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Data Article

Data on removal kinetics of pharmaceutical compounds, artificial sweeteners, and perfluoroalkyl substances from water using a passive treatment system containing zero-valent iron and biochar



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ABSTRACT

The data presented in this paper relate to the research paper “Removal of pharmaceutical compounds, artificial sweeteners, and perfluoroalkyl substances from water using a passive treatment system containing zero-valent iron and biochar” [1]. Four columns packed with different ratios of reactive media, including silica sand (SS), zero-valent iron (ZVI), and biochar (BC), were evaluated for simultaneous removal of 14 emerging contaminants from water. The target emerging contaminants included eight pharmaceuticals (carbamazepine, caffeine, sulfamethoxazole, 3,4-methylenedioxyamphetamine, 3,4-methylenedioxymethamphetamine, ibuprofen, gemfibrozil, and naproxen), four artificial sweeteners (acesulfame-K, sucralose, saccharin, and cyclamate), and two perfluoroalkyl substances (perfluorooctanoic acid and perfluorooctane sulfonic acid). The samples for target contaminant analysis were collected from the influent, effluent, and profile (along the flow direction) ports of each column. The removal data (concentration vs. residence time) for each target contaminant were fitted to the first-order (exponential decay equation) or zero-order (linear equation) model using SigmaPlot. The removal rate, removal rate constant (k_{obs}), mass normalized rate constant (k_M), surface area

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normalized rate constant (k_{SA} , specific reaction rate constant), and half-life ($t_{0.5}$) of target contaminants in Columns ZVI, BC, and (ZVI + BC) were calculated and summarized in this dataset.

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Specifications Table

Subject	Chemistry
Specific subject area	Organic chemistry, removal kinetics
Type of data	Table
How data were acquired	Software SigmaPlot
Data format	Analyzed
Parameters for data collection	The first-order kinetic data were obtained through the exponential decay fitting in the Regression Wizard in SigmaPlot; the zero-order kinetic data were obtained through the linear fitting in Regression Wizard in SigmaPlot.
Description of data collection	The removal kinetic data were collected through the data analysis (Regression Wizard) in SigmaPlot.
Data source location	University of Waterloo, Waterloo, Ontario Canada
Data accessibility	Data are available in this article
Related research article	YingYing Liu, David W. Blowes, Carol J. Ptacek, and Laura G. Groza Removal of pharmaceutical compounds, artificial sweeteners, and perfluoroalkyl substances from water using a passive treatment system containing zero-valent iron and biochar Science of the Total Environment https://doi.org/10.1016/j.scitotenv.2019.06.450

Value of the Data

- The data in this article provide important information on degradation kinetics such as removal rates and half-lives for 14 emerging contaminants treated by zero-valent iron (ZVI) and biochar (BC).
- Researchers working in the field of remediation of emerging contaminants in water can benefit from the data in this article.
- The data present in this article can provide useful information and guidelines for selecting the appropriate types of reactive media to remove specific emerging contaminants.
- The removal kinetic data (removal rate and half-life) can be used to design reactors or permeable reactive barriers (PRBs) for future large-scale field applications.

1. Data

The dataset showed the removal kinetic parameters, including removal rate constant (k_{obs}), mass normalized rate constant (k_M), surface area normalized rate constant (k_{SA} , specific reaction rate constant), and half-life ($t_{0.5}$), for 14 target emerging contaminants in Column ZVI, Column BC, and Column (ZVI + BC). The kinetic parameters for each contaminant are summarized in separate tables (Tables 1–14). The raw data (concentration vs. residence time) of each contaminant can be found in the related research article [1].

2. Experimental design, materials, and methods

2.1. Materials

The native analyte compounds carbamazepine (CBZ), caffeine (CAF), sulfamethoxazole (SMX), ibuprofen (IBU), gemfibrozil (GEM), naproxen (NAP), cyclamate (CYC), and saccharin (SAC) for calibration standards and input stock solution were obtained from Sigma-Aldrich (Oakville, ON, Canada).

Table 1

First-order removal rate constant (k_{obs}), mass normalized rate constant (k_M), surface area normalized rate constant (k_{SA} , specific reaction rate constant), and half-life ($t_{0.5}$) of pharmaceutical **carbamazepine** in Column ZVI, Column BC, and Column (ZVI + BC). k_{obs} is calculated using least-squares regression during two experimental stages. tC is the carbamazepine concentration.

Column	Stage	PV	Removal rate ^t , $\mu\text{mol L}^{-1} \text{d}^{-1}$ ($\mu\text{g L}^{-1} \text{d}^{-1}$)	k_{obs} , d^{-1}	k_M , $\text{L g}^{-1} \text{d}^{-1}$	k_{SA} , $\text{L m}^{-2} \text{d}^{-1}$	$t_{0.5}$, d	R^2	
Column 2 (ZVI)	1	1	$1.1\text{E}+01 \times C$	$1.1\text{E}+01$	$2.6\text{E}-03$	$2.8\text{E}-04$	0.06	0.999	
		13	$4.9 \times C$	4.9	$1.1\text{E}-03$	$1.2\text{E}-04$	0.14	0.975	
		25	$4.4 \times C$	4.4	$1.0\text{E}-03$	$1.1\text{E}-04$	0.16	0.965	
Column 3 (BC)	2	53	$1.2 \times C$	1.2	$2.9\text{E}-04$	$3.0\text{E}-05$	0.56	0.931	
		1	1	$5.4 \times C$	5.4	$1.2\text{E}-02$	$1.8\text{E}-04$	0.19	0.998
			13	$2.5 \times C$	2.5	$5.3\text{E}-03$	$8.2\text{E}-05$	0.28	0.998
Column 4 (ZVI + BC)	2	25	$1.9 \times C$	1.9	$4.2\text{E}-03$	$6.4\text{E}-05$	0.36	0.996	
		53	$0.7 \times C$	0.7	$1.5\text{E}-03$	$2.3\text{E}-05$	1.0	0.970	
		1	1	$8.2 \times C$	8.2	$7.2\text{E}-03$	$2.1\text{E}-04$	0.09	0.999
	13		$4.5 \times C$	4.5	$3.9\text{E}-03$	$1.2\text{E}-04$	0.16	0.966	
	2	53	$1.3 \times C$	1.3	$1.1\text{E}-03$	$3.3\text{E}-05$	0.55	0.992	

Table 2

First-order removal rate constant (k_{obs}), mass normalized rate constant (k_M), surface area normalized rate constant (k_{SA} , specific reaction rate constant), and half-life ($t_{0.5}$) of pharmaceutical **caffeine** in Column ZVI, Column BC, and Column (ZVI + BC). k_{obs} is calculated using least-squares regression during two experimental stages. tC is the caffeine concentration.

