\phi$  (in 2D space). The boundary between two fluids is represented by contour 0.5. The transition area with  $\phi$  less than 0.5 is air and  $\phi$  more than 0.5 represents silicone.

$$\begin{cases} 0 \leq \phi \leq 0 & \text{air} \\ \phi = 0.5 & \text{boundary} \\ 0.5 \leq \phi \leq 1 & \text{silicone} \end{cases} \quad (\text{A.10})$$

Density and viscosity of the two fluids change in the transition area according to the following equations using level-set function:

$$\rho = \rho_{air} + (\rho_{silicone} - \rho_{air})\phi \quad (\text{A.11})$$

$$\mu = \mu_{air} + (\mu_{silicone} - \mu_{air})\phi \quad (\text{A.12})$$

where  $\rho$  denotes the density and  $\mu$  denotes the viscosity.

The movement of the fluids interface under velocity field ( $\nu$ ) is described by Eq. A.13:

$$\frac{\partial \phi}{\partial t} + \nu \cdot \nabla \phi = 0 \quad (\text{A.13})$$

In the level-set method, the interface is considered to move normal to itself. Hence, only the normal component of the velocity field ( $\nu_n$ ) is important [184]. Replacing  $\nu_n = \nu \cdot \hat{n} = \nu \cdot \frac{\nabla \phi}{|\nabla \phi|}$  with  $\nu$  in above equation results in the level-set equation:

$$\frac{\partial \phi}{\partial t} + \nu_n |\nabla \phi| = 0 \quad (\text{A.14})$$

The level-set function should remain as a distance function ( $|\nabla \phi| = 1$ ) throughout the simulation process in order to depict the changes of interface accurately. In order to

solve this problem, numerical reinitialization and stabilization terms are added to level-set equation so that it is set back to distance function from the boundary after each time step [134, 185]. Following equation presents the non-conservative reinitialized level-set function and is solved in COMSOL multiphysics:

$$\rho\left(\frac{\partial\phi}{\partial t} + \nu \cdot \nabla\phi\right) = \Gamma[\epsilon\nabla \cdot \nabla\phi - \nabla \cdot (\phi(1 - \phi)\frac{\nabla\phi}{|\nabla\phi|})] \quad (\text{A.15})$$

where  $\epsilon$  is the thickness of the transition layer. Half of the size of the typical mesh size in the region passed by the droplet [186] is suggested for  $\epsilon$ .  $\Gamma$  is the reinitialization factor and is approximately equal to the maximum value of the velocity field.

## A.4 Fluid Flow Governing Equations

The flow of silicone in nozzle dispensing system is incompressible and laminar. Non-conservative time-dependent Navier-Stokes equations are solved for this model to demonstrate the transport of mass and momentum [185]:

$$\nabla \cdot \nu = 0 \quad (\text{A.16})$$

$$\rho\frac{\partial\nu}{\partial t} + \rho(\nu \cdot \nabla)\nu = \nabla \cdot [-PI + \mu(\nabla u + (\nabla u)^T)] + \rho g + F_{st} \quad (\text{A.17})$$

where  $\rho$  is the density,  $\nu$  is the velocity field,  $P$  is the pressure of silicone,  $I$  is the identity matrix,  $\mu$  is the dynamic viscosity,  $g$  is the acceleration of gravity,  $F_{st}$  denotes the surface tension force. Eq. A.18 is used to calculate the value of surface tension force.

$$F_{st} = \nabla \cdot [(\gamma(I - NN^T))\delta] \quad (\text{A.18})$$

where  $\gamma$  is the surface tension. Also,  $N$  denotes the normal to the interface and  $\delta$  is the Dirac delta function, which is formulized as following:

$$n = \frac{\nabla\Phi}{|\nabla\Phi|} \quad (\text{A.19})$$

$$\delta = 6|\Phi(1 - \Phi)||\nabla\Phi| \quad (\text{A.20})$$

Droplet generation on the surface is modeled by definition of wetted wall boundary condition parametrized with contact angle and slip length for the substrate. The slip length, i.e. the distance behind the substrate at which the velocity can be extrapolated to zero [187] is required for modeling the movement of the boundary between two fluids and to prevent singularity. The recommended slip length is equal to mesh size [188]. The wetted wall boundary condition is described using friction force ( $F_f$ ) in Eq. A.21:

$$\gamma(n - n_{int} \cos \theta)\delta = -F_f = \frac{\mu}{\beta} \nu \quad (\text{A.21})$$

where  $\beta$  is the slip length,  $\theta_c$  is the contact angle and  $F_f$  is the friction force.

# Appendix B

## Experimental Design for Material Extrusion

### B.1 Line Features

Table B.1:  $2^3$  full factorial design and measurements

Run	Variables			Coded Variables			Response		
	Pressure	Velocity	Working Distance	Pressure	Velocity	Working Distance	Average Width	Uniformity	Surface Quality
1	200	10	0.5	1	1	1	367.6	2.06	171.5
2	100	5	0.2	-1	-1	-1	289.3	4.27	65.8
3	200	10	0.2	1	1	-1	492	1.9	290.3
4	200	10	0.2	1	1	-1	675.6	0.8	83.6
5	100	5	0.2	-1	1	-1	266.6	1.96	140.2
6	100	5	0.5	-1	1	1	42.4	18.91	39.7
7	100	5	0.5	-1	-1	1	90.2	29.5	8
8	200	10	0.5	1	-1	1	541.8	2.79	125.9
9	100	5	0.2	-1	1	-1	338.2	6.4	155.6
10	200	10	0.5	1	1	1	321.6	2.24	26.1
11	100	5	0.2	-1	-1	-1	237.8	2.48	21.3
12	100	5	0.5	-1	-1	1	191.8	32.75	102
13	200	10	0.2	1	-1	-1	870.6	0.49	34.3
14	200	10	0.2	1	-1	-1	859.6	2.33	37.9
15	150	7.5	0.35	0	0	0	253.2	3.12	140.3
16	150	7.5	0.35	0	0	0	274.8	4.83	87.2
17	200	10	0.5	1	-1	1	488.4	4.27	37.6
18	100	5	0.5	-1	1	1	56.6	30.63	57.8