Column	Stage	PV	Removal rate ^t , $\mu\text{mol L}^{-1} \text{d}^{-1}$ ($\mu\text{g L}^{-1} \text{d}^{-1}$)	k_{obs} , d^{-1}	k_M , $\text{L g}^{-1} \text{d}^{-1}$	k_{SA} , $\text{L m}^{-2} \text{d}^{-1}$	$t_{0.5}$, d	R^2	
Column 2 (ZVI)	1	1	$1.6\text{E}+01 \times C$	$1.6\text{E}+01$	$3.7\text{E}-03$	$3.9\text{E}-04$	0.04	0.999	
		13	$7.2 \times C$	7.2	$1.7\text{E}-03$	$1.8\text{E}-04$	0.10	0.998	
		25	$5.1 \times C$	5.1	$1.2\text{E}-03$	$1.2\text{E}-04$	0.14	0.982	
Column 3 (BC)	2	53	$1.5 \times C$	1.5	$3.5\text{E}-04$	$3.6\text{E}-05$	0.47	0.961	
		1	1	$4.8 \times C$	4.8	$1.0\text{E}-02$	$1.6\text{E}-04$	0.14	0.999
			13	$2.8 \times C$	2.8	$6.0\text{E}-03$	$9.4\text{E}-05$	0.25	0.999
	2	25	$2.2 \times C$	2.2	$4.8\text{E}-03$	$7.4\text{E}-05$	0.31	0.996	
		53	$1.0 \times C$	1.0	$2.1\text{E}-03$	$3.3\text{E}-05$	0.70	0.973	
Column 4 (ZVI + BC)	1	1	$6.9 \times C$	6.9	$6.0\text{E}-03$	$1.8\text{E}-04$	0.10	0.996	
		13	$5.5 \times C$	5.5	$4.8\text{E}-03$	$1.4\text{E}-04$	0.13	0.989	
		25	$4.5 \times C$	4.5	$3.9\text{E}-03$	$1.2\text{E}-04$	0.15	0.973	
	2	53	$1.7 \times C$	1.7	$1.5\text{E}-03$	$4.5\text{E}-05$	0.40	0.996	

Table 3

First-order removal rate constant (k_{obs}), mass normalized rate constant (k_M), surface area normalized rate constant (k_{SA} , specific reaction rate constant), and half-life ($t_{0.5}$) of pharmaceutical **sulfamethoxazole** in Column ZVI, Column BC, and Column (ZVI + BC). k_{obs} is calculated using least-squares regression during two experimental stages. tC is the sulfamethoxazole concentration. “–” represents not applicable.

Column	Stage	PV	Removal rate ^t , $\mu\text{mol L}^{-1} \text{d}^{-1}$ ($\mu\text{g L}^{-1} \text{d}^{-1}$)	k_{obs} , d^{-1}	k_M , $\text{L g}^{-1} \text{d}^{-1}$	k_{SA} , $\text{L m}^{-2} \text{d}^{-1}$	$t_{0.5}$, d	R^2
Column 1 (Control)	1	25	$0.2 \times C$	0.2	–	–	3.6	0.877
	2	53	$0.4 \times C$	0.4	–	–	1.8	0.984
Column 2 (ZVI)	1	1	$4.5\text{E}+02 \times C$	$4.5\text{E}+02$	$1.1\text{E}-01$	$1.1\text{E}-02$	0.002	1.000
		13	$4.7\text{E}+02 \times C$	$4.7\text{E}+02$	$1.1\text{E}-01$	$1.1\text{E}-02$	0.001	1.000
		25	$4.6\text{E}+02 \times C$	$4.6\text{E}+02$	$1.1\text{E}-01$	$1.1\text{E}-02$	0.001	1.000
		53	$1.5\text{E}+02 \times C$	$1.5\text{E}+02$	$3.5\text{E}-02$	$3.7\text{E}-03$	0.005	1.000
Column 3 (BC)	1	1	$1.6 \times C$	1.6	$3.5\text{E}-03$	$5.4\text{E}-05$	0.43	0.999
		13	$1.2 \times C$	1.2	$2.5\text{E}-03$	$3.8\text{E}-05$	0.60	0.999
		25	$1.1 \times C$	1.1	$2.4\text{E}-03$	$3.8\text{E}-05$	0.61	0.993
	2	53	$0.5 \times C$	0.5	$1.1\text{E}-03$	$1.7\text{E}-05$	1.4	0.991
		1	1	$4.5\text{E}+02 \times C$	$4.5\text{E}+02$	$4.0\text{E}-01$	$1.2\text{E}-02$	0.002
13	$4.7\text{E}+02 \times C$		$4.7\text{E}+02$	$4.1\text{E}-01$	$1.2\text{E}-02$	0.001	1.000	
25	$4.6\text{E}+02 \times C$		$4.6\text{E}+02$	$4.1\text{E}-01$	$1.2\text{E}-02$	0.001	1.000	
2	53	$1.5\text{E}+02 \times C$	$1.5\text{E}+02$	$1.3\text{E}-01$	$3.9\text{E}-03$	0.005	1.000	

Table 4

First-order removal rate constant (k_{obs}), mass normalized rate constant (k_M), surface area normalized rate constant (k_{SA} , specific reaction rate constant), and half-life ($t_{0.5}$) of pharmaceutical **3,4-methylenedioxyamphetamine (MDA)** in Column ZVI, Column BC, and Column (ZVI + BC). k_{obs} is calculated using least-squares regression during two experimental stages. tC is the MDA concentration.

Column	Stage	PV	Removal rate ^t , $\mu\text{mol L}^{-1} \text{d}^{-1}$ ($\mu\text{g L}^{-1} \text{d}^{-1}$)	k_{obs} , d^{-1}	k_M , $\text{L g}^{-1} \text{d}^{-1}$	k_{SA} , $\text{L m}^{-2} \text{d}^{-1}$	$t_{0.5}$, d	R^2
Column 2 (ZVI)	1	1	$1.9\text{E}+02 \times C$	1.9E+02	4.3E-02	4.6E-03	0.004	1.000
		13	$1.3\text{E}+01 \times C$	1.3E+01	3.0E-03	3.1E-04	0.06	0.999
		25	$7.8 \times C$	7.8	1.8E-03	1.9E-04	0.09	0.998
Column 3 (BC)	1	1	$1.1\text{E}+01 \times C$	1.1E+01	2.4E-02	3.7E-04	0.06	0.999
		13	$8.1 \times C$	8.1	1.7E-02	2.7E-04	0.09	0.997
		25	$5.1 \times C$	5.1	1.1E-02	1.7E-04	0.14	0.998
Column 4 (ZVI + BC)	1	1	$2.0\text{E}+01 \times C$	2.0E+01	1.8E-02	5.3E-04	0.03	1.000
		13	$1.2\text{E}+01 \times C$	1.2E+01	1.0E-02	3.0E-04	0.06	0.999
		25	$8.7 \times C$	8.7	7.6E-03	2.3E-04	0.08	0.999
	2	53	$3.9 \times C$	3.9	3.4E-03	1.0E-04	0.18	0.999

Table 5

First-order removal rate constant (k_{obs}), mass normalized rate constant (k_M), surface area normalized rate constant (k_{SA} , specific reaction rate constant), and half-life ($t_{0.5}$) of pharmaceutical **3,4-methylenedioxymethamphetamine (MDMA)** in Column ZVI, Column BC, and Column (ZVI + BC). k_{obs} is calculated using least-squares regression during two experimental stages. tC is the MDMA concentration.

Column	Stage	PV	Removal rate ^t , $\mu\text{mol L}^{-1} \text{d}^{-1}$ ($\mu\text{g L}^{-1} \text{d}^{-1}$)	k_{obs} , d^{-1}	k_M , $\text{L g}^{-1} \text{d}^{-1}$	k_{SA} , $\text{L m}^{-2} \text{d}^{-1}$	$t_{0.5}$, d	R^2
Column 2 (ZVI)	1	1	$3.0\text{E}+02 \times C$	3.0E+02	6.9E-02	7.3E-03	0.002	1.000
		13	$3.5\text{E}+02 \times C$	3.5E+02	8.2E-02	8.7E-03	0.002	1.000
		25	$1.4\text{E}+01 \times C$	1.4E+01	3.2E-03	3.4E-04	0.05	1.000
Column 3 (BC)	1	1	$1.1\text{E}+01 \times C$	1.1E+01	2.3E-02	3.6E-04	0.07	0.999
		13	$7.7 \times C$	7.7	1.7E-02	2.6E-04	0.09	0.998
		25	$5.2 \times C$	5.2	1.1E-02	1.7E-04	0.13	0.997
Column 4 (ZVI + BC)	1	1	$2.5\text{E}+01 \times C$	2.5E+01	2.2E-02	6.6E-04	0.03	1.000
		13	$1.6\text{E}+01 \times C$	1.6E+01	1.4E-02	4.1E-04	0.04	1.000
		25	$1.0\text{E}+01 \times C$	1.0E+01	9.0E-03	2.7E-04	0.07	0.999
	2	53	$4.3 \times C$	4.3	3.8E-03	1.1E-04	0.16	1.000

Table 6

First-order removal rate constant (k_{obs}), mass normalized rate constant (k_M), surface area normalized rate constant (k_{SA} , specific reaction rate constant), and half-life ($t_{0.5}$) of pharmaceutical **ibuprofen** in Column ZVI, Column BC, and Column (ZVI + BC). k_{obs} is calculated using least-squares regression during two experimental stages. tC is the ibuprofen concentration.

Column	Stage	PV	Removal rate ^t , $\mu\text{mol L}^{-1} \text{d}^{-1}$ ($\mu\text{g L}^{-1} \text{d}^{-1}$)	k_{obs} , d^{-1}	k_M , $\text{L g}^{-1} \text{d}^{-1}$	k_{SA} , $\text{L m}^{-2} \text{d}^{-1}$	$t_{0.5}$, d	R^2
Column 2 (ZVI)	1	1	$2.6 \times C$	2.6	6.0E-04	6.3E-05	0.27	0.943
		13	$1.2 \times C$	1.2	2.9E-04	3.0E-05	0.56	0.926
		25	$0.9 \times C$	0.9	2.2E-04	2.3E-05	0.74	0.932
Column 3 (BC)	1	1	$1.9 \times C$	1.9	4.7E-05	4.9E-06	3.5	0.864
		13	$1.2 \times C$	1.2	4.2E-03	6.5E-05	0.36	0.992
		25	$1.1 \times C$	1.1	2.6E-03	4.0E-05	0.57	0.997
Column 4 (ZVI + BC)	1	1	$0.4 \times C$	0.4	2.4E-03	3.7E-05	0.63	0.996
		13	$1.1 \times C$	1.1	2.4E-03	3.7E-05	0.63	0.996
		25	$0.4 \times C$	0.4	8.9E-04	1.4E-05	1.7	0.992
Column 4 (ZVI + BC)	2	1	$2.9 \times C$	2.9	2.5E-03	7.6E-05	0.24	0.978
		13	$1.7 \times C$	1.7	1.5E-03	4.5E-05	0.41	0.958
		25	$1.6 \times C$	1.6	1.4E-03	4.1E-05	0.44	0.952
	2	53	$0.5 \times C$	0.5	4.0E-04	1.2E-05	1.5	0.941

Table 7

First-order removal rate constant (k_{obs}), mass normalized rate constant (k_M), surface area normalized rate constant (k_{SA} , specific reaction rate constant), and half-life ($t_{0.5}$) of pharmaceutical **gemfibrozil** in Column ZVI, Column BC, and Column (ZVI + BC). k_{obs} is calculated using least-squares regression during two experimental stages. tC is the gemfibrozil concentration.