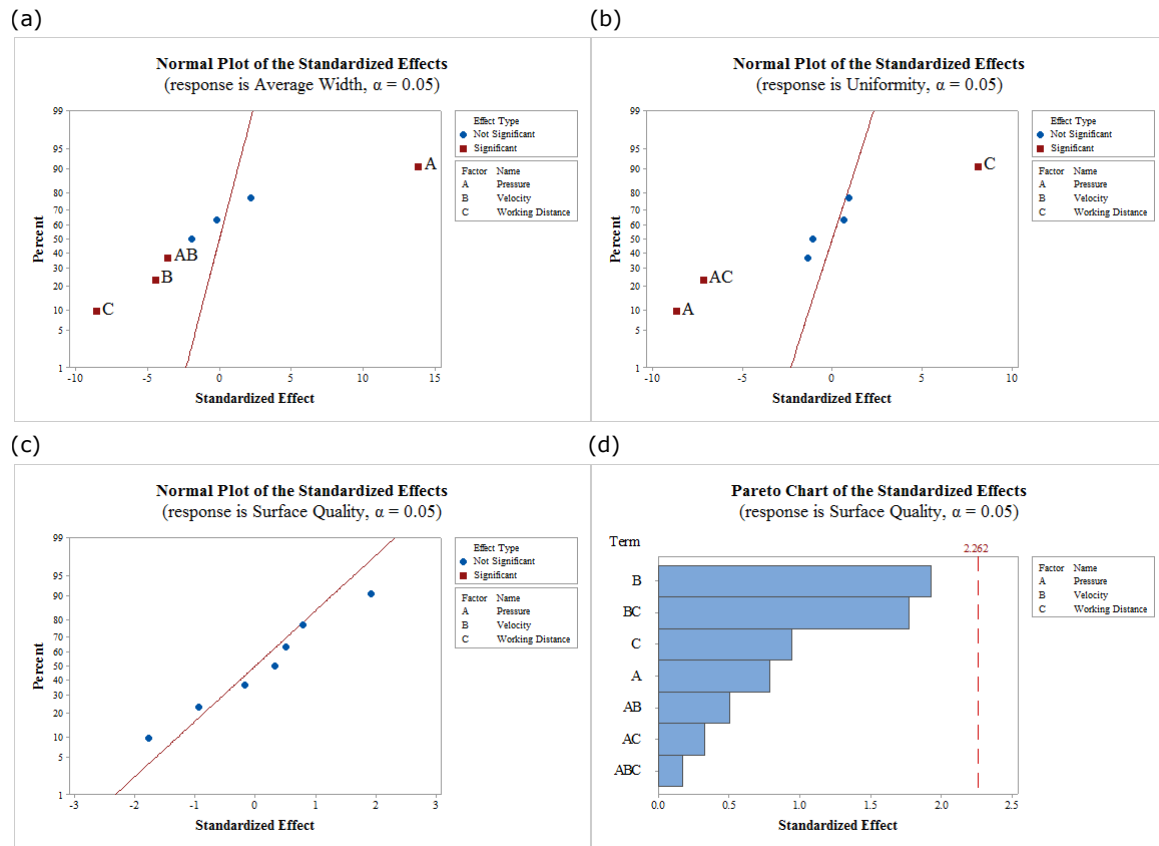


Figure B.1: Significant process parameters; (a) Normal plot for  $W_{avg}$ ; (b) Normal plot for  $W_{s.d.}$ ; (c) Normal plot for  $W_q$ ; (d) Pareto chart for surface quality.

Table B.2: Process parameter coefficients in regression equation

	$\beta_0$	$\beta_1$	$\beta_2$	$\beta_3$	$\beta_{12}$	$\beta_{13}$	$\beta_{23}$	$\beta_{123}$
$W_{avg}$	383.1	194	-63.1	-120.6	-49.9	0	0	-119.1
$W_{s.d.}$	8.986	-6.876	0	6.407	0	-5.677	0	-5.01
$W_q$	87.3	13.6	33.3	-16.3	8.7	5.7	-30.6	-2.9



Table B.3: ANOVA and model summary

	DF	Adj SS	Adj MS	P-Value
<hr/>				
<i>W<sub>avg</sub></i>				
Main Factors	3	602292	299516	0
<i>P</i>	1	898547	602292	0
<i>v</i>	1	63617	63617	0.003
<i>WD</i>	1	232637	232637	0
Second order interactions	1	39830	39830	0.012
<i>P*v</i>	1	39830	39830	0.012
Curvature	1	25231	25231	0.205
<hr/>				
R-squared	94.62%			
Adj R-squared	92.37%			
<hr/>				
<i>W<sub>s.d.</sub></i>				
Main Factors	2	1413.3	706.65	0
<i>P</i>	1	756.48	756.48	0
<i>WD</i>	1	656.81	656.81	0
Second order interactions	1	515.65	515.65	0
<i>P*WD</i>	1	515.65	515.65	0
Curvature	1	44.58	44.58	0.057
<hr/>				
R-squared	93.67%			
Adj R-squared	91.73%			
<hr/>				

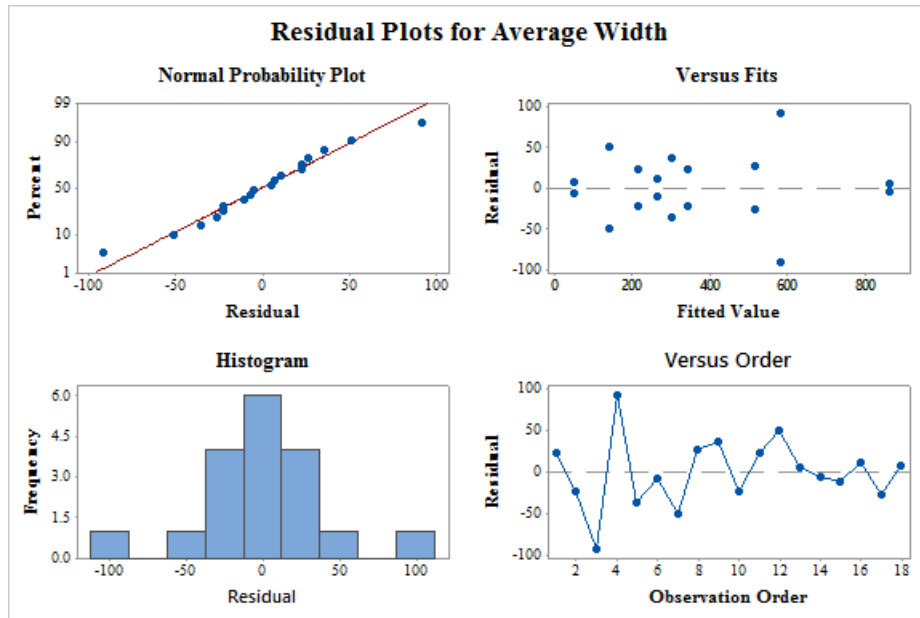


Figure B.2: Residual plots for  $W_{avg}$  show normality and independence assumptions are valid.

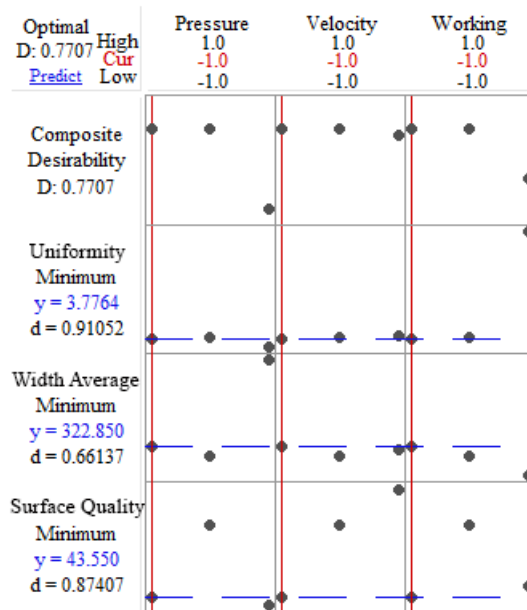


Figure B.3: Optimization plot: -1, -1, -1 level set treatment combination for  $P$ ,  $V$  and  $WD$ , respectively, gives the optimal results.

## B.2 Plane Features

Table B.4:  $2^4$  design and the response values

No.	$P$	$v$	$RW$	$WD$	$W_q$
9	150	10	0.1	0.2	2.571
11	150	20	0.1	0.2	11.53
4	200	20	0.1	0.1	2.129
8	200	20	0.2	0.1	5.531
12	200	20	0.1	0.2	1.98
31	200	10	0.2	0.2	6.098
5	150	10	0.2	0.1	4.087
23	200	10	0.2	0.1	4.547
34 (C)	Center	Center	Center	Center	3.942
3	150	20	0.1	0.1	4.248
6	200	10	0.2	0.1	4.906
20	150	20	0.1	0.1	2.239
32	150	20	0.2	0.2	13.905
13	150	10	0.2	0.2	8.838
21	200	20	0.1	0.1	1.498
18	150	10	0.1	0.1	2.25
2	200	10	0.1	0.1	3.095
33	200	20	0.2	0.2	7.183
14	200	10	0.2	0.2	5.211
27	200	10	0.1	0.2	3.145
28	150	20	0.1	0.2	6.063
7	150	20	0.2	0.1	5.172
24	150	20	0.2	0.1	4.516
26	150	10	0.1	0.2	2.645
16	200	20	0.2	0.2	5.108
17 (C)	Center	Center	Center	Center	3.097
22	150	10	0.2	0.1	3.004
10	200	10	0.1	0.2	1.977
29	200	20	0.1	0.2	1.599

Table B.5: ANOVA for  $W_q$  in  $2^4$  design

Factor	SS	DF	MS	F-observe	P-Value
$P$	117.2134	1	117.2134	10.19629	0.004044*
$v$	6.4064	1	6.4064	0.55729	0.462918
$RW$	156.2647	1	156.2647	13.59334	0.00122*
$WD$	102.1235	1	102.1235	8.88364	0.006689*
$P \times v$	5.4022	1	5.4022	0.46993	0.49987
$P \times RW$	7.3344	1	7.3344	0.63802	0.432601
$P \times WD$	87.7415	1	87.7415	7.63256	0.011078*
$v \times RW$	0.6992	1	0.6992	0.06082	0.807394
$v \times WD$	8.006	1	8.006	0.69644	0.412568
$RW \times WD$	68.1003	1	68.1003	5.92399	0.023114*
Error	264.4007	23	11.4957		
Total	823.6922	33			

Table B.6: ANOVA for  $W_q$  for the extruded planar features after removing the insignificant factors.

Factor	SS	DF	MS	F-observe	P-Value
$P$	117.2134	1	117.2134	11.23006	0.002316
$RW$	156.2647	1	156.2647	14.97152	0.000596
$WD$	102.1235	1	102.1235	9.78432	0.004083
$P \times WD$	87.7415	1	87.7415	8.4064	0.007194
$RW \times WD$	68.1003	1	68.1003	6.5246	0.016366
Error	292.2489	28	10.4375		
Total	823.6922	33			

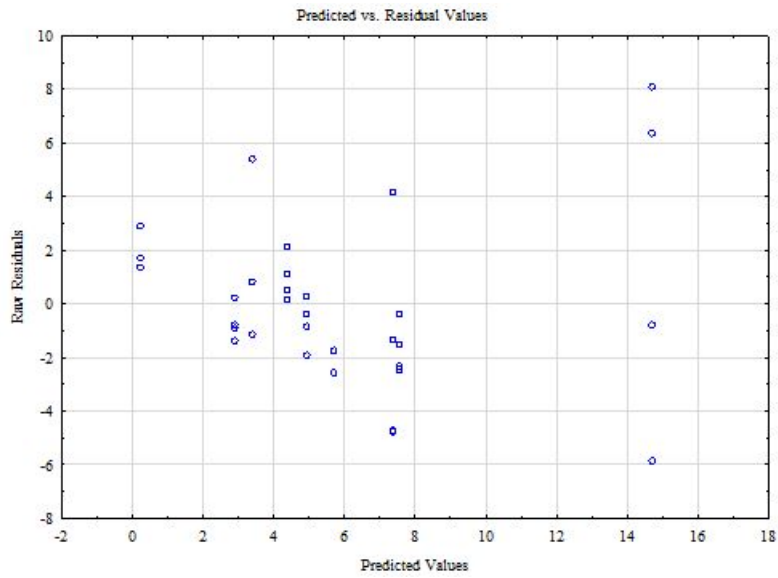


Figure B.4: *NPP* of residuals for the  $2^4$  design shows that the residuals fall along a straight line when ignoring the values at extremes, as a result, the normality assumption is valid.

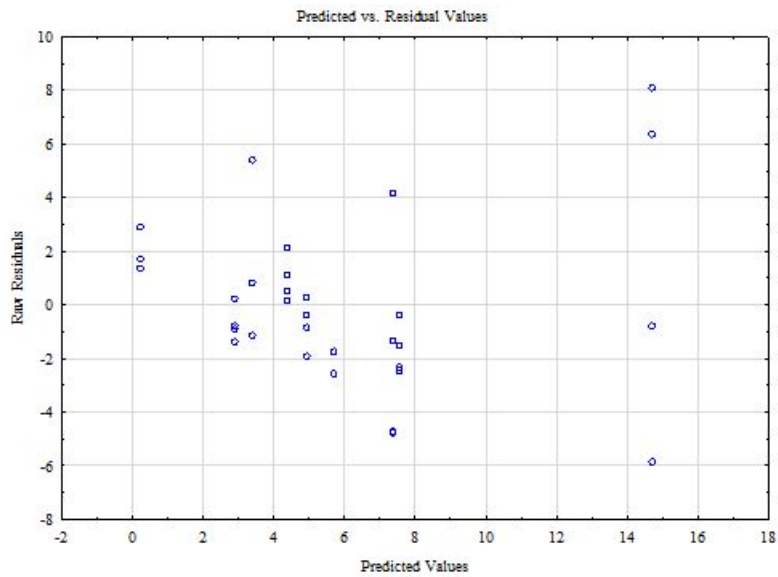


Figure B.5: Plot of residuals vs. predicted values is structureless and there is no tendency toward negative or positive residuals.

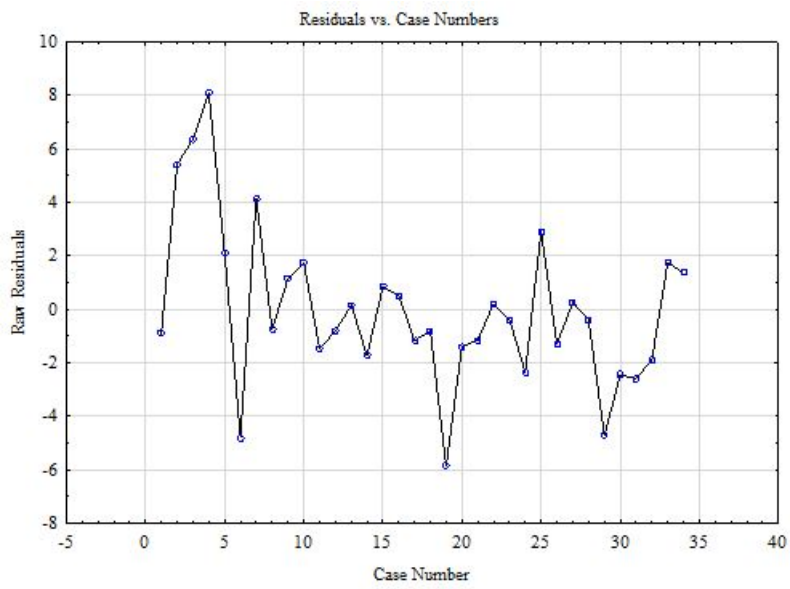


Figure B.6: The plot of residuals vs. time does not show any special pattern.

# Appendix C

## Experimental Design for Material Jetting

### C.1 Line Features: Screening

Given the fact that we are dealing with ten factors at the screening stage, running a full factorial design becomes prohibitive. Moreover, at this point we are only interested in identifying the significant factors, not their higher-order interactions. As a result, a  $2^{10-5}$  design with resolution  $V$  was selected for the purpose of factor screening. The design was replicated in order to estimate the sum of squares of errors. Two center points were added to the model as well. Hence, 66 independent experiments were run in a random order and the average and standard deviation values were measured for the width of the printed samples. The first and second replicates were run at different days in order to minimize the effect of the nuisance factors.

Table C.1:  $2^{10-5}_V$  design and the response values.

No.	$PT$	$CyT$	$T$	$V$	$Str\%$	$OT$	$CT$	$v$	$WD$	$P$	$W_{s.d.}$	$W_{avg}$
1	0.37	3.5	90	85	80	0.2	0.2	60	3	600	*	*
2	0.43	3.5	90	85	80	0.15	0.15	50	2	600	0.10	0.81
3	0.37	4	90	85	80	0.15	0.15	50	3	500	0.03	0.67
4	0.43	4	90	85	80	0.2	0.2	60	2	500	0.18	0.66
5	0.37	3.5	100	85	80	0.15	0.15	60	2	500	0.01	0.67