Column	Stage	PV	Removal rate ^t , $\mu\text{mol L}^{-1} \text{d}^{-1}$ ($\mu\text{g L}^{-1} \text{d}^{-1}$)	k_{obs} , d^{-1}	k_M , $\text{L g}^{-1} \text{d}^{-1}$	k_{SA} , $\text{L m}^{-2} \text{d}^{-1}$	$t_{0.5}$, d	R^2	
Column 2 (ZVI)	1	1	$9.3 \times C$	9.3	2.2E-03	2.3E-04	0.07	0.999	
		13	$4.6 \times C$	4.6	1.1E-03	1.1E-04	0.15	0.969	
		25	$3.5 \times C$	3.5	8.2E-04	8.6E-05	0.20	0.954	
Column 3 (BC)	2	53	$1.0 \times C$	1.0	2.4E-04	2.5E-05	0.67	0.927	
		1	1	$4.5 \times C$	4.5	9.7E-03	1.5E-04	0.15	0.997
			13	$2.4 \times C$	2.4	5.1E-03	8.0E-05	0.29	0.995
Column 4 (ZVI + BC)	2	25	$1.8 \times C$	1.8	3.8E-03	5.9E-05	0.39	0.996	
		53	$0.6 \times C$	0.6	1.4E-03	2.1E-05	1.1	0.981	
		1	1	$5.9 \times C$	5.9	5.1E-03	1.5E-04	0.12	0.990
	13		$3.5 \times C$	3.5	3.1E-03	9.2E-05	0.20	0.967	
	25		$2.8 \times C$	2.8	2.5E-03	7.4E-05	0.24	0.935	
	2	53	$0.9 \times C$	0.9	7.6E-04	2.3E-05	0.80	0.989	

Table 8

First-order removal rate constant (k_{obs}), mass normalized rate constant (k_M), surface area normalized rate constant (k_{SA} , specific reaction rate constant), and half-life ($t_{0.5}$) of pharmaceutical **naproxen** in Column ZVI, Column BC, and Column (ZVI + BC). k_{obs} is calculated using least-squares regression during two experimental stages. tC is the naproxen concentration.

Column	Stage	PV	Removal rate ^t , $\mu\text{mol L}^{-1} \text{d}^{-1}$ ($\mu\text{g L}^{-1} \text{d}^{-1}$)	k_{obs} , d^{-1}	k_M , $\text{L g}^{-1} \text{d}^{-1}$	k_{SA} , $\text{L m}^{-2} \text{d}^{-1}$	$t_{0.5}$, d	R^2	
Column 2 (ZVI)	1	1	$5.7 \times C$	5.7	1.3E-03	1.4E-04	0.12	0.988	
		13	$3.1 \times C$	3.1	7.2E-04	7.6E-05	0.22	0.908	
		25	$2.8 \times C$	2.8	6.4E-04	6.8E-05	0.25	0.949	
Column 3 (BC)	2	53	$0.6 \times C$	0.6	1.4E-04	1.5E-05	1.2	0.941	
		1	1	$3.7 \times C$	3.7	8.0E-03	1.2E-04	0.19	0.999
			13	$2.0 \times C$	2.0	4.2E-03	6.6E-05	0.35	0.996
Column 4 (ZVI + BC)	2	25	$1.7 \times C$	1.7	3.6E-03	5.6E-05	0.41	0.999	
		53	$0.6 \times C$	0.6	1.4E-03	2.2E-05	1.1	0.985	
		1	1	$4.7 \times C$	4.7	4.1E-03	1.2E-04	0.15	0.978
	13		$3.0 \times C$	3.0	2.6E-03	7.7E-05	0.23	0.959	
	25		$2.6 \times C$	2.6	2.2E-03	6.7E-05	0.27	0.977	
	2	53	$0.7 \times C$	0.7	6.5E-04	1.9E-05	0.94	0.980	

The isotope-labeled standards CBZ-d10, CAF-d3, IBU-d3, GEM-d6, and [¹³C]-NAP were obtained from Cambridge Isotope Laboratory Inc. (Tewksbury, MA, USA). The native analytes acesulfame-K (ACE-K), sucralose (SCL), and the isotope-labeled standards SMX-d4, CYC-d11, SAC-¹³C6, ACE-K-d4, and SCL-d6 were obtained from Toronto Research Chemicals Inc. (Toronto, ON, Canada). The native analytes 3,4-methylenedioxyamphetamine (MDA), 3,4-methylenedioxymethamphetamine (MDMA), and isotope-labeled MDA-d5 and MDMA-d5 were obtained from Cerilliant Corporation (Round Rock, TX, USA). The native analytes perfluorooctanoic acid (PFOA), perfluorooctane sulfonic acid (PFOS), and their isotope-labeled standards [¹³C]-PFOA and [¹³C]-PFOS were obtained from Wellington Laboratories Inc. (Guelph, ON, Canada). The analytes PFOA and PFOS as dry powder for preparation of the input stock solution were obtained from Sigma-Aldrich, Canada. The silica sand (SS; 0.6–0.8 mm) was obtained from US Silica Company Inc. (Ottawa, IL, USA). The granular zero-valent iron (ZVI; 0.25–1.19 mm) was obtained from Connelly-GPM Inc. (Chicago, IL, USA). The biochar (BC; oak hard wood; 0.50–2.36 mm) was obtained from Cowboy Charcoal Co. (Brentwood, TN, USA).