*Continued on next page*



No.	<i>PT</i>	<i>CyT</i>	<i>T</i>	<i>V</i>	<i>Str%</i>	<i>OT</i>	<i>CT</i>	<i>v</i>	<i>WD</i>	<i>P</i>	<i>W<sub>s.d.</sub></i>	<i>W<sub>avg</sub></i>
6	0.43	3.5	100	85	80	0.2	0.2	50	3	500	0.23	1.08
7	0.37	4	100	85	80	0.2	0.2	50	2	600	0.07	0.85
8	0.43	4	100	85	80	0.15	0.15	60	3	600	0.12	0.65
9	0.37	3.5	90	95	80	0.15	0.2	50	2	500	0.05	0.50
10	0.43	3.5	90	95	80	0.2	0.15	60	3	500	0.03	0.54
11	0.37	4	90	95	80	0.2	0.15	60	2	600	0.03	0.77
12	0.43	4	90	95	80	0.15	0.2	50	3	600	0.15	0.57
13	0.37	3.5	100	95	80	0.2	0.15	50	3	600	0.08	0.88
14	0.43	3.5	100	95	80	0.15	0.2	60	2	600	0.06	0.59
15	0.37	4	100	95	80	0.15	0.2	60	3	500	0.01	0.49
16	0.43	4	100	95	80	0.2	0.15	50	2	500	0.01	0.69
17	0.37	3.5	90	85	90	0.2	0.15	50	2	500	0.08	0.88
18	0.43	3.5	90	85	90	0.15	0.2	60	3	500	0.15	0.72
19	0.37	4	90	85	90	0.15	0.2	60	2	600	*	*
20	0.43	4	90	85	90	0.2	0.15	50	3	600	0.03	0.76
21	0.37	3.5	100	85	90	0.15	0.2	50	3	600	0.18	0.93
22	0.43	3.5	100	85	90	0.2	0.15	60	2	600	0.08	0.86
23	0.37	4	100	85	90	0.2	0.15	60	3	500	0.01	0.81
24	0.43	4	100	85	90	0.15	0.2	50	2	500	*	*
25	0.37	3.5	90	95	90	0.15	0.15	60	3	600	0.02	0.91
26	0.43	3.5	90	95	90	0.2	0.2	50	2	600	0.08	0.74
27	0.37	4	90	95	90	0.2	0.2	50	3	500	0.02	0.75
28	0.43	4	90	95	90	0.15	0.15	60	2	500	0.04	0.60
29	0.37	3.5	100	95	90	0.2	0.2	60	2	500	0.02	0.80
30	0.43	3.5	100	95	90	0.15	0.15	50	3	500	0.02	0.71
31	0.37	4	100	95	90	0.15	0.15	50	2	600	0.01	0.90
32	0.43	4	100	95	90	0.2	0.2	60	3	600	0.04	0.57
33	C	C	C	C	C	C	C	C	C	C	0.05	0.64
34	0.37	3.5	90	85	80	0.2	0.2	60	3	600	0.08	0.52
35	0.43	3.5	90	85	80	0.15	0.15	50	2	600	0.05	0.54
36	0.37	4	90	85	80	0.15	0.15	50	3	500	0.05	0.56
37	0.43	4	90	85	80	0.2	0.2	60	2	500	0.24	0.51
38	0.37	3.5	100	85	80	0.15	0.15	60	2	500	0.03	0.57
39	0.43	3.5	100	85	80	0.2	0.2	50	3	500	*	*
40	0.37	4	100	85	80	0.2	0.2	50	2	600	*	*
41	0.43	4	100	85	80	0.15	0.15	60	3	600	*	*
42	0.37	3.5	90	95	80	0.15	0.2	50	2	500	0.07	0.64

*Continued on next page*

No.	<i>PT</i>	<i>CyT</i>	<i>T</i>	<i>V</i>	<i>Str%</i>	<i>OT</i>	<i>CT</i>	<i>v</i>	<i>WD</i>	<i>P</i>	<i>W<sub>s.d.</sub></i>	<i>W<sub>avg</sub></i>
43	0.43	3.5	90	95	80	0.2	0.15	60	3	500	0.08	0.58
44	0.37	4	90	95	80	0.2	0.15	60	2	600	0.01	0.65
45	0.43	4	90	95	80	0.15	0.2	50	3	600	0.19	0.75
46	0.37	3.5	100	95	80	0.2	0.15	50	3	600	0.01	0.80
47	0.43	3.5	100	95	80	0.15	0.2	60	2	600	0.07	0.54
48	0.37	4	100	95	80	0.15	0.2	60	3	500	0.12	0.61
49	0.43	4	100	95	80	0.2	0.15	50	2	500	0.04	0.60
50	0.37	3.5	90	85	90	0.2	0.15	50	2	500	0.03	0.79
51	0.43	3.5	90	85	90	0.15	0.2	60	3	500	*	*
52	0.37	4	90	85	90	0.15	0.2	60	2	600	*	*
53	0.43	4	90	85	90	0.2	0.15	50	3	600	0.12	0.61
54	0.37	3.5	100	85	90	0.15	0.2	50	3	600	*	*
55	0.43	3.5	100	85	90	0.2	0.15	60	2	600	*	*
56	0.37	4	100	85	90	0.2	0.15	60	3	500	0.01	0.64
57	0.43	4	100	85	90	0.15	0.2	50	2	500	*	*
58	0.37	3.5	90	95	90	0.15	0.15	60	3	600	0.01	0.66
59	0.43	3.5	90	95	90	0.2	0.2	50	2	600	0.07	0.66
60	0.37	4	90	95	90	0.2	0.2	50	3	500	0.01	0.60
61	0.43	4	90	95	90	0.15	0.15	60	2	500	0.03	0.47
62	0.37	3.5	100	95	90	0.2	0.2	60	2	500	0.01	0.64
63	0.43	3.5	100	95	90	0.15	0.15	50	3	500	0.05	0.63
64	0.37	4	100	95	90	0.15	0.15	50	2	600	0.01	0.70
65	0.43	4	100	95	90	0.2	0.2	60	3	600	0.10	0.54
66	C	C	C	C	C	C	C	C	C	C	0.09	0.60

Table C.2: ANOVA for  $W_{s.d.}$  in  $2^{10-5}$  design

Factor	SS	DF	MS	F-observe	P-Value
<i>PT</i>	0.0277	1.0000	0.0277	17.6418	0.000128*
<i>CyT</i>	0.0000	1.0000	0.0000	0.0001	0.9934
<i>T</i>	0.0008	1.0000	0.0008	0.4816	0.4913
<i>V</i>	0.0310	1.0000	0.0310	19.7556	0.000059*
<i>Str%</i>	0.0066	1.0000	0.0066	4.1995	0.046427*
<i>OT</i>	0.0004	1.0000	0.0004	0.2578	0.6142
<i>CT</i>	0.0429	1.0000	0.0429	27.3297	0.000005*
<i>v</i>	0.0008	1.0000	0.0008	0.5217	0.4739
<i>WD</i>	0.0031	1.0000	0.0031	2.0024	0.1641
<i>P</i>	0.0009	1.0000	0.0009	0.5470	0.4635
Error	0.0690	44.0000	0.0016		
Total	0.1844	54.0000			

Table C.3: ANOVA for  $W_{s.d.}$  for the jetted line features after removing the insignificant factors.

Factor	SS	DF	MS	F-observe	P-Value
<i>PT</i>	0.0301	1.0000	0.0301	19.9138	0.0000
<i>V</i>	0.0318	1.0000	0.0318	21.0422	0.0000
<i>Str%</i>	0.0063	1.0000	0.0063	4.1638	0.0466
<i>CT</i>	0.0428	1.0000	0.0428	28.2725	0.0000
Error	0.0757	50.0000	0.0015		
Total	0.1844	54.0000			

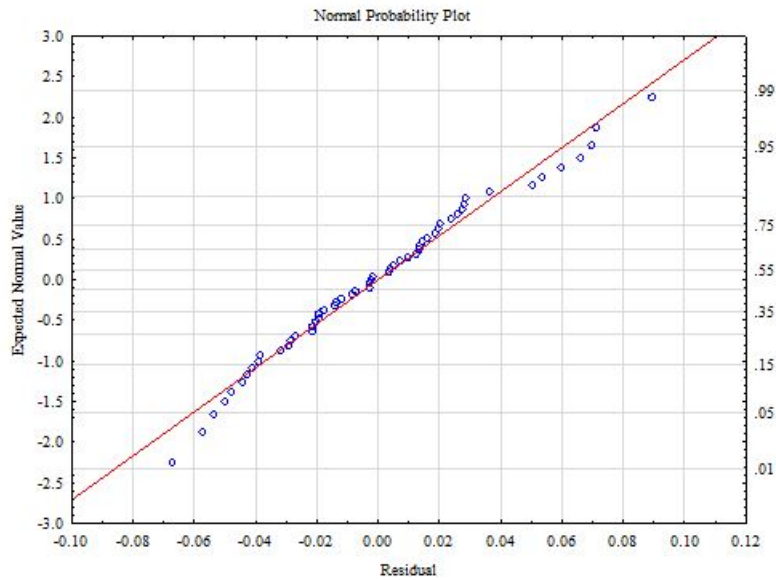


Figure C.1: NPP of residuals for the  $2^{10-5}$  design shows that the residuals fall along a straight line, as a result, the normality assumption is valid.

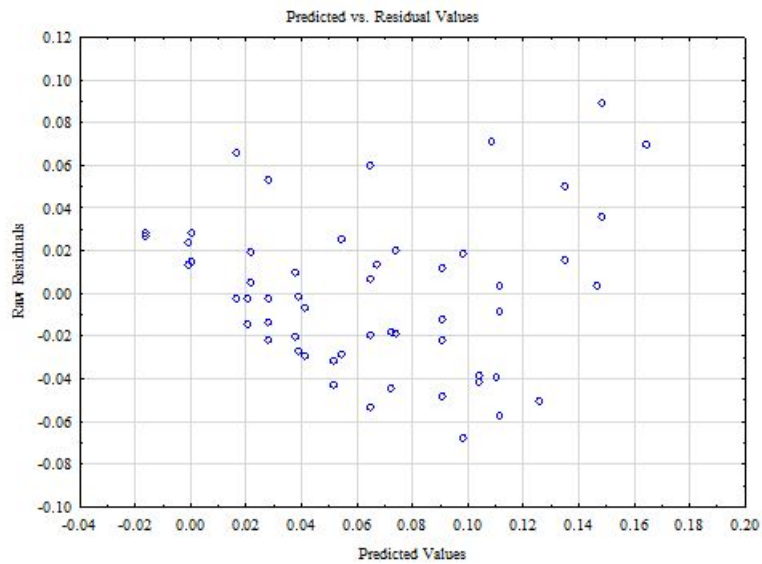


Figure C.2: Plot of residuals vs. predicted values is structureless and there is no tendency towards negative or positive residuals.

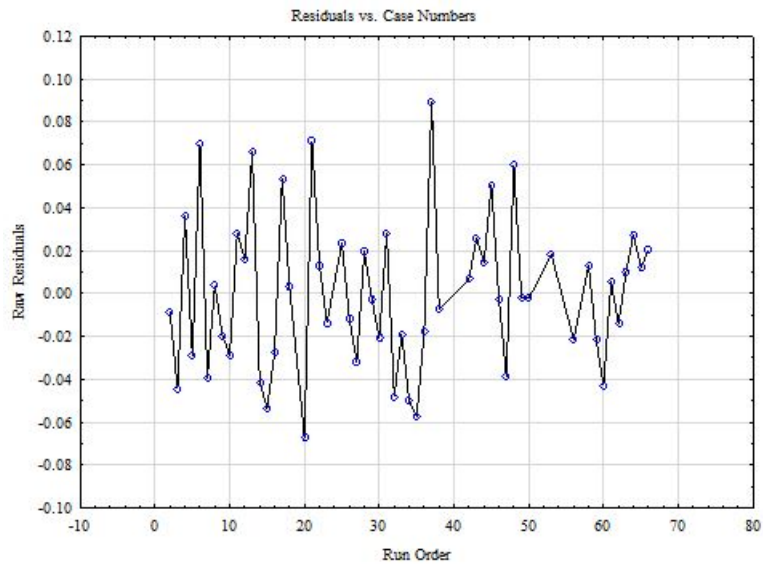


Figure C.3: The plot of residuals vs. time does not show any special pattern.

## C.2 Line Features: Optimization

Table C.4:  $3^{4-1}_{IV}$  design and the response values

No.	<i>PT</i>	<i>CT</i>	<i>V</i>	<i>Str%</i>	<i>W<sub>avg</sub></i>
1	0.35	0.15	93	86	0.875
2	0.35	0.15	95	90	0.919
3	0.35	0.15	97	88	0.904
4	0.35	0.17	93	90	0.819
5	0.35	0.17	95	88	0.807
6	0.35	0.17	97	86	0.790
7	0.35	0.19	93	88	0.750
8	0.35	0.19	95	86	0.859
9	0.35	0.19	97	90	0.925
10	0.37	0.15	93	90	0.860
11	0.37	0.15	95	88	0.846
12	0.37	0.15	97	86	0.871
13	0.37	0.17	93	88	0.789
14	0.37	0.17	95	86	0.827
15	0.37	0.17	97	90	0.829
16	0.37	0.19	93	86	0.725
17	0.37	0.19	95	90	0.799
18	0.37	0.19	97	88	0.812
19	0.39	0.15	93	88	0.835
20	0.39	0.15	95	86	0.836
21	0.39	0.15	97	90	0.866
22	0.39	0.17	93	86	0.718
23	0.39	0.17	95	90	0.811
24	0.39	0.17	97	88	0.775
25	0.39	0.19	93	90	0.727
26	0.39	0.19	95	88	0.706
27	0.39	0.19	97	86	0.653
28	0.37	0.17	95	88	0.818
29	0.37	0.17	95	88	0.846

Table C.5: ANOVA for  $W_{avg}$  in  $3^{4-1}_{IV}$  design

Factor	SS	DF	MS	F-observe	P-Value
<i>PT</i>	0.028736	1	0.028736	30.23031	0.0000784*
<i>PT</i> <sup>2</sup>	0.000932	1	0.000932	0.98068	0.338839
<i>CT</i>	0.040708	1	0.040708	42.82435	0.000013*
<i>CT</i> <sup>2</sup>	0.002732	1	0.002732	2.87429	0.11212
<i>V</i>	0.005962	1	0.005962	6.27236	0.02524*
<i>V</i> <sup>2</sup>	0.002749	1	0.002749	2.89188	0.111124
<i>Str%</i>	0.008916	1	0.008916	9.37919	0.00843*
<i>Str%</i> <sup>2</sup>	0.00074	1	0.00074	0.77873	0.392429
<i>PT</i> × <i>CT</i>	0.004813	1	0.004813	5.06356	0.04103*
<i>PT</i> × <i>V</i>	0.00136	1	0.00136	1.43088	0.251488
<i>PT</i> × <i>Str%</i>	0.000678	1	0.000678	0.71349	0.41249
<i>CT</i> × <i>V</i>	0.001564	1	0.001564	1.64542	0.220414
<i>CT</i> × <i>Str%</i>	0.001114	1	0.001114	1.17196	0.297294
<i>V</i> × <i>Str%</i>	0.0019	1	0.0019	1.99875	0.179279
Error	0.013308	14	0.000951		
Total	0.11806	28			

Table C.6: ANOVA for  $W_{avg}$  for the jetted line features after removing the insignificant factors.

Factor	SS	DF	MS	F-observe	P-Value
<i>PT</i>	0.028736	1	0.028736	24.60158	0.000052
<i>CT</i>	0.040708	1	0.040708	34.85067	0.000005
<i>V</i>	0.005962	1	0.005962	5.10448	0.033647
<i>Str%</i>	0.008916	1	0.008916	7.63283	0.011076
<i>PT</i> × <i>CT</i>	0.006874	1	0.006874	5.88469	0.023525
Error	0.026865	23	0.001168		
Total	0.11806	28			

Table C.7: Regression coefficients of the reduced model for jetting of line features.

Factor	Reg. Coeff.	SE	P-Value
Mean	0.813717	0.006346	0
<i>PT</i>	-0.039956	0.008056	0.000052
<i>CT</i>	-0.047556	0.008056	0.000005
<i>V</i>	0.0182	0.008056	0.033647
<i>Str%</i>	0.022256	0.008056	0.011076
<i>PT</i> × <i>CT</i>	-0.023933	0.009866	0.023525

In this resolution IV design, the main factors are confounded with the third order interaction factors. Also, the second order interactions are confounded with each other. Assuming that the third or higher order interactions are not significant, no further investigation is required for the significant main factors. The second order interaction *PT* × *CT* is confounded with *V* × *Str%* interaction. There is no straightforward method to associate the calculated sum of squares (0.00069) to one of these second order interactions or both. However, based on the smaller P-values for the pulse time and close time factors and the experience gained while running the experiments, we can conclude that *PT* × *CT* has a larger impact on the output compared to *V* × *Str%*.