2.2. Column experimental design

Four acrylic columns were used, each column was 30 cm in length and 5 cm inner diameter. Influent and effluent ports were installed on the bottom and top of each column, respectively, for introducing

Table 9

Zero- or first-order removal rate constant (k_{obs}), mass normalized rate constant (k_M), surface area normalized rate constant (k_{SA} , specific reaction rate constant), and half-life ($t_{0.5}$) of artificial sweetener **acesulfame-K** in Column ZVI, Column BC, and Column (ZVI + BC). Removal rate constant k_{obs} is calculated using least-squares regression during two experimental stages. ^cC is the acesulfame-K concentration. “—” represents no removal of acesulfame-K was observed.

Column	Stage	PV	Removal rate ^c , $\mu\text{mol L}^{-1} \text{d}^{-1}$ ($\mu\text{g L}^{-1} \text{d}^{-1}$)	k_{obs}	k_M	k_{SA}	$t_{0.5}$	R^2
Column 2 (ZVI)	1	1	$2.3\text{E-}01 \times \text{C}^a$	$2.3\text{E-}01^a$	$5.3\text{E-}05^a$	$5.6\text{E-}06^a$	3.1	0.749
		13	$1.0\text{E-}01 \times \text{C}^a$	$1.0\text{E-}01^a$	$2.4\text{E-}05^a$	$2.6\text{E-}06^a$	6.6	0.906
		25	$9.8\text{E-}02 \times \text{C}^a$	$9.8\text{E-}02^a$	$2.3\text{E-}05^a$	$2.4\text{E-}06^a$	7.0	0.874
Column 3 (BC)	1	1	$1.1\text{E-}01 \times \text{C}^a$	$1.1\text{E-}01^a$	$2.7\text{E-}05^a$	$2.8\text{E-}06^a$	6.1	0.870
		13	$1.6 \text{E}+01^b$	$1.6 \text{E}+01^b$	$3.4\text{E-}02^b$	$5.3\text{E-}04^b$	3.2	0.864
		25	—	—	—	—	—	—
Column 4 (ZVI + BC)	1	1	5.9^b	5.8^b	$5.1\text{E-}03^b$	$1.5\text{E-}04^b$	8.3	0.976
		13	4.2^b	4.2^b	$3.7\text{E-}03^b$	$1.1\text{E-}04^b$	12	0.634
		25	4.9^b	4.9^b	$4.3\text{E-}03^b$	$1.3\text{E-}04^b$	10	0.835
Column 4 (ZVI + BC)	2	1	3.2^b	3.2^b	$2.8\text{E-}03^b$	$8.3\text{E-}05^b$	17	0.866
		13	—	—	—	—	—	—
		25	—	—	—	—	—	—

^a Removal of acesulfame-K followed a first-order reaction rate, unit of k_{obs} is d^{-1} , unit of k_M is $\text{L g}^{-1} \text{d}^{-1}$, unit of k_{SA} is $\text{L m}^{-2} \text{d}^{-1}$.

^b Removal of acesulfame-K followed a zero-order reaction rate, unit of k_{obs} is $\mu\text{mol acesulfame-K L}^{-1} \text{d}^{-1}$ ($\mu\text{g acesulfame-K L}^{-1} \text{d}^{-1}$), unit of k_M is $\mu\text{mol acesulfame-K d}^{-1} \text{g}^{-1}$ ($\mu\text{g acesulfame-K d}^{-1} \text{g}^{-1}$), unit of k_{SA} is $\mu\text{mol acesulfame-K d}^{-1} \text{m}^{-2}$ ($\mu\text{g acesulfame-K d}^{-1} \text{m}^{-2}$).

input solution and discharging effluent. Seven sampling ports were installed along the length of each column at 3.75-cm intervals for profile sampling. Column *Control* was packed with 100% SS. Column ZVI and Column BC were packed with 50% (vol%) of ZVI and BC, respectively, and balanced with SS. Column (ZVI + BC) was packed with 10% (vol%) of ZVI, 40% (vol%) of BC, and balanced with SS.

Input solution contained $10 \mu\text{g L}^{-1}$ of pharmaceuticals CBZ, CAF, SMX, MDA, MDMA, IBU, GEM, and NAP; $100 \mu\text{g L}^{-1}$ of artificial sweeteners ACE-K, CYC, SAC, and SCL; and $50 \mu\text{g L}^{-1}$ of PFOA and 20–100 $\mu\text{g L}^{-1}$ of PFOS. The input solution was pumped through four columns from bottom to top at a flow rate of 0.3 pore volume (PV) d^{-1} before 50 PV during the first stage of the experiment; the flow rate was decreased to 0.1 PV d^{-1} after 50 PV during the second stage of the experiment. Three profile samplings (along the length of the columns) were performed during the first stage of the experiment after 1, 13, and 25 PV of flow through the columns; one profile sampling was conducted during the second stage of the experiment after 53 PV of flow.

All the emerging contaminant samples were spiked with isotopically-labeled internal standards before analysis. The pharmaceutical, PFOA, and PFOS samples were then concentrated through a solid phase extraction (SPE) process; their concentrations were determined using liquid chromatography (LC) followed by tandem mass spectrometry (MS). The concentrations of artificial sweeteners were directly analyzed by ion chromatography (IC) followed by MS without SPE. Detailed information on column experimental setup and analytical procedures for target emerging contaminants are summarized by Liu et al. [1].

2.3. Removal kinetics of target emerging contaminants by ZVI, BC, and (ZVI + BC)

The removal rates (k_{obs}) for target emerging contaminants during two experimental stages were calculated using least-squares regression in SigmaPlot. The removal of target pharmaceuticals within Columns ZVI, BC, and (ZVI+BC) followed a first-order rate model reported by Liu et al. [1] that can be described by equation (1). k_M and k_{SA} were calculated according to equations (2) and (3) which are defined by Johnson et al. [2]. The half-life ($t_{0.5}$) of the first-order rate for target pharmaceuticals was calculated following equation (4).

$$-\frac{dC}{dt} = k_{obs} C \quad (1)$$

Table 10

Zero-order removal rate constant (k_{obs}), mass normalized rate constant (k_M), surface area normalized rate constant (k_{SA} , specific reaction rate constant), and half-life ($t_{0.5}$) of artificial sweetener **cyclamate** in Column ZVI, Column BC, and Column (ZVI + BC). Removal rate constant k_{obs} is calculated using least-squares regression during two experimental stages. “–” represents no removal of cyclamate was observed.