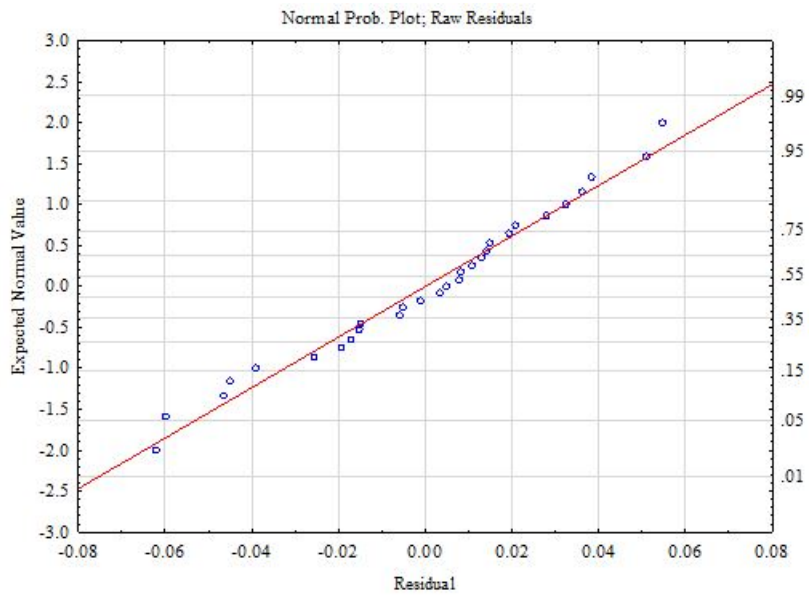


Figure C.4: NPP of residuals for the  $3^{4-1}_{IV}$  design shows that the residuals fall along a straight line, as a result, the normality assumption is valid.

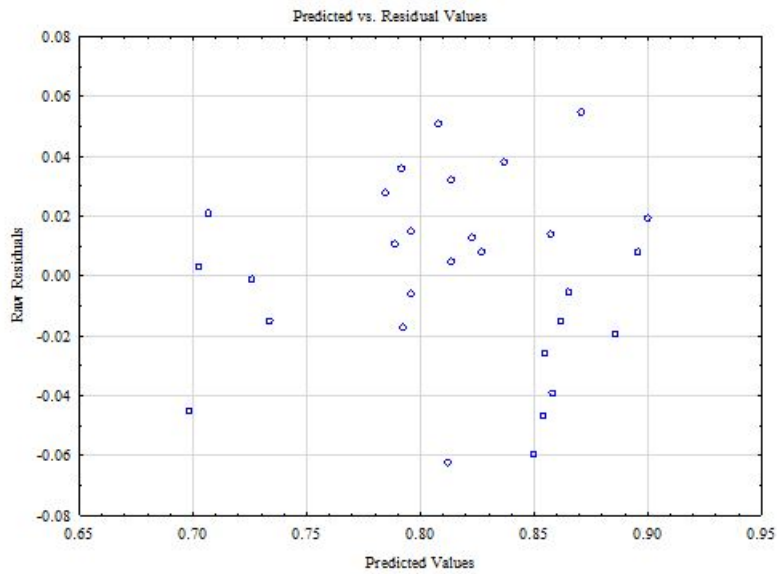


Figure C.5: Plot of residuals vs. predicted values is structureless and there is no tendency towards negative or positive residuals; however, there is slight indication of inconsistent variance which is negligible.

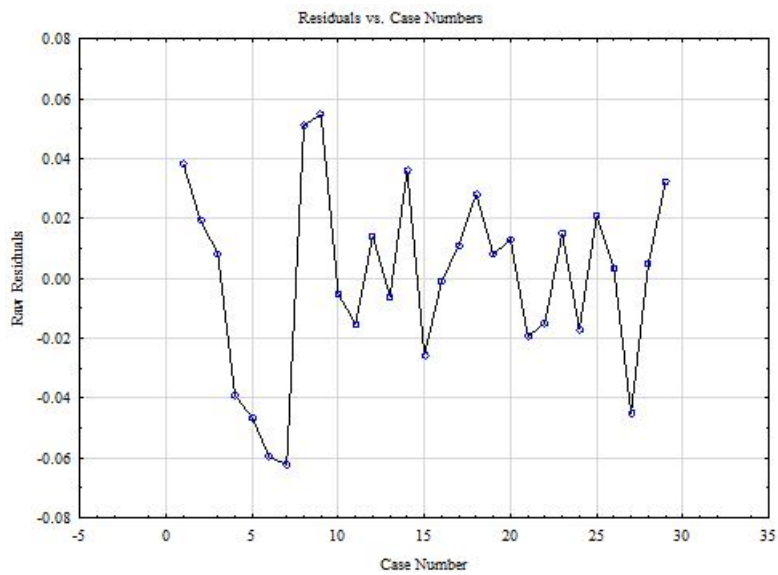


Figure C.6: The plot of residuals vs. time does not show any special pattern.

Table C.8: ANOVA for  $W_{avg}$  in CCD

Factor	SS	DF	MS	F-observe	P-Value
$PT$	0.001636	1	0.001636	3.01424	0.101749
$PT^2$	0.003088	1	0.003088	5.69153	0.029754*
$CT$	0.000427	1	0.000427	0.78728	0.388068
$CT^2$	0.002678	1	0.002678	4.93473	0.0411*
$PT \times CT$	0.006012	1	0.006012	11.07822	0.004257*
Error	0.008682	16	0.000543		
Total	0.024616	21			

Table C.9: Regression coefficients of the CCD model.

Factor	Reg. Coeff.	SE	P-Value
Mean	0.5929	0.0085	0.0000
$PT$	-0.0117	0.0067	0.1017
$PT^2$	0.0247	0.0103	0.0298
$CT$	-0.0060	0.0067	0.3881
$CT^2$	0.0230	0.0103	0.0411
$PT \times CT$	0.0274	0.0082	0.0043

### C.3 Plane Features: Optimization

Table C.10:  $2^2$  design and the response values.

No.	$v$	$RW$	$W_q$
2	100	0.4	22.609
10 (C)	80	0.45	40.308
7	100	0.4	22.275
8	60	0.5	51.943
3	60	0.5	50.614
9	100	0.5	40.151
5 (C)	80	0.45	46.611
6	60	0.4	49.197
4	100	0.5	38.31
1	60	0.4	54.195

Table C.11: ANOVA for  $W_q$  for the jetted planar features.

Factor	SS	DF	NS	F-observe	P-Value
$v$	852.928	1	852.9276	117.8215	0.000036
$RW$	134.005	1	134.0048	18.5111	0.005079
$v \times RW$	148.023	1	148.0232	20.4476	0.004009
Error	43.435	6	7.2391		
Total	1178.391	9			

Table C.12: Regression coefficients for the jetting of the planar features model.

Factor	Regr. Coeff.	SE	P-Value
Mean	41.6213	0.850832	0
$v$	-10.3255	0.951259	0.000036
$RW$	4.0928	0.951259	0.005079
$v \times RW$	4.3015	0.951259	0.004009

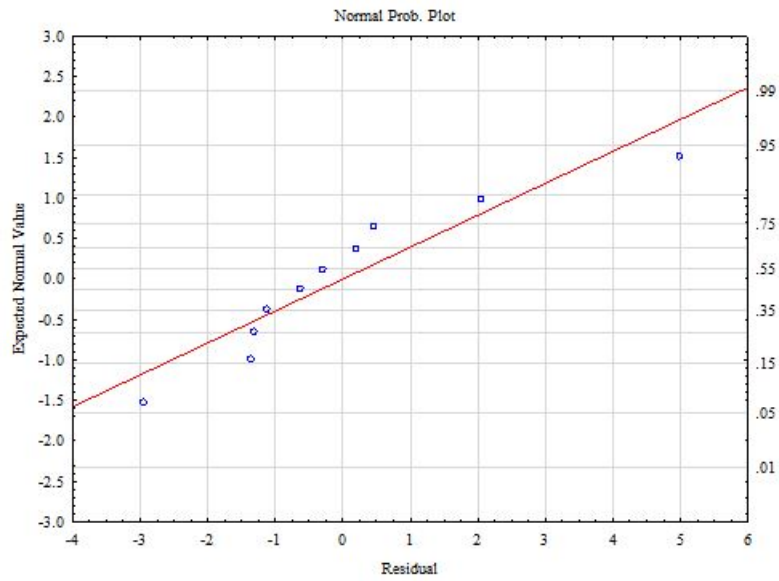


Figure C.7: NPP for the  $2^2$  design shows that the residuals fall along a straight line when ignoring the values at extremes, as a result, the normality assumption is valid.