Column	Stage	PV	Removal rate, $\mu\text{mol L}^{-1} \text{d}^{-1}$ ($\mu\text{g L}^{-1} \text{d}^{-1}$)	k_{obs} , $\mu\text{mol L}^{-1} \text{d}^{-1}$ ($\mu\text{g L}^{-1} \text{d}^{-1}$)	k_M , $\mu\text{mol g}^{-1} \text{d}^{-1}$ ($\mu\text{g g}^{-1} \text{d}^{-1}$)	k_{SA} , $\mu\text{mol m}^{-2} \text{d}^{-1}$ ($\mu\text{g m}^{-2} \text{d}^{-1}$)	$t_{0.5}$, d	R^2
Column 2 (ZVI)	1	1	1.5E+01	1.5E+01	3.6E-03	3.8E-04	3.3	0.697
		13	–	–	–	–	–	–
		25	–	–	–	–	–	–
Column 3 (BC)	1	1	8.4	8.4	1.8E-02	2.8E-04	5.8	0.839
		13	–	–	–	–	–	–
		25	–	–	–	–	–	–
Column 4 (ZVI + BC)	2	53	–	–	–	–	–	–
		1	1	2.0	2.0	1.8E-03	5.2E-05	23
	1	13	–	–	–	–	–	–
		25	–	–	–	–	–	–
2	53	–	–	–	–	–	–	

Note: The poor R^2 values at 1 PV in this table are likely due to little removal of cyclamate in the three treatment columns.

Table 11

Zero- or first-order removal constant (k_{obs}), mass normalized rate constant (k_M), surface area normalized rate constant (k_{SA} , specific reaction rate constant), and half-life ($t_{0.5}$) of artificial sweetener **saccharin** in Column ZVI, Column BC, and Column (ZVI + BC). Removal rate constant k_{obs} is calculated using least-squares regression during two experimental stages. tC is the saccharin concentration. “–” represents no removal of saccharin was observed.

Column	Stage	PV	Removal rate ^t , $\mu\text{mol L}^{-1} \text{d}^{-1}$ ($\mu\text{g L}^{-1} \text{d}^{-1}$)	k_{obs}	k_M	k_{SA}	$t_{0.5}$, d	R^2
Column 2 (ZVI)	1	1	3.5E+01 ^b	3.5E+01 ^b	8.1E-03 ^b	8.6E-04 ^b	1.5	0.898
		13	4.7 ^b	4.7 ^b	1.1E-03 ^b	1.2E-04 ^b	9.3	0.804
		25	–	–	–	–	–	–
Column 3 (BC)	1	53	1.7 ^b	1.7 ^b	3.9E-04 ^b	4.1E-05 ^b	32	0.583
		1	1.0 × C ^a	1.0 ^a	2.2E-03 ^a	3.4E-05 ^a	0.7	0.978
		13	0.5 × C ^a	0.5 ^a	9.8E-04 ^a	1.5E-05 ^a	1.5	0.981
Column 4 (ZVI + BC)	2	25	2.4E+01 ^b	2.4E+01 ^b	5.2E-02 ^b	8.0E-04 ^b	2.2	0.983
		53	2.6 ^b	2.6 ^b	5.6E-03 ^b	8.6E-05 ^b	21	0.828
		1	3.4E+01 ^b	3.4E+01 ^b	3.0E-02 ^b	8.9E-04 ^b	1.3	0.969
	1	13	1.4E+01 ^b	1.4E+01 ^b	1.2E-02 ^b	3.6E-04 ^b	3.1	0.960
		25	1.1E+01 ^b	1.1E+01 ^b	9.4E-03 ^b	2.8E-04 ^b	4.9	0.845
2	53	2.1 ^b	2.1 ^b	1.9E-03 ^b	5.6E-05 ^b	25	0.701	

^a Removal of saccharin followed a first-order reaction rate, unit of k_{obs} is d^{-1} , unit of k_M is $\text{L g}^{-1} \text{d}^{-1}$, unit of k_{SA} is $\text{L m}^{-2} \text{d}^{-1}$.

^b Removal of saccharin followed a zero-order reaction rate, unit of k_{obs} is $\mu\text{mol saccharin L}^{-1} \text{d}^{-1}$ ($\mu\text{g saccharin L}^{-1} \text{d}^{-1}$), unit of k_M is $\mu\text{mol saccharin d}^{-1} \text{g}^{-1}$ ($\mu\text{g saccharin d}^{-1} \text{g}^{-1}$), unit of k_{SA} is $\mu\text{mol saccharin d}^{-1} \text{m}^{-2}$ ($\mu\text{g saccharin d}^{-1} \text{m}^{-2}$).

Table 12

Zero- or first-order removal constant (k_{obs}), mass normalized rate constant (k_M), surface area normalized rate constant (k_{SA} , specific reaction rate constant), and half-life ($t_{0.5}$) of artificial sweetener **sucralose** in Column ZVI, Column BC, and Column (ZVI + BC). Removal rate constant k_{obs} is calculated using least-squares regression during two experimental stages. tC is the sucralose concentration.