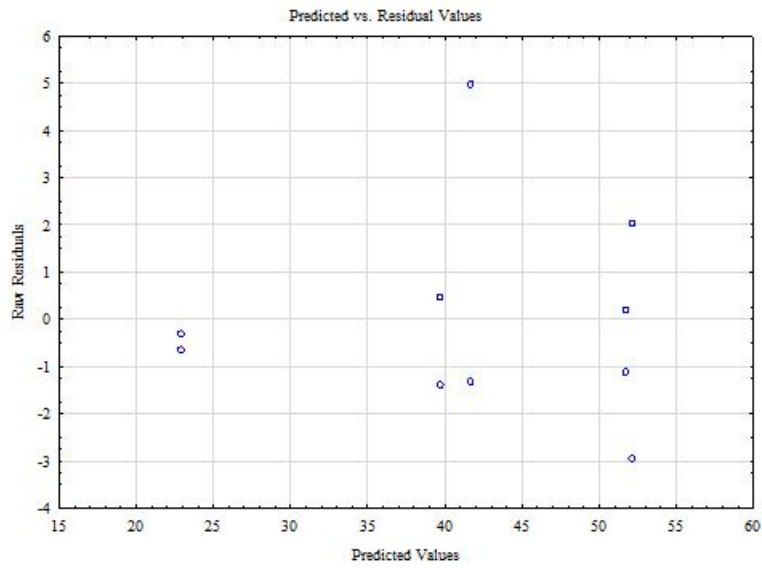


Figure C.8: Plot of residuals vs. predicted values is structureless and there is no tendency toward negative or positive residuals; however, there is slight indication of inconsistent variance which is negligible.

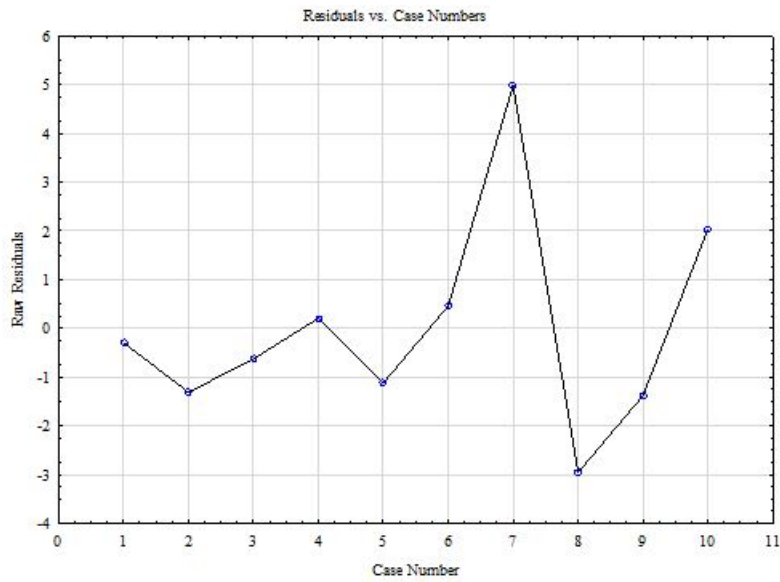


Figure C.9: The plot of residuals vs. time does not show any special pattern.

# Appendix D

## Experimental Design for PBBJ

### D.1 Screening

Table D.1: The measured values for  $H$ ,  $ID$ , and  $OD$ .

No.	$LT$ ( $\mu m$ )	$Fr$	$h$ ( $\mu m$ )	$ID$ ( $\mu m$ )	$DD$ ( $\mu m$ )
1	50	3	4130.676	5407.209	1563.818
2	50	1	5685.574	6966.943	1476.194
3	50	1	5907.289	6904.469	1256.984
4	100	3	3673.833	5579.145	1283.139
5	100	3	3863.966	5329.552	1930.681
6	50	2	3852.614	5685.995	1905.692
7	100	1	4894.481	7436.54	2126.095
8	50	3	4116.611	6160.803	2074.107
9	50	2	3909.257	6762.391	1615.955
10	100	2	3619.815	6588.914	1835.162
11	100	2	3645.568	6307.557	1137.825
12	100	1	5904.6	7353.762	1869.109

Table D.2: ANOVA results for  $H$ .

Source	DF	Adj SS	Adj MS	F-Value	P-Value
Model	5	8550286	1710057	18.49	0.001
Linear	3	8538548	2846183	30.78	0
$LT$	1	333253	333253	3.6	0.106
$Fr$	2	8205295	4102648	44.36	0
2-Way Interaction	2	11738	5869	0.06	0.939
$LT \times Fr$	2	11738	5869	0.06	0.939
Error	6	554859	92476		
Total	11	9105145			

Table D.3: ANOVA results for  $ID$ .

Source	DF	Adj SS	Adj MS	F-Value	P-Value
Model	5	5160132	1032026	6.59	0.02
Linear	3	4831906	1610635	10.29	0.009
$LT$	1	41732	41732	0.27	0.624
$Fr$	2	4790174	2395087	15.3	0.004
2-Way Interaction	2	328226	164113	1.05	0.407
$LT \times Fr$	2	328226	164113	1.05	0.407
Error	6	939373	156562		
Total	11	6099505			



Table D.4: ANOVA results for *OD*.

Source	DF	Adj SS	Adj MS	F-Value	P-Value
Model	5	534849	106970	0.94	0.516
Linear	3	23421	7807	0.07	0.975
<i>LT</i>	1	6973	6973	0.06	0.813
<i>Fr</i>	2	16449	8224	0.07	0.931
2-Way Interaction	2	511428	255714	2.25	0.187
<i>LT</i> × <i>Fr</i>	2	511428	255714	2.25	0.187
Error	6	682013	113669		
Total	11	1216862			

## D.2 Optimization

Table D.5: Desirability function response optimization.

Response	Goal	Lower	Target	Upper	Weight
<i>DD</i>	Minimum	*	1137.82	2126.09	1
<i>ID</i>	Target	4500	5000	7436.54	1
<i>h</i>	Target	2700	3000	5907.29	1

# Appendix E

## Supporting Experiments

### E.1 Experiments of Chapter 5

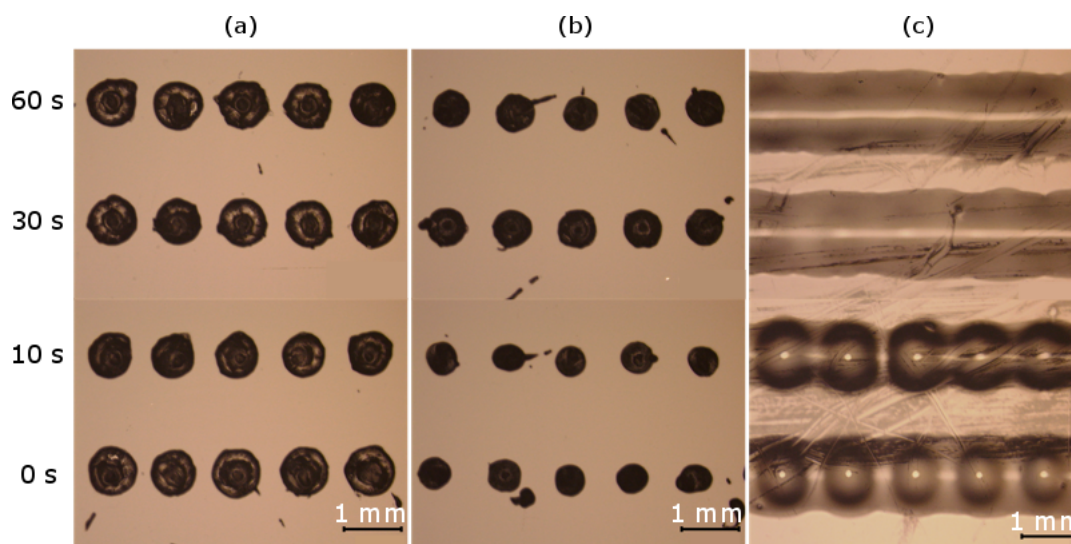


Figure E.1: Jetted droplets of inks (a) A, (b) 70A-30B, and (c) 45A-55B cured 0s, 10s, 30s, and 60 s after deposition. The slumping of ink 45A-55B has made the coalesce of droplets possible.

Table E.1: Measurement of mechanical properties and t-test comparisons.

Ink	Method	$\epsilon_f$ (%)	$\sigma_f$ (MPa)	$T_s$ (kN/m)	Hardness (00)	
A	Cast	Sample 1	389	1.38	10.26	75.1
		Sample 2	390	1.33	10.58	72.9
		Sample 3	364	1.35	11.7	71.7
		Avg.	381.000	1.353	10.847	73.233
		Std. Dev.	12.028	0.021	0.756	1.408
	AM-made	Sample 1	226	0.72	13.25	69.4
		Sample 2	257	0.81	8.99	70.7
		Sample 3	219	0.67	10.085	70.1
		Avg.	234.000	0.733	10.775	70.067
		Std. Dev.	16.513	0.058	2.212	0.531
	Percentage Change		38.58%	45.92%	0.66%	4.33%
P-value		0.001	0	0.96	0.041	
45A-55B	Cast	Sample 1	96.9	0.48	0.97	65.3
		Sample 2	92.7	0.46	0.99	66.9
		Sample 3	102.47	0.55	1.05	67.5
		Avg.	97.357	0.497	1.003	66.567
		Std. Dev.	4.002	0.039	0.042	0.929
	AM-made	Sample 1	76.28	0.44	0.91	63.7
		Sample 2	85.58	0.52	1.17	67
		Sample 3	93.55	0.55	1	63
		Avg.	85.137	0.503	1.027	64.567
		Std. Dev.	7.057	0.046	0.132	1.744
	Percentage Change		12.55%	2.04%	2.40%	3.01%
P-value		0.1	0.883	0.785	0.226	

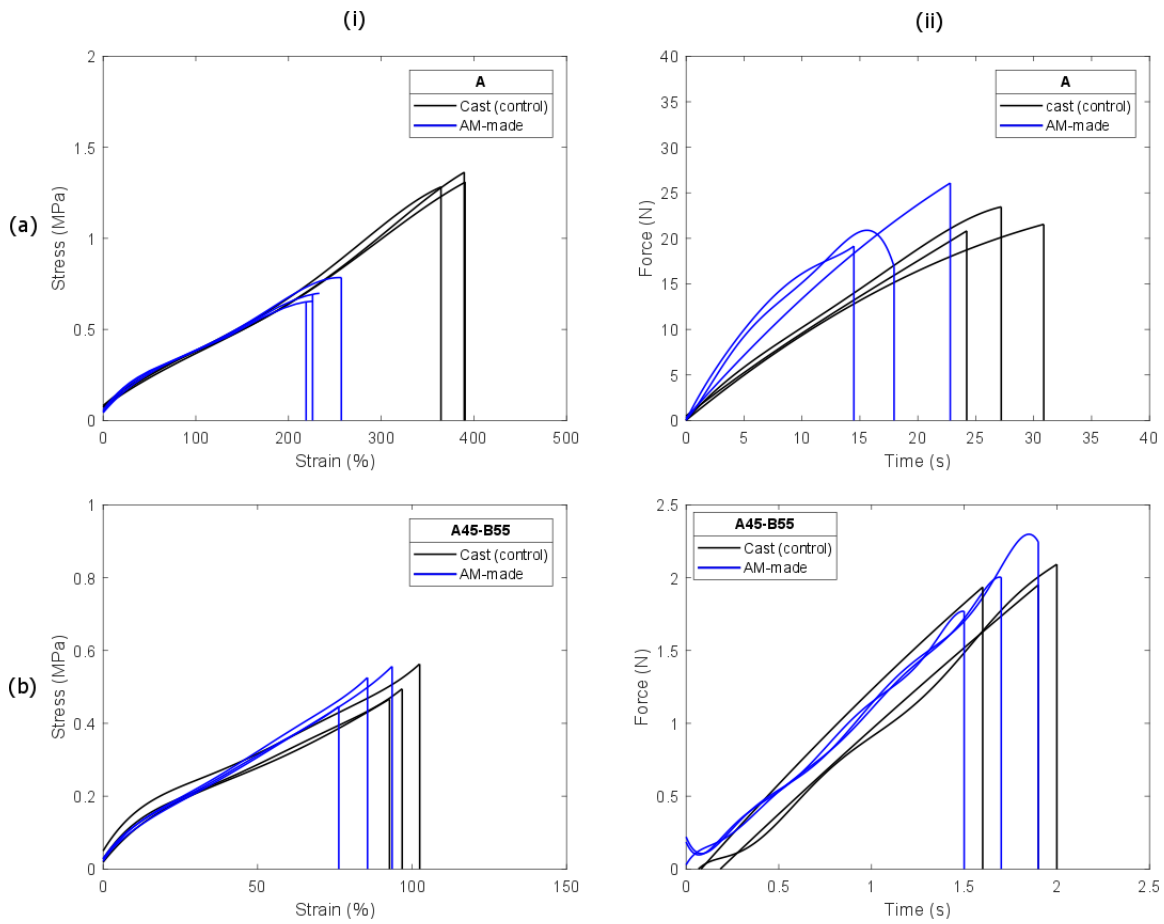


Figure E.2: (a-i) Tensile test and (a-ii) tearing test curves for ink A. (b-i) Tensile test and (b-ii) tearing test curves for ink 45A-55B.

## E.2 Experiments of Chapter 6

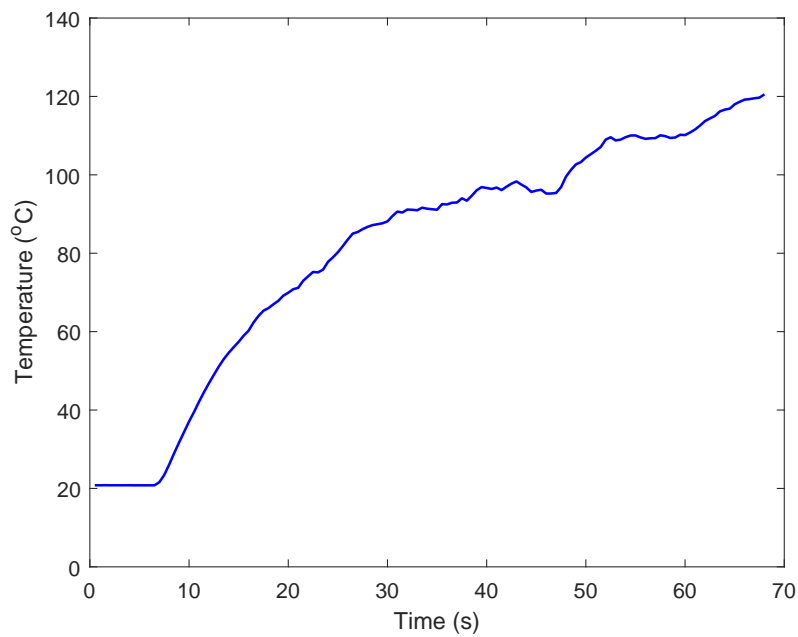


Figure E.3: Temperature of the powder bed vs. time.