Column	Stage	PV	Removal rate ^t , $\mu\text{mol L}^{-1} \text{d}^{-1}$ ($\mu\text{g L}^{-1} \text{d}^{-1}$)	k_{obs}	k_M	k_{SA}	$t_{0.5}$, d	R^2
Column 2 (ZVI)	1	1	2.1 × C ^a	2.1 ^a	4.8E-04 ^a	5.1E-05 ^a	0.3	0.922
		13	1.0 × C ^a	1.0 ^a	2.4E-04 ^a	2.5E-05 ^a	0.7	0.927
		25	4.4E+01 ^b	4.4E+01 ^b	1.0E-02 ^b	1.1E-03 ^b	1.4	0.963
Column 3 (BC)	2	53	1.2E+01 ^b	1.2E+01 ^b	2.8E-03 ^b	2.9E-04 ^b	4.9	0.995
		1	1.3 × C ^a	1.3 ^a	2.7E-03 ^a	4.2E-05 ^a	0.5	0.999
		13	0.9 × C ^a	0.9 ^a	1.9E-03 ^a	2.9E-05 ^a	0.8	0.983
Column 4 (ZVI + BC)	2	25	0.7 × C ^a	0.7 ^a	1.4E-03 ^a	2.2E-05 ^a	1.1	0.983
		53	0.2 × C ^a	0.2 ^a	4.3E-04 ^a	6.6E-06 ^a	3.5	0.981
		1	1.6 × C ^a	1.6 ^a	1.4E-03 ^a	4.2E-05 ^a	0.4	0.948
	1	13	0.9 × C ^a	0.9 ^a	8.1E-04 ^a	2.4E-05 ^a	0.8	0.961
		25	0.7 × C ^a	0.7 ^a	6.4E-04 ^a	1.9E-05 ^a	1.0	0.942
2	53	0.2 × C ^a	0.2 ^a	1.6E-04 ^a	4.7E-06 ^a	3.9	0.995	

^a Removal of sucralose followed a first-order reaction rate, unit of k_{obs} is d^{-1} , unit of k_M is $\text{L g}^{-1} \text{d}^{-1}$, unit of k_{SA} is $\text{L m}^{-2} \text{d}^{-1}$.

^b Removal of sucralose followed a zero-order reaction rate, unit of k_{obs} is $\mu\text{mol sucralose L}^{-1} \text{d}^{-1}$ ($\mu\text{g sucralose L}^{-1} \text{d}^{-1}$), unit of k_M is $\mu\text{mol sucralose d}^{-1} \text{g}^{-1}$ ($\mu\text{g sucralose d}^{-1} \text{g}^{-1}$), unit of k_{SA} is $\mu\text{mol sucralose d}^{-1} \text{m}^{-2}$ ($\mu\text{g sucralose d}^{-1} \text{m}^{-2}$).

$$k_M = \frac{k_{obs}}{\rho_m} \quad (2)$$

$$k_{SA} = \frac{k_{obs}}{\rho_a} = \frac{k_M}{a_s} \quad (3)$$

$$t_{0.5} = \frac{0.693}{k_{obs}} \quad (4)$$

Table 13

Zero- or first-order removal constant (k_{obs}), mass normalized rate constant (k_M), surface area normalized rate constant (k_{SA} , specific reaction rate constant), and half-life ($t_{0.5}$) of **perfluorooctanoic acid (PFOA)** in Column ZVI, Column BC, and Column (ZVI + BC). Removal rate constant k_{obs} is calculated using least-squares regression during two experimental stages. C is the PFOA concentration. “—” represents no removal of PFOA was observed.

Column	Stage	PV	Removal rate [†] , $\mu\text{mol L}^{-1} \text{d}^{-1}$ ($\mu\text{g L}^{-1} \text{d}^{-1}$)	k_{obs}	k_M	k_{SA}	$t_{0.5}$, d	R^2
Column 2 (ZVI)	1	1	2.2E+01 ^b	2.2E+01 ^b	5.2E-03 ^b	5.5E-04 ^b	1.3	0.821
		13	—	—	—	—	—	—
		25	—	—	—	—	—	—
Column 3 (BC)	1	1	1.0 × C ^a	1.0 ^a	2.1E-03 ^a	3.3E-05 ^a	0.7	0.980
		13	0.5 × C ^a	0.5 ^a	1.1E-03 ^a	1.8E-05 ^a	1.3	0.987
		25	1.2E+01 ^b	1.2E+01 ^b	2.5E-02 ^b	3.9E-04 ^b	2.3	0.956
Column 4 (ZVI + BC)	1	1	2.0E+01 ^b	2.0E+01 ^b	1.8E-02 ^b	5.3E-04 ^b	1.3	0.935
		13	7.7 ^b	7.7 ^b	6.7E-03 ^b	2.0E-04 ^b	3.3	0.933
		25	2.0 ^b	2.0 ^b	1.7E-03 ^b	5.1E-05 ^b	13	0.725
	2	53	—	—	—	—	—	

^a Removal of PFOA followed a first-order reaction rate, unit of k_{obs} is d^{-1} , unit of k_M is $\text{L g}^{-1} \text{d}^{-1}$, unit of k_{SA} is $\text{L m}^{-2} \text{d}^{-1}$.

^b Removal of PFOA followed a zero-order reaction rate, unit of k_{obs} is $\mu\text{mol PFOA L}^{-1} \text{d}^{-1}$ ($\mu\text{g PFOA L}^{-1} \text{d}^{-1}$), unit of k_M is $\mu\text{mol PFOA d}^{-1} \text{g}^{-1}$ ($\mu\text{g PFOA d}^{-1} \text{g}^{-1}$), unit of k_{SA} is $\mu\text{mol PFOA d}^{-1} \text{m}^{-2}$ ($\mu\text{g PFOA d}^{-1} \text{m}^{-2}$).

Table 14

Zero- or first-order removal constant (k_{obs}), mass normalized rate constant (k_M), surface area normalized rate constant (k_{SA} , specific reaction rate constant), and half-life ($t_{0.5}$) of **perfluorooctane sulfonic acid (PFOS)** in Column ZVI, Column BC, and Column (ZVI + BC). Removal rate constant k_{obs} is calculated using least-squares regression during two experimental stages. C is the PFOS concentration.

Column	Stage	PV	Removal rate [†] , $\mu\text{mol L}^{-1} \text{d}^{-1}$ ($\mu\text{g L}^{-1} \text{d}^{-1}$)	k_{obs}	k_M	k_{SA}	$t_{0.5}$, d	R^2
Column 2 (ZVI)	1	1	2.0 × C ^a	2.0 ^a	4.6E-04 ^a	4.9E-05 ^a	0.4	0.911
		13	0.9 × C ^a	0.9 ^a	2.1E-04 ^a	2.3E-05 ^a	0.8	0.834
		25	2.2E+01 ^b	2.2E+01 ^b	5.1E-03 ^b	5.4E-04 ^b	1.5	0.929
Column 3 (BC)	1	1	1.8 × C ^a	1.8 ^a	3.9E-03 ^a	6.0E-05 ^a	0.4	0.989
		13	0.5 × C ^a	0.5 ^a	1.2E-03 ^a	1.8E-05 ^a	1.3	0.511
		25	0.9 × C ^a	0.9 ^a	1.8E-03 ^a	2.8E-05 ^a	0.8	0.961
Column 4 (ZVI + BC)	1	1	0.2 × C ^a	0.2 ^a	4.6E-04 ^a	7.2E-06 ^a	3.2	0.967
		13	2.2 × C ^a	2.2 ^a	1.9E-03 ^a	5.7E-05 ^a	0.3	0.974
		25	0.7 × C ^a	0.7 ^a	5.8E-04 ^a	1.7E-05 ^a	1.1	0.881
Column 4 (ZVI + BC)	2	1	1.1 × C ^a	1.1 ^a	9.6E-04 ^a	2.9E-05 ^a	0.6	0.962
		53	7.0 ^b	7.0E+01 ^b	6.1E-03 ^b	1.8E-04 ^b	5.9	0.966

^a Removal of PFOS followed a first-order reaction rate, unit of k_{obs} is d^{-1} , unit of k_M is $\text{L g}^{-1} \text{d}^{-1}$, unit of k_{SA} is $\text{L m}^{-2} \text{d}^{-1}$.

^b Removal of PFOS followed a zero-order reaction rate, unit of k_{obs} is $\mu\text{mol PFOS L}^{-1} \text{d}^{-1}$ ($\mu\text{g PFOS L}^{-1} \text{d}^{-1}$), unit of k_M is $\mu\text{mol PFOS d}^{-1} \text{g}^{-1}$ ($\mu\text{g PFOS d}^{-1} \text{g}^{-1}$), unit of k_{SA} is $\mu\text{mol PFOS d}^{-1} \text{m}^{-2}$ ($\mu\text{g PFOS d}^{-1} \text{m}^{-2}$).

where C is the contaminant concentration ($\mu\text{mol L}^{-1}$ or $\mu\text{g L}^{-1}$), k_{obs} is the first-order removal rate constant (d^{-1}), k_M is the mass normalized first-order rate constant ($\text{L g}^{-1} \text{d}^{-1}$), k_{SA} is the specific first-order reaction rate constant or surface area normalized first-order rate constant ($\text{L m}^{-2} \text{d}^{-1}$), ρ_m is the mass concentration of reactive media (g L^{-1} of solution), ρ_a is the surface area concentration of reactive media ($\text{m}^2 \text{L}^{-1}$ of solution), a_s is the specific surface area of reactive media ($\text{m}^2 \text{g}^{-1}$), and $t_{0.5}$ is the half-life of contaminant (d). The specific surface areas of the reactive media ZVI, BC, and (ZVI + BC) used are 9.5, 64.5, and $33.6 \text{ m}^2 \text{g}^{-1}$ which are reported previously [3,4].

The removal of artificial sweeteners, PFOA, and PFOS within three treatment columns followed a first- or zero-order rate model or followed a first-order rate in the early stage of the experiment followed by a zero-order rate in the late stage of the experiment [1]. The k_{obs} , k_M , k_{SA} , and $t_{0.5}$ for the first-order rate of artificial sweeteners, PFOA, and PFOS were calculated following the equations (1)–(4). The

zero-order rate model can be described by equation (5). k_M and k_{SA} for the zero-order reaction can also be calculated according to equations (2) and (3). However, the half-life ($t_{0.5}$) of the zero-order reaction for target artificial sweeteners, PFOA, and PFOS was calculated following equation (6).

$$-\frac{dC}{dt} = k_{obs} \quad (5)$$

$$t_{0.5} = \frac{C_0}{2 k_{obs}} \quad (6)$$

where C_0 is the initial contaminant concentration ($\mu\text{mol L}^{-1}$ or $\mu\text{g L}^{-1}$). The units of k_{obs} , k_M , and k_{SA} for the zero-order rate were different from that for the first order rate. For the zero-order rate, the unit of k_{obs} is $\mu\text{mol contaminant L}^{-1} \text{d}^{-1}$ ($\mu\text{g contaminant L}^{-1} \text{d}^{-1}$), the unit of k_M is $\mu\text{mol contaminant d}^{-1} \text{g}^{-1}$ ($\mu\text{g contaminant d}^{-1} \text{g}^{-1}$), and the unit of k_{SA} is $\mu\text{mol contaminant d}^{-1} \text{m}^{-2}$ ($\mu\text{g contaminant d}^{-1} \text{m}^{-2}$).

Conflict of Interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this article.

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References

- [1] Y. Liu, C.J. Ptacek, D.W. Blowes, L.G. Groza, Removal of pharmaceutical compounds, artificial sweeteners, and perfluoroalkyl substances from water using a passive treatment system containing zero-valent iron and biochar, *Sci. Total Environ.* 691 (2019) 165–177. <https://doi.org/10.1016/j.scitotenv.2019.06.450>.
- [2] T.L. Johnson, M.M. Scherer, P.G. Tratnyek, Kinetics of halogenated organic compound degradation by iron metal, *Environ. Sci. Technol.* 30 (8) (1996) 2634–2640. <https://doi.org/10.1021/es9600901>.
- [3] J.H. Jamieson-Hanes, *Characterizing Chromium Isotope Fractionation during Reduction of Cr(VI): Batch and Column Experiments*, MSc Thesis, University of Waterloo, Waterloo, Ontario, Canada, 2012.
- [4] P. Liu, C.J. Ptacek, D.W. Blowes, Release of nutrients and trace elements from wood, agricultural residue and manure-based biochars, *Int. J. Environ. Res.* 13 (4) (2019) 747–758. <https://doi.org/10.1007/s41742-019-00209-5>.